## STATE OF MICHIGAN DEPARTMENT OF ENVIRONMENTAL QUALITY OFFICE OF THE DIRECTOR

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In the matter of administrative proceedings against **DETROIT RENEWABLE POWER**, a corporation organized under the laws of the State of Michigan and doing business at 5700 Russell Street in the City of Detroit, County of Wayne, State of Michigan

AQD No. 6-2017

SRN: M4148

### STIPULATION FOR ENTRY OF FINAL ORDER BY CONSENT

This proceeding resulted from allegations by the Michigan Department of Environmental Quality (MDEQ), Air Quality Division (AQD) against Detroit Renewable Power (Company), a Michigan corporation located at 5700 Russell Street in the City of Detroit, County of Wayne, State of Michigan, with State Registration Number (SRN) M4148. The MDEQ alleges that the Company is in violation of 40 Code of Federal Regulations (CFR) Part 52, Subpart A; 40 CFR Part 60, Subpart Cb, Db & Eb; 40 CFR Part 62 Subpart FFF; and its Renewable Operating Permit (ROP) MI-ROP-M4148-2011a, Table FGBOILERS011-13, Special Conditions 1.1, 1.9 & I.11. Specifically, the MDEQ alleges that the Company has violated air emission limitations for sulfur dioxide, carbon monoxide, and particulate emissions from the Refuse Derived Fuel Fired Boilers No. 11 and No. 12 as cited herein and in Violation Notices dated June 29, 2015, November 9, 2015, December 16, 2015, February 12, 2016, March 4, 2016, March 23, 2016, May 19, 2016, and June 9, 2016. The MDEQ also alleges that the Company failed to properly perform a cylinder gas audit for Refuse Derived Fuel Fired Boilers No. 11, No. 12, and No. 13 and reported a high percentage of continuous emissions monitor downtime during the first and second quarters of 2016 as cited herein and in Violation Notices dated June 9, 2016, September 2, 2016, and October 21, 2016. The Company and MDEQ stipulate to the termination of this proceeding by entry of this Stipulation for Entry of a Final Order by Consent (Consent Order).

The Company and MDEQ stipulate as follows:

1. The Natural Resources and Environmental Protection Act, 1994 PA 451 (Act 451), MCL 324.101 *et seq.* is an act that controls pollution to protect the environment and natural resources in this State.

2. Article II, Pollution Control, Part 55 of Act 451 (Part 55), MCL 324.5501 *et seq.* provides for air pollution control regulations in this State.

3. The MDEQ was created as a principal department within the Executive Branch of the State of Michigan pursuant to Executive Order 2011-1 and has all statutory authority, powers, duties, functions and responsibilities to administer and enforce all provisions of Part 55.

4. The Director of the Michigan Department of Environmental Quality has delegated authority to the Director of the AQD (AQD Director) to enter into this Consent Order.

5. The termination of this matter by a Consent Order pursuant to Section 5528 of Part 55 is proper and acceptable.

6. The Company and the MDEQ agree that the signing of this Consent Order is for settlement purposes only and does not constitute an admission by the Company of any fact or that the law has been violated.

7. This Consent Order becomes effective on the date of execution (effective date of this Consent Order) by the AQD Director.

8. The Company shall achieve compliance with the aforementioned regulations in accordance with the requirements contained in this Consent Order.

### COMPLIANCE PROGRAM AND IMPLEMENTATION SCHEDULE

### 9.A. Flexible Group FGBOILERS011-013 Requirements

1. On and after the effective date of this Consent Order, the Company shall comply with all particulate emission limitations specified in ROP MI-ROP-M4148-2011a, Flexible Group FGBOILERS011-13, or any subsequent permit revision/federal regulation change applicable to this flexible group during the term of this Consent Order.

2. On and after the effective date of this Consent Order, the Company shall comply with the 24-hour carbon monoxide emission limitation specified in ROP MI-ROP-M4148-2011a, Flexible Group FGBOILERS011-13, Emission Limit(s) table 11.a, or any subsequent permit revision/federal regulation change applicable to this flexible group during the term of this Consent Order.

