Marathon Petroleum Company LP Coker Heater Report on Particulate Matter Testing

# 1. PROJECT OVERVIEW

# Test Program Summary

Marathon Petroleum Company LP contracted CleanAir Engineering (CleanAir) to complete testing on the Coker Heater (EU70-COKERHTR-S1) at the Detroit Refinery. The test program included particulate matter (PM) testing intended to demonstrate compliance with the MDEQ Permit No. MI-ROP-A9831-2012c.

For the testing described in this report, CleanAir mistakenly provided the crew with filters prepared for Method 5B instead of Method 5. The methods differ in how the filters are prepared prior to testing and how the filters are analyzed after testing. As further discussed in a memorandum from CleanAir to MPC dated September 24, 2020 presented in Appendix I of this report, this difference imparted a significant positive bias to the measured particulate emissions. Due to this error and the resulting bias, these tests results are not representative of true unit emissions and should be discarded. Consequently, particulate emissions are presented in this report but not evaluated against the applicable limits.

Section 2 Results provides a more detailed account of the test conditions and data analysis. Test program information, including the test parameters, on-site schedule and a project discussion, begin below.

# Test Program Details

### Parameters

The test program included the following emissions measurements:

- particulate matter (PM) as filterable particulate matter (FPM)
- total particulate matter less than 10 microns in diameter (PM<sub>10</sub>), assumed equivalent to the sum of the following constituents:
  - o FPM
  - o condensable particulate matter (CPM)
  - flue gas composition (e.g., O<sub>2</sub>, CO<sub>2</sub>, H<sub>2</sub>O)
- flue gas temperature
- flue gas flow rate

CleanAir

| Marathon Petroleum Company LP        | CleanAir Project No. 14199-3 |
|--------------------------------------|------------------------------|
| Coker Heater                         | Revision 0, Final Report     |
| Report on Particulate Matter Testing | Page 2                       |

### Schedule

Testing was performed on August 11 and 12, 2020. The on-site schedule followed during the test program is outlined in Table 1-1.

#### Table 1-1: Test Schedule

| Run<br>Number | Location     | Method               | Analyte | Date     | Start<br>Time | End<br>Time |
|---------------|--------------|----------------------|---------|----------|---------------|-------------|
| 1             | Coker Heater | USEPA Method 5 / 202 | FPM/CPM | 08/11/20 | 13:10         | 14:16       |
| 2             | Coker Heater | USEPA Method 5 / 202 | FPM/CPM | 08/11/20 | 14:53         | 15:59       |
| 3             | Coker Heater | USEPA Method 5 / 202 | FPM/CPM | 08/11/20 | 16:25         | 17:30       |
| 4             | Coker Heater | USEPA Method 5 / 202 | FPM/CPM | 08/12/20 | 07:43         | 08:49       |

### Discussion

### PM & PM<sub>10</sub> Testing

A total of four (4) 60-minute EPA Method 5/202 test runs were performed. PM and PM<sub>10</sub> emission results were calculated in units of pounds per million Btu (lb/MMBtu). The final result was expressed as the average of the three (3) highest runs.

 $PM_{10}$  is assumed equivalent to the sum of FPM and CPM. The Method 5/202 sample train yields a front-half, FPM result and a back-half, CPM result. The total PM result (FPM plus CPM) from Method 5/202 can be used as a worst-case estimation of total  $PM_{10}$  since Method 5 collects all FPM present in the flue gas (regardless of particle size). The final result was expressed as the average of the three (3) highest runs.

### **Calculations**

Emission results in units of dry volume-based concentration (lb/dscf, ppmdv) were converted into units of pound per million BTU (lb/MMBtu) using an oxygen-based fuel factor (F<sub>d</sub>) for refinery gas provided by MPC.

### Test Conditions

The unit was operated at the maximum normal operating capacity during each of the emissions compliance test runs. MPC was responsible for logging any relevant process-related data and providing it to CleanAir for inclusion in the test reports.

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CleanAir Project No. 14199-3 Revision 0, Final Report Page 3

Marathon Petroleum Company LP Coker Heater

**Report on Particulate Matter Testing** 

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# 2. RESULTS

This section summarizes the test program results. Additional results are available in the report appendices, specifically Appendix C Parameters.

