

Relative Accuracy Test Audit Test Report

Billerud Quinnesec LLC Quinnesec Mill Package Boiler Outlet Duct, Waste Fuel Boiler Outlet Duct, Recovery Boiler Outlet Duct, and Lime Kiln Stack Quinnesec, Michigan Test Dates: May 9 through 11, 2023

> Report Submittal Date June 16, 2023

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Project No. M231804B

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Project No. M231804B Package Fuel Boiler Outlet Duct, Waste Fuel Boiler Outlet Duct, Recovery Fuel Boiler Outlet Duct, and Lime Kiln Stack i

1.0 EXECUTIVE SUMMARY

Mostardi Platt conducted a Relative Accuracy Test Audit (RATA) test program for Billerud Quinnesec LLC at the Quinnesec, Michigan facility. This report summarizes the results of the test program and test methods used.

The test locations, test dates, and test parameters are summarized below.

TEST INFORMATION					
Test Locations	RATA Test Dates	Test Parameters			
Package Boiler Outlet Duct	May 10, 2023	Nitrogen Oxides (NOx), Carbon Monoxide (CO), and Oxygen (O ₂)			
Waste Fuel Boiler Outlet Duct	May 11, 2023	NO _x , Sulfur Dioxide (SO ₂), Carbon Dioxide (CO ₂), O ₂ , and Volumetric Flow			
Recovery Boiler Outlet Duct	May 10 and 11, 2023	NO _X , SO ₂ , O ₂ , CO, Total Reduced Sulfur (TRS), and Volumetric Flow			
Lime Kiln Stack	May 9 and 10, 2023	TRS and O ₂			

The purpose of the test program was to demonstrate the relative accuracy of the parameters listed above. Selected results of the test program are summarized below. A complete summary of emission test results, for each location, follows the narrative portion of this report.

TRS results were corrected to eight percent O_2 on the Recovery Boiler and ten percent O_2 on the Lime Kiln.

PACKAGE BOILER OUTLET DUCT								
Date	Parameter	Units	Acceptance Criteria	Relative Accuracy				
	NOx	lb/mmBtu	< 20% of the mean reference method value	12.92%				
	NOx	lb/hr	< 20% of the mean reference method value	1.08%				
5/10/2023	O2	% dry	< 20% of the mean reference method value	2.34%				
5/10/2023	со	lb/mmBtu	< 10% of the mean reference method value	0.00%				
	со	ppm	< 5 ppm mean difference + confidence coefficient	0.55 ppm mean difference + confidence coefficient				
	со	lb/hr	< 5% of applicable standard of 25.5 lb/hr	0.29% of applicable standard of 25.5 lb/hr				

Also note that this RATA serves as a portion of the initial certifications for a new Waste Fuel Boiler SO2 analyzer (Thermo 43iQ, SN 1180930080), which was installed on 4/25/2021, and a new Recovery Furnace flue gas flow meter (OSI OFS2000-W, SN 15110807E), which was installed on 4/26/23 – the additional certification requirements for these analyzers will be included in the 2nd Quarter 2023 CEMS/COMS Excess Emission and Quality Assurance Report.

	WASTE FUEL BOILER OUTLET DUCT								
Date	Parameter	Units	Acceptance Criteria	Relative Accuracy					
	NOx	lb/mmBtu	< 20% of the mean reference method value	10.49%					
	NOx	lb/hr	< 20% of the mean reference method value	15.60%					
	CO₂	% dry <a>< 20% of the mean reference method value		0.63%					
5/11/2023	O ₂	% dry	< 20% of the mean reference method value	3.98%					
	SO₂	lb/mmBtu	< 10% of applicable standard of 1.2 lb/mmBtu	8.33% of applicable standard of 1.2 lb/mmBtu					
	SO₂	lb/hr	< 10% of applicable standard of 476 lb/hr	5.16% of applicable standard of 476 lb/hr					
	Volumetric Flow	dscfm	< 20% of the mean reference method value	5.85%					

		RECO	VERY BOILER OUTLET DUC	Т
Date	Parameter	Units	Acceptance Criteria	Relative Accuracy
	NOx	ppmvd @ 8% O2	< 20% of the mean reference method value	3.61%
5/10/2023	O2	% dry	< 20% of the mean reference method value	3.35%
5/10/2023	SO₂	ppmvd @ 8% O₂	< 10% of applicable standard of 50 ppmvd@ 8% O ₂	0.45% of applicable standard of 50 ppmvd@ 8% O ₂
	со	ppmvd @ 8% O₂	< 5% of applicable standard of 500 ppmvd@ 8% O ₂	0.33% of applicable standard of 500 ppmvd@ 8% O ₂
5/11/2023			≤ 10.0% of App. Standard of 5 ppmvd @ 8% O₂	4.42% of App. Standard of 5 ppmvd @ 8% O₂
5/9/2023	1023 setting decting		< 20% of the mean reference method value	5.68%

LIME KILN STACK							
Date Parameter Units Acceptance Criteria Relative Accurac							
5/9/2023 & 5/10/2023	TRS	ppmvd @ 10% O₂	< 20% of the mean reference method value	9.70%			
	O2	% dry	< 20% of the mean reference method value	12.93%			

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	GAS CYLINDER INFORMATION							
Parameter	Gas Vendor	Cylinder Serial Number	Cylinder Value	Expiration Date				
NOx	Airgas	CC82975	124.3 ppm	4/5/2030				
NOx	Airgas	CC14792X	241.5 ppm	2/19/2029				
SO ₂	Airgas	CC502390	49.95 ppm	2/28/2031				
SO ₂	Airgas	CC310555	90.56 ppm	2/26/2030				
SO ₂	Airgas	CC1505161	254.3 ppm	10/29/2027				
SO ₂	Airgas	CC500227	482.4 ppm	12/13/2024				
O ₂	Àirgas	EB0162279	10.14%	3/21/2031				
O ₂	Airgas	CC743660	19.35%	6/18/2029				
O2	Airgas	CC12390	5.064%	3/11/2030				
O ₂	Airgas	CC431939	9.034%	3/21/2030				
CO2	Airgas	EB0162279	9.743%	3/21/2031				
CO ₂	Airgas	CC743660	18.76%	6/18/2029				
CO	Airgas	CC445058	250.7 ppm	6/21/2030				
СО	Airgas	CC194994	434.0 ppm	3/23/2030				
CO	Airgas	CC713835	920.9 ppm	8/12/2027				

The gas cylinders used to perform the RATA are summarized below.

The identifications of the individuals associated with the test program are summarized below.

Location	Address	Contact
Test Facility	Billerud Quinnesec LLC W-679 U. S. Highway 2 Quinnesec, Michigan 49876	Ms. Paula LaFleur Environmental Engineer (906) 779-3494 (phone) paula.lafleur@billerud.com
Testing Company Representative	Mostardi Platt 888 Industrial Drive Elmhurst, Illinois 60126	Mr. Daniel Kossack Project Manager (630) 993-2100 (phone) dkossack@mp-mail.com

The test crew consisted of Messrs. C. Trezak, M. Sather, V. Vang, and D. Kossack of Mostardi Platt.

2.0 TEST METHODOLOGY

Emissions testing was conducted following the methods specified in 40CFR, Part 40 CFR, Part 60, Appendix A. Schematics of the test section diagrams and sampling trains used are included in Appendix A and B, respectively. Copies of example calculation and nomenclature are included in Appendix C. Copies of analyzer print-outs for each test run are included in Appendix D. CEM data and process data as provided by Billerud Quinnesec, LLC are included in Appendix E.

The following methodologies were used during the test program:

Method 1 Traverse Point Determination

Test measurement points were selected in accordance with Method 1. The characteristics of the measurement locations are summarized below.

Location	Upstream Distance	Downstream Distance	Test Parameter	Number of Sampling Points
Waste Fuel Boiler Outlet Duct	20 feet	100 feet	Volumetric	10
Recovery Boiler Outlet Duct	2 x Diameter	9 x Diameter	Flow	18

Method 2 Volumetric Flowrate Determination

Gas velocity was measured following Method 2, for purposes of calculating stack gas volumetric flow rate at the Waste Fuel Boiler Outlet Duct and Recovery Boiler Outlet Duct. An S-type pitot tube, differential pressure gauge, thermocouple and temperature readout were used to determine gas velocity at each sample point at each test location. Copies of field data sheets are included in Appendix F. All of the equipment used was calibrated in accordance with the specifications of the Method. Calibration data are presented in Appendix G. This testing met the performance specifications as outlined in the Method.

Method 3A Oxygen (O₂)/ Carbon Dioxide (CO₂) Determination

Stack gas O_2 and/or CO_2 concentrations were determined in accordance with USEPA Method 3A. Servomex analyzers were used to determine the O_2 and/or CO_2 concentrations in the manner specified in the Method. Each instrument has a paramagnetic detector and the O_2 operates in the nominal range of 0% to 25% with the specific range determined by the high-level calibration gas and the CO_2 operates in the nominal range of 0 to 20% with the specific range determined by the high-level calibration gas. High-range calibrations were performed using USEPA Protocol gas. Zero nitrogen (a low ppm pollutant in balance nitrogen calibration gases) was introduced during other instrument calibrations to check instrument zero. High- and a mid-range % O_2 and/or CO_2 levels in balance nitrogen were also introduced. Zero and mid-range calibrations were performed using USEPA Protocol gas after each test run. Copies of the gas cylinder certifications are found in Appendix H. This testing met the performance specifications as outlined in the Method.

