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AIR QUALITY DIVISION

**Relative Accuracy Test Audit  
Test Report**

**Billerud Escanaba LLC  
Escanaba Mill  
No. 8 Power Boiler Stack and  
No. 11 Power Boiler Stack  
Escanaba, Michigan  
September 13 and 15, 2022**

**Report Submittal Date  
November 2, 2022**

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Mostardi Platt

**Project No. M223711A**

*A0884-test-20220913*



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## 1.0 EXECUTIVE SUMMARY

Mostardi Platt conducted a Continuous Emissions Monitoring System (CEMS) Relative Accuracy Test Audit (RATA) test program for Billerud Escanaba LLC at the Escanaba Mill in Escanaba, Michigan, on the No. 8 Power Boiler Stack and No. 11 Power Boiler Stack on September 13 and 15, 2022. No. 8 Power Boiler also had a even day drift completed to complete the certification requirements. This report summarizes the results of the test program and test methods.

The test locations, RATA test dates, and test parameters are summarized below.

TEST INFORMATION		
Test Locations	Test Dates	Test Parameters
No. 8 Power Boiler Stack and No. 11 Power Boiler Stack	September 13 and 15, 2022	Oxygen (O <sub>2</sub> ) and Nitrogen Oxides (NO <sub>x</sub> )

The purpose of the test program was to demonstrate the relative accuracies of the No. 8 Power Boiler Stack and No. 11 Power Boiler Stack O<sub>2</sub> and NO<sub>x</sub> analyzers during the specified operating condition. The test results from this test program indicate that each CEMS meets the United States Environmental Protection Agency (USEPA) annual performance specification for relative accuracy and certifications as published in 40 Code of Federal Regulations Part 60 (40CFR60). The seven day drift data for the certification is appended.

RATA RESULTS					
Test Location	Date	Parameter	Units	Relative Accuracy Acceptance Criteria	Relative Accuracy (RA)
No. 8 Power Boiler Stack	9/15/22	NO <sub>x</sub>	lb/mmBtu	≤ 20.0% of the mean reference value	3.18%
		NO <sub>x</sub>	ppmvd	≤ 20.0% of the mean reference value	9.10%
		O <sub>2</sub>	% dry	≤ 1% mean difference	-0.87% mean difference
No. 11 Power Boiler Stack	9/13/22	NO <sub>x</sub>	lb/mmBtu	≤ 20.0% of the mean reference value	2.04%
		O <sub>2</sub>	% dry	≤ 1% mean difference	0.211% mean difference

The gas cylinders used to perform the RATA are summarized below.

GAS CYLINDER INFORMATION				
Parameter	Gas Vendor	Cylinder Serial Number	Cylinder Value	Expiration Date
NO <sub>x</sub>	Airgas	CC447414	0.0 ppm	4/25/2030
NO <sub>x</sub>	Airgas	ALM-057189	148.2 ppm	1/31/2030
NO <sub>x</sub>	Airgas	ALM-058205	284.8 ppm	7/8/2027
O <sub>2</sub>	Airgas	ALM-057189	0.0%	1/31/2030
O <sub>2</sub>	Airgas	CC447414	5.054%	4/25/2030
O <sub>2</sub>	Airgas	ALM-013475	10.02%	8/23/2030

The identifications of the individuals associated with the test program are summarized below.

TEST PERSONNEL INFORMATION		
Location	Address	Contact
Test Coordinator and Test Facility	Billerud Escanaba LLC 7100 County Road 426 M.5 Rd Escanaba, MI 49829	Mr. Adam Becker Environmental Engineer (906) 233-2929 (phone) Adam.Becker@versoco.com
Testing Company Personnel	Mostardi Platt 888 Industrial Drive Elmhurst, Illinois 60126	Mr. Michael Sather Senior Project Manager 630-993-2100 (phone) msather@mp-mail.com

The test crew consisted of D. Jordan, J. Devereux, K. West, and M. Sather of Mostardi Platt.

## 2.0 TEST METHODOLOGY

Emission testing was conducted following the USEPA methods specified in 40CFR60, Appendix A, in addition to the Mostardi Platt Quality Manual. Schematics of the test section diagram and sampling trains used are included in Appendix A and B respectively. Calculation nomenclature are included in Appendix C. Copies of analyzer print-outs and field data sheets for each test run are included in Appendix D. CEM data and process data as provided by Billerud Escanaba LLC are included in Appendix E.