3. On and after the effective date of this Consent Order, the Company shall comply with the 24-hour sulfur dioxide emission limitation specified in ROP MI-ROP-M4148-2011a, Flexible Group FGBOILERS011-13, Emission Limit(s) table 9.a, or any subsequent permit revision/federal regulation change applicable to this flexible group during the term of this Consent Order.

4. On and after the effective date of this Consent Order, the Company shall comply with the 1-hour carbon monoxide emission limitation specified in ROP MI-ROP-M4148-2011a, Flexible Group FGBOILERS011-13, Emission Limit(s) table 11.b, or any subsequent permit revision/federal regulation change applicable to this flexible group during the term of this Consent Order.

9.B. Abnormal Condition Startup/Shutdown Malfunction Abatement Plan

1. On and after the effective date of this Consent Order, the Company shall fully comply with the approved Startup, Shutdown and Malfunction Plan (SSM), dated November 4, 2016 and revisions thereto attached as Exhibit A, incorporated by reference and made an enforceable part of this Consent Order.

2. On and after the effective date of this Consent Order, any acceptable changes or updates to the SSM, as reasonably requested by the Company, shall be promptly submitted to the AQD Detroit Office District Supervisor. The revised SSM shall be attached and become an enforceable part of this Consent Order.

3. On and after the effective date of this Consent Order, the Company shall submit a revised SSM plan if new equipment is installed that requires SSM Plan revision or upon the request from the AQD Detroit Office District Supervisor if AQD has determined that the current version of the SSM plan is not adequate for its stated purposes within 30 days of the installation or request. The revised SSM plan shall take effect upon written notice from the AQD Detroit Office District Supervisor or 60 days after submittal, whichever is earlier.

9.C. Cylinder Gas Audit Requirements

1. On and after the effective date of this Consent Order, the Company shall comply with 40 CFR Part 60 Appendix F.

2. On and after the effective date of this Consent Order, the Company shall maintain cylinder gas certification records onsite and make them available to the AQD upon request.

### GENERAL PROVISIONS

10. This Consent Order in no way affects the Company's responsibility to comply with any other applicable state and federal, or local laws or regulations, including without limitation, any amendments to the federal Clean Air Act, 42 USC 7401 *et seq.*, Act 451, Part 55 or their rules and regulations, or to the State Implementation Plan.

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11. This Consent Order constitutes a civil settlement and satisfaction as to the resolution of the violations specifically addressed herein; however, it does not resolve any criminal action that may result from these same violations.

12. Within thirty (30) days after the effective date of this Consent Order, the Company shall pay to the General Fund of the State of Michigan, in the form of a check made payable to the "State of Michigan" and mailed to the Michigan Department of Environmental Quality, Accounting Services Division, Cashier's Office, P.O. Box 30657, Lansing, Michigan 48909-8157, a settlement amount of \$149,000.00, which includes AQD costs for investigation and enforcement. The total sum of \$149,000.00 shall be made in two (2) payments as follows: a payment of \$74,500.00 shall be paid within thirty (30) days of the effective date of this Consent Order; a final payment of \$74,500.00 shall be made on or before August 1, 2017. To ensure proper credit, all payments made pursuant to this Consent Order shall include the "Payment Identification Number AQD40165" on the front of the check and/or in the cover letter with the payment.

13. On and after the effective date of this Consent Order, if the Company fails to comply with paragraph 9.A.1 of this consent Order, the Company is subject to a stipulated fine of up to \$5,000.00 per violation per day, limited to a maximum of \$40,000.00 per stack testing event. On and after the effective date of this Consent Order, if the Company fails to comply with paragraph 9.A.2 or 9.A.3 of this consent Order, the Company is subject to a stipulated fine as follows:

Fine Per Violation	Total Number of violation notice(s) issued
\$1,000.00	1st through 5th
\$2,000.00	6th through 10th
\$5,000.00	11th and beyond

