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Marathon Petroleum Company LP 1300 South Fort Street Detroit, MI 48217

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REPORT ON RATA & COMPLIANCE TESTING

Performed for: MARATHON PETROLEUM COMPANY LP DETROIT REFINERY

COKER HEATER STACK (SV70-H1)

Client Reference No: 4100665755 CleanAir Project No: 13082-1 Revision 0: November 7, 2016

To the best of our knowledge, the data presented in this report are accurate, complete, error free, legible and representative of the actual emissions during the test program. Clean Air Engineering operates in conformance with the requirements of ASTM D7036-04 Standard Practice for Competence of Air Emission Testing Bodies.

Submitted by,

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Authorized by 199	RENEN R 4 P.A. 451, as amended.	NABLE OF EPORT CE	PERATING PERM ERTIFICATION ide this information may re	l IT sult in ci	AIR QUALITY DIV.
Reports submitted pursuant to F must be certified by a responsib for at least 5 years, as specified upon request.	t 336.1213 (Rule 213), le official. Additional in Rule 213(3)(b)(li), a	subrules (3)(c) information reg nd be made av	and/or (4)(c), of Michigar arding the reports and d allable to the Departmen	n's Rena locumer it of Env	ewable Operating Permit (ROP) program ntation listed below must be kept on file vironmental Quality, Air Quality Divisior
Source Name Marathon I	etroleum Company	γLP			County Wayne
Source Address 1300 Sou	th Fort Street			City	_Detroit
AQD Source ID (SRN) A98	31	ROP No.	MI-ROP-A9831- 2012c		ROP Section No.
Please check the appropriate b	ox(es):	and the state of the second	1991		1971, ann an 1971 an 1971 an 1971 an 1972 an 1971 an 1972 an 19
Annual Compliance Cert	ification (Pursuant f	to Rule 213(4)	(c))		
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Semi-Annual (or More Fi	requent) Report Cert	ification (Pur	suant to Rule 213(3)(c))	
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X Other Report Certificatio	n				
Reporting period (provide i Additional monitoring repor Submittal of Stack	nclusive dates): F ts or other applicable Testing and RAT	from 08/30 documents rec A results.	/2016 To 0 uired by the ROP are a	9/14/2 ttached	2016 as described:
I certify that, based on informa supporting enclosures are true,	ition and belief forme accurate and complet	ed after reasor e MPC investm	able inquiry, the stater ent LLC,	nents a	and information in this report and the

Deputy Assistant Secretary 313-843-9100 David T. Roland Name of Responsible Official (print or type) Title Phone Number 2010 11 11 Date

Signature of Responsible Official

* Photocopy this form as needed.

EQP 5736 (Rev 11-04)



MICHIGAN DEPARTMENT OF ENVIRONMENTAL QUALITY AIR QUALITY DIVISION

NOV 1 4 2016

its General Partner

Client Reference No: 4100665755 CleanAir Project No: 13082-1

PROJECT OVERVIEW

INTRODUCTION

Marathon Petroleum Company LP (MPC) contracted Clean Air Engineering (CleanAir) to perform emission measurements at the Detroit Refinery for relative accuracy test audit (RATA) and compliance purposes.

All testing was conducted in accordance with the regulations set-forth by the United States Environmental Protection Agency (USEPA) and the Michigan Department of Environmental Quality (DEQ). The permit limits are referenced in Michigan Department of Environmental Quality, Air Quality Division Permit to Install No. 63-08D, issued May 12, 2014.

Key Project Participants

Individuals responsible for coordinating and conducting the test program were:

Crystal Davis – MPC Joe Reidy – MPC Thomas Gasloli – DEQ Chad Eilering – CleanAir

Test Program Parameters

The testing was performed at the Coker Heater Stack (Emission Unit ID No. EU70-COKERHTR-S1; Stack ID No. SV70-H1) on September 16, 2016, and included the following emissions measurements:

- particulate matter (PM), assumed equivalent to filterable particulate matter (FPM) only
- total particulate matter less than 10 microns (μ m) in diameter (Total PM₁₀), assumed equivalent to the sum of the following constituents:
 - filterable particulate matter (FPM)
 - condensable particulate matter (CPM)
- volatile organic compounds (VOCs), assumed equivalent to total hydrocarbons (THC) minus the following constituents:
 - methane (CH4)
 - ethane (C_2H_6)
- nitrogen oxides (NO_X)
- flue gas composition (e.g., O₂, CO₂, H₂O)
- flue gas flow rate

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PROJECT OVERVIEW

TEST PROGRAM SYNOPSIS

Test Schedule

The on-site schedule followed during the test program is outlined in Table 1-1.