Method 4 Moisture Determination

USEPA Method 4, 40CFR60, Appendix A, was utilized to determine water (H_2O) content of the exhaust gas Waste Fuel Boiler Outlet Duct and Recovery Boiler Outlet Duct. 100 milliliters (ml) of water were added to each of the first two impingers, the third impinger was left empty, and the fourth impinger was charged with approximately 200 grams of silica gel. The impingers were placed in an ice bath to maintain the sampled gas passed through the silica gel impinger outlet below 68°F in order to increase the accuracy of the sampled dry gas volume measurement. The water volumes

of the impinger train were measured and the silica gel was weighed before and after each test run to determine the mass of moisture condensed.

Each sample was extracted through a heated stainless-steel probe and filter assembly at a constant sample rate of approximately 0.75 cubic feet per minute, which was maintained throughout the course of the test run. Approximately 21 dry standard cubic feet (dscf) were sampled for, each moisture run. After each run, a leak check of the sampling train was performed at a vacuum greater than the sampling vacuum to determine if any leakage had occurred during sampling. Following the leak check, the impingers were removed from the ice bath, water levels were measured, and the silica gel weight was recorded.

All of the equipment used was calibrated in accordance with the specifications of the Method.

Copies of field data sheets are included in Appendix F. Calibration data is presented in Appendix G. This testing met the performance specifications as outlined in the Method.

Method 6C Sulfur Dioxide (SO₂) Determination

Stack gas SO₂ concentrations and emission rates were determined in accordance with USEPA Method 6C, 40CFR60, Appendix A at the Waste Fuel Boiler Outlet Duct and Recovery Boiler Outlet Duct. A Thermo Scientific Model 43C Pulsed Fluorescence Sulfur Dioxide Analyzer was used to determine sulfur dioxide concentrations, in the manner specified in the Method. The instrument for the Recovery Boiler operated in the nominal range of 0 ppm to 100 ppm with the specific range determined by the high-level span calibration gas of 90.56 ppm. The instrument for the Waste Fuel Boiler operated in the nominal range of 0 ppm with the specific range determined by the high-level span calibration gas of 482.4 ppm.

The Model 43C High Level is based on the principle that SO₂ molecules absorb ultraviolet (UV) light and become excited at one wavelength, then decay to a lower energy state emitting UV light at a different wavelength. Specifically,

$$SO_2 + hv_1 \rightarrow SO_2^* \rightarrow SO_2 + hv_2$$

The sample is drawn into the Model 43C High Level through the sample bulkhead. The sample passes a pressure sensor then flows through a capillary and a flow sensor. The sample then flows into the fluorescence chamber, where pulsating UV light excites the SO_2 molecules. The condensing lens focuses the pulsating UV light into the mirror assembly. The mirror assembly contains four selective mirrors that reflect only the wavelengths which excite SO_2 molecules. As the excited SO_2 molecules decay to lower energy states they emit UV light that is proportional to the SO_2 concentration. The bandpass filter allows only the wavelengths emitted by the excited SO_2 molecules to reach the photomultiplier tube (PMT). The PMT detects the UV light emission from the decaying SO_2 molecules. The photodetector, located at the back of the fluorescence chamber, continuously monitors the pulsating UV light source and is connected to a circuit that compensates for fluctuations in the UV light.

The sample then flows to the pump and is exhausted out the exhaust bulkhead of the analyzer. The Model 43C High Level outputs the SO_2 concentration to the front panel display and the analog outputs.

Stack gas was delivered to the analyzer via a Teflon[®] sampling line, heated to a minimum temperature of 250°F. Excess moisture in the stack gas was removed using a refrigerated

condenser. The entire system was calibrated in accordance with the Method, using certified calibration gases introduced at the probe, before and after each test run.

A list of calibration gases used and the results of all calibration and other required quality assurance checks are found in Appendix F. Copies of the gas cylinder certifications are found in Appendix G. This testing met the performance specifications as outlined in the Method.

Method 7E Nitrogen Oxide (NO_x) Determination

Stack gas NO_X concentrations and emission rates were determined in accordance with USEPA Method 7E, 40CFR60, Appendix A, at the Package Boiler Outlet Duct, Waste Fuel Boiler Outlet Duct, and Recovery Boiler Outlet Duct. A Thermo Scientific Model 42i Chemiluminescence Nitrogen Oxides Analyzer was used to determine nitrogen oxides concentrations, in the manner specified in the Method. The instrument operated in the nominal range of 0 ppm to 500 ppm with the specific range determined by the high-level span calibration gas of 241.5 ppm.

The Model 42i operates on the principle that nitric oxide (NO) and ozone (O_3) react to produce a characteristic luminescence with an intensity linearly proportional to the NO concentration. Infrared light emission results when electronically excited NO₂ molecules decay to lower energy states. Specifically,

$$NO+O_3 \rightarrow NO_2+O_2+hv$$

Nitrogen dioxide (NO₂) must first be transformed into NO before it can be measured using the chemiluminescent reaction. NO₂ is converted to NO by a stainless steel NO₂-to-NO converter heated to about 625°C. The flue gas sample is drawn into the Model 42*i* through the sample bulkhead. The sample flows through a capillary, and then to the mode solenoid valve. The solenoid valve routes the sample either straight to the reaction chamber (NO mode) or through the NO₂-to-NO converter and then to the reaction chamber (NO_X mode). A flow sensor prior to the reaction chamber measures the sample flow. Dry air enters the Model 42*i* through the dry air bulkhead, passes through a flow switch, and then through a silent discharge ozonator. The ozonator generates the ozone needed for the chemiluminescent reaction. At the reaction chamber, the ozone reacts with the NO in the sample to produce excited NO₂ molecules. A photomultiplier tube (PMT) housed in a thermoelectric cooler detects the luminescence generated during this reaction. From the reaction chamber, the exhaust travels through the ozone (O₃) converter to the pump, and is released through the vent.

The NO and NO_X concentrations calculated in the NO and NO_X modes are stored in memory. The difference between the concentrations is used to calculate the NO₂ concentration. The Model 42i outputs NO, NO₂, and NO_X concentrations to the front panel display, the analog outputs, and also makes the data available over the serial or ethernet connection.

Stack gas was delivered to the analyzer via a Teflon[®] sampling line, heated to a minimum temperature of 250°F. Excess moisture in the stack gas was removed using a refrigerated condenser. The entire system was calibrated in accordance with the Method, using certified calibration gases introduced at the probe, before and after each test run. This testing met the performance specifications as outlined in the Method.

A list of calibration gases used and the results of all calibration and other required quality assurance checks are found in Appendix G. Copies of the gas cylinder certifications are found in Appendix H. The NO₂ to NO converter tests can be found in Appendix I. This testing met the performance specifications as outlined in the Method.

Method 10 Carbon Monoxide (CO) Determination

Stack gas CO concentrations and emission rates were determined in accordance with USEPA Method 10, 40CFR60, Appendix A at the Package Boiler Outlet Duct and Recovery Boiler Outlet Duct. A Fischer Scientific Model 48C Gas Filter Correlation Carbon Monoxide was used to determine carbon monoxide concentrations, in the manner specified in the Method. The instrument operated in the nominal range of 0 ppm to 500 ppm or 1,000 ppm with the specific range determined by the high-level span calibration gas of 434.0 ppm and 920.9 ppm.

The Model 48C High Level is based on the principle that CO absorbs infrared radiation at a wavelength of 4.6 microns. Because infrared absorption is a nonlinear measurement technique, it is necessary for the instrument electronics to transform the basic analyzer signal into a linear output. The Model 48C High Level uses an exact calibration curve to accurately linearize the instrument output over any range up to a concentration of 20,000 ppm. The sample is drawn into the analyzer through the sample bulkhead. The sample flows through the optical bench. Radiation from an infrared source is chopped and then passed through a gas filter alternating between CO and N2. The radiation then passes through a narrow bandpass interference filter and enters the optical bench where absorption by the sample gas occurs. The infrared radiation then exits the optical bench and falls on an infrared detector. The CO gas filter acts to produce a reference beam which cannot be further attenuated by CO in the sample cell. The N₂ side of the filter wheel is transparent to the infrared radiation and therefore produces a measure beam which can be absorbed by CO in the cell. The chopped detector signal is modulated by the alternation between the two gas filters with an amplitude related to the concentration of CO in the sample cell. Other gases do not cause modulation of the detector signal since they absorb the reference and measure beams equally. Thus, the GFC system responds specifically to CO. The Model 48C High Level outputs the CO concentration to the front panel display and the analog outputs.

Stack gas was delivered to the analyzer via a Teflon[®] sampling line, heated to a minimum temperature of 250°F. Excess moisture in the stack gas was removed using a refrigerated condenser. The entire system was calibrated in accordance with the Method, using certified calibration gases introduced at the probe, before and after each test run.

A list of calibration gases used and the results of all calibration and other required quality assurance checks are found in Appendix G. Copies of the gas cylinder certifications are found in Appendix H. This testing met the performance specifications as outlined in the Method.

Method 16A Total Reduced Sulfur (TRS) Determination

Integrated gas samples were extracted from the Lime Kiln and Recovery Boiler Outlet Duct gas streams in accordance with Method 16A (impinger technique), 40CFR60, for the determination of total reduced sulfur (TRS) emissions from stationary sources. This method selectively removed sulfur dioxide (SO₂) by bubbling the gas sample through a citrate buffer solution, then thermally oxidizing TRS compounds present to SO₂. The SO₂ was then collected in hydrogen peroxide as sulfate and analyzed by the Method 6 barium-thorin titration procedure, 40CFR60.