Parameter	USEPA Reference Method	Notes/Remarks
O <sub>2</sub> %	USEPA Method 3A, 40CFR60, Appendix A	Instrument Analysis of O <sub>2</sub> % on a dry basis
NO <sub>x</sub>	USEPA Method 7E, 40CFR60, Appendix A	Instrument Analysis of NO <sub>x</sub> ppmvd to calculate NO <sub>x</sub> lb/mmBtu
Fd	USEPA Method 19, 40CFR60, Appendix A	Standard fuel factors of 8,710 and 9,820 dscf/mmBtu were used to calculate lb/mmBtu

The sampling location for testing on the No. 11 Boiler exhaust is located within the duct prior to the breach of the No. 11 Boiler stack which is within the vicinity of the facility's CEMS probes and is where annual RATA certification tests are conducted. This sample location is rectangular and is equipped with a single sample port. Previous testing and certification of the facility's CEMS has indicated an absence of stratification at this sample location. Therefore, sampling was conducted within the centroidal region of the duct for Methods 3A and 7E. Sampling for NO<sub>x</sub> on Boiler 8 was at the stack location.

The following methodologies were used during the test program:

### Method 3A Oxygen (O<sub>2</sub>)/ Determination

Stack gas O<sub>2</sub> concentrations were determined in accordance with USEPA Method 3A. A Servomex analyzer was used to determine the O<sub>2</sub> concentrations in the manner specified in the Method. The instrument has a paramagnetic detector and the O<sub>2</sub> operates in the nominal range of 0% to 25% with the specific range determined by the high-level calibration gas. High-range calibrations were performed using USEPA Protocol gas. Zero nitrogen (a low ppm pollutant in balance nitrogen calibration gases) was introduced during other instrument calibrations to check instrument zero. High- and a mid-range % O<sub>2</sub> levels in balance nitrogen were also introduced.

Zero and mid-range calibrations were performed using USEPA Protocol gas after each test run. Copies of the gas cylinder certifications are found in Appendix G. This testing met the performance specifications as outlined in the Method.

### Method 7E Nitrogen Oxides (NO<sub>x</sub>) Determination

Stack gas NO<sub>x</sub> concentrations and emission rates were determined in accordance with USEPA Method 7E, 40CFR60, Appendix A. A Thermo Scientific Model 42i Chemiluminescence Nitrogen Oxides Analyzer was used to determine nitrogen oxides concentrations, in the manner specified in the Method. The instrument operated in the nominal range of 0 ppm to 1000 ppm with the specific range determined by the high-level span calibration gas.

The Model 42i High Level is based on the principle that nitric oxide (NO) and ozone (O<sub>3</sub>) react to produce a characteristic luminescence with an intensity linearly proportional to the NO concentration. Infrared light emission results when electronically excited nitrogen dioxide (NO<sub>2</sub>) molecules decay to lower energy states. Specifically,



NO<sub>2</sub> must first be transformed into NO before it can be measured using the chemiluminescent reaction. NO<sub>2</sub> is converted to NO by a stainless steel NO<sub>2</sub>-to-NO converter heated to about 625°C. The flue gas air sample is drawn into the Model 42i High Level through the sample bulkhead. The sample flows through a particulate filter, a capillary, and then to the mode solenoid valve. The solenoid valve routes the sample either straight to the reaction chamber (NO mode) or through the NO<sub>2</sub>-to-NO converter and then to the reaction chamber (NO<sub>x</sub> mode).

Dry air enters the Model 42i High Level through the dry air bulkhead, through a flow sensor, and then through a silent discharge ozonator. The ozonator generates the necessary ozone concentration needed for the chemiluminescent reaction. The ozone reacts with the NO in the ambient air sample to produce electronically excited NO<sub>2</sub> molecules. A photomultiplier tube (PMT) housed in a thermoelectric cooler detects the NO<sub>2</sub> luminescence.

