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Relative Accuracy Test Audit Test Report

Lansing Board of Water and Light Erickson Station Unit 1 Stack Lansing, Michigan August 4 through 6, 2015

> Report Submittal Date August 25, 2015

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Project No. M153106

888 Industrial Drive Elmhurst, Illinois 60126 630-993-2100

Authorized by 199	RE 4 P.A. 451, as amended.	EPORT CE	RTIFICATION	'esult in ci	ivil and/or criminal pen	alties.
Reports submitted pursuant to F must be certified by a responsib for at least 5 years, as specified upon request.	t 336.1213 (Rule 213), s le official. Additional ir in Rule 213(3)(b)(ii), ar	ubrules (3)(c) a nformation reg nd be made ava	and/or (4)(c), of Michiga arding the reports and ailable to the Departme	an's Rene documer ant of Env	ewable Operating Pentating Pentation listed below r vironmental Quality,	rmit (ROP) program nust be kept on file Air Quality Division
Source Name Lansing Bo	oard of Water & L	ight			County Eaton	
Source Address3725_S.	Canal Road			City	Lansing	
AQD Source ID (SRN) B40	01	ROP No.	MI-ROP-B4001- 2010		ROP Section No.	NA
Please check the appropriate b	ox(es):		an a		n an	and a start a s
Annual Compliance Cert	ification (Pursuant to	o Rule 213(4)((c))			
Reporting period (provide	inclusive dates): F	rom	То			
1. During the entire rep- term and condition of wh method(s) specified in th	orting period, this source ich is identified and incone ROP.	ce was in com cluded by this	pliance with ALL terms reference. The metho	s and co d(s) user	nditions contained in d to determine comp	n the ROP, each bliance is/are the
2. During the entire report of the condition of will deviation report(s). The unless otherwise indicate	porting period this soun nich is identified and in method used to detern ad and described on th	rce was in co included by thi mine compliar re enclosed de	mpliance with all terms is reference, EXCEPT nce for each term and aviation report(s).	s and co for the conditior	nditions contained i deviations identified n is the method sper	in the ROP, each I on the enclosed cified in the ROP,
Semi-Annual (or More F	requent) Report Cert	- ification (Put	reuant to Rule 213(3)((c))	·····	
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Reporting period (provide	inclusive dates): F	rom	To			the sector of the
deviations from these rep	oning period, ALL mor quirements or any othe	and as and as ar terms or cor	aditions occurred.	ig require	ements in the rur 1	were met and no
2. During the entire reputed in the entire reputed in the entire reputed in the enclosed deviation report enclosed deviation report	orting period, all monito quirements or any othe t(s).	oring and asso er terms or cor	ciated recordkeeping ditions occurred, EXC	requirem EPT for t	tents in the ROP we the deviations identi	re met and no ified on the
M Other Report Certificatio						
Reporting period (provide	inclusive dates): F	from NA	To	NA		
Additional monitoring report	its or other applicable (documents rec	uired by the ROP are	attachec	l as described:	
Mostardi Platt (MP) prepared the at	ttached tes	st report as requ	ired b	У	
MDEQ MI-ROP-B4001-	2010 at the reque	est of Lans	sing Board of Wat	er & L:	ight. MP perfo	rmed
a NOx, SO2, CO2 an	d flow RATA of th	he CEMS ass	sociated with Emi	ssion 1	Unit EU001 unde	:r
the operating cond	litions described	•				

I certify that, based on information and belief formed after reasonable inquiry, the statements and information in this report and the supporting enclosures are true, accurate and complete

MarkMatus	Manager, Env Services	(517) 702-6153
Name of Responsible Official (print/or type)	Title	Phone Number
Ulles titles		8/27/2015
Signature of Responsible Official		Date

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* Photocopy this form as needed.

EQP 5736 (Rev 11-04)



MICHIGAN DEPARTMENT OF ENVIRONMENTAL QUALITY AIR QUALITY DIVISION

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1.0 EXECUTIVE SUMMARY

MOSTARDI PLATT conducted a Continuous Emissions Monitoring System (CEMS) Relative Accuracy Test Audit (RATA) test program for Lansing Board of Water and Light at the Erickson Station in Lansing, Michigan, on the Unit 1 Stack on August 4 through 6, 2015. This report summarizes the results of the test program and test methods used in accordance with the Mostardi Platt Site Specific Test Plan dated August 3, 2015. Mostardi Platt is a self-certified air emissions testing body (AETB). A copy of Mostardi Platt's self-certification can be found in Appendix A.

