

Particulate Matter Compliance Emissions Test Report

Holcim (US) Inc. d/b/a Lafarge Alpena Alpena Cement Plant Kilns 20, 21, 22, and 23 Indirect Firing Baghouses Alpena, Michigan June 22 through 23, 2022 and July 6 and July 8, 2022

> Report Submittal Date August 30, 2022

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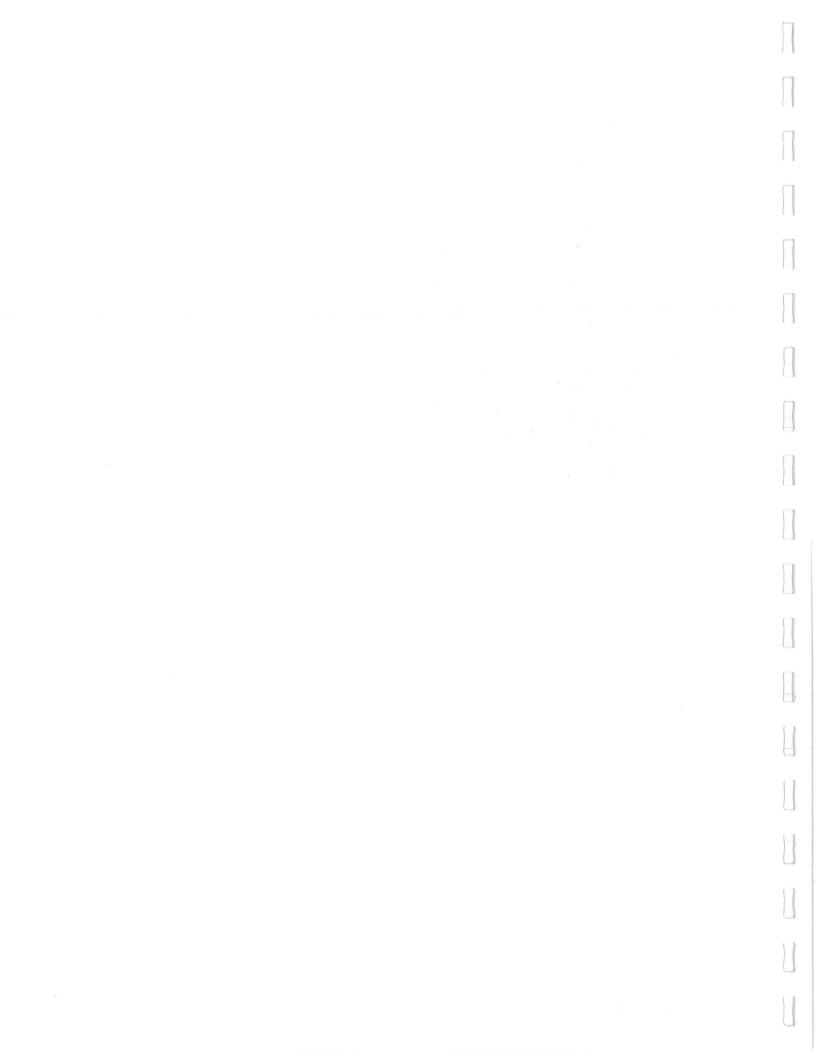
Project No. M222412A

Corporate Headquarters 888 Industrial Drive Elmhurst, Illinois 60126 630-993-2100



TABLE OF CONTENTS

1.0 EXECUTIVE SUMMARY	1
2.0 TEST METHODOLOGY Method 1 Sample and Velocity Traverse Determination	
Method 2 Volumetric Flow Rate Determination	
Method 201A Filterable Particulate Matter Determination Method 202 Condensable Particulate Determination	
3.0 TEST RESULTS SUMMARIES	4
4.0 CERTIFICATION	
APPENDICES	
Appendix A - Test Section Diagrams	
Appendix B - Sample Train Diagrams	
Appendix C - Calculation Nomenclature and Formulas	
Appendix D - Laboratory Analysis Data	
Appendix E - Reference Method Test Data	
Appendix F - Plant Operating Data	
Appendix G - Field Data Sheets	
Appendix H - Calibration Data	



1.0 EXECUTIVE SUMMARY

Mostardi Platt conducted a total particulate matter compliance test program on the Kiln 20, 21, 22, and 23 Indirect Firing Baghouses for Holcim (US) Inc. d/b/a Lafarge Alpena at the Alpena Cement Plant in Alpena, Michigan. This report summarizes the results of the test program and test methods.