### Table 2-1: Coker Heater – FPM & PM<sub>10</sub> Emissions

| Run No                  | ).  | 1        | 2        | 3*       | 4        | Average  |
|-------------------------|---|----------|----------|----------|----------|----------|
| Date (2020)             |   | Aug 11   | Aug 11   | Aug 11   | Aug 12   |          |
| Start Time (approx.)    |   | 13:10    | 14:53    | 16:25    | 07:43    |          |
| Stop Ti                 | me (approx.)  | 14:16    | 15:59    | 17:30    | 08:49    |          |
| Proces                  | ss Conditions                                       |          |          |          |          |          |
| $R_P$                   | Production Rate (BPD)                               | 38,500   | 38,500   | 38,500   | 38,500   | 38,500   |
| P <sub>1</sub>          | Fuel Consumption (mscf/day)                         | 4,191    | 4,219    | 4,179    | 4,180    | 4,192    |
| $F_{d}$                 | Oxygen-based F-factor (dscf/MMBtu)                  | 8,605    | 8,605    | 8,605    | 8,608    | 8,606    |
| Hi                      | Actual heat input (MMBtu/hr)                        | 208      | 209      | 207      | 209      | 208      |
| Gas Co                  | onditions   |          |          |          |          |          |
| O <sub>2</sub>          | Oxygen (dry volume %)                               | 6.6      | 6.7      | 6.7      | 6.6      | 6.6      |
| $CO_2$                  | Carbon dioxide (dry volume %)                       | 8.2      | 8.0      | 8.1      | 8.3      | 8.2      |
| $T_s$                   | Stack temperature (°F)                              | 401      | 402      | 404      | 392      | 398      |
| $B_{w}$                 | Actual water vapor in gas (% by volume)             | 14.4     | 14.6     | 14.0     | 14.0     | 14.3     |
| Gas Flo                 | ow Rate   |          |          |          |          |          |
| Qa                      | Volumetric flow rate, actual (acfm)                 | 98,700   | 97,300   | 96,900   | 98,900   | 98,300   |
| $Q_s$                   | Volumetric flow rate, standard (scfm)               | 58,700   | 57,800   | 57,400   | 60,000   | 58,900   |
| <b>Q</b> <sub>std</sub> | Volumetric flow rate, dry standard (dscfm)          | 50,300   | 49,400   | 49,400   | 51,600   | 50,400   |
| Sampli                  | ing Data  |          |          |          |          |          |
| Vmstd                   | Volume metered, standard (dscf)                     | 31.61    | 32.10    | 32.52    | 34.30    | 32.67    |
| %1                      | lsokinetic sampling (%)                             | 96.1     | 99.4     | 100.7    | 101.6    | 99.1     |
| Labora                  | itory Data <sup>1</sup>                             |          |          |          |          |          |
| mn                      | Total FPM (g)                                       | 0.00337  | 0.00329  | 0.00339  | 0.00373  |          |
| m <sub>CPM</sub>        | Total CPM (g)                                       | 0.00288  | 0.00267  | 0.00061  | 0.00192  |          |
| m <sub>Part</sub>       | Total particulate matter (g)                        | 0.00625  | 0.00596  | 0.00400  | 0.00565  |          |
| FPM Re                  | esults <sup>2</sup>                                 |          |          |          |          |          |
| $C_{sd}$                | Particulate Concentration (lb/dscf)                 | 2.35E-07 | 2.26E-07 | 2.30E-07 | 2.40E-07 | 2.35E-07 |
| E <sub>lb/hr</sub>      | Particulate Rate (lb/hr)                            | 0.710    | 0.669    | 0.681    | 0.742    | 0.711    |
| $E_{Fd}$                | Particulate Rate - F <sub>d</sub> -based (Ib/MMBtu) | 0.00296  | 0.00286  | 0.00291  | 0.00302  | 0.00296  |
| CPM R                   | esults  |          |          |          |          |          |
| $C_{sd}$                | Particulate Concentration (lb/dscf)                 | 2.01E-07 | 1.84E-07 | 4.14E-08 | 1.23E-07 | 1.37E-07 |
| E <sub>lb/hr</sub>      | Particulate Rate (lb/hr)                            | 0.606    | 0.544    | 0.123    | 0.381    | 0.413    |
| $E_{Fd}$                | Particulate Rate - F <sub>d</sub> -based (lb/MMBtu) | 0.00252  | 0.00233  | 0.00052  | 0.00155  | 0.00173  |
| PM <sub>10</sub> R      | esults <sup>3</sup>                                 |          |          |          |          |          |
| C <sub>sd</sub>         | Particulate Concentration (lb/dscf)                 | 4.36E-07 | 4.10E-07 | 2.71E-07 | 3.63E-07 | 4.03E-07 |
| E <sub>lb/hr</sub>      | Particulate Rate (lb/hr)                            | 1.32     | 1.21     | 0.804    | 1.12     | 1.217    |
| E <sub>Fd</sub>         | Particulate Rate - F <sub>d</sub> -based (Ib/MMBtu) | 0.00548  | 0.00519  | 0.00343  | 0.00457  | 0.00508  |

The particulate results in this table are not believed to be representative of true emissions.