The test location, test dates, and test parameters are summarized below.

TEST INFORMATION							
Test Location Test Dates Test Parameters							
Unit 1 Stack	August 4 through 6, 2015	Carbon Dioxide (CO ₂), Sulfur Dioxide (SO ₂), Nitrogen Oxides (NO _x), and Volumetric Flow					

The purpose of the test program was to demonstrate the relative accuracies of the Unit 1 Stack CO_2 , SO_2 , NO_x , and volumetric flow analyzers during the specified operating conditions. The test results from this test program indicate that each CEMS component meets the United States Environmental Protection Agency (USEPA) annual performance specification for relative accuracy as published in 40 Code of Federal Regulations Part 75 (40CFR75).

RATA RESULTS										
Test Location	Date	Parameter	Units	Relative Accuracy Acceptance Criteria	Relative Accuracy (RA)	Bias Adjustment Factor (BAF)				
	8/4/15	NOx	lb/mmBtu	≤ 7.5 % of the mean reference value	4.21 %	1.034				
		SO ₂	ppmv	≤ 7.5 % of the mean reference value	1.47 %	1.012				
		CO2	% wet	≤ 7.5 % of the mean reference value	0.46 %	N/A				
Unit 1 Stack		Volumetric Flow – High (Normal) Load	scfh	≤ 7.5% of the mean reference value	1.11 %	1.000				
	8/5/15	Volumetric Flow - Mid Load	scfh	≤ 7.5% of the mean reference value	2.54 %	1.000				
	8/5 and 6/15	Volumetric Flow - Low Load	scfh	≤ 7.5% of the mean reference value	1.40 %	1.000				

GAS CYLINDER INFORMATION									
Parameter	Gas Vendor	Cylinder Serial Number	Cylinder Value	Expiration Date					
NOx	Zero Air Material	N/A	0.0 ppm	N/A					
NOx	Airgas	CC422751	89.47 ppm	6/29/23					
NOx	Airgas	CC12497	180.3 ppm	4/17/22					
SO ₂	Zero Air Material	N/A	⁻ 0.0 ppm	N/A					
SO2	Airgas	CC284773	252.5 ppm	7/21/22					
SO ₂	Airgas	CC452296	481.3 ppm	2/23/23					
CO ₂	Zero Air Material	N/A	0.0 %	N/A					
CO ₂	Airgas	SG9133187BAL	10.22 %	6/23/23					
CO ₂	Airgas	CC105628	19.42 %	5/13/23					

The gas cylinders used to perform the RATA are summarized below.

No deviations, additions, or exclusions from the site specific test plan, test methods, the Mostardi Platt Quality Manual, or the ASTM D7036-12 occurred. The specific test conditions encountered did not interfere with the collection of the data.

The identifications of the individuals associated with the test program are summarized below.

TEST PERSONNEL INFORMATION									
Location	Address	Contact							
Test Coordinator	Lansing Board of Water and Light	Ms. Shannon Whiton							
	Erickson Station	Senior Environmental Engineer							
	3725 South Canal Road	(517) 702-6003 (phone)							
	Lansing, Michigan 48917	smw@LBWL.COM							
Testing	Mostardi Platt	Mr. Jacob Howe							
Company	888 Industrial Drive	Project Manager							
Supervisor	Elmhurst, Illinois 60126	630-993-2100 (phone)							
		jhowe@mp-mail.com							
		QI Group V (certified on 9/8/11 and							
		2/1/13)							
Testing		Mr. Tom Nelson							
Company		Test Engineer							
Personnel		QI Group V (certified on 4/3/15)							
		Mr. William Disselhorst							
		Test Technician							

Copies of the QI certifications for test personnel are included in Appendix B.