On and after the effective date of this Consent Order, if the Company fails to comply with paragraph 9.A.4 of this Consent Order for a period of longer than three (3) hours in a single day, the Company is subject to a stipulated fine of up to \$1,000.00 per violation per day. On and after the effective date of this Consent Order, if the Company fails to comply with paragraph 9.B.1, 9.B.2, 9.B.3, 9.B.4, 9.C.1, or 9.C.2 of this Consent Order, the Company is subject to a stipulated fine of up to \$1,000.00 per violation. On and after the effective date of this Consent Order, the Company is subject to a stipulated fine of up to \$1,000.00 per violation. On and after the effective date of this Consent Order, the Company is subject to a stipulated fine of up to \$1,000.00 per violation. On and after the effective date of this Consent Order, if the Company fails to comply with any other provision of this Consent Order, the Company is subject to a stipulated fine of up to \$1,000.00 per violation.

to \$500.00 per violation. The amount of the stipulated fines imposed pursuant to this paragraph shall be within the discretion of the MDEQ. Stipulated fines submitted under this Consent Order shall be by check, payable to the "State of Michigan" within thirty (30) days of written demand and shall be mailed to the Michigan Department of Environmental Quality, Accounting Services Division, Cashier's Office, P.O. Box 30657, Lansing, Michigan 48909-8157. To ensure proper credit, all payments made pursuant to this Consent Order shall include the "Payment Identification Number AQD40165-S" on the front of the check and/or in the cover letter with the payment. Payment of stipulated fines shall not alter or modify in any way the Company's obligation to comply with the terms and conditions of this Consent Order.

14. The AQD, at its discretion, may seek stipulated fines or statutory fines for any violation of this Consent Order which is also a violation of any provision of applicable federal and state law, rule, regulation, permit, or MDEQ administrative order. However, the AQD is precluded from seeking both a stipulated fine under this Consent Order and a statutory fine for the same violation.

15. To ensure timely payment of the settlement amount assessed in paragraph 12 and any stipulated fines assessed pursuant to paragraph 13 of this Consent Order, the Company shall pay an interest penalty to the State of Michigan each time it fails to make a complete or timely payment under this Consent Order. The interest penalty shall be determined at a rate of interest that is equal to one percent (1%) plus the average interest rate paid at auctions of 5-year United States treasury notes during the six months immediately preceding July 1 and January 1, as certified by the state treasurer, compounded annually, using the full increment of amount due as principal, calculated from the due date specified in this Consent Order until the date that delinquent payment is finally paid in full. Payment of an interest penalty by the Company shall be made to the State of Michigan in accordance with paragraph 13 of this Consent Order. Interest payments shall be applied first towards the most overdue amount or outstanding interest penalty owed by the Company before any remaining balance is applied to subsequent payment amount or interest penalty.

16. The Company agrees not to contest the legal basis for the settlement amount assessed pursuant to paragraph 12. The Company also agrees not to contest the legal basis for any stipulated fines assessed pursuant to paragraph 13 of this Consent Order, but reserves the right to dispute in a court of competent jurisdiction the factual basis upon which a demand by MDEQ of stipulated fines is made. In addition, the Company agrees that said fines have not been assessed by the MDEQ pursuant to Section 5529 of Part 55 and therefore are not reviewable under Section 5529 of Part 55.

17. This compliance program is not a variance subject to the 12 month limitation specified in Section 5538 of Part 55.

18. This Consent Order shall remain in full force and effect for a period of at least two (2) years. Thereafter, the Consent Order shall terminate only upon written notice of termination issued by the AQD Director. Prior to issuance of a written notice of termination, the Company shall submit a request, to the AQD Director at the Michigan Department of Environmental Quality, Air Quality Division, P.O. Box 30260, Lansing, Michigan 48909-7760, consisting of a written certification that the Company has fully complied with all the requirements of this Consent Order and has made all payments including all stipulated fines required by this Consent Order. Specifically, this certification shall include: (i) the date of compliance with each provision of the compliance program and the date any payments or stipulated fines were paid; (ii) a statement that all required information has been reported to the AQD Detroit Office District Supervisor; (iii) confirmation that all records required to be maintained pursuant to this Consent Order are being maintained at the facility; and, (iv) such information as may be requested by the AQD Director.

19. In the event Detroit Renewable Power sells or transfers the facility, with SRN M4148, it shall advise any purchaser or transferee of the existence of this Consent Order in connection with such sale or transfer. Within thirty (30) calendar days, the Company shall also notify the AQD Detroit Office Supervisor, in writing, of such sale or transfer, the identity and address of any purchaser or transferee, and confirm the fact that notice of this Consent Order has been given to the purchaser and/or transferee. As a condition of the sale, Detroit Renewable Power must obtain the consent of the purchaser and/or transferee, in writing, to assume all of the obligations of this Consent Order. A copy of that agreement shall be forwarded to the AQD Detroit Office Supervisor within thirty (30) days of assuming the obligations of this Consent Order.