<sup>1</sup> Front half filter tare weights were determined subsequent to baking at 160°C, final weights were determined subsequent to baking at 105°C.

<sup>2</sup> FPM final average is the average of the three (3) highest FPM runs.

 $^3\,\text{PM}_{10}$  final average is the average of the three (3) highest  $\text{PM}_{10}$  runs.

Marathon Petroleum Company LP Coker Heater Report on Particulate Matter Testing

# 3. DESCRIPTION OF INSTALLATION

# Process Description

MPC's facility in Detroit, Michigan, produces refined petroleum products from crude oil. MPC must continue to demonstrate that select process units are in compliance with permitted emission limits.

The Coker unit (EU70-COKER) converts Vacuum Resid (Crude Vacuum Tower Bottoms), a product normally sold as asphalt or blended into residual fuel oil, into lighter, more valuable products. The Vacuum Resid feedstock is heated before it enters the main fractionator, where lighter material vaporizes. The fractionator bottoms are routed through a fired heater and then into a coke drum. This emission unit consists of process vessels (fractionators), coke drums, heater (EU70-COKERHTR-S1), cooling tower, compressors, pumps, piping, drains and various components (pumps and compressor seals, process valves, pressure relief valves, flanges, connectors, etc.). This emission group includes the Coke Handling System, which collects, sizes and transports the petroleum coke created during the coking process. The system consists of a coke pit, storage pad, enclosed crusher, enclosed conveyors and surge bins.

The Coker Heater is fired by refinery fuel gas. Emissions are vented to the atmosphere via the Coker Heater Stack (SV70-H1) where testing was performed.

## Test Location

The sample point locations were determined by EPA Method 1. Table 3-1 presents the sampling information for the test location described in this report. The figure shown on page 5 represents the layout of the test location.

### Table 3-1: Sampling Point Information

| <u>Source</u><br>Constituent | Method (USEPA) | Run No. | Ports | Points per<br>Port | Minutes<br>per Point | Total<br>Minutes | Figure |
|------------------------------|----------------|---------|-------|--------------------|----------------------|------------------|--------|
| Coker Heater Stack           |                |         |       |                    |                      |                  |        |
| FPM/CPM                      | 5 / 202        | 1-4     | 4     | 3                  | 5                    | 60               | 3-1    |

Marathon Petroleum Company LP Coker Heater Report on Particulate Matter Testing

Figure 3-1:

CleanAir Project No. 14199-3 Revision 0, Final Report Page 5

### FPM & PM<sub>10</sub> Sample Point Layout 107.5 in.-Port 1 North + Gas Flow Out of Page ++ Port 4 Port 2 + -+ + + + + + + Port 3 Port to Point Sampling % of Stack Distance Point Diameter (inches) 1 29.6 31.8 2 14.6 15.5 3 4.4 4.7 Duct diameters upstream from flow disturbance (A): 5.2 Limit: 0.5 Duct diameters downstream from flow disturbance (B): 8.3 Limit: 2.0

Marathon Petroleum Company LP Coker Heater Report on Particulate Matter Testing

# 4. METHODOLOGY

# Procedures and Regulations

The test program sampling measurements followed procedures and regulations outlined by the USEPA and Michigan Department of Environment, Great Lakes, and Energy (EGLE). These methods appear in detail in Title 40 of the CFR and at https://www.epa.gov/emc.

CleanAir follows specific QA/QC procedures outlined in the individual methods and in USEPA "Quality Assurance Handbook for Air Pollution Measurement Systems: Volume III Stationary Source-Specific Methods," EPA/600/R-94/038C. Appendix D contains additional QA/QC measures, as outlined in CleanAir's internal Quality Manual.

### Title 40 CFR Part 60, Appendix A

| Method 1     | "Sample and Velocity Traverses for Stationary Sources"   |
|--------------|--|
| Method 2     | "Determination of Stack Gas Velocity and Volumetric Flow Rate (Type S Pitot Tube)"   |
| Method 3     | "Gas Analysis for the Determination of Dry Molecular Weight"   |
| Method 3A    | "Determination of Oxygen and Carbon Dioxide Concentrations in Emissions from Stationary Sources (Instrumental Analyzer Procedure)" |
| Method 3B    | "Gas Analysis for the Determination of Emission Rate Correction Factor or Excess Air"  |
| Method 4     | "Determination of Moisture Content in Stack Gases"   |
| Method 5     | "Determination of Particulate Matter Emissions from Stationary Sources"  |
| Title 40 CFI | R Part 51, Appendix M  |

Method 202 "Dry Impinger Method for Determining Condensable Particulate Emissions from Stationary Sources"

Marathon Petroleum Company LP Coker Heater Report on Particulate Matter Testing

# Methodology Discussion

### PM & PM<sub>10</sub> Testing – USEPA Method 5/202

PM and PM<sub>10</sub> emissions were determined using EPA Method 5/202. Filters for this test were mistakenly prepared for Method 5B rather than for Method 5 resulting in a high bias for particulate matter emissions. See Appendix I for more details.