2.0 TEST METHODOLOGY

Emission testing was conducted following the United States Environmental Protection Agency (USEPA) methods specified in 40CFR75 and 40 Code of Federal Regulations (40CFR60), Appendix A, and ASTM E337-02 in addition to the Mostardi Platt Quality Manual and the site

specific test plan. Schematics of the test section diagrams and sampling trains used are included in Appendix C and D respectively. Calculation and nomenclature are included in Appendix E. Copies of analyzer print-outs for each test run are included in Appendix F. CEM data and process data as provided by Lansing Board of Water and Light are included in Appendix G.

The following methodologies were used during the test program:

Method 1 Sample and Velocity Traverse Determination

Test measurement points were selected in accordance with USEPA Method 1, 40CFR60, Appendix A. The characteristics of the measurement location are summarized below.

TEST POINT INFORMATION AT UNIT 1 STACK										
Stack Diameter (Feet)	Stack Area (Square Feet)	No. of Ports	Port Length (inches)	Upstream Diameters	Downstream Diameters	Test Parameter	Number of Sampling Points			
47.0	000.00		70.0	7.04	44.70	Volumetric Flow	16			
17.0	220.98	4	78.0	7.94	11.76	Stratification Test	12			

Method 2 Volumetric Flow Rate Determination

Gas velocity was measured following USEPA Method 2, 40CFR60, Appendix A, for purposes of calculating stack gas volumetric flow rate. A 12.0 foot long S-type pitot tube, 0-10 inch differential pressure gauge, and K-type thermocouple and temperature readout were used to determine gas velocity at each sample point. All of the equipment used was calibrated in accordance with the specifications of the Method. Copies of field data sheets are included in Appendix H. Calibration data are presented in Appendix I. This testing met the performance specifications as outlined in the Method.

Method 3 Oxygen (O₂)/Carbon Dioxide (CO₂) Determination

Stack gas molecular weight was determined in accordance with USEPA Method 3, 40CFR60, Appendix A, during each volumetric flow rate determination. A Fyrite analyzer was used to determine stack gas O_2 and CO_2 content and, by difference, nitrogen content. Multiple gas extractions were performed during each test run to ensure a stable reading. Chemicals are changed frequently and inspected for reactivity prior to each use. This testing met the performance specifications as outlined in the Method.

Stratification Test for Gaseous Sampling

A twelve point stratification test was performed prior to the RATA test. All of the results were less than 10% difference and consequently three points were used for the RATA test.

Method 3A Carbon Dioxide (CO₂) Determination

Stack gas CO_2 concentrations were determined in accordance with USEPA Method 3A, 40CFR60, Appendix A. A Thermo Scientific Model 41C Gas Filter Correlation Carbon Dioxide Analyzer was used to determine carbon dioxide concentrations in the manner specified in the Method. The instrument has a nondispersive infrared-based detector and operated in the nominal range of 0% to 20% with the specific range determined by the high-level span calibration gas of 19.42%.

The Model 41C High Level is based on the principle that CO_2 absorbs infrared radiation. Because infrared absorption is a non-linear measurement technique, it is necessary for the instrument electronics to transform the basic analyzer signal into a linear output. The analyzer uses an exact calibration curve to accurately linearize the instrument output over any range up to a concentration of 2000 ppm.

The sample is drawn into the analyzer through the sample bulkhead. The sample flows through the optical bench. Radiation from an infrared source is chopped and then passed through a gas filter alternating between CO_2 and N_2 . The radiation then passes through a narrow bandpass interference filter and enters the optical bench where absorption by the sample gas occurs. The infrared radiation then exits the optical bench and falls on an infrared detector.

The CO_2 side of the filter wheel acts to produce a reference beam which cannot be further attenuated by CO_2 in the sample cell. The N_2 side of the filter wheel is transparent to the infrared radiation and therefore produces a measure beam which can be absorbed by CO_2 in the cell. The rotating gas filter wheel causes the detector signal to be modulated. The amplitude of the detector signal is directly proportional to the concentration of CO_2 in the sample cell. Gases other than CO_2 do not cause modulation of the detector signal since they absorb the reference and measure beams equally. Thus the GFC system responds specifically to CO_2 . The Model 41C High Level outputs the CO_2 concentration to the front panel display and the analog outputs.

Stack gas was delivered to the analyzer through an EPM in-situ dilution sampling system. Stack gas concentrations were diluted at a nominal 100:1 ratio utilizing purified dilution air. The entire system was calibrated in accordance with the Method, using USEPA Protocol gases introduced at the probe, before and after each test run.