20. Prior to the effective date of this Consent Order and pursuant to the requirements of Sections 5511 and 5528(3) of Part 55, the public was notified of a 30-day public comment period and was provided the opportunity for a public hearing.

21. Section 5530 of Part 55 may serve as a source of authority but not a limitation under which the Consent Order may be enforced. Further, Part 17 of Act 451 and all other applicable laws and any other legal basis or applicable statute may be used to enforce this Consent Order.

22. The Company hereby stipulates that entry of this Consent Order is a result of an action by MDEQ to resolve alleged violations of its facility located at 5700 Russell Street in Detroit, Michigan. The Company further stipulates that it will take all lawful actions necessary to fully comply with this Consent Order, even if the Company files for bankruptcy in the future. The Company will not seek discharge of the settlement amount and any stipulated fines imposed hereunder in any future bankruptcy proceedings, and the Company will take necessary steps to ensure that the settlement amount and any future stipulated fines are not discharged. The Company, during and after any future bankruptcy proceedings, will ensure that the settlement amount and any future stipulated fines remain an obligation to be paid in full by the Company to the extent allowed by applicable bankruptcy law.

The undersigned certifies that he/she is fully authorized by the Company to enter into this Consent Order and to execute and legally bind the Company to it.

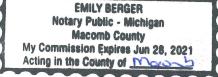
### **DETROIT RENEWABLE POWER**

R INWOOD Print Name and Title \_\_\_\_ Date: <u>6-1-17</u> Signature

The above signatory subscribed and sworn to before me this 1 day of  $30 \sim 20$ ,  $20 \sim 20$ 



Notary Public Signature EMILY BERGER



Approved as to Content:

Lynn Fiedler, Division Director Afr QUALITY DIVISION DEPARTMENT OF ENVIRONMENTAL QUALITY

Dated: 6/19/17

Approved as to Form:

Neil D. Gordon, Section Head ENVIRONMENTAL REGULATION SECTION ENVIRONMENT, NATURAL RESOURCES, AND AGRICULTURE DIVISION DEPARTMENT OF ATTORNEY GENERAL

Dated: June 7, 2017

### FINAL ORDER

The Director of the Air Quality Division having had opportunity to review the Consent Order and having been delegated authority to enter into Consent Orders by the Director of the Michigan Department of Environmental Quality pursuant to the provisions of Part 55 of Act 451 and otherwise being fully advised on the premises,

HAS HEREBY ORDERED that the Consent Order is approved and shall be entered in the record of the MDEQ as a Final Order.

MICHIGAN DEPARTMENT OF ENVIRONMENTAL QUALITY

Lynn Fiedler, Division Director Air Quality Division

Effective Date: <u>Le/19/17</u>

# EXHIBIT A

Abnormal Condition Startup/Shutdown Malfunction Abatement Plan

AQD No. 6-2017

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Detroit Renewable Power		
Startup, Shutdown, Malfunction Plan Ta	able of Documents	
Last Rev. 11/04/16		
Document	Document Number	Last Revised
SSM Plan	AIR-001	10/31/16
Documents below included for reference	е	
Boiler Start-up	SOP-1018	10/31/16
Boiler Shutdown	SOP 1022	11/04/16
Loss of Station Power	SOP 0110	11/04/16
SDA Malfunctions	SOP 0120	10/31/16
Boiler Feed Chute	SOP 0130	10/31/16
Boiler Grate Malfunction	SOP 0140	10/31/16
CO Excursion	SOP 0150	10/31/16
High SO2	SOP 0160	10/31/16
High NOx	SOP 0170	10/31/16
High Opacity	SOP 0180	10/31/16
Preventive Maintenance Schedule	Schedule 0001 SSM-Form-014 SSM-Form-015 SSM-Form-016 SSM-Form-017 SSM-Form-018	10/31/16 11/04/16 11/04/16 11/04/16 11/04/16 11/04/16
Boiler Critical Spare Parts List		11/04/16
AAO Slaker Logs 1-4		11/04/16
AO Grate Logs 1-2		11/04/16
Control Room Log (2 pages)		11/04/16