Interferences caused by particulate matter entering the sampling train were eliminated by the use of a heated filter medium placed at the end of the heated Teflon®-lined (or glass-lined) probe.

Sampling included three 1-hour tests followed by one 30-minute system validation to be completed as one test run. A description of the test train utilized is appended. Sampling train preparation was in accordance with Method 16A, 40CFR60, and included the following:

- 1. All probes, filter holders, and sampling lines were cleaned prior to each test.
- 2. The SO₂ scrubber was charged with 100 mls of citrate buffer solution into each of the first two impingers prior to each test. Citrate buffer solution was prepared by dissolving 300 g of potassium citrate (or 284 g of sodium citrate) and 41 g of anhydrous citric acid in one liter of water. The pH of the solution was then adjusted to between 5.4 and 5.6 with potassium citrate or citric acid, as required.
- 3. The probe and heated filter media were maintained at approximately 250°F to prevent moisture condensation.
- 4. The thermal oxidation furnace was maintained at 800°C±100°C during the test time.
- 5. The SO₂ portion of the train was prepared and analyzed in accordance with the methods described for sulfur dioxide testing listed previously.

The validations involved sampling a known concentration of hydrogen sulfide (H_2S) and comparing the analyzed concentration with the known concentration. The H_2S recovery gas was mixed with combustion gas in a dilution system. The flowrates were adjusted to generate an H_2S concentration in the range of the stack gas. The samples were collected and analyzed in the same manner as a normal stack test. The sample was collected through the end of the probe to ensure extraction of a representative sample. System validations were performed following each set of three 1-hour tests.

A list of calibration gases used and the results of all calibration and other required quality assurance checks can be found in Appendix F. Copies of calibration gas certifications can be found in Appendix G.

3.0 TEST RESULT SUMMARIES

Client: Billerud Quinnesec, LLC Facility: Quinnesec Mill Project #: M231804 Fuel Type: Natural Gas Location: Package Boiler Outlet Duct Date: 5/10/23 Test Method: 7E, 3A Fuel Factor: 8710

O2 based NOx lb/mmBtu RATA CEM Analyzer Information

CEM Analyzer Information								
NO	_x Monit	tor/Model:	Therm	o 42iQ		NO _x Serial # :		090011
0	O2 Monitor/Model		Thermo CTL902C		O2 Serial #		11803	390002
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM NO _x Ib/MMBtu	CEM NO _x Ib/MMBtu	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)
1	1	05/10/23	08:05	08:25	0.05	0.05	0.00	0.0000
1	2	05/10/23	08:43	09:03	0.05	0.05	0.00	0.0000
1	3	05/10/23	10:45	11:05	0.06	0.05	0.01	0.0001
1	4	05/10/23	11:31	11:51	0.06	0.05	0.01	0.0001
1	5	05/10/23	12:14	12:34	0.06	0.06	0.00	0.0000
1	6	05/10/23	12:51	13:11	0.06	0.06	0.00	0.0000
1	7	05/10/23	13:25	13:45	0.06	0.05	0.01	0.0001
0	8	05/10/23	14:01	14:21	0.06	0.05	0.01	0.0001
1	9	05/10/23	14:36	14:56	0.05	0.05	0.00	0.0000
1	10	05/10/23	15:11	15:31	0.05	0.05	0.00	0.0000
				n		Э ^й		
				t(0.975)	2.3	06		
		Mean Re	ference Me	thod Value	0.0)56	RM avg	
			Mean	CEM Value	0.0)52	CEM avg	
	Sum of Differences				0.0)30	di	
Mean Difference					0.0	003	d	
Sum of Differences Squared					0.0	0.000 di ²		
Standard Deviation				0.0	0.005 sd			
Confidence Coefficient 2.5% Error (1-tail)				0.0)04	cc		
			Relativ	e Accuracy	12	.92	RA	

Client:	Billerud Quinnesec, LLC
Facility:	Quinnesec Mill

Project #: M231804

Location: Package Boiler Outlet Duct Date: 5/10/23

Test Method: 7E, 2

Applicable Standard: 41.9

NO_x Ib/hr RATA CEM Analyzer Information

NO	_x Moni	tor/Model:	Therm	o 42iQ		NO _x Serial # :	11800	090011	
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM NO _x Ib/hr	CEM NO _x Ib/hr	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)	
1	1	05/10/23	08:05	08:25	8.7	8.8	-0.1	0.01	
1	2	05/10/23	08:43	09:03	8.8	8.9	-0.1	0.01	
1	3	05/10/23	10:45	11:05	9.2	9.0	0.2	0.04	
1	4	05/10/23	11:31	11:51	9.1	9.0	0.1	0.01	
0	5	05/10/23	12:14	12:34	9.2	9.0	0.2	0.04	
1	6	05/10/23	12:51	13:11	9.0	9.0	0.0	0.00	
1	7	05/10/23	13:25	13:45	9.0	9.0	0.0	0.00	
1	8	05/10/23	14:01	14:21	9.1	9.0	0.1	0.01	
1	9	05/10/23	14:36	14:56	9.0	9.0	0.0	0.00	
1	10	05/10/23	15:11	15:31	8.9	8.9	0.0	0.00	
				n		9			
				t(0.975)	2.3	306			
		Mean Re	ference Me	thod Value	8.	978	RM avg		
			Mean	CEM Value	8.956 CEM avg				
	Sum of Differences					0.200 di			
Mean Difference				0.022		d			
Sum of Differences Squared					0.080 di ²		di ²	di ²	
Standard Deviation					0.	097	sd		
C	Confidence Coefficient 2.5% Error (1-tail)					075	CC		
			Relativ	e Accuracy	1	.08	RA		

Project No. M231804B Package Fuel Boiler Outlet Duct, Waste Fuel Boiler Outlet Duct, Recovery Fuel Boiler Outlet Duct, and Lime Kiln Stack

Client:	Billerud Quinnesec, LLC
Facility:	Quinnesec Mill
Project #:	M231804

Location: Package Boiler Outlet Duct Date: 5/10/23 Test Method: 3A

$O_2 \%$ (dry) RATA

	CEM Analyzer Information											
02	Monite	or/Model:	Thermo	CTL902C		O ₂ Serial # :	11803	390002				
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM O₂ % (dry)	CEM O₂ % (dry)	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)				
1	1	05/10/23	08:05	08:25	4.0	4.0	0.0	0.00				
0	2	05/10/23	08:43	09:03	3.9	4.1	-0.2	0.04				
1	3	05/10/23	10:45	11:05	4.2	4.4	-0.2	0.04				
1	4	05/10/23	11:31	11:51	4.4	4.4	0.0	0.00				
1	5	05/10/23	12:14	12:34	4.4	4.4	0.0	0.00				
1	6	05/10/23	12:51	13:11	4.4	4.4	0.0	0.00				
1	7	05/10/23	13:25	13:45	4.3	4.4	-0.1	0.01				
1	8	05/10/23	14:01	14:21	4.3	4.4	-0.1	0.01				
1	9	05/10/23	14:36	14:56	4.3	4.3	0.0	0.00				
1	10	05/10/23	15:11	15:31	4.3	4.3	0.0	0.00				
				n	a an	Э с с с с с с с с с с с с с с с с с с с		-				
				t(0.975)	2.3	306						
		Mean Re	ference Me	thod Value	4.:	289	RM avg					
				CEM Value		333	CEM avg					
			Sum of	Differences	-0,	400	di					
			Mean	Difference	-0.	044	d					
		Sum	of Differenc	es Squared	0.0	060	di ²					
			Standar	d Deviation	0.0	073	sd					
С	onfide	nce Coeffi	icient 2.5% I	Error (1-tail)	0.056 cc							
			Relativ	e Accuracy	2.	34	RA					

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Project No. M231804B Package Fuel Boiler Outlet Duct, Waste Fuel Boiler Outlet Duct, Recovery Fuel Boiler Outlet Duct, and Lime Kiln Stack

Client: Facility: Project #: Fuel Type:	Quinne M2318	04	e, LLC				r Outlet Duct		
ruer type.	Natura	Gas	Applicable	Standard		0710			
				Standard:					
					b/mmBtu RA	ATA			
					r Information				
		tor/Model:		o 48iQ	*	CO Serial # :		930081	
0	2 Moni	tor/Model:	Thermo	CTL902C		O2 Serial # :	11803	390002	
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM CO Ib/MMBtu	CEM CO Ib/MMBtu	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)	
1	1	05/10/23	08:05	08:25	0.00	0.00	0.00	0.0000	
1	2	05/10/23	08:43	09:03	0.00	0.00	0.00	0.0000	
1	3	05/10/23	10:45	11:05	0.00	0.00	0.00	0.0000	
1	4	05/10/23	11:31	11:51	0.00	0.00	0.00	0.0000	
1	5	05/10/23	12:14	12:34	0.00	0.00	0.00	0.0000	
1	6	05/10/23	12:51	13:11	0.00	0.00	0.00	0.0000	
1	7	05/10/23	13:25	13:45	0.00	0.00	0.00	0.0000	
1	8	05/10/23	14:01	14:21	0.00	0.00	0.00	0.0000	
1	9	05/10/23	14:36	14:56	0.00	0.00	0.00	0.0000	
1	10	05/10/23	15:11	15:31	0.00	0.00	0.00	0.0000	
				n		0			
				t(0.975)	2.2				
		Mean Re	ference Me	and set they are subscored.	0.0		RM avg		
			2110 CA14	CEM Value	0.0		CEM avg		
			1753 HELESKOOL 200 14 4	Differences	0.000		di		
				Difference	0.000 d		12.5.56.2		
		Sum	of Difference			000	di²		
				d Deviation	0.0		sd		
(Confide	nce Coeffi	cient 2.5% E		0.0		cc		
			Relativ	e Accuracy	0.	00	RA		