The front-half of the sampling train consisted of a glass nozzle, glass liner and filter holder heated to 248°F ± 25°F and a quartz fiber filter. Flue gas samples were extracted isokinetically per Method 5 requirements.

The back-half (Method 202 portion) of the sampling train is designed to mimic ambient conditions and collect only the particles that would truly form CPM in the atmosphere by minimizing the sulfur dioxide (SO<sub>2</sub>) and nitrogen oxide (NO<sub>X</sub>) interferences observed with earlier versions of the method, in which flue gas was bubbled through cold water, and SO<sub>2</sub> and NO<sub>X</sub> were absorbed and partially oxidized before they could be purged out with nitrogen (N<sub>2</sub>).

Flue gas exiting the front-half heated filter passes through a coiled condenser and dry impinger system jacketed by water continually circulated at ambient temperature. Moisture is removed from the flue gas without bubbling through the condensed water. Flue gas then passes through a tetrafluoromethane (TFE) membrane filter at ambient temperature. The temperature of the flue gas at the exit of the filter was directly measured with an in-line thermocouple and maintained in the temperature range of 65°F to 85°F.

After exiting the ambient filter, the flue gas passes through two (2) additional impingers surrounded by ice in a "cold" section of the impinger bucket. The moisture collected in these impingers will not be analyzed for CPM and is only collected to determine the flue gas moisture and to thoroughly dry the gas. The sample gas then flows into a calibrated dry gas meter where the collected sample gas volume is determined.

The front-half portion of the sample train (nozzle, probe and heated filter) was recovered per Method 5 requirements, using acetone as the recovery solvent. The back-half of the sample train (heated filter outlet, condenser, dry impingers and TFE membrane filter) was recovered per Method 202 requirements. The impinger train was purged with  $N_2$  at a rate of 14 liters per minute (lpm) for one (1) hour following each test run and prior to recovery.

A field train blank was assembled, purged and recovered as if it were an actual test sample; analysis of the field train blank was used to blank-correct the test run results. Reagent blanks were collected to quantify background contamination. All samples and blanks were returned to CleanAir Analytical Services in Palatine, Illinois, for gravimetric analysis. Method 202 samples were maintained at a temperature < 85°F during transport to the laboratory.

All samples and blanks were returned to CleanAir Analytical Services in Palatine, Illinois, for gravimetric analysis. Upon receipt, the filters dessicated for 24 hours at ambient temperature followed by an oven dry at 220°F. The front-half rinses were evaporated at ambient temperature and pressure. The masses from each fraction were then summed for a total FPM mass.

Marathon Petroleum Company LP Coker Heater Report on Particulate Matter Testing CleanAir Project No. 14199-3 Revision 0, Final Report Page 8

# 5. APPENDIX

Appendix A: Test Method Specifications Appendix B: Sample Calculations Appendix C: Parameters Appendix D: QA/QC Data Appendix E: Field Data Appendix F: Field Data Printouts Appendix G: Facility Process & Fuel Analysis Data Appendix H: Laboratory data Appendix I: Filter Memo Appendix J: CleanAir Resumes and Certifications

# APPENDIX A: TEST METHOD SPECIFICATIONS

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### **Specification Sheet for**

### EPA Method 5/202

**Standard Method Specification** 

Source Location Name(s) Pollutant(s) to be Determined Other Parameters to be Determined from Train Coker Heater Stack Filterable Particulate Matter (FPM) and Condensable Particulate Matter (CPM) Gas Density, Moisture, Flow Rate

| Dellestent | 0        |             |
|------------|----------|-------------|
| Pollutant  | Sampling | Information |

Duration of Run No. of Sample Traverse Points Sample Time per Point Sampling Rate

#### Sampling Probe

Nozzle Material Nozzle Design Probe Liner Material Effective Probe Length Probe Temperature Set-Point

#### **Velocity Measuring Equipment**

Pitot Tube Design Pitot Tube Coefficient Pitot Tube Calibration by Pitot Tube Attachment

#### **Metering System Console**

Meter Type Meter Accuracy Meter Resolution Meter Size Meter Calibrated Against Pump Type Temperature Measurements Temperature Resolution ΔP Differential Pressure Gauge ΔH Differential Pressure Gauge Barometer