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	Detroit Renew	vable Energy	
	Document No.: AIR-001	Approval Date: 10/31/2016	D
Startup, Shutdown, and Malfunction Plan	Revision No.: 04 Next Revision Date: 10/25/2017		Page
	Document Custodian: Environmen	ntal, Health & Safety	1 of 5

### **1.0 PURPOSE**

This guideline summarizes the Detroit Renewable Energy's (DRE's) SSM Plan for their facility located at 5700 Russell St. Detroit as required by the conditions of Renewable Operating Permit (ROP) MI-ROP-M4148-2011a. The purpose of this plan is to ensure:

- Units are operated and maintained in a manner consistent with good air pollution control practices and which satisfies the general duty to minimize emissions.
- DRE is prepared to correct malfunctions as soon as practicable to minimize excess emissions of Hazardous Air Pollutants (HAPs).
- Preventative actions are taken to minimize the occurrences of incidents
- Predictive and preventative maintenance operations are conducted

Detroit Renewable Energy (DRE) operates its facility to reduce the frequency of excess emissions. The operating philosophy at DRE is to operate the plant within the permit limits required by the Renewable Operating Permit (ROP). To achieve these goals, the boilers will be operated in the most efficient manner possible, which in turn, will conserve fuel and provide for complete combustion. However, DRE recognizes that exceedances of permit limits may occur which are unavoidable under certain malfunction situations, as well as startup and shutdown of the boilers and associated control equipment. Therefore, the equipment will be operated and maintained in such a manner to minimize the duration and magnitude of these incidents. The operation of the plant will be performed utilizing properly trained and experienced operators.

The primary cause of excess emissions is due to the inherently inconsistent fuel. Municipal solid waste (MSW) is received in all shapes, sizes, and consistencies which can cause equipment wear, breakdown, and pile up of MSW feed in the boilers. DRE works to remedy this potential cause of permit limit exceedances by sorting, shredding and screening the MSW to create a more cohesive fuel, also known as Refuse Derived Fuel (RDF). DRE conducts routine inspections and maintenance of equipment to reduce breakdowns and in the event the feed does pile up, alarms are in place to notify the operators. In addition to proper operation, it is equally important to establish inspection and maintenance procedures that will allow the plant to continue running in an optimum operating condition. These procedures will include regularly scheduled inspections. The quantity and type of spare parts selected for inventory will be based on plant operating experience. Properly trained and experienced plant operators and maintenance personnel will perform the inspections.

Events that occur during Abnormal Condition, Startup, Shutdown, or Malfunction (SSM) have the potential to exceed permit limits. The purpose of this document is to provide a prescribed plan of action to be taken to minimize emissions if one of the events occurs. As long as the steps contained within this Plan and the applicable Standard Operating Procedures (SOPs) are followed, then the excess emissions are not a violation of the standard. Documentation is required for each event to show that the facility did or did not follow the prescribed steps for the event. Note that this document referenced the SOPs for specific actions to excess emission events and startup and shutdown of the boilers. Specific reference to the SOPs is intended to ensure operations personnel are referencing the most accurate and up-to-date SOP. In addition, the SSM plan includes very specific requirements in the event of an SSM event. These steps will be completed in addition to the SOP. These formal steps are listed in the form on page 5 of this document. This form must be filled out for each SSM event that occurs at the facility and maintained for five years. If the steps on page 5 and/or the SOP are not followed then an investigation must be completed to determine why the steps were not followed and measures must be taken to ensure conformance in the future.

#### 2.0 DEFINITIONS

Start-up, shutdown, malfunction, and plan of action are generally defined in Table 1.