Client: Billerud Quinnesec, LLC Facility: Quinnesec Mill Project #: M231804 Location: Package Boiler Outlet Duct Date: 5/10/23 Test Method: 10

Applicable Standard: 195

CO ppmvd RATA

CEM Analyzer Information

C) Moni	tor/Model:	Therm	o 48iQ		CO Serial # :	11809	930081
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM CO ppmvd	CEM CO ppmvd	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)
0	1	05/10/23	08:05	08:25	0.0	1.7	-1.7	2.89
1	2	05/10/23	08:43	09:03	0.0	0.1	-0.1	0.01
1	3	05/10/23	10:45	11:05	0.0	0.2	-0.2	0.04
1	4	05/10/23	11:31	11:51	0.0	0.5	-0.5	0.25
1	5	05/10/23	12:14	12:34	0.0	-0.3	0.3	0.09
1	6	05/10/23	12:51	13:11	0.0	-0.5	0.5	0.25
1	7	05/10/23	13:25	13:45	0.0	-0.4	0.4	0.16
1	8	05/10/23	14:01	14:21	0.0	-0.5	0.5	0.25
1	9	05/10/23	14:36	14:56	0.0	-0.9	0.9	0.81
1	10	05/10/23	15:11	15:31	0.0	-0.2	0.2	0.04
		Moon Po	ference Me	n t(0.975) thod Value	2.3	9 606 000	RM avg	
	······			CEM Value		222	CEM avg	
				Differences		000	di	
				Difference	0.2	222	d	
		Sum	of Difference	•		900	di ²	
				d Deviation		127	sd	
(Confide		cient 2.5% E			328	cc	
		R	elative Accu	iracy - APS	0.	55	ppm + cc d	ifference ^A

^A Relative accuracy based upon alternate performance standard of +/- 5 ppm CO plus the confidence coefficient.

Client: Billerud Quinnesec, LLC Facility: Quinnesec Mill

Project #: M231804

Location: Package Boiler Outlet Duct Date: 5/10/23 Test Method: 10, 2

Applicable Standard: 25.5

CO lb/hr RATA

CEM Analyzer Information

C	O Moni	tor/Model:	Therm	o 48iQ		CO Serial # :	11809	930081
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM CO lb/hr	CEM CO lb/hr	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)
0	1	05/10/23	08:05	08:25	0.0	0.2	-0.2	0.04
1	2	05/10/23	08:43	09:03	0.0	0.0	0.0	0.00
1	3	05/10/23	10:45	11:05	0.0	0.0	0.0	0.00
1	4	05/10/23	11:31	11:51	0.0	0.1	-0.1	0.01
1	5	05/10/23	12:14	12:34	0.0	0.0	0.0	0.00
1	6	05/10/23	12:51	13:11	0.0	-0.1	0.1	0.01
1	7	05/10/23	13:25	13:45	0.0	0.0	0.0	0.00
1	8	05/10/23	14:01	14:21	0.0	-0.1	0.1	0.01
1	9	05/10/23	14:36	14:56	0.0	-0.1	0.1	0.01
1	10	05/10/23	15:11	15:31	0.0	0.0	0.0	0.00
				n		9		
				t(0.975)		306		
		Mean Re	eference Me			000	RM avg	
				CEM Value		022	CEM avg	
				Differences		200	di	
				Difference		022	d	
		Sum	of Difference			040	di ²	
				d Deviation		067	sd	
(Confide		icient 2.5% E		0.051 cc		cc	
		R	elative Accu	iracy - APS	0.	29	RA	

^A Relative accuracy based upon +/- 5% of applicable standard

Client: Billerud Quinnesec, LLC Facility: Quinnesec Mill Project #: M231804 Fuel Type: Other Location: Waste Fuel Boiler Outlet Duct Date: 5/11/23 Test Method: 7E, 3A Fuel Factor: 9518

O2 based NOx lb/mmBtu RATA CEM Analyzer Information

NO	_x Monit	tor/Model:	Therm	o 42iQ		NO _x Serial # :		030057				
0	2 Moni	tor/Model:	Thermo	CTL902C		O2 Serial # :	11805	530001				
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM NO _x Ib/MMBtu	CEM NO _x Ib/MMBtu	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)				
1	1	05/11/23	14:00	14:20	0.15	0.14	0.01	0.0001				
1	2	05/11/23	14:55	15:15	0.15	0.14	0.01	0.0001				
1	3	05/11/23	15:40	16:00	0.13	0.12	0.01	0.0001				
1	4	05/11/23	16:20	16:40	0.17	0.16	0.01	0.0001				
1	5	05/11/23	17:00	17:20	0.15	0.13	0.02	0.0004				
1	6	05/11/23	17:40	18:00	0.14	0.13	0.01	0.0001				
1	7	05/11/23	18:25	18:45	0.15	0.13	0.02	0.0004				
0	8	05/11/23	19:05	19:25	0.15	0.13	0.02	0.0004				
1	9	05/11/23	19:45	20:05	0.14	0.13	0.01	0.0001				
1	10	05/11/23	20:25	20:45	0.16	0.15	0.01	0.0001				
				n		9						
		an tan Anta		t(0.975)	2.3	806	A CARACTER STATE					
		Mean Re	ference Me	thod Value	0.1	149	RM avg					
			Mean	CEM Value	0.1	137	CEM avg					
			Sum of	Differences	0.1	110	di					
			Mean	Difference	0.0	012	d					
		Sum	of Difference	es Squared	0.0	002	di ²					
			Standar	d Deviation	0.0	004	sd					
	Confide	nce Coeff	cient 2.5% E	Error (1-tail)	0.0	003	CC					
			Relativ	e Accuracy	10	.49	RA					

Client:	Billeru	d Quinnesed	s, LLC			: Waste Fuel Bo	oiler Outlet Du	uct
Facility:					Date:	: 5/11/23		
Project #:	M2318	04			Test Method:	: 7E, 2		
			Applicable	e Standard:	437			
				NO _x lb/h	nr RATA			
			C	EM Analyze	r Information	า		
NO	_x Moni	tor/Model:	Therm	o 42iQ	0.00	NO _x Serial # :	11800	030057
1=accept 0=reject	1=accept Test Test Date			End Time	RM NO _x Ib/hr	CEM NO _x Ib/hr	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)
1	1	05/11/23	14:00	14:20	62.7	54.8	7.9	62.41
1	2	05/11/23	14:55	15:15	59.7	50.5	9.2	84.64
1	3	05/11/23	15:40	16:00	53.9	44.9	9.0	81.00
1	4	05/11/23	16:20	16:40	63.3	56.9	6.4	40.96
1	5	05/11/23	17:00	17:20	60.5	49.9	10.6	112.36
1	6	05/11/23	17:40	18:00	55.3	46.7	8.6	73.96
1	7	05/11/23	18:25	18:45	56.2	49.5	6.7	44.89
0	8	05/11/23	19:05	19:25	58.5	47.9	10.6	112.36
1	9	05/11/23	19:45	20:05	57.3	49.0	8.3	68.89
1	10	05/11/23	20:25	20:45	63.2	57.1	6.1	37.21
	1			n		9		
				t(0.975)	2.	306		
		Mean Re	ference Me	thod Value	59	.122	RM avg	
			Mean	CEM Value	51	.033	CEM avg	
				Differences	72	2.800	di	
				Difference	8.089		d	
Sum of Differences Squared					606	6.320	di ²	
				d Deviation	1.477		sd	
(Confide	ence Coeffi	icient 2.5% I	Error (1-tail)	1.	.135	cc	
			Relativ	e Accuracy	1	5.60	RA	

		Quinnese	ec, LLC		Location: Waste Fuel Boiler Outlet Duct			
Facility:					Date: 5/11/23			
Project #:	10123180	04			Test Method:	3A		
					dry) RATA			
				CEM Analyz	er Information	l	•	
4	Test	Teat					(RM-CEM)	(RM-CEM)
1=accept	Test	Test	Start Time	End Time	RM CO ₂ %	CEM CO ₂ %	Difference	Difference ²
0=reject	Run	Date			(dry)	(dry)	(di)	(di²)
1	1	05/11/23	14:00	14:20	13.8	13.8	0.0	0.00
1	2	05/11/23	14:55	15:15	13.8	13.8	0.0	0.00
1	3	05/11/23	15:40	16:00	13.8	13.8	0.0	0.00
0	4	05/11/23	16:20	16:40	12.9	12.7	0.2	0.04
1	5	05/11/23	17:00	17:20	14.2	14.2	0.0	0.00
1	6	05/11/23	17:40	18:00	14.0	14.0	0.0	0.00
1	7	05/11/23	18:25	18:45	13.6	13.6	0.0	0.00
1	8	05/11/23	19:05	19:25	14.3	14.1	0.2	0.04
1	9	05/11/23	19:45	20:05	14.1	14.0	0.1	0.01
1	10	05/11/23	20:25	20:45	13.6	13.6	0.0	0.00
				'n	5			
				t(0.975)		306		
		Mean Re	ference Me			911	RM avg	
	Mean CEM Value					878	CEM avg	
	Sum of Differences					300	di	
Mean Difference					0.033		d	
	Sum of Differences Squared					050	di ²	
				d Deviation	0.071 sd		sd	
C	onfider	nce Coeffi	icient 2.5% I	Error (1-tail)	0.0	054	cc	
			Relativ	e Accuracy	0.	63	RA	