The test locations, test dates, and test parameter are summarized below.

TEST INFORMATION					
Test Locations	Test Dates	Test Parameter			
Kilns 20, 21, 22, and 23 Indirect Firing Baghouses	June 22 through 23, July 6, and July 8, 2022	Filterable Particulate Matter (FPM), Condensable Particulate Matter (CPM), and Total Particulate Matter (TPM/PM10)			

The purpose of the test program was to demonstrate compliance with the State of Michigan Renewal Operating Permit, specifically, to demonstrate that each of the below listed sources meet their FPM (and <PM₁₀, as applicable) emission limit.

Test Location	Parameter	Test Result	Emission Limit
Kiln 20 Indirect Firing Baghouse	FPM	0.002 lb/1,000 lb exhaust gas, dry	0.15 lb/1,000 lb exhaust gas, dry
Kiln 20 Indirect Firing Baghouse	PM10	0.2 lb/hr	1.8 lb/hr
Kiln 21 Indirect Firing Baghouse	FPM	0.016 lb/1,000 lb exhaust gas, dry	0.15 lb/1,000 lb exhaust gas, dry
Kiln 21 Indirect Firing Baghouse	PM10	1.4 lb/hr	1.8 lb/hr
Kiln 22 Indirect Firing Baghouse	FPM	0.019 lb/1,000 lb exhaust gas, dry	0.15 lb/1,000 lb exhaust gas, dry
Kiln 22 Indirect Firing Baghouse	PM ₁₀	2.5 lb/hr	2.9 lb/hr
Kiln 23 Indirect Firing Baghouse	FPM	0.012 lb/1,000 lb exhaust gas, dry	0.15 lb/1,000 lb exhaust gas, dry
Kiln 23 Indirect Firing Baghouse	PM10	2.0 lb/hr	2.9 lb/hr

The identifications of the individuals associated with the test program are summarized below.

TEST PERSONNEL INFORMATION				
Location	Address	Contact		
Test Facility	Holcim (US) Inc.	Ms. Mallory Miller		
	Alpena Plant	Area Environmental Engineer		
	1435 Ford Avenue	224-517-6896		
	Alpena, MI 49707	Mallory.miller@lafargeholcim.com		
Testing Company	Mostardi Platt	Mr. Chris Trezak		
Supervisor	888 Industrial Drive	Senior Project Manager		
	Elmhurst, Illinois 60126	630-993-2100 (phone)		
		ctrezak@mp-mail.com		

The test crew consisted of Messrs. C. Buglio, K. Beckham, D. Jordan, M. Friduss, D. Jordan, R. Spoolstra, J. Meyerhoff, and C. Trezak.

2.0 TEST METHODOLOGY

Emission testing was conducted following the United States Environmental Protection Agency (USEPA) methods specified in 40CFR60, Appendix A and 40CFR51, Appendix M in addition the Mostardi Platt Quality Manual. Schematics of the test section diagrams and sampling trains used are included in Appendix A and B respectively. Calculation nomenclature are included in Appendix C. Laboratory analysis for each test run are included in Appendix D. The computerized reference method test data is included in Appendix E. CEM data and process data as provided by Holcim (US) Inc. are also included in Appendix F.

The following methodologies were used during the test program:

Method 1 Sample and Velocity Traverse Determination

Test measurement points were selected in accordance with USEPA Method 1, 40CFR60, Appendix A. The characteristics of the measurement location are summarized below.