Startup, Shutdowns, and Malfunction Plan Doc. No.: AIR-001 Rev. No.: 04 Page 2 of 5

Term	Definition
Start-up	The setting in operation of the affected facility for any purpose. "Start-up" includes starting up from a shutdown caused by a malfunction. The startup period commences when the affected facility begins the continuous burning of municipal solid waste and does not include any warmup period when the affected facility is combusting fossil fuel or other non-municipal solid waste fuel, and no municipal solid waste is being fed to the combustor.
Shutdown	The cessation of operation of an affected facility for any purpose. The shutdown period commences at the time MSW is no longer being continuously fed to the unit. The shutdown period ends and the affected facility is "off line" when the oxygen concentration in the flue gas is sustained at a value greater than or equal to 16%. Note, however, for SO2 and NOx, 40 CFR 60.58b(b)(8) allows a diluent cap of 14%. This option is available for definition of shutdown periods for these limits. When a facility is "off line" it shall not be considered to be operating.
Malfunction	A sudden, infrequent, or not reasonably preventable failure of air pollution control equipment, process equipment, or a process to operate in a normal, or usual manner which causes excess emissions. Failures that are caused in part by poor maintenance or careless operation are not malfunctions. The malfunction period ends at the time in which the unit is back to normal steady state operation, or when the unit has been shut down in response to the malfunction. Potential malfunctions may include, but not limited to, stoker grate failure, fuel feed chute failure, or auger issues.
Plan of Action	Each Startup, Shutdown and Malfunction event has a prescribed list of actions that must be taken when they occur. The actions are consistent with the units' SOPs, although the SOPs are not incorporated into this document. Follow SOPs IMMEDIATELY upon SSM event. SOPs will specifically address the corrective actions to be taken when issues such as stoker grate failure, fuel feed chute failure, auger issues, and other malfunctions that may occur. These procedures are intentionally left out of this Plan to ensure the most current version of the SOP is being used by operations personnel.

### 3.0 SCOPE

This guideline has been written to satisfy permit requirements for Boiler #11, #12, and #13 during periods of start-up, shutdown, and malfunction.

Table 2

Area	Control Device	Continuous Monitoring System
Boilers #11, #12,	Combustion Controls	CO and/or O2 CEMS
and #13	Scrubber	SO2 CEMS

### 4.0 PROCEDURE

Table 3 outlines some basic responses to SSM events however the SOP should be followed for specific instructions. The Operator, Supervisor, or other designee must complete the SSM Form at the end of this procedure for each incident. The completed checklist must be filled out completely and returned to the Environmental Manager by the next business day. SSM events will be investigated to determine what, if any, preventative measures can be put in place to minimize the occurrences. Note the current SOPs are written to minimize the occurrences of SSM events.

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Startup, Shutdowns, and Malfunction Plan

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Tab	e 3	- P	lan	of	Action

SSM Scenario	Response Action(s)
Boiler Start-up SOP-1018 (Replaces SOP- 0101-01.01	To the extent possible, maintain good combustion characteristics while the boiler is being brought on-line. Verify the following: - Oil fire in boiler - Lime addition available/started - Baghouse in service - Water wall temperature above 200 <sup>®</sup> F - Baghouse inlet above 250 <sup>®</sup> F - Boiler bank inlet temperature above 850 <sup>®</sup> F - Boiler furnace temperature 1800 <sup>®</sup> F, 1 second above the grate level
Boiler Shutdown SOP-1022 (Replaces SOP- 0101-01.01)	To the extent possible, maintain good combustion characteristics while the boiler is being brought down. Verify the following: - Operation of all soot blowers prior to reduction of steam flow - Reduction of RDF firing rate - Ignitors and oil guns in service at 250k lb/hr - Maintain 1800°F furnace temperature as load is being lowered
Boiler Upset or Malfunction SOPs 0110, 0120, 0130, 0131, 0140, 0150, 0160, 0170, 0180)	<ul> <li>To the extent possible, maintain good combustion characteristics while the boiler is being brought on-line.</li> <li>Potential actions to be taken depending on the issue: <ul> <li>Adjust undergrate air dampers to maintain proper combustion temperature, utilize ignitors and oil guns as needed</li> <li>Identify plugged chute and clear it</li> <li>Adjust TOFA</li> <li>Adjust the grate speed and/or auger bias</li> <li>Maintain even combustion bed thickness</li> <li>Manually adjust dampers</li> <li>Secure RDF feed and allow fuel on grates to completely combust</li> <li>Ensure proper lime slurry flow</li> <li>Reduce exit flue gas air temperature</li> </ul> </li> </ul>

### 5.0 CONTINUOUS EMISSION MONITORING SYSTEMS (CEMS)

Procedures to address failures of the CEMS are not included in this document.