Client: Facility:		l Quinnese sec Mill	ec, LLC			Waste Fuel Bo 5/11/23	iler Outlet Du	ict
Project #:					Test Method: 3A			
				O₂ % (d	ry) RATA			
				_	er Information	1		
0,	Monit	or/Model:		CTL902C		O ₂ Serial # :	11805	530001
1=accept		Test Date	Start Time		RM O ₂ %	CEM O ₂ %	(RM-CEM) Difference	(RM-CEM) Difference ²
0=reject	Run	Date			(dry)	(dry)	(di)	(di ²)
1	1	05/11/23	14:00	14:20	5.9	6.1	-0.2	0.04
1	2	05/11/23	14:55	15:15	5.9	6.1	-0.2	0.04
0	3	05/11/23	15:40	16:00	5.8	6.1	-0.3	0.09
1	4	05/11/23	16:20	16:40	6.8	7.1	-0.3	0.09
1	5	05/11/23	17:00	17:20	5.6	5.8	-0.2	0.04
1	6	05/11/23	17:40	18:00	5.7	5.9	-0.2	0.04
1	7	05/11/23	18:25	18:45	6.2	6.4	-0.2	0.04
1	8	05/11/23	19:05	19:25	5.6	5.8	-0.2	0.04
1	9	05/11/23	19:45	20:05	5.7	5.9	-0.2	0.04
1	10	05/11/23	20:25	20:45	6.2	6.4	-0.2	0.04
				n	9			
				t(0.975)	2.3			
		Mean Re	ference Me			956	RM avg	
				CEM Value		167	CEM avg	
				Differences		900	di	
				Difference	-0.211		d	
		Sum	of Difference			410	di²	
				d Deviation	0.033 sd			
C	onfide	nce Coeffi		Error (1-tail)		026	cc	
			Relativ	e Accuracy	3.	98	RA	

Client: Billerud Quinnesec, LLC Facility: Quinnesec Mill Project #: M231804 Fuel Type: Other Location: Waste Fuel Boiler Outlet Duct Date: 5/11/23 Test Method: 6C, 3A Fuel Factor: 9518

Applicable Standard: 1.2

O2 based SO2 lb/mmBtu RATA

	CEM Analyzer Information											
		tor/Model:		o 43iQ		SO ₂ Serial # :	11809	930080				
0	2 Moni	tor/Model:	Thermo	CTL902C		O2 Serial # :	1180	530001				
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM SO₂ Ib/mmBtu	CEM SO ₂ Ib/mmBtu	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)				
1	1	05/11/23	14:00	14:20	0.1	0.0	0.1	0.01				
1	2	05/11/23	14:55	15:15	0.1	0.0	0.1	0.01				
1	3	05/11/23	15:40	16:00	0.1	0.0	0.1	0.01				
1	4	05/11/23	16:20	16:40	0.1	0.0	0.1	0.01				
1	5	05/11/23	17:00	17:20	0.1	0.0	0.1	0.01				
1	6	05/11/23	17:40	18:00	0.1	0.0	0.1	0.01				
1	7	05/11/23	18:25	18:45	0.1	0.0	0.1	0.01				
1	8	05/11/23	19:05	19:25	0.1	0.0	0.1	0.01				
1	9	05/11/23	19:45	20:05	0.1	0.0	0.1	0.01				
0	10	05/11/23	20:25	20:45	0.0	0.0	0.0	0.00				
				n		9						
				t(0.975)	2.3	806						
		Mean Re	ference Me	thod Value	0.1	100	RM avg					
			Mean	CEM Value	0.0	000	CEM avg					
			Sum of	Differences	0.9	900	di					
			Mean	Difference	0.1	100	d					
		Sum o	of Difference	es Squared	0.0	090	di ²					
			Standar	d Deviation	0.0	000	sd					
(Confide	nce Coeffi	cient 2.5% E	Error (1-tail)	0.000		сс					
		R	elative Accu	iracy - APS	8.	33	RA ^A					

^A Relative accuracy based upon +/- 10% of applicable standard of 1.2 In/mmBtu

Project No. M231804B Package Fuel Boiler Outlet Duct, Waste Fuel Boiler Outlet Duct, Recovery Fuel Boiler Outlet Duct, and Lime Kiln Stack

Client:	Billerud Quinnesec, LLC
Facility:	Quinnesec Mill
Project #:	M231804

Location: Waste Fuel Boiler Outlet Duct Date: 5/11/23 Test Method: 6C, 2

Applicable Standard: 476

SO2 lb/hr RATA

CEM Analyzer Information

SC	0 ₂ Moni	tor/Model:		o 43iQ		SO ₂ Serial # :	1180930080	
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM SO₂ Ib/hr	CEM SO₂ Ib/hr	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)
1	1	05/11/23	14:00	14:20	44.1	15.5	28.6	817.96
0	2	05/11/23	14:55	15:15	46.8	15.5	31.3	979.69
1	3	05/11/23	15:40	16:00	32.6	12.8	19.8	392.04
1	4	05/11/23	16:20	16:40	19.3	10.5	8.8	77.44
1	5	05/11/23	17:00	17:20	40.8	13.9	26.9	723.61
1	6	05/11/23	17:40	18:00	28.8	10.6	18.2	331.24
1	7	05/11/23	18:25	18:45	23.7	8.2	15.5	240.25
1	8	05/11/23	19:05	19:25	39.3	14.9	24.4	595.36
1	9	05/11/23	19:45	20:05	28.9	9.5	19.4	376.36
1	10	05/11/23	20:25	20:45	15.5	10.2	5.3	28.09
				n		9		
				t(0.975)	2.3	306		
		Mean Re	ference Me	thod Value	30	.333	RM avg	
			Mean	CEM Value	11.	.789	CEM avg	
			Sum of	Differences		6.900	di	
			Mean	Difference	18	.544	d	
		Sum o	of Difference	es Squared	358	2.350	di ²	
			Standar	d Deviation	7.	805	sd	
(Confide	nce Coeffi	cient 2.5% E	Error (1-tail)	5.999		сс	
		R	elative Accu	iracy - APS	5	.16	RA ^A	

^A Relative accuracy based upon +/- 10% of applicable standard of 476 lb/hr

Client:	Billeru	d Quinnes	ec, LLC		Test Location:	Waste Fuel Boiler O	utlet Duct			
Facility:	Quinn	esec Mill			Test Date: 5/11/2023					
Project #:	M2318	304			Test Method:	2				
-					CEM Analyzer Info	rmation				
				Vol	umetric How RATA -	Normal Load	*****			
	Flow	Monitor/	Model:		Deterich	Flow Serial # :	22-F-C-17	9, 274797.01.1		
1=accept 0=reject			End Time	Reference Method Flow DSCFM	CEM Flow DSCFM	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)			
1	1	05/11/23	14:00	14:08	90,083	85,894	4,189	17,547,070		
1	2	05/11/23	14:55	15:02	87,523	83,157	4,366	19,062,542		
1	3	05/11/23	15:40	15:47	87,934	82,562	5,372	28,857,147		
1	4	05/11/23	16:20	16:27	88,175	89,401	-1,226	1,501,962		
0	5	05/11/23	17:00	17:07	88,192	81,529	6,663	44,396,511		
1	6	05/11/23	17:40	17:47	86,808	82,333	4,475	20,029,060		
1	7	05/11/23	18:25	18:32	86,259	85,313	946	894,730		
1	8	05/11/23	19:05	19:13	85,162	79,001	6,161	37,956,761		
1	9	05/11/23	19:45	19:52	87,677	83,729	3,948	15,590,364		
1	10	05/11/23	20:25	20:32	87,176	87,404	-228	51,984		
				: n	9					
			t	(0.975)	2.30	6				
M	ean R	eference	Method	Value	87421	.998	RM avg			
		Mea	an CEN	l Value	84310	.444	CEM avg			
		Sum	of Diffe	rences	28003	.984	di			
		Me	an Diff	erence	3111.	554	d			
	Sum	of Differe	nces S	quared	1414916	19.403	di ²			
		Stand	lard De	viation	2606.	619	sd			
Confidence	e Coef	ficient 2.5	% Error	(1-tail)	2003.	621	сс			
		Rela	tive Ac	curacy	5.8	5	RA			

		Quinnese	c, LLC		Location: Recovery Boiler Outlet Duct			
Facility:					Date: 5/10/23			
Project #:	M2318	04			Test Method:	7E, 3A		
			Applicable	e Standard:	110			
) 8% O2 RA	TA		
					er Information			
NO	_x Moni	tor/Model:	Therm	o 42iQ		NO _x Serial # :	1180	090013
0	2 Moni	tor/Model:	Thermo	CTL902C		O ₂ Serial # :	1180	240002
4	T				RM NOx	CEM NOx	(RM-CEM)	(RM-CEM)
1=accept	Test	Test Date	Start Time	End Time	ppmvd @ 8	ppmvd @ 8	Difference	Difference ²
0=reject	Run	102			%O2	%02	(di)	(di²)
1	1	05/10/23	09:52	10:12	80.0	82.8	-2.8	7.7
1	2	05/10/23	10:36	10:56	80.0	82.8	-2.8	7.7
1	3	05/10/23	11:23	11:43	80.7	83.6	-2.9	8.5
1	4	05/10/23	12:10	12:30	84.6	87.4	-2.8	7.8
1	5	05/10/23	12:47	13:07	83.1	85.7	-2.6	6.8
1	6	05/10/23	13:28	13:48	84.1	87.1	-3.0	8.8
1	7	05/10/23	14:20	14:40	80.7	83.9	-3.2	10.1
0	8	05/10/23	14:57	15:17	83.5	86.9	-3.4	11.6
1	9	05/10/23	15:37	15:57	84.6	87.1	-2.5	6.4
1	10	05/10/23	16:25	16:45	81.7	83.8	-2.1	4.5
				n)		
				t(0.975)	2.3	06		
		Mean Re	ference Me	thod Value	82.	171	RM avg	
			Mean	CEM Value	84.	911	CEM avg	
				Differences		660	di	
				Difference	-2.	740	d	
		Sum	of Difference		68.285		di²	
				d Deviation	0.299 sd		sd	
C	Confide	nce Coeffi	cient 2.5% E		0.230 cc			
			Relativ	e Accuracy	3.	61	RA	

.