The NO and NO<sub>x</sub> concentrations calculated in the NO and NO<sub>x</sub> modes are stored in memory. The difference between the concentrations is used to calculate the NO<sub>2</sub> concentration. The Model 42i High Level outputs NO, NO<sub>2</sub>, and NO<sub>x</sub> concentrations to both the front panel display and the analog outputs.

Stack gas was delivered to the analyzer via a Teflon® sampling line, heated to a minimum temperature of 250°F. Excess moisture in the stack gas was removed using a refrigerated condenser. The entire system was calibrated in accordance with the Method, using certified calibration gases introduced at the probe, before and after each test run. This testing met the performance specifications as outlined in the Method.

A list of calibration gases used and the results of all calibration and other required quality assurance checks are found in Appendix F. Copies of the gas cylinder certifications are found in Appendix G. The NO<sub>2</sub> to NO converter test can be found in Appendix H. This testing met the performance specifications as outlined in the Method.

### Method 19 Determination of Nitrogen Oxides (NO<sub>x</sub>) Emission Rates

Stack gas NO<sub>x</sub> emission rates were determined in accordance with USEPA Method 19, 40CFR60, Appendix A. A standard Fd factor of 8,710 dscf/mmBtu for natural gas was used to convert NO<sub>x</sub> ppmvd to NO<sub>x</sub> lb/mmBtu on the No. 8 Power Boiler. A standard Fd factor of 9,820 dscf/mmBtu for sub-bituminous coal was used to convert NO<sub>x</sub> ppmvd to NO<sub>x</sub> lb/mmBtu on the No. 11 Power Boiler.

### 3.0 TEST RESULT SUMMARIES

Client: Billerud Escanaba LLC				Location: No. 8 Power Boiler Stack					
Facility: Escanaba Mill				Date: 9/15/22					
Project #: M223711				Test Method: 7E, 3A					
Fuel Type: Natural Gas				Fuel Factor: 8710					
O2 based NOx lb/mmBtu RATA									
CEM Analyzer Information									
NO <sub>x</sub> Monitor/Model:				Thermo 42 IQ		NO <sub>x</sub> Serial # :		1181030037	
O2 Monitor/Model:				TEI 25595003		O2 Serial # :		CC111105-5	
1=accept 0=reject	Test Run	Steam Flow KLB/HR	Test Date	Start Time	End Time	RM NO <sub>x</sub> lb/MMBtu	CEM NO <sub>x</sub> lb/MMBtu	(RM-CEM) Difference (di)	(RM-CEM) Difference <sup>2</sup> (di <sup>2</sup> )
1	1	241.9	09/15/22	07:15	07:44	0.189	0.184	0.005	0.000025
0	2	266.3	09/15/22	08:00	08:29	0.165	0.158	0.007	0.000049
1	3	250.4	09/15/22	08:45	09:14	0.158	0.153	0.005	0.000025
1	4	250.3	09/15/22	09:30	09:59	0.147	0.143	0.004	0.000016
1	5	249.6	09/15/22	10:15	10:44	0.133	0.129	0.004	0.000016
1	6	256.7	09/15/22	11:00	11:29	0.128	0.126	0.002	0.000004
1	7	281.3	09/15/22	11:45	12:14	0.143	0.140	0.003	0.000009
1	8	254.7	09/15/22	12:30	12:59	0.122	0.119	0.003	0.000009
1	9	254.6	09/15/22	13:15	13:44	0.117	0.114	0.003	0.000009
1	10	254.5	09/15/22	14:00	14:29	0.117	0.113	0.004	0.000016
n						9			
t(0.975)						2.306			
Mean Reference Method Value						0.139		RM avg	
Mean CEM Value						0.136		CEM avg	
Sum of Differences						0.033		di	
Mean Difference						0.004		d	
Sum of Differences Squared						0.000		di <sup>2</sup>	
Standard Deviation						0.001		sd	
Confidence Coefficient 2.5% Error (1-tail)						0.001		cc	
Relative Accuracy						3.18		RA	