TEST POINT INFORMATION						
Test Location	Stack Dimensions	No. of Ports	Upstream Diameters	Downstream Diameters	Test Parameter	Number of Sampling Points
Kiln 20 Indirect Firing Baghouse	2.33 Feet	2	>2.0	>8.0	FPM/PM ₁₀	12
Kiln 21 Indirect Firing Baghouse	2.29 Feet	2	5.5	3.8	FPM/PM ₁₀	12
Kiln 22 Indirect Firing Baghouse	3.0 Feet	2	>0.5	>2.0	TPM/PM ₁₀	24
Kiln 23 Indirect Firing Baghouse	3.04167 Feet	2	2.6	9.9	FPM/PM10	12

Method 2 Volumetric Flow Rate Determination

Gas velocity was measured following USEPA Method 2, 40CFR60, Appendix A, for purposes of calculating stack gas volumetric flow rate and particulate emission rates on a lb/hr basis. S-type pitot tubes, 0-10" differential pressure gauge, and K-type thermocouple and temperature readout were used to determine gas velocity at each sample point. All of the equipment used was

calibrated in accordance with the specifications of the Method. Copies of field data sheets are included in Appendix G. Calibration data are presented in Appendix H. This testing met the performance specifications as outlined in the Method. All testing was considered to be ambient, per section 8.6 of USEPA Method 2, and therefore a dry molecular weight of 29.0 was used at this location.

Method 201A Filterable Particulate Matter Determination

Stack gas PM₁₀ emission rates were determined in accordance with Method 201A, 40CFR51, Appendix M. An Environmental Supply Company, Inc. sampling train was used to sample stack gas at an isokinetic rate, as specified in the Method. The samples were analyzed by Mostardi Platt in accordance with the Method in the Elmhurst, Illinois laboratory. Laboratory data is found in Appendix D. All of the equipment used was calibrated in accordance with the specifications of the Method. Calibration data is presented in Appendix H.

Method 202 Condensable Particulate Determination

Stack gas condensable particulate matter concentrations and emission rates were determined in accordance with USEPA Method 202, in conjunction with Method 5 or Method 201A filterable particulate sampling. This method applies to the determination of CPM emissions from stationary sources. It is intended to represent condensable matter as material that condenses after passing through a filter and as measured by this method.

The CPM was collected in impingers after filterable particulate material was collected using Method 202. Compared to the December 17, 1991 promulgated Method 202, this Method includes the addition of a condenser, followed by a water dropout impinger immediately after the final heated filter. One modified Greenburg Smith impinger and an ambient temperature filter follow the water dropout impinger.

CPM was collected in the water dropout, modified Greenburg Smith impinger and ambient filter portion of the sampling train as described in this Method. The impinger contents were purged with nitrogen (N_2) immediately after sample collection to remove dissolved sulfur dioxide (SO₂) gases from the impingers. The impinger solution was then extracted with deionized water and hexane. The organic and aqueous fractions were dried and the residues weighed. The total of the aqueous, organic, and ambient filter fractions represents the CPM.

All sample recovery was performed at the test site by the test crew. Mostardi Platt personnel at the laboratory in Elmhurst, Illinois, performed all final particulate sample analyses. All of the equipment used was calibrated in accordance with the specifications of the Method. Calibration data are presented in Appendix H.