#### **FPM Filter Description**

Filter Location Filter Holder Material Filter Support Material Cyclone Material Filter Heater Set-Point Filter Material

#### **Other Components**

Description Location Operating Temperature Stainless Steel or Glass Button-Hook or Elbow Glass or Teflon N/A 248°F±25°F

Isokinetic (90-110%)

N/A

N/A

N/A

Type S N/A Geometric or Wind Tunnel Attached to Probe

Dry Gas Meter ±2% N/A N/A Wet Test Meter or Standard DGM N/A N/A 5.4°F Inclined Manometer or Equivalent Inclined Manometer or Equivalent Mercury or Aneroid

After Probe Quartz Glass Frit N/A 248°F±25°F Glass Fiber

Condenser Before Impinger 1 ≤85°F Borosilicate Glass Button-Hook Borosilicate Glass 6 feet

Isokinetic (90-110%)

60 minutes

5 minutes

12

Actual Specification Used

Type S 0.830 Wind-Tunnel Attached to Probe

248°F±25°F

Dry Gas Meter ±1% 0.01 cubic feet 0.1 dcf/revolution Wet Test Meter Rotary Vane Type K Thermocouple/Pyrometer 1.0°F Inclined Manometer Inclined Manometer Digital Barometer calibrated w/Mercury Aneroid

Exit of Probe Borosilicate Glass Teflon None 248°F±25°F Quartz Fiber

Condenser Before 1st Impinger ≤85°F

### **Specification Sheet for**

#### Impinger Train Description

Type of Glassware Connections Connection to Probe or Filter by Number of Impingers Impinger Stem Types Impinger 1 Impinger 2 Impinger 3 Impinger 4 Impinger 5 Impinger 6 Impinger 7 Impinger 8

#### **CPM Filter Description**

Filter Location Filter Holder Material Filter Support Material Cyclone Material Filter Heater Set-Point Filter Material

#### **Gas Density Determination**

Sample Collection Sample Collection Medium Sample Analysis

#### Sample Recovery Information

Nozzle Brush Material Nozzle Rinse Reagent Nozzle Rinse Wash Bottle Material Nozzle Rinse Storage Container Filter Recovered? Filter Storage Container Impinger Contents Recovered? Impinger Rinse Reagent Impinger Wash Bottle Impinger Storage Container

#### **Analytical Information**

Method 4 H<sub>2</sub>O Determination by Filter Preparation Conditions Front-Half Rinse Preparation Back-Half Analysis Additional Analysis

### EPA Method 5/202

#### **Standard Method Specification**

Leak-Free Glass Connectors Direct or Flexible Connection 4

Shortened Stem (open tip) Modified Greenburg-Smith Modified Greenburg-Smith Modified Greenburg-Smith

#### Actual Specification Used

Ground Glass with Silicone O-Ring Flexible Teflon Line 4

Shortened Stem (open tip) Modified Greenburg-Smith Modified Greenburg-Smith Modified Greenburg-Smith

Between 2nd and 3rd Impingers Glass, Stainless Steel or Teflon Teflon None >65°F but ≤85°F Teflon Membrane

Multi-point integrated Flexible Gas Bag Orsat or CEM Analyzer

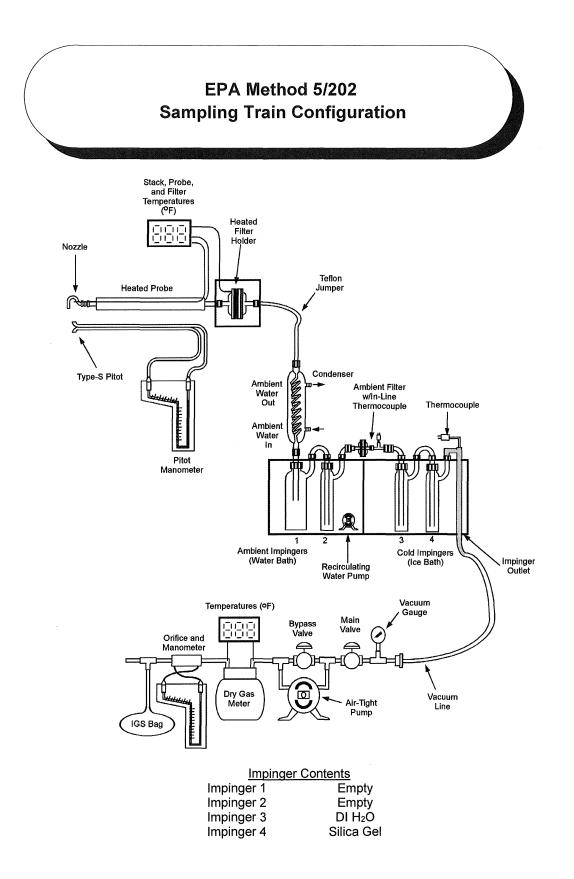
Nylon Bristle or Teflon Acetone Glass or Polyethylene Glass or Polyethylene Yes FH filter in petri dish, CPM filter in petri dish Yes DI Water/Acetone/Hexane Inorganic in polyethylene, organic in Teflon Inorganic in polyethylene, organic in glass