		Schedule of	Activities			
Run Number	Location	Method	Analyte	Date	Start Tíme	End Time
1	Coker Heater Stack	USEPA Method 5/202	FPM/CPM	09/16/16	10:37	12:47
2	Coker Heater Stack	USEPA Method 5/202	FPM/CPM	09/16/16	14:14	16:24
3	Coker Heater Stack	USEPA Method 5/202	FPM/CPM	09/16/16	17:25	19:33
1	Coker Heater Stack	USEPA Method 3A/7E	O ₂ /CO ₂ /NO _X	09/16/16	10:03	10:24
2	Coker Heater Stack	USEPA Method 3A/7E	O ₂ /CO ₂ /NO _X	09/16/16	10:36	10:57
3	Coker Heater Stack	USEPA Method 3A/7E	O ₂ /CO ₂ /NO _X	09/16/16	11:09	11:30
4	Coker Heater Stack	USEPA Method 3A/7E	O ₂ /CO ₂ /NO _X	09/16/16	11:39	12:00
5	Coker Heater Stack	USEPA Method 3A/7E	O ₂ /CO ₂ /NO _X	09/16/16	12:10	12:31
6	Coker Heater Stack	USEPA Method 3A/7E	O ₂ /CO ₂ /NO _X	09/16/16	12:43	13:04
7	Coker Heater Stack	USEPA Method 3A/7E	O ₂ /CO ₂ /NO _X	09/16/16	14:17	14:38
8	Coker Heater Stack	USEPA Method 3A/7E	O ₂ /CO ₂ /NO _X	09/16/16	14:49	15:10
9	Coker Heater Stack	USEPA Method 3A/7E	O ₂ /CO ₂ /NO _X	09/16/16	15:21	15:42
10	Coker Heater Stack	USEPA Method 3A/7E	O ₂ /CO ₂ /NO _X	09/16/16	15:56	16:17
1	Coker Heater Stack	USEPA Method 3A/18/25A	O ₂ /CO ₂ /CH ₄ /C ₂ H ₆ /THC	09/16/16	10:03	11:30
2	Coker Heater Stack	USEPA Method 3A/18/25A	O2/CO2/CH4/C2H8/THC	09/16/16	11:39	13:04
3	Coker Heater Stack	USEPA Method 3A/18/25A	O ₂ /CO ₂ /CH ₄ /C ₂ H ₆ /THC	09/16/16	14:17	15:42

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Table 1-1: Schedulo of Activition

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PROJECT OVERVIEW

Results Summary

Table 1-2 and Table 1-3 summarize the results of the test program. A more detailed presentation of the test conditions and results of analysis are shown on pages 2-1 through 2-7.

Su	Ta mmary of Emission	ble 1-2: n Compliance	e Test Results	
<u>Source</u> Constituent (Units)	Sampling (USEF	Method PA) A	verage Emission	Permit Limit ¹
Coker Heater Stack				
PM (lb/MMBtu)	5		0.0014	0.0019
PM ₁₀ (lb/MMBtu)	5/20	02	0.0041	0.0076
VOC (lb/MMBtu)	25A /	18	<0.0006	0.0055
	Ta Summary o	ble 1-3: of RATA Resu	ults	
<u>Source</u> Constituent (Units)	Reference Method (USEPA)	Applicable Specification	Relative Accuracy (%)	Specification Limit ¹
Coker Heater Stack				
O ₂ (% dv)	ЗA	PS3	0.14	±1.0% dv
NO _x (ppmdv @ 0%O ₂)	7E	PS2	5.0	20% of RM
NO _X (lb/MMBtu)	7E	PS2	1.8	20% of RM

¹ Specification limits obtained from 40 CFR 60, Appendix B, Performance Specifications.

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Discussion of Test Program

FPM and CPM Testing - USEPA Method 5/202

For this test program, PM emission rate is assumed equivalent to FPM emission rate and PM_{10} emission rate is assumed equivalent to the sum of FPM and CPM emission rates (units of lb/hr, Ton/yr, or lb/MMBtu for all constituents).