A list of calibration gases used and the results of all calibration and other required quality assurance checks are found in Appendix I. Copies of the gas cylinder certifications are found in Appendix J. This testing met the performance specifications as outlined in the Method.

Method 4 Moisture Determination

USEPA Method 4, 40CFR60, Appendix A, was utilized to determine water (H_2O) content of the exhaust gas. 100 milliliters (ml) of water were added to each of the first two impingers, the third impinger was left empty, and the fourth impinger was charged with approximately 200 grams of silica gel. The impingers were placed in an ice bath to maintain the sampled gas passed through the silica gel impinger outlet below 68°F in order to increase the accuracy of the sampled dry gas volume measurement. The water volumes of the impinger train were measured and the silica gel was weighed before and after each test run to determine the mass of moisture condensed.

Each sample was extracted through a heated stainless-steel probe and filter assembly at a constant sample rate of approximately 0.75 cubic feet per minute, which was maintained throughout the course of the test run. A minimum of 21 dry standard cubic feet (dscf) are sampled for, each moisture run. After each run, a leak check of the sampling train was performed at a vacuum greater than the sampling vacuum to determine if any leakage had occurred during sampling. Following the leak check, the impingers were removed from the ice bath, water levels were measured, and the silica gel weight was recorded.

All of the equipment used was calibrated in accordance with the specifications of the Method.

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Copies of field data sheets are included in Appendix H. Calibration data is presented in Appendix I. This testing met the performance specifications as outlined in the Method.

Method 6C Sulfur Dioxide (SO₂) Determination

Stack gas SO₂ concentrations and emission rates were determined in accordance with USEPA Method 6C, 40CFR60, Appendix A. A Thermo Scientific Model 43i Pulsed Fluorescence Sulfur Dioxide Analyzer was used to determine sulfur dioxide concentrations, in the manner specified in the Method. The instrument operated in the nominal range of 0 ppm to 500 ppm with the specific range determined by the high-level span calibration gas of 481.3 ppm.

The Model 43i operates on the principle that SO_2 molecules absorb ultraviolet (UV) light and become excited at one wavelength, then decay to a lower energy state emitting UV light at a different wavelength. Specifically,

 $SO_2 + hv_1 \rightarrow SO_2^* \rightarrow SO_2 + hv_2$

The sample is drawn into the Model 43*i* through the sample bulkhead. The sample flows through a hydrocarbon "kicker", which removes hydrocarbons from the sample by forcing the hydrocarbon molecules to permeate through the tube wall. The SO₂ molecules pass through the hydrocarbon "kicker" unaffected.

The sample flows into the fluorescence chamber, where pulsating UV light excites the SO_2 molecules. The condensing lens focuses the pulsating UV light into the mirror assembly. The mirror assembly contains four selective mirrors that reflect only the wavelengths which excite SO_2 molecules.

As the excited SO_2 molecules decay to lower energy states, they emit UV light that is proportional to the SO_2 concentration. The bandpass filter allows only the wavelengths emitted by the excited SO_2 molecules to reach the photomultiplier tube (PMT). The PMT detects the UV light emission from the decaying SO_2 molecules. The photodetector, located at the back of the fluorescence chamber, continuously monitors the pulsating UV light source and is connected to a circuit that compensates for fluctuations in the lamp intensity.

As the sample leaves the optical chamber, it passes through a flow sensor, a capillary, and the "shell" side of the hydrocarbon kicker. The Model 43*i* outputs the SO₂ concentration to the front panel display, the analog outputs, and also makes the data available over the serial or Ethernet connection.

Stack gas was delivered to the analyzer through an EPM in-situ dilution sampling system. Stack gas concentrations were diluted at a nominal 100:1 ratio utilizing purified dilution air. The entire system was calibrated in accordance with the Method, using USEPA Protocol gases introduced at the probe, before and after each test run.

A list of calibration gases used and the results of all calibration and other required quality assurance checks are found in Appendix I. Copies of the gas cylinder certifications are found in Appendix J. This testing met the performance specifications as outlined in the Method.