Facility:	Quinne		ec, LLC		Location: Recovery Boiler Outlet Duct Date: 5/10/23				
Project #:	M23180	04			Test Method: 3A				
				O ₂ % (d	ry) RATA				
				er Information	1				
O2	Monite	or/Model:	Thermo	CTL902C		O ₂ Serial # :	11802	240002	
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM O₂ % (dry)	CEM O ₂ % (dry)	(RM-CEM) Difference	(RM-CEM) Difference ²	
	·····						(di)	(di ²)	
1	1	05/10/23	09:52	10:12	4.7	4.8	-0.1	0.01	
1	2	05/10/23	10:36	10:56	4.7	4.9	-0.2	0.04	
1	3	05/10/23	11:23	11:43	4.8	5.0	-0.2	0.04	
1	4	05/10/23	12:10	12:30	4.6	4.7	-0.1	0.01	
1	5	05/10/23	12:47	13:07	4.6	4.7	-0.1	0.01	
1	6	05/10/23	13:28	13:48	4.6	4.7	-0.1	0.01	
1	7	05/10/23	14:20	14:40	4.6	4.7	-0.1	0.01	
0	8	05/10/23	14:57	15:17	4.6	4.8	-0.2	0.04	
1	9	05/10/23	15:37	15:57	4.7	4.8	-0.1	0.01	
1	10	05/10/23	16:25	16:45	4.6	4.7	-0.1	0.01	
				n)			
				t(0.975)		306			
		Mean Re	ference Me			656	RM avg		
				CEM Value		778	CEM avg		
				Differences		100	di		
			Mean	Difference		122	d		
	Sum of Differences Squared					0.150		di ²	
			Standar	d Deviation	0.044		sd		
c	onfide	nce Coeff	icient 2.5% l	Error (1-tail)	0.0	0.034		CC	
			Relativ	e Accuracy	3.	3.35 RA			

Client: Facility:		l Quinneseo sec Mill	s, LLC			Recovery Boile 5/10/23	r Outlet Duct		
Project #:	M2318	04			Test Method:	6C, 3A			
			Applicable	Standard:					
			SO	nnmvd (7 8% O2 RA	ТА			
SO2 ppmvd @ 8% O2 RATA CEM Analyzer Information									
SO	Moni	tor/Model:		o 43iQ		SO ₂ Serial # :	1180	090009	
		tor/Model:		CTL902C		O ₂ Serial # :		240002	
			menno	0113020	B M 0.00	_		(RM-CEM)	
1=accept	Test	Tast Data	Oto at Time	End Time	RM SO2	CEM SO2	(RM-CEM)		
0=reject	Run	Test Date	Start Time	End Time	ppmvd @ 8	ppmvd @ 8	Difference	Difference ²	
					%O2	%O2	(di)	(di²)	
1	1	05/10/23	09:52	10:12	0.0	0.1	-0.1	0.01	
1	2	05/10/23	10:36	10:56	0.1	0.1	0.0	0.00	
1	3	05/10/23	11:23	11:43	0.4	0.1	0.3	0.09	
1	4	05/10/23	12:10	12:30	0.4	0.1	0.3	0.09	
1	5	05/10/23	12:47	13:07	0.3	0.1	0.2	0.04	
1	6	05/10/23	13:28	13:48	0.2	0.1	0.1	0.01	
1	7	05/10/23	14:20	14:40	0.1	0.1	0.0	0.00	
1	8	05/10/23	14:57	15:17	0.3	0.1	0.2	0.04	
0	9	05/10/23	15:37	15:57	0.5	0.1	0.4	0.16	
1	10	05/10/23	16:25	16:45	0.1	0.1	0.0	0.00	
				n					
				t(0.975)	2.3				
		Mean Re	ference Me			211	RM avg		
				CEM Value		100	CEM avg		
				Differences		000	di		
	Mean Difference					11	d		
		Sum o	of Difference	•		280	di ²		
				d Deviation	0.145		sd		
(Confide	nce Coeffi	cient 2.5% E	Error (1-tail)	0.112 cc				
		R	elative Accu	uracy - APS	0	45	RA ^A		

 $^{\rm A}$ Relative accuracy based upon +/- 10% of applicable standard of 50 ppmvd @ 8% ${\rm O_2}$

Client: Billerud Quinnesec, LLC Facility: Quinnesec Mill Project #: M231804 Location: Recovery Boiler Outlet Duct Date: 5/10/23 Test Method: 10, 3A

les

Applicable Standard: 425

CO ppmvd @ 8% O2 RATA CEM Analyzer Information

C	O Moni	tor/Model:	Therm	o 48iQ		CO Serial # :	11706	680002	
0	2 Moni	tor/Model:	Thermo CTL902C		O ₂ Serial # :		1180240002		
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM CO ppmvd @ 8 %O2	CEM CO ppmvd @ 8 %O2	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)	
1	1	05/10/23	09:52	10:12	2.7	2.1	0.6	0.36	
1	2	05/10/23	10:36	10:56	3.9	3.2	0.7	0.49	
1	3	05/10/23	11:23	11:43	16.8	18.9	-2.1	4.41	
1	4	05/10/23	12:10	12:30	3.1	2.2	0.9	0.81	
1	5	05/10/23	12:47	13:07	3.9	3.8	0.1	0.01	
1	6	05/10/23	13:28	13:48	1.0	0.1	0.9	0.81	
1	7	05/10/23	14:20	14:40	1.0	1.9	-0.9	0.81	
1	8	05/10/23	14:57	15:17	1.4	2.3	-0.9	0.81	
1	9	05/10/23	15:37	15:57	4.6	7.2	-2.6	6.76	
0	10	05/10/23	16:25	16:45	25.3	33.5	-8.2	67.24	
		х. ¹		n t(0.975)	2.3	9 306			
		Mean Re	ference Me			267	RM avg		
				CEM Value		633	CEM avg		
				Differences		300	di		
				Difference		367	d		
Sum of Differences Squared					15.	270	di ²		
				d Deviation		1.326		sd	
(Confide	nce Coeffi	icient 2.5% I	Error (1-tail)	1.019		CC		
		R	elative Accu	uracy - APS	0.	33	RA		

^A Relative accuracy based upon +/- 10% of applicable standard of 500 ppmvd @ 8% O₂

Client: Facility: Project #:	Quinne		c, LLC		Location: Recovery Boiler Outlet Duct Date: 5/11/23 Test Method: 16A, 3A			
			Applicabl	e Standard:	5			
					d @ 8% O2 R itor Informatio			
TRS Monitor	Model:		Thermo 43i0	2	TRS Monite	or Serial # :	11800	090010
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM TRS asSO ₂ ppmvd @ 8% O ₂	CEM TRS asSO ₂ ppmvd @ 8% O ₃	(RM-CEM) Difference (di)	(RM-CEM) Difference (di ²)
1	1	05/11/23	8:32	9:32	1.9	1.6	0.3	0.09
1	2	05/11/23	9:47	10:47	1.9	1.8	0.1	0.01
1	3	05/11/23	10:58	11:58	1.7	1.5	0.2	0.04
1	4	05/11/23	12:58	13:58	1.6	2.0	-0.4	0.16
1	5	05/11/23	14:09	15:09	1.3	1.8	-0.5	0.25
1	6	05/11/23	15:19	16:19	1.9	1.8	0.1	0.01
1	7	05/11/23	17:19	18:19	1.9	1.9	0.0	0.00
1	8	05/11/23	18:30	19:30	2.2	1.9	0.3	0.09
1	9	05/11/23	19:40	20:40	1.8	1.9	-0.1	0.01
				n	Ş)		
				t(0.975)	2.3	06		
		Mean R	eference Me	ethod Value	1.8	800	RM avg	
			Mean	1.8	800	CEM avg		
			Sum of	0.0	000	di		
			Mean	0.000		d		
		Sum	of Differenc	0.6	60	di ²		
			Standar	0.287		sd		
	Confid	ence Coef	ficient 2.5%	Error (1-tail)	0.2	221	cc	
		F	Relative Acc	uracy - APS	4.4	42	RA ^A	