The analytical procedures in EPA Method 202 include an ammonium titration of the inorganic sample fractions with pH less than 7.0 to neutralize acids with hygroscopic properties such as H_2SO_4 that may be present in the sample. This step speeds up the sample desiccation process and allows the samples to come to a constant weight prior to weighing. The weight of ammonium added to the sample as a result of the titration is subtracted from the analytical result.

The laboratory performing the gravimetric analysis (Clean Air Analytical Services) has determined that only samples with an initial pH less than 4.5 require a significant amount of ammonium neutralization, resulting in a correction in excess of 0.5 mg. Based on this observation, the laboratory has altered their procedures to read that a sample must have a pH lower than 4.5 in order to be titrated.

While all of the inorganic sample fractions from Runs 1-3 had a pH less than 4.5 and were titrated, the field train reagent blank had a pH of about 6.8 and was not titrated, per Clean Air Analytical Services' modified procedure. The sample fraction was observed to come to a constant weight without having to titrate the sample.

Three (3) 120-minute Method 5/202 test runs were performed on September 16, 2016. The final result for PM & PM₁₀ was expressed as the average of three (3) valid runs.

O₂ and NO_X RATA Testing - USEPA Methods 3A & 7E; Performance Specifications 2 & 3

Minute-average data points for O_2 and NO_X (dry basis) were collected over a period of 21 minutes for each RATA Reference Method (RM) run. The average result for each RM run was calculated and compared to the average result from the facility's CEMS over an identical time interval in order to calculate relative accuracy (RA).

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VOC Testing - USEPA Method 25A and Method 18

VOC testing was performed concurrently with the RATA testing. Nine (9) 21-minute Method 25 test runs for THC were performed concurrently with three (3) Method 18 bag collections for CH_4 and C_2H_6 , with each M-18 sample collected over a period of about 63 minutes. The M-18 samples were collected as follows:

- Method 18 Run 1: Collected during Method 25A Runs 1, 2 and 3
- Method 18 Run 2: Collected during Method 25A Runs 4, 5 and 6
- Method 18 Run 3: Collected during Method 25A Runs 7, 8 and 9

The VOC emission rate is normally equivalent to THC emission rate, minus CH₄ and C_2H_6 emission rate. The calculated emission rate of CH₄ detected through analysis of each Method 18 sample bag exceeded the amount of THC measured by the on-line THC analyzer.

This is likely due to variations in the calibration standards, measurement and analytical technique. Therefore, VOC emissions are reported as a value "less than" 1% of the calibration span of THC instrument. The final results were calculated using the average of three valid test runs, all using a concentration of 1% of the instrument span and reported as "less than" the amount.

Calculation of Final Results

Emission results in units of dry volume-based concentration (lb/dscf, ppmdv) were converted to units of pounds per million Btu (lb/MMBtu) by calculating an oxygenbased fuel factor (F_d) for refinery gas per USEPA Method 19 specifications. The heat content and F_d factor were calculated from percent volume composition analytical data provided by MPC and tabulated heating values for each of the measured constituents.

Fuel analysis for September 16, 2016, was not available. Instead an average F_d was calculated from the fuel analyses of September 15, 2016, and September 17, 2016.

