# 40 CFR 63 Subpart FFFF National Emission Standards for Hazardous Air Pollutants Emissions Miscellaneous Organic Chemicals (MON) Compliance Test Report

# Reinforced Resin Polymer (602 Building) Process Condenser DV23967

Sample Date June 25, 2019

DOW SILICONES CORPORATION Midland, Michigan

\* Please note the process unit is the final copy holder and owner of this document. A temporary electronic copy will be retained by internal stack testing group for a short period of time.

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# **1.0 INTRODUCTION**

## **1.1 Summary of Test Program**

Dow Silicones Corporation (DSC) operates a chemical manufacturing facility in Midland, Michigan. The facility uses a glycol condenser followed by a carbon tote to control emissions in its Reinforced Resin Polymer (RRP) Process. The purpose of this compliance test was to demonstrate compliance with the option to either reduce emissions of total organic HAP by  $\geq$ 98% or to an outlet process concentration of  $\leq$  20 ppmv as TOC for Group 1 continuous process vents subject to MON, 40 CFR 63 Subpart FFFF.

Responsible Groups	<ul> <li>Dow Silicones Corporation</li> <li>Michigan Department of Environment, Great Lakes, and Energy (EGLE)</li> </ul>
	Environmental Protection Agency (EPA)
Applicable Regulations	Michigan Rule 290
	<ul> <li>40 CFR Part 63 Subpart FFFF</li> </ul>
Industry / Plant	Silicone Manufacturing Reinforced Resin
	Polymer (RRP) (602 Building)
Plant Location	Dow Silicones Corporation
	Midland, Michigan 48686
<b>Air Pollution Control Equipment</b>	Condenser DV23967 and carbon tote
Emission Points	<ul> <li>NA - Operates under a Rule 290 exemption (EU602-01)</li> </ul>
Pollutants/Diluent Measured	<ul> <li>≥98% Reduction efficiency</li> </ul>
Test Date Scheduled	• June 25, 2019

The following table summarizes the pertinent data for this compliance test:

### 1.2 Key Personnel

The key personnel who coordinated the test program are:

- Sara Gibson provided support as a Process Focal Point. The Process Focal Point is responsible for coordinating the plant operation during the test and ensuring the unit is operating at the agreed upon conditions in the test plan. They also serve as the key contact for collecting any process data required and providing all technical support related to process operation.
- Jenny Kraut provided support as the Environmental Focal Point for this unit. The Environmental Focal Point is responsible for ensuring that all regulatory requirements and citations are reviewed and considered for the testing. All agency communication will be completed through this role. Contact information is 989-496-7133.
- Chuck Glenn provided support as the Test Plan Coordinator. The Test Plan Coordinator is responsible for the overall leadership of the sampling program, developing the overall testing plan and determining the correct sample methods.
- Spencer Hurley provided support as the back-up for the Test Plan Coordinator and serves in a technical review role of the test data.
- Michael Abel provided support as a technical review of the test data.
- James Edmister provided support as the Sample Team Leader. The Sample Team Leader is responsible for ensuring the data generated meets the quality assurance objectives of the plan.

# 2.0 PLANT AND SAMPLING LOCATION DESCRIPTION

### 2.1 Facility Description

The Reinforced Resin Polymer (RRP) Process is a continuous process that operates under EU602-01. Condenser DV23967 removes organic HAPs and is a control device for the RRP Vacuum Pump Separator Tank (DV23964). Other equipment such as the DV6600 / DV6603 surge control vessels (not subject to control) also vent to the DV23967 condenser.

## 2.2 Control Equipment Description

DV23967 is a glycol condenser that operates with an operational parameter of 90°F (32°C) (maximum) on the exit gas temperature. The condenser is followed by a carbon tote.

### 2.3 Flue Gas Sampling Locations

Sampling was completed on both the inlet andoutlet of the condenser and the outlet of the carbon tote. All points are installed meeting the EPA Method 1 location requirements.