Client: Billerud Escanaba LLC  
 Facility: Escanaba Mill  
 Project #: M223711

Location: No. 8 Power Boiler Stack  
 Date: 9/15/22  
 Test Method: 7E

**NO<sub>x</sub> ppmvd RATA**  
**CEM Analyzer Information**

NO <sub>x</sub> Monitor/Model:				Thermo 42 IQ		NO <sub>x</sub> Serial # :		1181030037	
1=accept 0=reject	Test Run	Steam Flow KLB/HR	Test Date	Start Time	End Time	RM NO <sub>x</sub> ppmvd	CEM NO <sub>x</sub> ppmvd	(RM-CEM) Difference (di)	(RM-CEM) Difference <sup>2</sup> (di <sup>2</sup> )
1	1	241.9	09/15/22	07:15	07:44	134.4	123.8	10.6	112.36
0	2	266.3	09/15/22	08:00	08:29	117.6	106.2	11.4	129.96
1	3	250.4	09/15/22	08:45	09:14	112.6	103.0	9.6	92.16
1	4	250.3	09/15/22	09:30	09:59	104.8	96.4	8.4	70.56
1	5	249.6	09/15/22	10:15	10:44	94.4	86.8	7.6	57.76
1	6	256.7	09/15/22	11:00	11:29	91.4	85.0	6.4	40.96
1	7	281.3	09/15/22	11:45	12:14	102.0	93.6	8.4	70.56
1	8	254.7	09/15/22	12:30	12:59	86.7	80.3	6.4	40.96
1	9	254.6	09/15/22	13:15	13:44	83.5	77.0	6.5	42.25
1	10	254.5	09/15/22	14:00	14:29	83.4	76.4	7.0	49.00
n						9			
t(0.975)						2.306			
Mean Reference Method Value						99.244		RM avg	
Mean CEM Value						91.367		CEM avg	
Sum of Differences						70.900		di	
Mean Difference						7.878		d	
Sum of Differences Squared						576.570		di <sup>2</sup>	
Standard Deviation						1.501		sd	
Confidence Coefficient 2.5% Error (1-tail)						1.154		cc	
Relative Accuracy						9.10		RA	

<b>Client:</b> Billerud Escanaba LLC				<b>Location:</b> No. 8 Power Boiler Stack					
<b>Facility:</b> Escanaba Mill				<b>Date:</b> 9/15/22					
<b>Project #:</b> M223711				<b>Test Method:</b> 3A					
<b>O<sub>2</sub> % (dry) RATA</b>									
<b>CEM Analyzer Information</b>									
<b>O<sub>2</sub> Monitor/Model:</b>				TEI 25595003		<b>O<sub>2</sub> Serial # :</b>		CC111105-5	
<b>1=accept 0=reject</b>	<b>Test Run</b>	<b>Steam Flow KLB/HR</b>	<b>Test Date</b>	<b>Start Time</b>	<b>End Time</b>	<b>RM O<sub>2</sub> % (dry)</b>	<b>CEM O<sub>2</sub> % (dry)</b>	<b>(RM-CEM) Difference (di)</b>	<b>(RM-CEM) Difference<sup>2</sup> (di<sup>2</sup>)</b>
1	1	241.9	09/15/22	07:15	07:44	5.5	6.3	-0.8	0.64
1	2	266.3	09/15/22	08:00	08:29	5.4	6.3	-0.9	0.81
1	3	250.4	09/15/22	08:45	09:14	5.4	6.3	-0.9	0.81
1	4	250.3	09/15/22	09:30	09:59	5.4	6.3	-0.9	0.81
1	5	249.6	09/15/22	10:15	10:44	5.4	6.3	-0.9	0.81
1	6	256.7	09/15/22	11:00	11:29	5.4	6.3	-0.9	0.81
0	7	281.3	09/15/22	11:45	12:14	5.4	6.4	-1.0	1.00
1	8	254.7	09/15/22	12:30	12:59	5.4	6.3	-0.9	0.81
1	9	254.6	09/15/22	13:15	13:44	5.4	6.2	-0.8	0.64
1	10	254.5	09/15/22	14:00	14:29	5.4	6.2	-0.8	0.64
<b>n</b>						<b>9</b>			
<b>t(0.975)</b>						<b>2.306</b>			
<b>Mean Reference Method Value</b>						<b>5.411</b>		<b>RM avg</b>	
<b>Mean CEM Value</b>						<b>6.278</b>		<b>CEM avg</b>	
<b>Sum of Differences</b>						<b>-7.800</b>		<b>di</b>	
<b>Mean Difference</b>						<b>-0.867</b>		<b>d</b>	
<b>Sum of Differences Squared</b>						<b>6.780</b>		<b>di<sup>2</sup></b>	
<b>Standard Deviation</b>						<b>0.050</b>		<b>sd</b>	
<b>Confidence Coefficient 2.5% Error (1-tail)</b>						<b>0.038</b>		<b>cc</b>	
<b>Relative Accuracy</b>						<b>-0.87</b>		<b>RA</b>	