3.0 TEST RESULTS SUMMARIES

Client: Facility: Test Location: Test Method:	Holcim (US) Inc. Alpena Cement Plant Indirect Firing Baghouse 20 201A/202				
	Source Condition	Normal	Normal	Normal	
	Date	7/8/22	7/8/22	7/8/22	
	Start Time	8:20	10:22	12:22	
	End Time	9:53	11:53	13:53	
	04	Run 1	Run 2	Run 3	Average
		onditions	151.1	150.0	450.5
	verage Gas Temperature, °F	150.3	151.1	150.0	150.5
	loisture, percent by volume	5.2%	5.7%	4.7%	5.2%
Av	erage Flue Pressure, in. Hg	29.64	29.64	29.64	29.64
	Gas Sample Volume, dscf	35.720	35.513	35.402	35.545
	Average Gas Velocity, ft/sec	81.698	81.526	80.701	81.308
	Volumetric Flow Rate, acfm	20,901	20,857	20,646	20,801
	olumetric Flow Rate, dscfm	16,980	16,840	16,870	16,897
Gas Volumetric Flow Rate, scfm		17,909	17,850	17,700	17,820
	103.4	103.6	103.1	103.4	
Filterable <pm10 (method="" 201a)<="" th=""><th>10 S - 11 - 1</th><th></th></pm10>			10 S - 11 - 1		
	grams collected	0.00235	0.00057	0.00259	0.00184
	grains/acf	0.0008	0.0002	0.0009	0.0006
	grains/dscf	0.0010	0.0002	0.0011	0.0008
	lb/hr	0.1	0.0	0.2	0.1
	lb/1000 lb of stack gas	0.002	0.000	0.002	0.002
	Condensable F	PM (Metho			1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1
	grams collected	0.00213	0.00194	0.00024	0.00144
	grains/acf	0.0007 0.0009	0.0007	0.0001	0.0005
	grains/dscf		0.0008	0.0001	0.0006
	lb/hr	0.1	0.1	0.0	0.1
	Total PM<10 (N	lethod 201		1.	
	grams collected	0.00448	0.00251	0.00283	0.00328
	grains/acf	0.0016	0.0009	0.0010	0.0012
	grains/dscf	0.0019	0.0011	0.0012	0.0014
	lb/hr	0.3	0.2	0.2	0.2

Client:	Holcim (US) Inc.				
Facility:	Alpena Cement Plant				
Test Location: Test Method:	Indirect Firing Baghouse 21 201A/202				
	Source Condition Date	Normal 7/6/22	Normal 7/6/22	Normal 7/6/22	
	Start Time	11:40	14:55	17:20	
	End Time	13:14	16:28	18:52	
		Run 1	Run 2	Run 3	Average
	Stack Cor	nditions	1.15		
Av	verage Gas Temperature, °F	156.2	156.3	156.5	156.3
Flue Gas N	loisture, percent by volume	5.9%	5.5%	5.9%	5.8%
Av	erage Flue Pressure, in. Hg	29.43	29.43	29.43	29.43
	Gas Sample Volume, dscf	34.664	34.572	35.070	34.769
	Average Gas Velocity, ft/sec	80.714	80.502	80.429	80.548
Gas	Volumetric Flow Rate, acfm	19,946	19,894	19,876	19,905
	olumetric Flow Rate, dscfm	15,828	15,849	15,753	15,810
Gas	16,813	16,765	16,745	16,774	
	95.2	94.8	96.7	95.6	
	Filterable <pm10< th=""><th>(Method 2</th><th></th><th></th><th></th></pm10<>	(Method 2			
	grams collected	0.02185	0.01168	0.02465	0.01939
	grains/acf	0.0077	0.0042	0.0086	0.0068
	grains/dscf	0.0097	0.0052	0.0108	0.0086
	lb/hr	1.3	0.7	1.5	1.2
4	lb/1000 lb of stack gas	0.019	0.010	0.021	0.016
	Condensable PM				
	grams collected	0.00143	0.00698	0.00347	0.00396
	grains/acf	0.0005	0.0025	0.0012	0.0014
	grains/dscf	0.0006	0.0031	0.0015	0.0017
	lb/hr	0.1	0.4	0.2	0.2
	Total PM<10 (Met	thod 201A/:	202)	_	
	grams collected	0.02328	0.01866	0.02812	0.02335
	grains/acf	0.0082	0.0066	0.0098	0.0082
	grains/dscf	0.0104	0.0083	0.0124	0.0104
	lb/hr	1.4	1.1	1.7	1.4