End of Section 1 – Project Overview

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2-1

	Tab Coker Heater Stack – FPM, CPM and	le 2-1: Total PM ₁₀ Emis	sions (Me	thod 5 / 20	2)
Run No	Э.	1	2	3	Average
Date (2	016)	Sep 16	Sep 16	Sep 16	
Start Ti	me (approx.)	10:37	14:14	17:25	
Stop Ti	me (approx.)	12:47	16:24	19:33	
Proces	s Conditions				
P ₁	Fuel gas flow rate (Mscf/day)	4,543	4,565	4,564	4,557
P ₂	Charge rate (bpd)	40,100	40,100	40,100	40,100
Fd	Oxygen-based F-factor (dscf/MMBtu)	8,339	8,339	8,339	8,339
Cap	Capacity factor (hours/year)	8,760	8,760	8,760	8,760
Gas Co	nditions				
O ₂	Oxygen (dry volume %)	5.3	5.1	5.1	5.2
CO_2	Carbon dioxide (dry volume %)	8.8	9.1	9.1	9.0
Τ _s	Sample temperature (°F)	400	402	402	401
B _w	Actual water vapor in gas (% by volume)	13.7	16.7	14.7	15.0
Gas Flo	ow Rate				
Q_a	Volumetric flow rate, actual (acfm)	88,400	88,400	87,500	88,100
Q_s	Volumetric flow rate, standard (scfm)	53,300	53,100	52,600	53,000
Q _{std}	Volumetric flow rate, dry standard (dscfm)	46,000	44,300	44,900	45,100
Sampli	ng Data				
V _{rnstd}	Volume metered, standard (dscf)	68.63	67.51	68.40	68.18
%i	Isokinetic sampling (%)	102.2	104.5	104.4	103.7
Labora	torv Data				
m,	Total FPM (g)	0.00534	0.00381	0.00267	
m _{CPM}	Total CPM (g)	0.00504	0.00949	0.00792	
m _{Part}	Total particulate (expressed as PM-10) (g)	0.01038	0.01330	0.01059	
n _{MDL}	Number of non-detectable fractions	N/A	N/A	N/A	
DLC	Detection level classification	ADL	ADL	ADL	
FPM R	esults				
C _{sd}	Particulate Concentration (lb/dscf)	1.7E-07	1.2E-07	8.6E-08	1.3E-07
Elp/hr	Particulate Rate (lb/hr)	0.47	0.33	0.23	0.35
E _{T/yr}	Particulate Rate (Ton/yr)	2,1	1.4	1.0	1.5
E _{Fd}	Particulate Rate - F _d -based (lb/MMBtu)	0.0019	0.0014	0.00095	0.0014
CPM R	esults				
C _{sd}	Particulate Concentration (lb/dscf)	1.6E-07	3.1E-07	2.6E-07	2.4E-07
E _{lb/hr}	Particulate Rate (lb/hr)	0.45	0,82	0.69	0.65
E _{T/yr}	Particulate Rate (Ton/yr)	2.0	3.6	3.0	2.9
E _{Fd}	Particulate Rate - F _d -based (lb/MMBtu)	0.0018	0.0034	0.0028	0.0027
Total P	articulate (as PM10) Results				
C _{sd}	Particulate Concentration (lb/dscf)	3.3E-07	4.3E-07	3.4E-07	3.7E-07
E _{lb/hr}	Particulate Rate (lb/hr)	0.92	1.2	0.92	1.00
E _{T/yr}	Particulate Rate (Ton/yr)	4.0	5.1	4.0	4.4
E _{Fd}	Particulate Rate - F _d -based (lb/MMBtu)	0.0037	0.0048	0.0038	0.0041

Average includes 3 runs.

Detection level classifications are defined as follows:

ADL = Above Detection Level - all fractions are above detection limit

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MARATHON PETROLEUM COMPANY LP DETROIT REFINERY

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2-2

		ncortainty Analysis	Ta EPM C	ble 2-2: PM and Total PM	(Mothod	5 / 202)
		FPM Results (Ib/MMBtu)	<u> </u>	CPM Results (lb/MMBtu)	Total	PM (as PM10) Results (Ib/MMBtu)
Method		5		202		5/202
Run No.	1	0.0019	1	0.0018	1	0.0037
	2	0.0014	2	0.0034	2	0.0048
	3	0.00095	3	0.0028	3	0.0038
SD		4.85E-04		8.14E-04		6.04E-04
AVG		0,00141		0,00268		0.00409
RSD		34.3%		30.3%		14.7%
N		3		3		3
SE		2.80E-04		4.70E-04		3.49E-04
RSE		19.8%		17.5%		8.5%
P		95.0%		95.0%		95.0%
TINV		4.30		4.30		4.30
CI +		0.00262		0.00470		0.00559
AVG		0.00141		0.00268		0.00409
CI -		0.00021		0.00066		0.00259
тв +		0.00513		0.00891		0.00872

AVG (average) is the mean value of the runs; N is the number of individual runs.

SD (standard deviation) and RSD (relative standard deviation) are measures of the variability of individual runs.

SE (standard error) and RSE (relative standard error) are measures of the variability of the average of the runs.

P (probability) is the confidence level associated with the two-tailed Student's t-distribution.