### 6.0 RECORDKEEPING AND REPORTING

Specific recordkeeping and reporting is required to comply with the ROP and federal regulations during an SSM event.

a. Recordkeeping

Complete a Start-up Shutdown Malfunction Checklist (found on page 5 of this document) for each SSM event. Additional records, such as CEMS data, may be included as required. When the actions taken during an SSM event are consistent with the SSM plan, records will be kept that demonstrate that the procedures in the plan were followed.

The emission guideline standards do not apply during periods of startup and shutdown. The duration of the startup/shutdown period is limited to 3 hours per occurrence 40 CFR 60.58b(a)(1). During periods of startup, shutdown, or malfunction, monitoring data shall be dismissed or excluded from compliance calculations, but shall be recorded and reported.

Additionally, if a loss of boiler water level control (e.g., boiler waterwall tube failure) or loss of combustion air control (e.g., loss of combustion fan, induced draft fan, combustion grate bar failure) is determined to be a malfunction, the duration of the malfunction period is limited to 15 hours per occurrence for Carbon Monoxide (40 CFR 60.58b(a)(1)(iii)). During such periods of malfunction,

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monitoring data shall be dismissed or excluded from compliance calculations, but shall be recorded and reported.

A signed confirmation that the procedures in this SSM plan were followed will be included in the semiannual ROP certification report. If actions taken during an SSM are not consistent with the plan, the actions taken for that event will be reported in the semi-annual ROP certification report. If this SSM plan fails to address or inadequately addresses an event that meets the characteristics of a malfunction, the plan will be revised within 45 days after the event.

This SSM plan will be maintained for the operating life of the units listed in this document, unless the units are no longer subject to SSM plan requirements. If the plan is revised, the previous (superseded) version will be retained for five years. Any updates to the facility's SSM plan will be submitted to MDEQ for approval. If submitted changes have not been rejected within ninety (90) days, they shall be deemed approved per the ROP.

#### b. Reporting

The ROP section A. General Conditions number 25 requires notice of abnormal condition, start-up, shutdown, or malfunction that results in emissions of a hazardous or toxic air pollutant which continue for more than one hour in excess of any applicable standard or limitation, or emissions of any air contaminant continuing for more than two hours in excess of an applicable standard or limitation, as required in Rule 912, to the appropriate AQD District Office. The electronic or telephonic notice shall be provided no later than two business days after the start-up, shutdown, or discovery of the abnormal conditions or malfunction. Written reports, if required under Rule 912, must be submitted to the appropriate AQD District Supervisor within 10 days after the start-up or shutdown occurred, within 10 days after the abnormal conditions or malfunction, whichever is first. The written reports shall include all of the information required in Rule 912(5) and shall be certified by a responsible official in a manner consistent with the CAA.

#### 7.0 DEFINITIONS

7.1 AQD - Air Quality Division

- 7.2 CEMS Continuous Emission Monitoring System
- 7.3 HAP Hazardous Air Pollutant
- 7.4 SSM Start-up, Shutdown, Malfunction

#### **8.0 REFERENCES**

8.1 40 CFR Part 60, Subpart Eb (§60.58b)

#### 9.0 ATTACHMENTS

9.1 Start-up, Shutdown, Malfunction Checklist (Page 5 of this document)

Revision number	Description of change	Written by	Checked by	Effective date
01	Original procedure	TLP	DD	05/06/2016
02	Original procedure – changes per MDEQ	TLP	DD	09/01/2016
03	Original procedure – minor wording changes	TLP	DD	10/25/2016
04	Added references to SOPs	DGD	RS	10/31/2016