<sup>A</sup> Alternate Performance Standard for O<sub>2</sub> analyzers of ≤ 1.0 % for annual RATA testing,

<b>Client:</b> Billerud Escanaba LLC <b>Facility:</b> Escanaba Mill <b>Project #:</b> M223711 <b>Fuel Type:</b> Coal, Sub-Bituminous	<b>Location:</b> No. 11 Power Boiler Breeching <b>Date:</b> 9/13/22 <b>Test Method:</b> 7E, 3A <b>Fuel Factor:</b> 9820
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**O2 based NOx lb/mmBtu RATA**

<b>NO<sub>x</sub> Monitor/Model:</b>		Thermo 42i			<b>NO<sub>x</sub> Serial # :</b>		1308857366	
<b>O2 Monitor/Model:</b>		Thermo 25595003			<b>O2 Serial # :</b>		CC111105-5	
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM NO <sub>x</sub> lb/MMBtu	CEM NO <sub>x</sub> lb/MMBtu	(RM-CEM) Difference (di)	(RM-CEM) Difference <sup>2</sup> (di <sup>2</sup> )
1	1	09/13/22	07:10	07:39	0.166	0.164	0.002	0.000004
1	2	09/13/22	07:50	08:19	0.154	0.154	0.000	0.000000
1	3	09/13/22	08:35	09:04	0.148	0.145	0.003	0.000009
1	4	09/13/22	09:18	09:47	0.206	0.197	0.009	0.000081
1	5	09/13/22	10:00	10:29	0.395	0.401	-0.006	0.000036
1	6	09/13/22	10:40	11:09	0.409	0.418	-0.009	0.000081
0	7	09/13/22	11:30	11:59	0.413	0.424	-0.011	0.000121
1	8	09/13/22	12:12	12:41	0.163	0.166	-0.003	0.000009
1	9	09/13/22	12:53	13:22	0.186	0.184	0.002	0.000004
1	10	09/13/22	13:32	14:01	0.169	0.171	-0.002	0.000004
<b>n</b>					<b>9</b>			
<b>t(0.975)</b>					<b>2.306</b>			
<b>Mean Reference Method Value</b>					<b>0.222</b>		<b>RM avg</b>	
<b>Mean CEM Value</b>					<b>0.222</b>		<b>CEM avg</b>	
<b>Sum of Differences</b>					<b>-0.004</b>		<b>di</b>	
<b>Mean Difference</b>					<b>0.000</b>		<b>d</b>	
<b>Sum of Differences Squared</b>					<b>0.000</b>		<b>di<sup>2</sup></b>	
<b>Standard Deviation</b>					<b>0.005</b>		<b>sd</b>	
<b>Confidence Coefficient 2.5% Error (1-tail)</b>					<b>0.004</b>		<b>cc</b>	
<b>Relative Accuracy</b>					<b>2.04</b>		<b>RA</b>	