^A Relative accuracy based upon alternate standard of 5 ppmvd @ 8 % O2

		d Quinnes	ec, LLC			Recovery Boiler Out	et Duct			
Facility:					Test Date: 5/9/2023					
Project #:	M2318	304			Test Method:					
				vo	- Lumetric How RATA CEM Analyzer Info					
Flow	Monit	or/Model:	OFS-20	00W	CEW Analyzer Into	Flow Serial # :	1	5110807E		
							•	1		
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	Reference Method Flow DSCFM	CEM Flow DSCFM	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)		
1	1	05/09/23	13:35	13:45	185,871	178,334	7,537	56,810,346		
1	2	05/09/23	13:46	13:53	184,736	178,780	5,956	35,478,460		
1	3	05/09/23	14:23	14:30	185,965	179,373	6,592	43,449,454		
1	4	05/09/23	16:20	16:27	182,369	177,111	5,258	27,646,451		
1	5	05/09/23	16:28	16:34	186,266	177,027	9,240	85,372,626		
1	6	05/09/23	17:05	17:13	188,270	176,911	11,358	129,012,692		
1	7	05/09/23	17:28	17:34	187,367	176,439	10,928	119,420,710		
1	8	05/09/23	17:35	17:41	187,896	176,451	11,445	130,998,521		
0	9	05/09/23	17:42	17:48	190,348	176,570	13,778	189,827,122		
1	10	05/09/23	18:05	18:10	187,097	176,982	10,115	102,313,223		
				n	9					
				t(0.025)	2.30					
N	lean R	leference			186204		RM avg			
				l Value	17748		CEM avg			
•				rences	78429		di			
Mean Difference					8714.		d			
	Sum	of Differe			7305024	<u>, , , , , , , , , , , , , , , , , , , </u>	di ²			
				viation	2424.	<u> a anna a mara a mara a</u>	sd			
Confidence	e Coef				1863.		сс			
		Rela	ative Ac	curacy	5.6	8	RA			

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Project No. M231804B Package Fuel Boiler Outlet Duct, Waste Fuel Boiler Outlet Duct, Recovery Fuel Boiler Outlet Duct, and Lime Kiln Stack 27 of 340

Client: Facility: Project #:	Quinne		, LLC		Location: Lime Kiln Stack Date: 5/9/23 and 5/10/23 Test Method: 16A, 3A			
			Applicable	e Standard:	10			
		-			@ 10% O2 I tor Informatio			
TRS Monitor	Model:		Thermo 43iC	2	TRS Monite	or Serial # :	11800	090014
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM TRS asSO₂ ppmvd @ 10% O₂	CEM TRS asSO ₂ ppmvd @ 10% O ₃	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)
1	1	05/09/23	11:55	12:55	4.1	3.8	0.3	0.09
1	2	05/09/23	15:02	16:02	4.0	4.0	0.0	0.00
1	3	05/09/23	16:07	17:07	4.2	4.3	-0.1	0.01
1	4	05/10/23	7:39	8:39	4.7	4.7	0.0	0.00
1	5	05/10/23	8:45	9:45	5.0	4.9	0.1	0.01
1	6	05/10/23	9:55	10:55	5.6	4.9	0.7	0.49
1	7	05/10/23	13:06	14:06	4.5	4.2	0.3	0.09
1	8	05/10/23	14:18	15:18	4.3	4.1	0.2	0.04
1	9	05/10/23	15:23	16:23	4.8	4.2	0.6	0.36
				n		Э		
				t(0.975)	2.3			
		Mean R	eference Me			578	RM avg	
				CEM Value		344	CEM avg	
				Differences		100	di	
			Mear	n Difference	0.2	233	d	
		Sum	of Differenc	es Squared	1.090		di ²	
				d Deviation	0.274		sd	
	Confid	ence Coef	ficient 2.5%	Error (1-tail)	0.211		CC	
			Re <u>lativ</u>	e Accuracy	9.	70	RA	

Client:	Billerud	Quinnese	c, LLC		Location: Lime Kiln Stack				
Facility:	Quinne	sec Mill			Date: 5/9/23 and 5/10/23				
Project #:	M2318	04			Test Method:	3A			
				O₂ % (dr	y) RATA				
			С	EM Analyze	r Information				
0	2 Moni	tor/Model:	Thermo	CTL902C		O ₂ Serial # :	1180	570001	
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM O2 % (dry)	CEM O2 % (dry)	(RM-CEM) Difference	(RM-CEM) Difference ²	
0 10,000	Itan				((()))	((a) y)	(di)	(di²)	
1	1	05/09/23	11:55	12:55	4.17	3.72	0.45	0.20	
1	2	05/09/23	15:02	16:02	3.28	3.55	-0.27	0.07	
1	3	05/09/23	16:07	17:07	2.95	3.21	-0.26	0.07	
1	4	05/10/23	7:39	8:39	3.73	4.15	-0.42	0.18	
1	5	05/10/23	8:45	9:45	3.56	3.97	-0.41	0.17	
1	6	05/10/23	9:55	10:55	3.65	3.97	-0.32	0.10	
1	7	05/10/23	13:06	14:06	3.40	3.78	-0.38	0.14	
1	8	05/10/23	14:18	15:18	3.33	3.69	-0.36	0.13	
1	9	05/10/23	15:23	16:23	4.10	4.42	-0.32	0.10	
				n	9)			
				t(0.975)	2.3			·	
		Mean Re	ference Me	thod Value	3.	57	RM avg		
			Mean	CEM Value	3.	83	CEM avg		
			Sum of	Differences	-2.	29	di		
Mean Difference					-0.25		d		
	Sum of Differences Squared					1.17		di ²	
				d Deviation	0.270		sd		
C	Confide	nce Coeffi	icient 2.5% I	Error (1-tail)	0.208		cc		
			Relativ	e Accuracy	12.93 RA				

4.0 CERTIFICATION

Mostardi Platt is pleased to have been of service to Billerud Quinnesec, LLC. If you have any questions regarding this test report, please do not hesitate to contact us at 630-993-2100.

As project manager, I hereby certify that this test report represents a true and accurate summary of emissions test results and the methodologies employed to obtain those results, and the test program was performed in accordance with the methods specified in this test report.

MOSTARDI PLATT

Program Manager

Daniel Kossack

anal

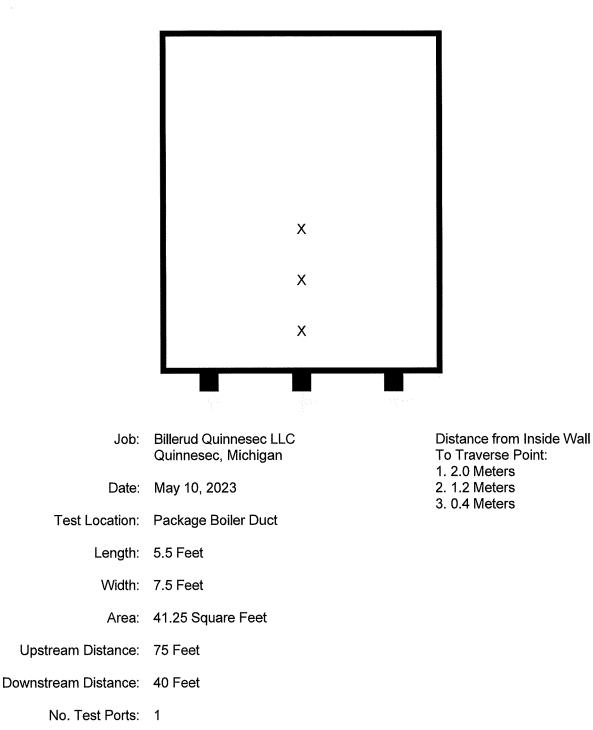
Scott W. Banach

Quality Assurance

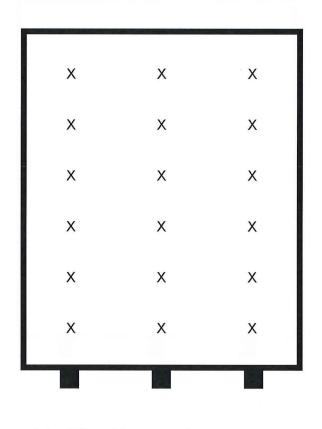
APPENDICES

Appendix A - Test Section Diagrams

THREE POINT GASEOUS TRAVERSE FOR RECTANGULAR DUCTS



EQUAL AREA TRAVERSE FOR RECTANGULAR DUCTS



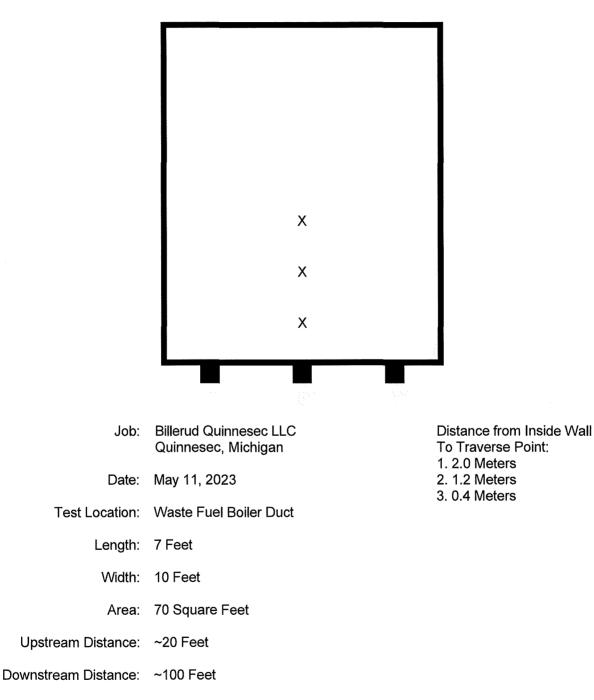
Job: Billerud Quinnesec LLC Quinnesec, Michigan