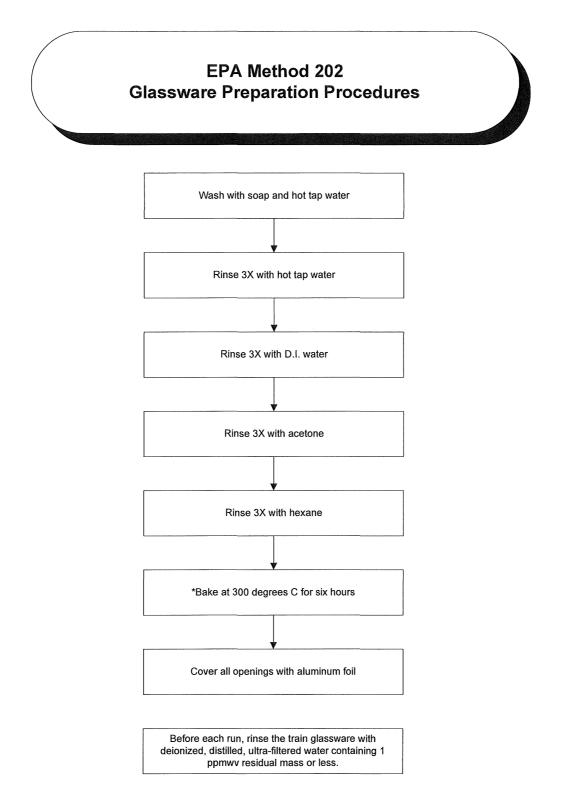
Volumetric or Gravimetric Dessicate 24 Hours or Filter Extraction Evaporate at ambient temperature and pressure Sonication and Extraction N/A Between 2nd and 3rd Impingers Borosilicate Glass Teflon None >65°F but ≤85°F Teflon Membrane

Multi-Point Integrated Vinyl Bag CEM

Nylon Bristle Acetone Inorganic in polyethylene, organic in Teflon Glass Yes FH filter in petri dish, CPM filter in petri dish Yes DI Water/Acetone/Hexane Inorganic in polyethylene, organic in Teflon Inorganic in amber glass, organic in amber glass

Gravimetric and Volumetric See Analytical Flow Chart Evaporate at ambient temperature and pressure See Analytical Flow Chart None