Method 7E Nitrogen Oxides (NO_x) Determination

Stack gas NO_x concentrations and emission rates were determined in accordance with USEPA Method 7E, 40CFR60, Appendix A. A Thermo Scientific Model 42C Chemiluminescence

Nitrogen Oxides Analyzer was used to determine nitrogen oxides concentrations, in the manner specified in the Method. The instrument operated in the nominal range of 0 ppm to 500 ppm with the specific range determined by the high-level span calibration gas of 180.3 ppm.

The Model 42C High Level is based on the principle that nitric oxide (NO) and ozone (O₃) react to produce a characteristic luminescence with an intensity linearly proportional to the NO concentration. Infrared light emission results when electronically excited nitrogen dioxide (NO₂) molecules decay to lower energy states. Specifically,

$NO+O_3 \rightarrow NO_2+O_2+hv$

 NO_2 must first be transformed into NO before it can be measured using the chemiluminescent reaction. NO_2 is converted to NO by a molybdenum NO_2 -to-NO converter heated to about 318°C. The flue gas air sample is drawn into the Model 42C High Level through the sample bulkhead. The sample flows through a particulate filter, a capillary, and then to the mode solenoid valve. The solenoid valve routes the sample either straight to the reaction chamber (NO mode) or through the NO_2 -to-NO converter and then to the reaction chamber (NO mode).

Dry air enters the Model 42C High Level through the dry air bulkhead, through a flow sensor, and then through a silent discharge ozonator. The ozonator generates the necessary ozone concentration needed for the chemiluminescent reaction. The ozone reacts with the NO in the ambient air sample to produce electronically excited NO₂ molecules. A photomultiplier tube (PMT) housed in a thermoelectric cooler detects the NO₂ luminescence.

The NO and NO_x concentrations calculated in the NO and NO_x modes are stored in memory. The difference between the concentrations are used to calculate the NO₂ concentration. The Model 42C High Level outputs NO, NO₂, and NO_x concentrations to both the front panel display and the analog outputs.

Stack gas was delivered to the analyzer through an EPM in-situ dilution sampling system. Stack gas concentrations were diluted at a nominal 100:1 ratio utilizing purified dilution air. The entire system was calibrated in accordance with the Method, using USEPA Protocol gases introduced at the probe, before and after each test run.

A list of calibration gases used and the results of all calibration and other required quality assurance checks are found in Appendix I. Copies of the gas cylinder certifications are found in Appendix J. The NO_2 to NO converter test can be found in Appendix K. This testing met the performance specifications as outlined in the Method.

3.0 TEST RESULT SUMMARIES

Client:	Lansing	g Board	Water and	Light		Location: Unit 1 Stack					
Facility:	Erickso	on Statio	n			Date: 8/4/15					
Project #:	M15310)6				Test Method: 7E, 3A					
Fuel Type:	Sub Bit	uminou	s Coal			Fuel Factor:	1840				
				NO	/lb/mmBt	u RATA					
CEM Monitor Information											
· · · · · · · · · · · · · · · · · · ·	NC), Moni	tor/Model:	Teledyn	e T200H		NO _v Serial # :		71		
	CC	2 Moni	tor/Model:	Teledyne	• T360M		CO ₂ Serial # :	(33		
		1							(RM-CEM)		
1=accept	Test	55.44	Tect Date	Start Time	End Time	RM NO _x	CEM NO _x		Difforonco ²		
0=reject	Run	541.44	Test Date	Start Time		lb/mmBtu	lb/mmBtu		Chiefence		
		400.5	00/04/45	00.40					<u>(ur)</u>		
		103.5	08/04/15	08:10	08:30	0.207	0.202	0.005	0.000		
		163,4	08/04/15	08:50	09:10	0.207	0.203	0.004	0.000		
1	3	102.8	08/04/15	09:30	09:50	0.213	0.208	0.005	0.000		
	4	161.7	08/04/15	10:10	10:30	0.211	0.207	0.004	0.000		
	5	162.4	08/04/15	10:50	11:10	0.213	0.205	0.008	0.000		
1	6	162.1	08/04/15	11:30	11:50	0.214	0.204	0.010	0.000		
1		162.1	08/04/15	12:10	12:30	0.217	0.207	0.010	0.000		
1	8	163.3	08/04/15	12:50	13:10	0.223	0.213	0.010	0.000		
0	9	163.6	08/04/15	13:30	13:50	0.228	0.214	0.014	0.000		
1	10	163.8	08/04/15	14:10	14:30	0,217	0.210	0.007	0.000		
					n)				
			N	6	t(0.025)	2.3	06				
			wean ke	terence we		0.2	14	Rivi avg			
				wean Sum of		0.2	.07	CEW avg			
				Moon	Difference	0.0	03	d			
			Sum d	of Difference	e Sanarad	0.0	00	ч			
			Junit	Standard	Deviation	0.0	03	ui ed			
	c	Confide	nce Coeffi	cient 2.5% E	rror (1-tail)	0.0	02	su cc			
				Relativ	Accuracy	4,2	21	RA			
			E	Bias Adjustr	ent Factor	1.034		BAF			