TINV (t-value) is the value of the Student's t-distrubution as a function of P (probability) and N-1 (degrees of freedom).

Cl (confidence interval) indicates that if the test is conducted again under the same conditions, the average would be expected to fall within the interval (Cl- to Cl+) about 95% of the time.

TB+ (upper tolerance bound) is the value below which 95% of future runs are expected to fall (assuming testing at the same conditions).

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RESULTS

2-3

	Tab	le 2-3:			
	Coker Heater Stack – THC, CH ₄ , C ₂ H ₆ ,	and VOC Emise	sions (Met	hod 25A / '	18)
Run No.	· · · · · · · · · · · · · · · · · · ·	1	2	3	Average
Date (20	016)	Sep 16	Sep 16	Sep 16	
Start Tin	ne (approx.)	10:03	11:39	14:17	
Stop Tim	ne (approx.)	11:30	13:04	15:42	
Process	Conditions				
P1	Fuel gas flow rate (Mscf/day)	4,541	4,546	4,561	4,549
P ₂	FCC charge rate (bpd)	40,100	40,100	40,100	40,100
Fd	Oxygen-based F-factor (dscf/MMBtu)	8,339	8,339	8,339	8,339
Gas Co	nditions				
O ₂	Oxygen (dry volume %)	5.2	5.3	5.2	5.2
CO2	Carbon dioxide (dry volume %)	9.3	9.3	9.3	9.3
Bw	Actual water vapor in gas (% by volume) ¹	13.7	13.7	16.7	14.7
THC Re	sults ²				
C_{sd}	Concentration (ppmdv as C ₃ H ₈)	<0.52	<0.52	<0.45	<0.50
C_{sd}	Concentration (lb/dscf)	<6.0E-08	<6.0E-08	<5.1E-08	<5.7E-08
E _{Fd}	Emission Rate - F _d -based (Ib/MMBtu)	< 0.00066	< 0.00066	< 0.00057	< 0.00063
Methan	e Results				
C_{sd}	Concentration (ppmdv)	2.1	2.2	2.0	2.1
C _{sd}	Concentration (Ib/dscf)	8.8E-08	9.2E-08	8.5E-08	8.8E-08
E_{Fd}	Emission Rate - F _d -based (lb/MMBtu)	0.0010	0.0010	0.0009	0.0010
Ethane	Results ³				
C_{sd}	Concentration (ppmdv)	<0.22	<0.22	<0.22	<0.22
C_{sd}	Concentration (lb/dscf)	<1.7E-08	<1.7E-08	<1.7E-08	<1.7E-08
E_{Fd}	Emission Rate - F _d -based (Ib/MMBtu)	< 0.00019	< 0.00019	< 0.00019	< 0.00019
VOC Re	sults ⁴				
E _{Fd}	Emission Rate - F _d -based (lb/MMBtu)	<0.00066	<0.00066	<0.00057	< 0.00063

Average includes 3 runs.

¹ Moisture data used for ppmwv to ppmdv correction obtained from nearly-concurrent M-5/202 runs.

² For THC, '<' indicates a measured response below the detection limit (assumed to be 1% of the instrument calibration span).

³ For ethane, '<' indicates a measured response below the analytical detection limit determined by the laboratory.

⁴ For VOCs, '<' indicates at least one non-detectable fraction was used in the calculations.

For all calcuated averages, "<" values are treated as the entire value of the detection limit.