# **3.0 SUMMARY AND DISCUSSION OF TEST RESULTS**

#### **3.1 Objectives and Test Matrix**

The purpose of this test was to demonstrate compliance with the MON, 40 CFR 63 Subpart FFFF. The specific objectives of the test were:

- Measure TOC inlet feed rate and outlet emissions from the Condenser DV23967.
  - Establish the maximum operating temperature limit for the condenser exit gas temperature based on values measured during the performance test which can be supplemented by engineering assessments and/or manufacturer's recommendations.
- DSC also measured the TOC outlet emissions from the carbon tote since compliance could not be demonstrated using only the condenser.
  - Establish a carbon tote weight limit based on manufacturer's specifications.
  - Note: On November 21, 2013, EPA Region 5 approved an alternative monitoring request submitted as part of a Precompliance Report (dated August 12, 2013) for specific carbon drums used to control vents at DSC, including SV602-002 in MCPU-25. In August 2013, the 602 Building carbon system was made up of a carbon tote followed by a carbon drum in series. The carbon drum was on a scale and was weighed continuously. Since the original Pre-compliance Report submittal, DSC has changed the configuration to two carbon totes in series with the second tote on a scale. An updated pre-compliance report will be submitted in Q3-2019.

#### 3.2 Facility Operations

Sampling was conducted when RRP was running product 6-3445 at a 90% feed rate. This feed rate represents the maximum representative operating conditions for the process as required by 63.997(e)(1)(i). Feed rates of 6-3444 and SFD-117 (raw materials) from Mix tanks TK6603 and TK6600 will be set at 90% output on the pump, P1-6603, speed controller SC-363.

#### 3.3 Comments/Exceptions

- Jeremey Howe of the Michigan Department of Environment, Great Lakes, and Energy (EGLE) was present during the Performance Test sampling.
- THC outlet sampling did not meet QA requirements of EPA M25A. The actual gas concentration run averages were above the span gas calibration range. Re-testing will be completed as soon as possible. EGLE agrees no sample plan will be required. Dow will contact EGLE when a sample date is determined.

Emission Results								
SAMPLE TYPE TES METH	-	SAMPLING TIME (MINUTES)		Actual Emission Rate		ALLOWABLE EMISSION		
TOC'S EPA Me 25/		60 >99%			>99% Reduction ≥ Efficiency		98% Reduction Efficiency	
Field Sample Data								
PARAMETER		RUN 1		RUN 2	RI	JN 3	AVERAGE	
Run Date		06/25/19		06/25/19	06/	25/19	n/a	
Run Times		1310/1410		1530/1630	1830	0/1930	n/a	
Outlet THC as Propane (ppn	יעע)	105.0		108.1	1	10.2	107.8	
Outlet THC Corr Prop (ppm)	w)	105.9		108.5	· 1:	13.0	109.1	
Outlet Flow (scfh)		167		250	Ž	228	215	
<b>Outlet TOC Emissions (Ib</b>	/hr)	0.002		0.003	0.	003	0.003	
Cond Out THC as Prop (ppm	ivw)	1279.1		805.9	90	55.9	1017	
Cond Out THC Corr (ppmvw)		1253.4		777.4	936.6		989.1	
Cond Out THC Corr for Dilution		11281		10106	11239		10875	
Cond Out Flow (scfh)		169		213	228		203	
Cond Out TOC Feed (lb/hr)		0.219		0.246	0.293		0.253	
Cond In THC as Prop (ppmvw)		2653.2		1244.5	1037.8		1645.2	
Cond In THC Corr (ppmvw)		2729.8		1252.6	1038.5		1673.6	
Cond In THC Corr for Dilution		30027		21294	28040		26454	
Cond In Flow (scfh)		171		192	178		1.80	
Cond In TOC Feed (lb/hr	)	0.587		0.469	0.	571	0.542	
SRE over System (%)		99.7		99.4	9	9.5	99.5	

Please note the information above cannot be used to demonstrate compliance because of analytical QA issues. Results are not expected to be different in the re-test since the analyzer is considered linear.

#### **Process Data Summary**

Process Tag	Description	<b>Operating Rate Over Sample Period</b>		
WT-46565	Carbon tote weight	2.03 lbs		
TC-27084	Condenser DV23967 exit gas temperature	2.0 °C		
FQ-23726*	SFD-117 Feed meter totalizer	Confidential Process Data		
FQ-1735*	6-3444 Feed meter totalizer	Confidential Process Data		
SC-363*	P1-6603 Speed controller	90 %		

\* This information is considered confidential pursuant to Section 324.5516 of Act 451. Disclosure of this information would jeopardize the competitive position of the Dow Silicones Corporation. Therefore, this information will be submitted under separate cover letter.