Client:	Lansing	g Board	Water and	Light		Location: Unit 1 Stack						
Facility:	Erickso	on Statio	วท			Date: 8/4/15						
Project #:	M15310	06				Test Method: 6C						
	SO ₂ ppmv RATA											
[CEM Monitor Information											
	sc	0₂ Moni	tor/Model:	Teledyn	e T100H		SO ₂ Serial # :		61			
1=accept 0=reject	Test Run	Mw	Test Date	Start Time	End Time	RM SO₂ ppmv	CEM SO ₂ ppmv	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)			
1	1	163.5	08/04/15	08.10	08:30	276 7	273.0	27	137			
1	2	163.0	08/04/15	08:50	00:30	267.5	273.0	<u> </u>	20.3			
1	3	162.8	08/04/15	00:30	09:50	263.5	259.5	4.0	16.0			
	4	161.7	08/04/15	10:10	10:30	259.2	256.8	24	5.8			
1	5	162.4	08/04/15	10:50	11:10	261.2	258.0	3.2	10.2			
0	6	162,1	08/04/15	11:30	11:50	269.6	265.0	4.6	21.2			
1	7	162.1	08/04/15	12:10	12:30	266.9	262.7	4.2	17.6			
1	8	163.3	08/04/15	12:50	13:10	265.8	263.9	1.9	3.6			
1	9	163.6	08/04/15	13:30	13:50	265.4	263.4	2.0	4.0			
1	10	163.8	08/04/15	14:10	14:30	266.7	264.6	2.1	4.4			
					n)					
					t(0.025)	2.3	06					
			Mean Re	ference Me	thod Value	26	5.9	RM avg				
				Mean	CEM Value	26	2.8	CEM avg				
				Sum of	Differences	28	3.0	di				
				Mean	Difference	3	.1	d				
			Sum	of Difference	es Squared	9{	5.6	di ²	····			
				Standard	d Deviation	1.0	030	sd				
	(Confide	nce Coeffi	cient 2.5% E	Error (1-tail)	0.7	792	cc				
			_	Relativ	e Accuracy	1.47		RA				
			E	<u> 3ias Adjustn</u>	nent Factor	<u>1.012</u> BAF						

Client:	Lansing	g Board	Water and	Light	Location:	Unit 1 Stack		· · · · · · · · · · · · · · · · · · ·			
Facility:	Erickso	on Static	n			Date: 8/4/15					
Project #:	M15310)6				Test Method:	ЗA		ĺ		
CO ₂ % (wet) RATA											
CEM Monitor Information											
	CO2	2 Monite	or/Model:	Teledyne	e T360M		CO2 Serial # :	(63		
		[(RM-CEM)	(RM-CEM)		
1=accept	Test	Mw	Test	Start Time	End Time	RM CO ₂ %	CEM CO₂ %	Difference	Difference ²		
0=reject	Run		Date			(wet)	(wet)	(di)	(di ²)		
1	1	163.5	08/04/15	08:10	08:30	12.6	12.5	01	0.01		
1	2	163.4	08/04/15	08:50	09:10	12.5	12.5	0.1	0.00		
1	3	162.8	08/04/15	00:30	09:10	12.0	12.5	0.0	0.00		
1	4	161.7	08/04/15	10:10	10:30	12.4	12.4	0.0	0.00		
1	5	162.4	08/04/15	10:50	11:10	12.4	12.5	-0.1	0.01		
1	6	162.1	08/04/15	11:30	11:50	12.5	12.6	-0.1	0.01		
1	7	162.1	08/04/15	12:10	12:30	12.5	12.5	0.0	0.00		
1	8	163.3	08/04/15	12:50	13:10	12.4	12.4	0.0	0.00		
0	9	163.6	08/04/15	13:30	13:50	12.1	12.3	-0.2	0.04		
1	10	163.8	08/04/15	14:10	14:30	12.5	12.5	0.0	0.00		
					n)				
					t(0.025)	2.3	306				
			Mean Re	ference Me	thod Value	12.	467	RM avg			
				Mean	CEM Value	12.	478	CEM avg			
				Sum of	Differences	-0.	100	di			
			_	Mean	Difference	-0.	011	d			
			Sum o	of Difference	es Squared	0.0	030	di ²			
	-	6 1	<u> </u>	Standard	d Deviation	0.060		sd			
	С	onfider	nce Coeffi	cient 2.5% E	rror (1-tail)	0.046 cc					
				Relativ	e Accuracy	0.46 RA					