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RESULTS

2-4

		Tab	le 2-4:				
	Coker Heater	Stack - NO	O _x Emissi	ons (Meth	nod 7E)		
Run No.		1	2	3	4	5	6
Date (20)16)	Sep 16	Sep 16	Sep 16	Sep 16	Sep 16	Sep 16
Start Tin	ne (approx.)	10:03	10:36	11:09	11:39	12:10	12:43
Stop Tim	ne (approx.)	10:24	10:57	11:30	12:00	12:31	13:04
Process	Conditions						
P ₁	Fuel gas flow rate (Mscf/day)	4,533	4,560	4,531	4,536	4,550	4,558
P ₂	Charge rate (bpd)	40,100	40,100	40,100	40,100	40,100	40,100
Fd	Oxygen-based F-factor (dscf/MMBtu)	8,339	8,339	8,339	8,339	8,339	8,339
Gas Co	nditions						
O ₂	Oxygen (dry volume %)	5.2	5.2	5.3	5.3	5.2	5.3
CO_2	Carbon dioxide (dry volume %)	9.4	9.4	9.3	9.3	9.3	9.3
Nitroger	n Oxides Results						
C _{sd}	Concentration (ppmdv)	23.5	23.4	23.6	23.5	23.4	23.6
C _{sd-x}	Concentration @ 0% O ₂ (ppmdv)	31.3	31.1	31.6	31.4	31.3	31.6
Csd	Concentration (lb/dscf)	2.81E-06	2.80E-06	2.81E-06	2.80E-06	2.80E-06	2.82E-06
E_{Fd}	Emission Rate - F _d -based (lb/MMBtu)	0.0312	0.0309	0.0315	0.0313	0.0311	0.0314
		7					
Run No.			7	8	9	10	Average
Date (20	16)		Sep 16	Sep 16	Sep 16	Sep 16	
Start Tim	ne (approx.)		14:17	14:49	15:21	15:56	
Stop Tin	ie (approx.)		14:38	15:10	15:42	16:17	
Process	Conditions						
P ₁	Fuel gas flow rate (Mscf/day)		4,558	4,569	4,559	4,570	4,552
P₂	Charge rate (bpd)		40,100	40,100	40,100	40,100	40,100
F_{d}	Oxygen-based F-factor (dscf/MMBtu)		8,339	8,339	8,339	8,339	8,339
Gas Cor	nditions						
O ₂	Oxygen (dry volume %)		5.2	5.2	5.3	5.1	5.2
CO2	Carbon dioxide (dry volume %)		9.3	9.4	9.3	9.4	9.3
Nitroger	n Oxides Results						
C_{sd}	Concentration (ppmdv)		23.5	23.2	23.2	23.1	23.4
C_{sd-x}	Concentration @ 0% O ₂ (ppmdv)		31.3	30.9	31.1	30.6	31.2
C_{sd}	Concentration (lb/dscf)		2,81E-06	2.78E-06	2.78E-06	2.76E-06	2.80E-06
E _{Fd}	Emission Rate - F _d -based (lb/MMBtu)		0.0312	0.0307	0.0309	0.0304	0.0311

Average includes 10 runs.