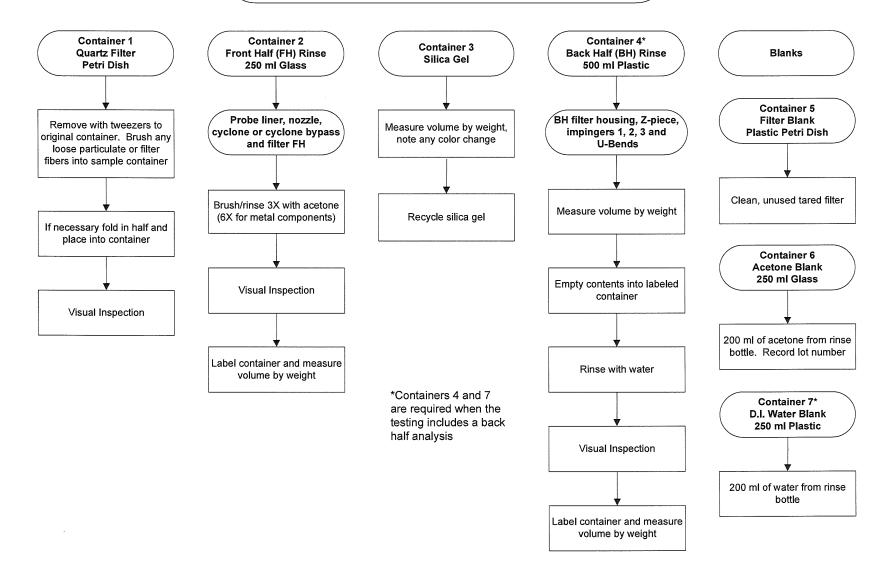


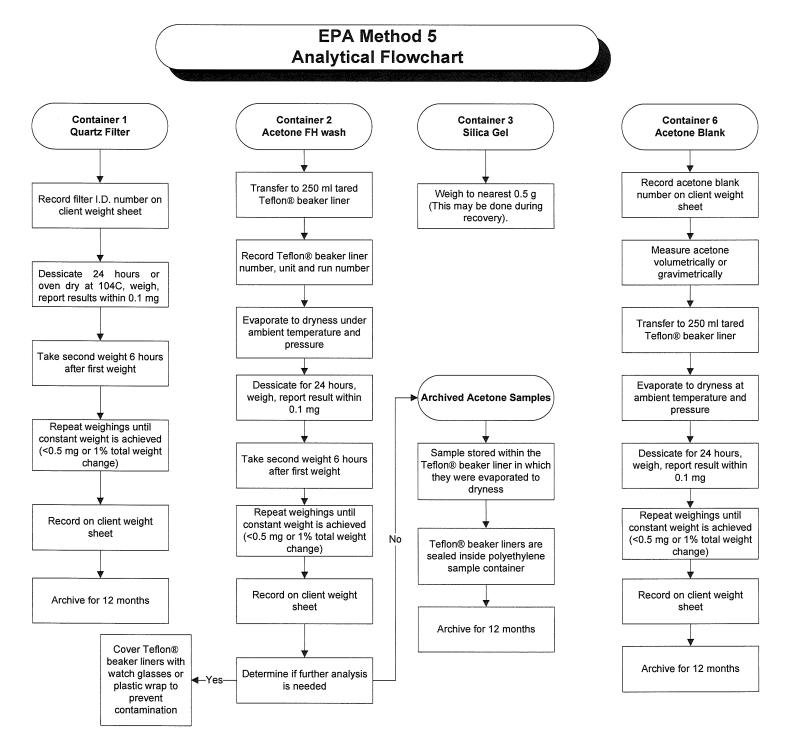


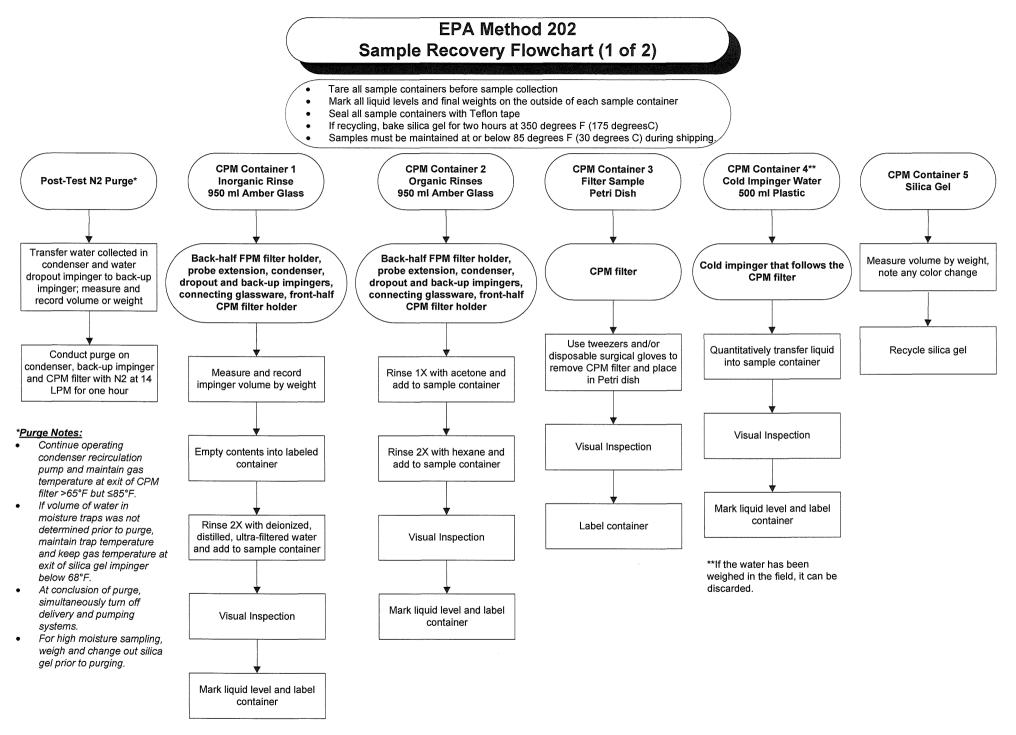
\*As an alternative to baking glassware, a field train proof blank can be performed on the sampling train glassware.