	Client:	Holcim (US) Inc.				
	Facility:	Alpena Cement Plant				
	Test Location:	Indirect Firing Baghouse 22	2			
	Test Method:	201A/202	-			
	· · · · · · · · · · · · · · · · · · ·	Source Condition	Normal	Normal	Normal	
		Date	6/22/22	6/22/22	6/23/22	
		Start Time	14:23	16:25	6:00	
		End Time	16:03	18:05	7:40	
			Run 1	Run 2	Run 3	Average
		Stack Co	onditions			
	Av	verage Gas Temperature, °F	159.6	160.1	160.0	159.9
	Flue Gas M	loisture, percent by volume	4.2%	3.5%	3.5%	3.7%
	Av	erage Flue Pressure, in. Hg	28.83	28.83	28.83	28.83
		Gas Sample Volume, dscf	37.888	38.209	38.511	38.203
	1	Average Gas Velocity, ft/sec	83.923	84.211	84.259	84.131
	Gas	Volumetric Flow Rate, acfm	35,593	35,715	35,736	35,681
	Gas V	olumetric Flow Rate, dscfm	27,987	28,276	28,309	28,191
Gas Volumetric Flow Rate, scfm			29,229	29,304	29,326	29,286
Isokinetic Variance			99.6	98.7	99.4	99.2
		Filterable <pm1< th=""><th>0 (Method 2</th><th>201A)</th><th></th><th></th></pm1<>	0 (Method 2	201A)		
		grams collected	0.02393	0.02391	0.02501	0.02428
		grains/acf	0.0077	0.0076	0.0079	0.0077
		grains/dscf	0.0097	0.0097	0.0100	0.0098
		lb/hr	2.3	2.3	2.4	2.4
		lb/1000 lb of stack gas	0.019	0.019	0.019	0.019
		Condensable P			-	
		grams collected	0.00208	0.00086	0.00111	0.00135
		grains/acf	0.0007	0.0003	0.0004	0.0005
		grains/dscf	0.0008	0.0003	0.0004	0.0005
		lb/hr	0.2	0.1	0.1	0.1
		Total PM<10 (Me				
		grams collected	0.02601	0.02477	0.02612	0.02563
		grains/acf	0.0083	0.0079	0.0083	0.0082
		grains/dscf	0.0106	0.0100	0.0105	0.0104
		lb/hr	2.5	2.4	2.5	2.5

1

Client: Facility: Test Location:	Holcim (US) Inc. Alpena Cement Plant Indirect Firing Baghouse 23				
Test Method:	201A/202				
	Source Condition	Normal	Normal	Normal	
	Date	7/6/22	7/6/22	7/6/22	
	Start Time	11:03	13:53	16:18	
	End Time	12:38	15:28	17:53	
		Run 1	Run 2	Run 3	Average
	Stack Cor	ditions			
Av	verage Gas Temperature, °F	155.1	155.9	155.0	155.3
Flue Gas N	loisture, percent by volume	6.0%	5.7%	5.5%	5.7%
Av	erage Flue Pressure, in. Hg	29.42	29.42	29.42	29.42
	Gas Sample Volume, dscf	35.540	35.353	35.481	35.458
	Average Gas Velocity, ft/sec	85.428	84.449	84.361	84.746
Gas	Volumetric Flow Rate, acfm	37,245	36,818	36,780	36,948
Gas V	olumetric Flow Rate, dscfm	29,550	29,269	29,358	29,392
Gas	31,442	31,040	31,054	31,179	
	Isokinetic Variance	100.7	101.1	101.2	101.0
	(Method 2	01A)			
	grams collected	0.02389	0.00756	0.01090	0.01412
	grains/dscf	0.0104	0.0033	0.0047	0.0061
	lb/hr	2.6	0.8	1.2	1.5
	lb/1000 lb of stack gas	0.020	0.006	0.009	0.012
	Condensable PM				
	grams collected	0.00558	0.00195	0.00581	0.00445
	grains/acf	0.0019	0.0007	0.0020	0.0015
	grains/dscf	0.0024	0.0009	0.0025	0.0019
	lb/hr	0.6	0.2	0.6	0.5
	Total PM<10 (Met	hod 201A/	202)		
	grams collected	0.02947	0.00951	0.01671	0.01856
	grains/acf	0.0102	0.0033	0.0058	0.0064
	grains/dscf	0.0128	0.0042	0.0073	0.0081
	lb/hr	3.2	1.0	1.8	2.0