Client: Billerud Escanaba LLC				Location: No. 11 Power Boiler Breaching				
Facility: Escanaba Mill				Date: 9/13/22				
Project #: M223711				Test Method: 3A				
<b>O<sub>2</sub> % (dry) RATA</b>								
<b>CEM Analyzer Information</b>								
O <sub>2</sub> Monitor/Model:			Thermo 25595003		O <sub>2</sub> Serial # :		CC111105-5	
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM O <sub>2</sub> % (dry)	CEM O <sub>2</sub> % (dry)	(RM-CEM) Difference (di)	(RM-CEM) Difference <sup>2</sup> (di <sup>2</sup> )
1	1	09/13/22	07:10	07:39	7.1	6.8	0.3	0.09
1	2	09/13/22	07:50	08:19	7.3	7.1	0.2	0.04
1	3	09/13/22	08:35	09:04	7.1	6.8	0.3	0.09
0	4	09/13/22	09:18	09:47	8.0	7.5	0.5	0.25
1	5	09/13/22	10:00	10:29	8.3	7.9	0.4	0.16
1	6	09/13/22	10:40	11:09	8.2	7.9	0.3	0.09
1	7	09/13/22	11:30	11:59	8.1	7.7	0.4	0.16
1	8	09/13/22	12:12	12:41	7.8	7.7	0.1	0.01
1	9	09/13/22	12:53	13:22	7.8	7.8	0.0	0.00
1	10	09/13/22	13:32	14:01	7.0	7.1	-0.1	0.01
n					9			
t(0.025)					2.306			
Mean Reference Method Value					7.633		RM avg	
Mean CEM Value					7.422		CEM avg	
Sum of Differences					1.900		di	
Mean Difference					0.211		d	
Sum of Differences Squared					0.650		di <sup>2</sup>	
Standard Deviation					0.176		sd	
Confidence Coefficient 2.5% Error (1-tail)					0.136		cc	
Relative Accuracy - APS					0.211		% difference <sup>A</sup>	

<sup>A</sup> Alternate Performance Standard for O<sub>2</sub> analyzers of ≤ 1.0 % for annual RATA testing.

## 4.0 CERTIFICATION

Mostardi Platt is pleased to have been of service to Billerud Escanaba LLC. If you have any questions regarding this test report, please do not hesitate to contact us at 630-993-2100.

As the program manager, I hereby certify that this test report represents a true and accurate summary of emissions test results and the methodologies employed to obtain those results. The test program was performed in accordance with the test methods and the Mostardi Platt Quality Manual, as applicable.

MOSTARDI PLATT



Michael Sather

Program Manager



Scott W. Banach

Quality Assurance

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## APPENDICES

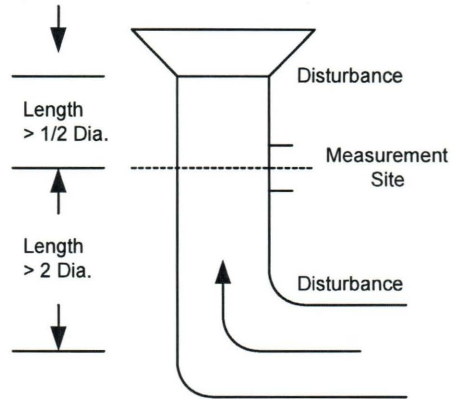
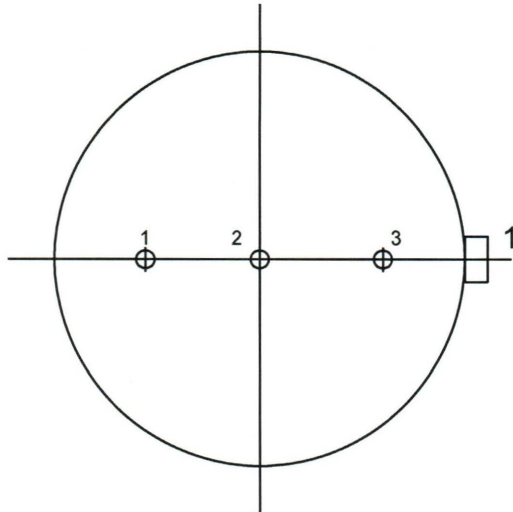
**Appendix A - Test Section Diagrams**

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## GASEOUS TRAVERSE FOR ROUND DUCTS



Job: Verso Corporation  
Escanaba Mill  
Escanaba, Michigan

Date: September 13, 2022

Test Location: No. 8 Power Boiler Stack

Stack Diameter: 7.0 Feet

Stack Area: 38.485 Square Feet

No. Sample Points: 3

Distance from Inside Wall  
To Traverse Point:

1. 83.3 % of diameter
2. 50.0 % of diameter
3. 16.7 % of diameter



**Appendix B - Sample Train Diagram**

# USEPA Methods 3A and 7E Extractive Gaseous Sampling Diagram