Client: Lansing Board Water and Light Test Location: Unit 1 Stack Facility: Erickson Station Test Date: 8/4/2015 Project #: M153106 Test Method: 2										
CEM Monitor Information										
Volumetric How RATA - High(Normal) Load										
Flow Monitor/Model: Teledyn					e Ultraflow 150	Flow Serial # :	11	501157		
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	Reference Method Flow SCFH CEM Flow SCFH		(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)		
0	1	08/04/15	08:15	08:27	26,741,000	30,618,000	-3,877,000	15,031,129,000,000		
1	2	08/04/15	08:34	08:42	29,587,000	29,957,000	-370,000	136,900,000,000		
1	3	08/04/15	08:46	08:54	29,765,000	29,966,000	-201,000	40,401,000,000		
1	4	08/04/15	09:10	09:17	30,218,000	29,997,000	221,000	48,841,000,000		
1	5	08/04/15	09:18	09:25	30,290,000	30,550,000	-260,000	67,600,000,000		
1	6	08/04/15	09:26	09:34	29,952,000	30,334,000	-382,000	145,924,000,000		
1	7	08/04/15	09:50	09:58	30,160,000	29,750,000	410,000	168,100,000,000		
1	8	08/04/15	09:59	10:06	30,190,000	29,670,000	520,000	270,400,000,000		
1	9	08/04/15	10:07	10:13	30,054,000	29,716,000	338,000	114,244,000,000		
1	10	08/04/15	10:14	10:20	29,991,000	29,750,000	241,000	58,081,000,000		
				n	9					
1			1	(0.025)	2.30	6	<u> </u>			
M	lean R	eference	Method	1 Value	3002300	0.000	RM avg			
		Mea	an CEN	1 Value	2996555	5.556	CEM avg			
		Sum	of Diffe	rences	<u> </u>	.000	di			
		Me	an Diff	erence	57444.	.444	d			
	Sum	of Differe	nces S	quared	105049100	0000.000	di ²			
		Stand	lard De	viation	357210	.061	sd			
Confidence	e Coef	ficient 2.5	% Error	[•] (1-tail)	274575.467		CC			
Relative Accuracy					1.11		RA			
	_	Bias Adju	stment	Factor	1.00	0	BAF			