#### **Operational Process Rate**

Parameter	Design Maximum	Proposed	Normal Operating	Actual Operating	
	Operating Rate	Operating Rate	Rate	Rate	
P1-6603 Speed controller**	100%	90%	90%	90%	

\*\* The pump output of 90% during the duration of the test is the "maximum operating rate" condition the unit can control. The feed rate does not directly determine the rate going through the condenser and carbon totes.

# 4.0 SAMPLING AND ANALYTICAL PROCEDURES

### 4.1 Test Methods

The TOC emissions were determined using the following methods:

- Methods 1-4 of 40 CFR Part 60, Appendix A, as appropriate for selection of sampling sites, gas volumetric flow rate, gas molecular weight, and moisture content of stack gas;
- Method 25A for THC as Propane

#### 4.2 Procedures

The above methods were performed using mobile continuous emission monitors provided by AECOMs internal testing team. Gas was withdrawn from the stack and transported to monitors located at ground level. A stainless-steel probe was inserted into the stack and used to collect sample gas. A Teflon sample line heated to 250°F was used to transport sample gas from the probe to the analyzers. The analyzers were be kept at a constant temperature inside the mobile laboratory. Sample gas was collected continuously from the stack for a period of 60 minutes per run.

#### EPA Method 1 (Sample Point Determination)

The number and location of traverse points in the stack is determined according to the procedures outlined in EPA Method 1. Since the duct was two inch in diameter, flow readings were collected from a single point.

#### EPA Method 2 (Flue Gas Velocity and Volumetric Flow Rate)

The flue gas velocity and volumetric flow rate was determined according to the procedures outline in 40 CFR 60, Appendix A, EPA Method 2. Velocity measurements are made using S-type pitot tubes conforming to the geometric specifications outlined in EPA Method 2. Differential pressures were measured with a manometer. Flue gas temperature, velocity, and volumetric flow rate data are recorded.

#### EPA Method 3A (Flue Gas Composition and Molecular Weight)

EPA Method 3A (Instrumental Method) is utilized to determine the diluent during each run on the outlet.

An analyzer measures  $O_2$  content on the basis of the strong paramagnetic properties of  $O_2$  relative to other compounds present in combustion gases. In the presence of a magnetic field,  $O_2$  molecules become temporary magnets. The analyzer determines the sample gas  $O_2$  concentration by detecting the displacement torque of the sample test body in the presence of a magnetic field.

An analyzer measures  $CO_2$  based on its absorption of infrared radiation. The infrared unit uses a single beam, single wavelength technique, with wavelength selection being achieved by a carefully specified narrow band optical filter making it highly selective for  $CO_2$  measurement in the presence of other infrared-absorbing gases.

Please note the stream make-up was N2. Therefore, all O2 and CO2 results were 0.0. The molecular weight of nitrogen was used for emission calculations.

#### EPA Method 4 (Moisture)

A calibrated Method 5 console pulled stack gas samples through a Method 5 probe to determine percent moisture of the stack gas. Stack gas was bubbled through two impingers containing water, one empty impinger, and one impinger containing silica gel. All of the impingers were weighed prior to sampling. The impinger train was kept iced in order to knock out all moisture in the stack gas. After the final leak check following each run, the exterior of the impingers are dried off and the impingers are weighed to determine percent moisture.

#### EPA Method 25A (Total VOC Sampling and Analysis)

EPA Method 25A was utilized to determine total THC as propane concentrations during each run on the outlet. EPA M25A data calculations are used to determine TOC by multiplying the number of carbons (3) by the actual readings. Propane is selected as the best standard since it is has a good response when compared to xylenes and ethylbenzene (the predominate HAPs).

A gas sample was extracted from the source through a heated line to a flame ionization analyzer (FIA). Results are reported as volume concentration equivalent to propane.

# FIGURE 4.1: SAMPLING TRAIN USED FOR CO<sub>2</sub> & O<sub>2</sub> (M3A)