Date: May 11, 2023

Test Location: Waste Fuel Boiler Duct

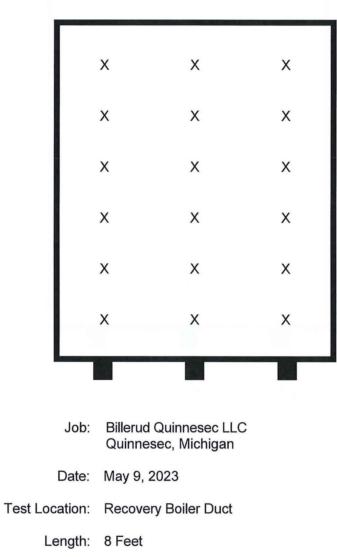
- Length: 7 Feet
- Width: 10 Feet
- Area: 70 Square Feet
- No. Test Ports: 3

THREE POINT GASEOUS TRAVERSE FOR RECTANGULAR DUCTS



No. Test Ports: 1

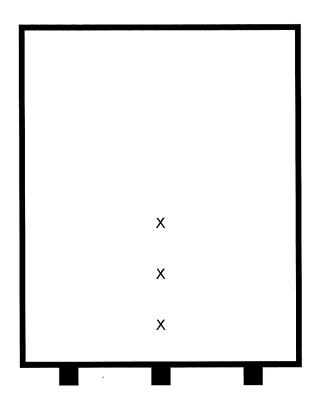
EQUAL AREA TRAVERSE FOR RECTANGULAR DUCTS



Width:	12.25 Feet

- Area: 98 Square Feet
- No. Test Ports: 3

THREE POINT GASEOUS TRAVERSE FOR RECTANGULAR DUCTS



Job: Billerud Quinnesec LLC Quinnesec, Michigan

Date: May 10, 2023

Test Location: Recovery Boiler Duct

Length: 8 Feet

Width: 12.25 Feet

Area: 98 Square Feet

Upstream Distance: ~20 Feet

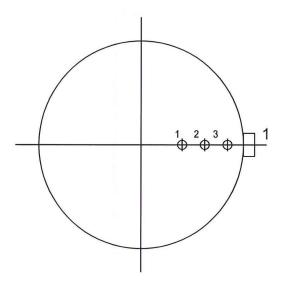
Downstream Distance: ~20 Feet

No. Test Ports: 1

Tests Points per Port: 3

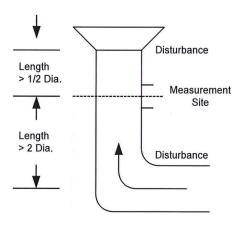
Project No. M231804B Package Fuel Boiler Outlet Duct, Waste Fuel Boiler Outlet Duct, Recovery Fuel Boiler Outlet Duct, and Lime Kiln Stack Distance from Inside Wall To Traverse Point: 1. 2.0 Meters 2. 1.2 Meters 3. 0.4 Meters

THREE POINT GASEOUS TRAVERSE FOR ROUND DUCTS



Job: Billerud Quinnesec LLC Quinnesec, Michigan

- Date: May 9 and 10, 2023
- Test Location: Lime Kiln Stack
- Stack Diameter: 8.0 Feet
 - Stack Area: 50.265 Square Feet
- No. Sample Points: 3
- Upstream Disturbance: Approximately 75 Feet
- Downstream Disturbance Approximately 40 Feet

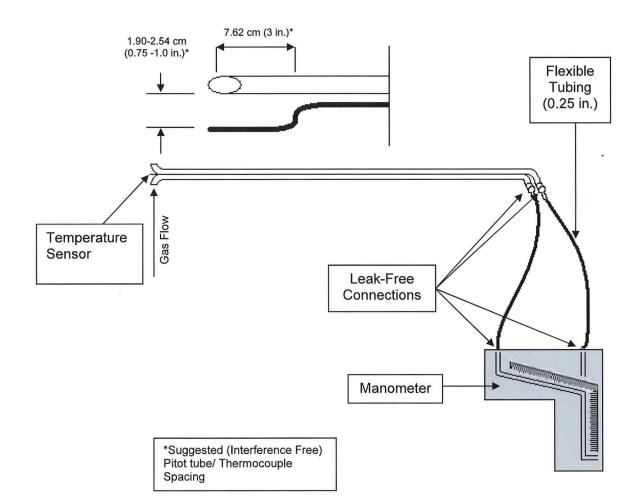


Distance from Inside Wall To Traverse Point: 1. 2.0 Meters

- 2. 1.2 Meters
- 3. 0.4 Meters

Appendix B - Sample Train Diagrams

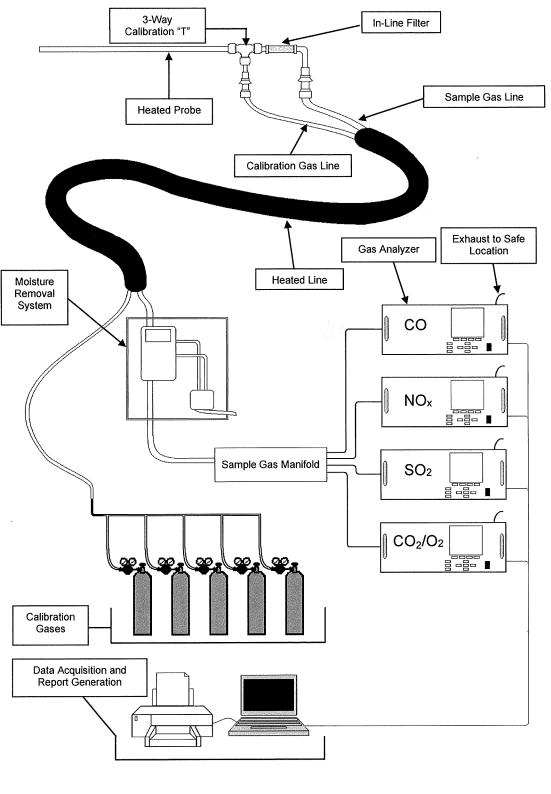
1



USEPA Method 2 – Type S Pitot Tube Manometer Assembly

ATD-001 USEPA Method 2

Project No. M231804B Package Fuel Boiler Outlet Duct, Waste Fuel Boiler Outlet Duct, Recovery Fuel Boiler Outlet Duct, and Lime Kiln Stack 40 of 340

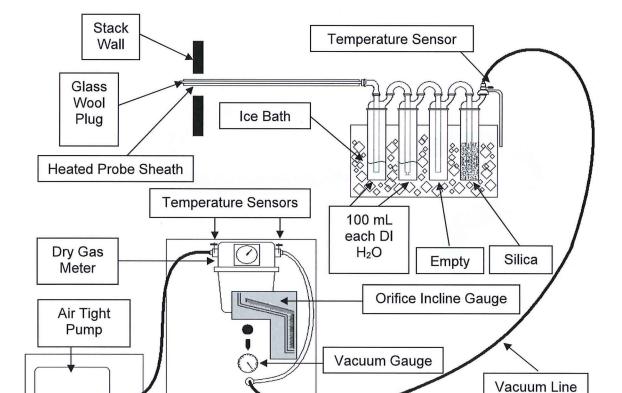


USEPA Methods 3A, 6C, 7E, and 10 Extractive Gaseous Sampling Diagram

ATD-005 Extractive 3A 6C 7E and 10

Project No. M231804B Package Fuel Boiler Outlet Duct, Waste Fuel Boiler Outlet Duct, Recovery Fuel Boiler Outlet Duct, and Lime Kiln Stack 1/1/2021

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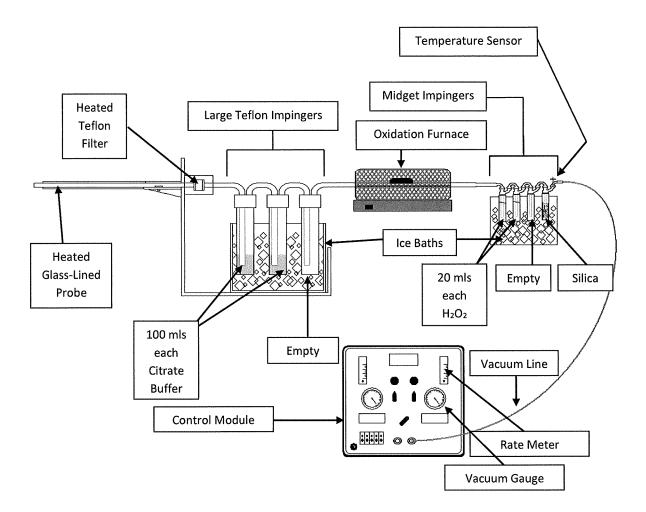
USEPA Method 4- Moisture Content Sample Train Diagram

ATD-032 USEPA Method 4

Project No. M231804B Package Fuel Boiler Outlet Duct, Waste Fuel Boiler Outlet Duct, Recovery Fuel Boiler Outlet Duct, and Lime Kiln Stack Rev. 1.2

1/1/2021

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USEPA Method 16A – Total Reduced Sulfur Sample Train Diagram

Appendix C - Calculation Nomenclature and Formulas