Client: Lansing Board Water and Light Test Location: Unit 1 Stack Facility: Erickson Station Test Date: 8/5/2015 Project #: M153106 Test Method: 2 CEM Monitor Information											
Volumetric How RATA - Mid Load											
Flow	Monit	or/Model:	· ·	Teledyn	e Ultraflow 150	Flow Serial # :	1	501157			
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	Reference Method Flow SCFH	CEM Flow SCFH	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)			
0	1	08/05/15	20:05	20:14	22,935,000	24,361,000	-1,426,000	2,033,476,000,000			
1	2	08/05/15	20:19	20:25	24,038,000	24,510,000	-472,000	222,784,000,000			
1	3	08/05/15	20:26	20:33	24,161,000	24,755,000	-594,000	352,836,000,000			
1	4	08/05/15	20:45	20:54	24,293,000	24,927,000	-634,000	401,956,000,000			
1	5	08/05/15	20:55	21:05	24,462,000	24,756,000	-294,000	86,436,000,000			
1	6	08/05/15	21:06	21:14	24,463,000	24,806,000	-343,000	117,649,000,000			
1	7	08/05/15	21:23	21:30	24,689,000	24,658,000	31,000	961,000,000			
1	8	08/05/15	21:31	21:39	24,322,000	24,879,000	-557,000	310,249,000,000			
1	9	08/05/15	21:40	21:47	24,245,000	25,018,000	-773,000	597,529,000,000			
1	10	08/05/15	21:48	21:53	24,542,000	24,572,000	-30,000	900,000,000			
				n	9						
			t	(0.025)	2.30	6					
M	ean R	leference	Methoo	l Value	2435722	2.222	RM avg				
}		Mea	an CEN	l Value	2476455	5.556	CEM avg				
		Sum	of Diffe	rences	-366600	0,000	di				
ļ		Me	an Diff	erence	-407333	3.333	d				
	Sum	of Differe	nces S	quared	209130000	000.000	di ²				
		Stand	lard De	viation	273408	.120	sd				
Confidence Coefficient 2.5% Error (1-tail)					210159	.708	cc				
Relative Accuracy					2.54	1	RA				
L		Bias Adju	stment	Factor	1.00	0	BAF				

Client: Lansing Board Water and Light Test Location: Unit 1 Stack								
Facility: Erickson Station Test Date: 8/5-6/15								
Project #: M153106 Test Method: 2								
CEM Monitor Information								
Volumetric How RATA - Low Load								
Flow Monitor/Model: Teled			Teledyn	e Ultraflow 150	Flow Serial # :	1501157		
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	Reference Method Flow SCFH	CEM Flow SCFH	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)
1	1	08/05/15	23:02	23:09	20,220,000	20,515,000	-295,000	87,025,000,000
1	2	08/05/15	23:13	23:20	20,459,000	20,853,000	-394,000	155,236,000,000
0	3	08/05/15	23:21	23:29	20,469,000	20,905,000	-436,000	190,096,000,000
1	4	08/05/15	23:36	23:43	20,584,000	20,771,000	-187,000	34,969,000,000
1	5	08/05/15	23:44	23:51	20,731,000	20,907,000	-176,000	30,976,000,000
1	6	8/ <u>5-6</u> /15	23:52	00:02	20,793,000	20,903,000	-110,000	12,100,000,000
1	7	08/06/15	00:13	00:20	20,859,000	21,074,000	-215,000	46,225,000,000
1	8	08/06/15	00:21	00:28	20,795,000	20,849,000	-54,000	2,916,000,000
1	9	08/06/15	00:29	00:35	20,672,000	20,976,000	-304,000	92,416,000,000
0	10	08/06/15	00:36	00:41	20,723,000	21,266,000	-543,000	294,849,000,000
1	11	08/06/15	00:42	00:47	20,690,000	20,768,000	-78,000	6,084,000,000
n					9			
t(0.025)					2.306			
Mean Reference Method Value					20644777.778		RM avg	
Mean CEM Value					20846222.222		CEM avg	
Sum of Differences					-1813000.000		di	
Mean Difference					-201444.444		d	
Sum of Differences Squared					467947000000.000		di ²	
Standard Deviation					113318.259		sd	
Confidence Coefficient 2.5% Error (1-tail)					87103.968		cc	
Relative Accuracy					1.40		RA	
Bias Adjustment Factor					1.000		BAF	

4.0 CERTIFICATION

MOSTARDI PLATT is pleased to have been of service to Lansing Board of Water and Light. If you have any questions regarding this test report, please do not hesitate to contact us at 630-993-2100.

CERTIFICATION

As the program manager, I hereby certify that this test report represents a true and accurate summary of emissions test results and the methodologies employed to obtain those results. The test program was performed in accordance with the site specific test plan, test methods, the Mostardi Platt Quality Manual, and the ASTM D7036-12, as applicable.

MOSTARDI PLATT

Of Hove

Jacob Howe

Acotten Barace

Scott W. Banach

Program Manager

Quality Assurance

Project No. M153106 Unit 1 Stack