# EPA Method 5 Sample Recovery Flowchart

- Tare all sample containers before sample collection
- Mark all liquid levels and final weights on the outside of each sample container
- Seal all sample containers with Teflon tape
- If recycling, bake silica gel for two hours at 350 degrees F (175 degrees C)

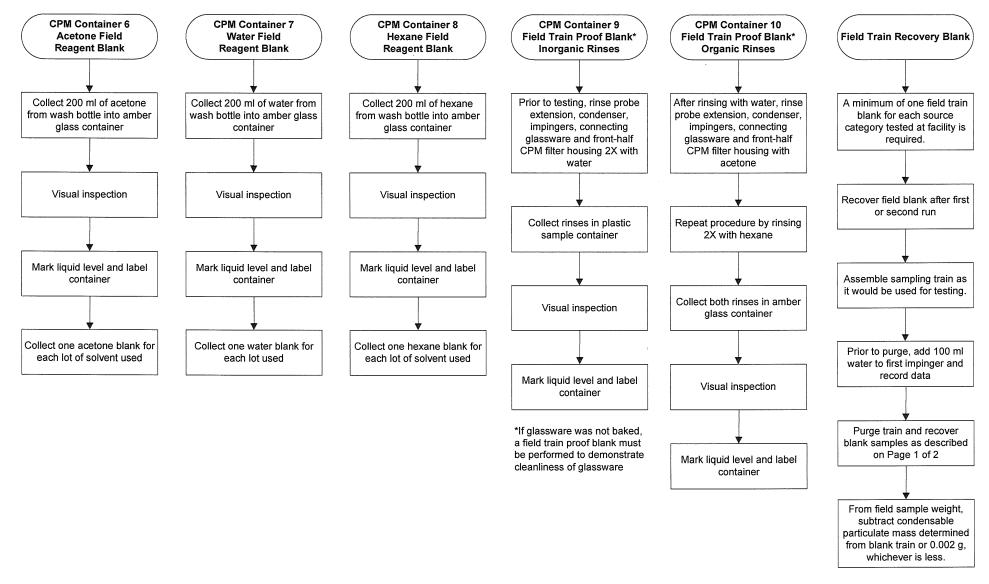


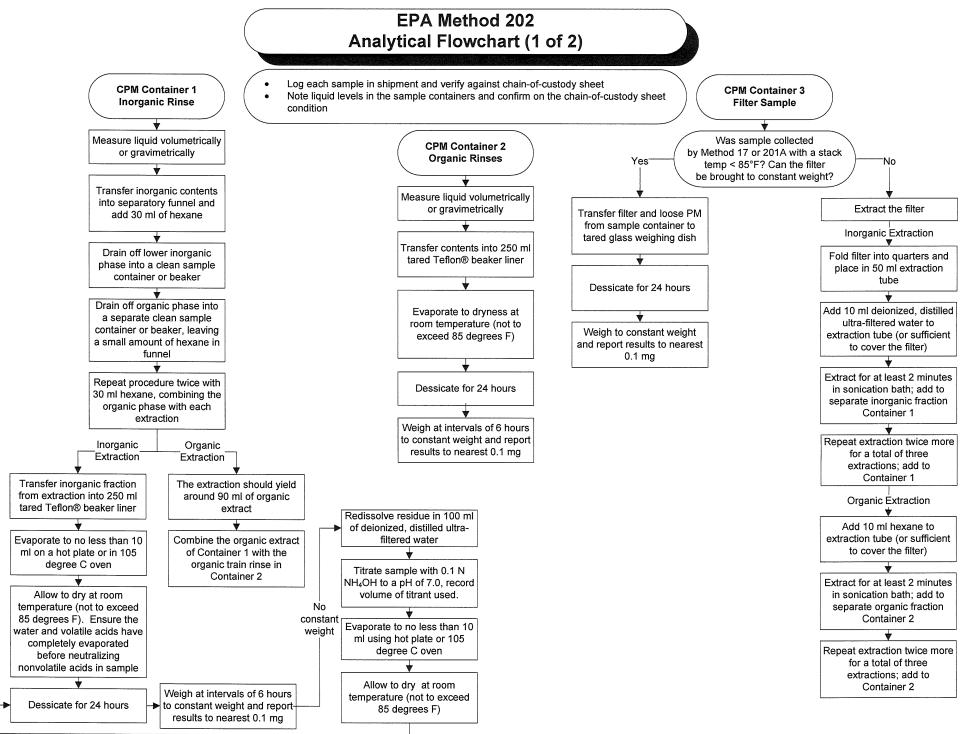




## EPA Method 202 Sample Recovery Flowchart (2 of 2)

- Tare all sample containers before sample collection
- Mark all liquid levels and final weights on the outside of each sample container
- Seal all sample containers with Teflon tape
- If recycling, bake silica gel for two hours at 350 degrees F (175 degrees C)
- Samples must be maintained at or below 85 degrees F (30 degrees C) during shipping.





A - 11