4.0 CERTIFICATION

Mostardi Platt is pleased to have been of service to Holcim (US) Inc. If you have any questions regarding this test report, please do not hesitate to contact us at 630-993-2100.

As the program manager, I hereby certify that this test report represents a true and accurate summary of emissions test results and the methodologies employed to obtain those results. The test program was performed in accordance with the test methods and the Mostardi Platt Quality Manual, as applicable.

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Project Manager

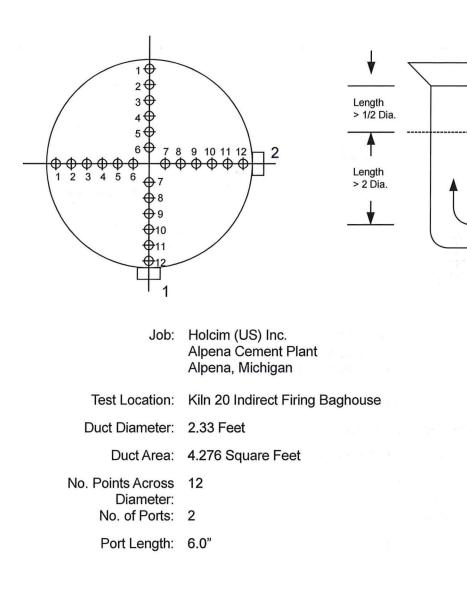
Timothy E. Russ

Stuart T. Sands

Quality Assurance

APPENDICES

Appendix A - Test Section Diagrams

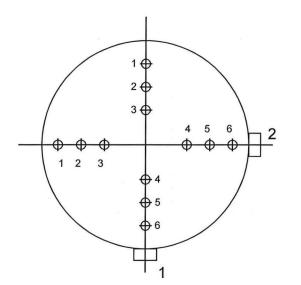


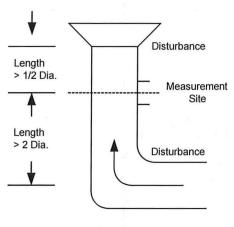
Disturbance

Disturbance

Measurement

Site





Job: Holcim (US) Inc. Alpena Cement Plant Alpena, Michigan

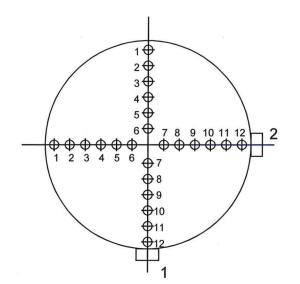
Test Location:	Kiln 21	Indirect	Firing	Baghouse
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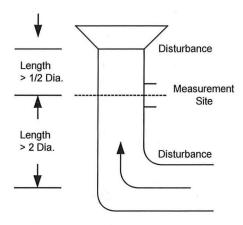
Duct Diameter: 2.25 Feet

Duct Area: 3.976 Square Feet

No. Points Across 6 Diameter: No. of Ports: 2

Port Length: 6.0"





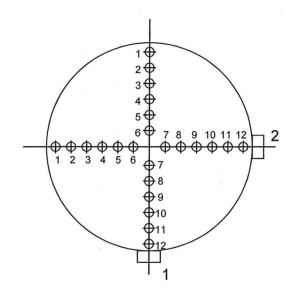
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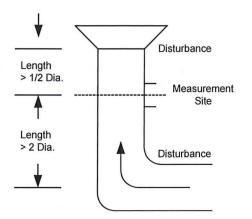
- Test Location: Kiln 22 Indirect Firing Baghouse
- Duct Diameter: 3.0 Feet
 - Duct Area: 7.069 Square Feet