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RUIN	Start	Date	RM Data	CEMS Data	Difference	Difference
No.	Time	(2016)	(ppm@0%O2)	(ppm@0%O2)	(ppm@0%O2)	Percent
1	10:03	Sep 16	31.32	29.77	1.55	4.9%
2	10:36	Sep 16	31.08	29.58	1.50	4.8%
3	11:09	Sep 16	31.59	29.92	1.67	5.3%
4	11:39	Sep 16	31.41	29.99	1.42	4.5%
5	12:10	Sep 16	31.26	29.98	1,28	4.1%
6	12:43	Sep 16	31.57	30.02	1.55	4.9%
7	14:17	Sep 16	31.33	29.95	1.38	4.4%
8	14:49	Sep 16	30.85	29.38	1.47	4.8%
9	15:21	Sep 16	31.07	29.73	1.34	4.3%
10 *	15:56	Sep 16	30.56	28.75	1.81	5.9%
	Average		31.28	29.81	1.46	4.7%
			Relative Ac	curacy Test Audit	Results	
	Star	Idard Deviat	tion of Differences	0.121		
		Confidenc	e Coefficient (CC)	0.093		
		t-Valı	ue for 9 Data Sets	2.306		
					Limit	
	Re	ative Accu	racv (as % of RM)	5.0%	Limit 20.0%	
	Re Relative	elative Accu Accuracy (a	racy (as % of RM) as % of Appl. Std.)	5.0% 2.6%	Limit 20.0% 10.0%	
M = F	Relative App Reference = Continu	alative Accu Accuracy (a I. Std. = 60 Method (Cl uous Emissi	racy (as % of RM) as % of Appl. Std.) ppm@0%O2 eanAir Data) ons Monitoring Syste	5.0% 2.6%	Limit 20.0% 10.0% 	101116 1204
M = F EMS ATA	Relative App Reference = Continu calculatio	elative Accu Accuracy (a I. Std. = 60 Method (Cl ious Emissi ns are base	racy (as % of RM) as % of Appl. Std.) ppm@0%O2 eanAir Data) ons Monitoring Syste d on 9 of 10 runs. * ii	5.0% 2.6% em (Marathon Petrolo ndicates the exclude	Limit 20.0% 10.0% eum Company Data) d run.	101116 1204
XM = F EMS XATA (38	Relative App Reference = Continu calculatio	elative Accu Accuracy (a I. Std. = 60 Method (Cl ious Emissi ns are base	racy (as % of RM) as % of Appl. Std.) ppm@0%O2 eanAir Data) ons Monitoring Syste d on 9 of 10 runs. * ii	5.0% 2.6% em (Marathon Petrole ndicates the exclude	Limit 20.0% 10.0% eum Company Data) d run.	101116 1204
2M = F EMS ATA 38	Relative App Reference = Continu calculatio	elative Accu Accuracy (a I. Std. = 60 Method (Cl ious Emissi ns are base	racy (as % of RM) as % of Appl. Std.) ppm@0%O2 eanAir Data) ons Monitoring Syste d on 9 of 10 runs. * ii	5.0% 2.6% em (Marathon Petrole ndicates the exclude	Limit 20.0% 10.0% eum Company Data) d run.	101116 1204
2M = F EMS 24 30 28	Relative App Reference = Continu calculatio	elative Accu Accuracy (a I. Std. = 60 Method (Cl ious Emissi ins are base	racy (as % of RM) as % of Appl. Std.) ppm@0%O2 eanAir Data) ons Monitoring Syste d on 9 of 10 runs. * ii	5.0% 2.6% em (Marathon Petrole ndicates the exclude	Limit 20.0% 10.0% eum Company Data) d run.	101116 1204
M = F EMS 24TA 4 38 30 28 20	Relative App Reference = Continu calculatio	elative Accu Accuracy (a I. Std. = 60 Method (Cl ious Emissi ins are base	racy (as % of RM) as % of Appl. Std.) ppm@0%O2 eanAir Data) ons Monitoring Syste d on 9 of 10 runs. * ii	5.0% 2.6% em (Marathon Petrole ndicates the exclude	Limit 20.0% 10.0% eum Company Data) d run.	101116 1204
20 = F EMS 20 = A 30 20 20 20 10	Relative App Reference = Continu calculatio	elative Accu Accuracy (a I. Std. = 60 Method (Cl ious Emissi ins are base	racy (as % of RM) as % of Appl. Std.) ppm@0%O2 eanAir Data) ons Monitoring Syste d on 9 of 10 runs. * ii	5.0% 2.6% em (Marathon Petrole ndicates the exclude	Limit 20.0% 10.0% eum Company Data) d run.	101116 1204
20 20 20 20 10 20	Relative App Reference = Continu calculatio	elative Accu Accuracy (a I. Std. = 60 Method (Cl ious Emissi ns are base	racy (as % of RM) as % of Appl. Std.) ppm@0%O2 eanAir Data) ons Monitoring Syste d on 9 of 10 runs. * ii	5.0% 2.6% em (Marathon Petrole ndicates the exclude	Limit 20.0% 10.0% eum Company Data) d run.	101116 1204
20 20 20 20 20 10 10	Relative App Reference = Continu calculatio	alative Accu Accuracy (a I. Std. = 60 Method (Cl ious Emissi ns are base	racy (as % of RM) as % of Appl. Std.) ppm@0%O2 eanAir Data) ons Monitoring Syste d on 9 of 10 runs. * ii	5.0% 2.6% em (Marathon Petrole ndicates the exclude	Limit 20.0% 10.0% eum Company Data) d run.	
M = F EMS 36 36 26 26 16 10 5	Relative App Reference = Continu calculatio 5.00 5.00 5.00 5.00 5.00 5.00 5.00 5.00 5.00 5.00 5.00 5.00	elative Accu Accuracy (a I. Std. = 60 Method (Cl Jous Emissi Ins are base	racy (as % of RM) as % of Appl. Std.) ppm@0%O2 eanAir Data) ons Monitoring Syste d on 9 of 10 runs. * ii	5.0% 2.6% em (Marathon Petrole ndicates the exclude	Limit 20.0% 10.0% eum Company Data) d run.	

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Client Reference No: 4100665755 CleanAir Project No: 13082-1

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End of Section 2 - Results