No. Points Across 6 Diameter: No. of Ports: 2

Port Length: 6.5"

Project No. M222412A Kilns 20, 21, 22, and 23 Indirect Firing Baghouses ©Mostardi Platt

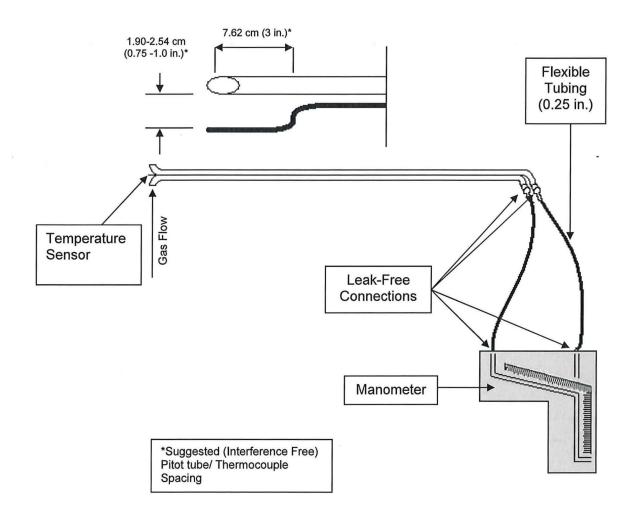




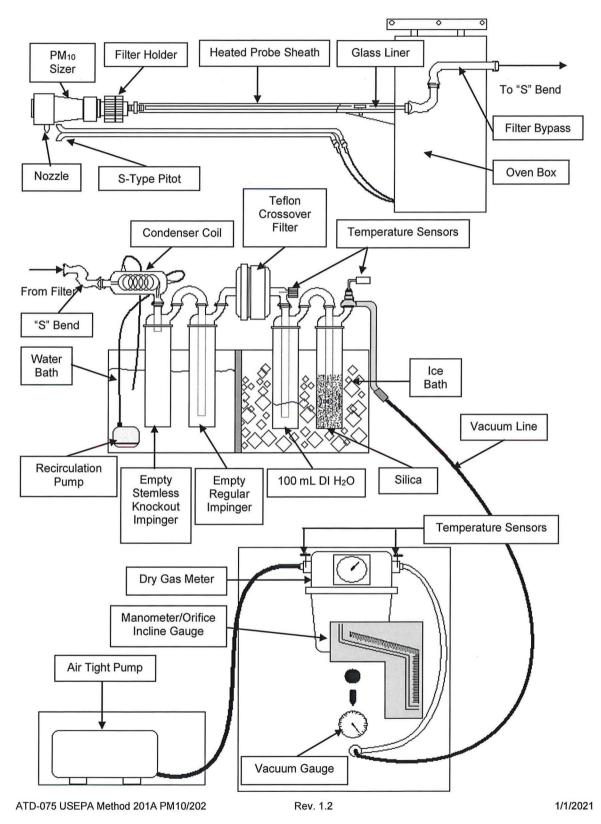
Job:	Holcim (US) Inc. Alpena Cement Plant
Test Location:	Kiln 23 Indirect Firing Baghouse
Duct Diameter:	3.0416 Feet
Duct Area:	7.266 Square Feet
No. Points Across Diameter:	12
No. of Ports:	2
Port Length:	5.5"

Project No. M222412A Kilns 20, 21, 22, and 23 Indirect Firing Baghouses ©Mostardi Platt

Appendix B - Sample Train Diagrams



USEPA Method 2 – Type S Pitot Tube Manometer Assembly



USEPA Method 201a/202- PM₁₀ and Condensable Particulate Matter

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