#### 10.0 Revision History

When a start-up, shutdow         this checklist and sut         a. Event type:         Description         Malfunction (unplanned)         b. Equipment affected:         Description         Boiler #11         c. Event Date/Time:         Malfunction Start date:         Malfunction End date:         Start-up Start date:         Start-up End date:	Detroit Renewabl	nt occurs, the Supervisor mu ental Manager by the next b	ust comple usiness da			
When a start-up, shutdow this checklist and sut a. Event type: Malfunction (unplanned) b. Equipment affected: Boiler #11 c. Event Date/Time: Malfunction Start date: Malfunction End date: Start-up Start date: Start-up End date:	vn, or malfunction even omit it to the Environm Port I – Genen Distart-up	nt occurs, the Supervisor mu ental Manager by the next be al information	usiness da			
Malfunction (unplanned)  Description (unplanned)  Description affected: Boiler #11  C. Event Date/Time: Malfunction Start date: Malfunction End date: Start-up Start date: Start-up End date:	Start-up	🗆 Shutdow	n			
☐ Malfunction (unplanned) <b>b. Equipment affected:</b> ☐ Boiler #11 <b>c. Event Date/Time:</b> Malfunction Start date: Malfunction End date: Start-up Start date: Start-up End date:	A Low and the second		n			
Malfunction (unplanned)  Description (unplanned)  Description affected: Boiler #11  C. Event Date/Time: Malfunction Start date: Malfunction End date: Start-up Start date: Start-up End date:	A Low and the second		n			
b. Equipment affected: Boiler #11 C. Event Date/Time: Malfunction Start date: Malfunction End date: Start-up Start date: Start-up End date:	A Low and the second	Boiler #1				
Boiler #11 C. Event Date/Time: Malfunction Start date: Malfunction End date: Start-up Start date: Start-up End date:	Boiler #12	Boiler #1				
Malfunction Start date: Malfunction End date: Start-up Start date: Start-up End date:			3			
Malfunction End date: Start-up Start date: Start-up End date:						
Start-up Start date: Start-up End date:		Malfunction Start time:			-	
Start-up End date:		Malfunction End time:				
		Start-up Start time:				
		Start-up End time:		_		
Shutdown Start date:		Shutdown Start time:				
Shutdown End date: d. Reason for Shutdown or Malf		Shutdown End time:			_	
a. Boiler (must answer all): Did we achieve/maintain good combust Did we verify that there is oil ignited in Did we verify the lime addition system Did we verify the baghouse is operating Did we ensure the water wall temperatu Did we ensure the baghouse inlet tempe	the boiler? is operating correctly? g correctly? ire is above 200°F?	on/long as possible?	1 1 1 1	Yes Yes Yes Yes	No     No	
Did we ensure the boiler bank inlet temp					No No	
Did we ensure the boiler furnace tempe		2010	1	Yes	No No	
Did we operate all soot blowers prior to		(for shutdown/malfunction only	/)? [	Yes	No No	
Did we reduce the RDF firing rate (for	shutdown/malfunction on	ıly)?	1	Yes	No No	0 N//
Did we introduce the ignitors and oil gu			iiy).		No No	
Did we maintain 1800°F furnace tempe					No No	0 N//
Did we follow the appropriate Standard	Operating Procedures (S	SOPs)? (list them below)		Yes	□ No	
SOP(s) followed:						
	Part III -	- Details				
a. Provide details for the questions	above and a descriptio	n of any corrective actions pl	anned/tak	en (co	ntinu	e on
back if there is not enough space):						
	is report was submitte	49	☐ Yes			
Was incident on-going at the time th			□ Yes			
	manufiction in comor					
Was incident on-going at the time the Were all actions taken to correct the Print name below:	Sign nam			Date		

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# Boiler Startup Standard Operating Procedure SOP-1018

### 1.0 Purpose:

To bring Steam boiler from a cold or hot start to full load operation in conjunction with other Steam Generators or Turbine/Generator.

### 2.0 Scope:

Detroit Renewable Power - Power Block.

### 3.0 Responsibilities:

Department Manager or designee is responsible for implementing and maintaining this procedure.

Department Supervisor(s) and Control Room operators (CRO) are responsible for adhering to this procedure.

- 3.1 Power Block Supervisor gives CRO permission to distribute pre-operational check sheets
  - Appendix 1Turbine Operator Start Up Check ListAppendix 2Grate Operator Start Up Check ListAppendix 3Ash Operator Start Up Check ListAppendix 4Slaker Operator Start Up Check ListAppendix 5Auger Operator Start Up Check ListAppendix 6Maintenance Start Up Check ListAppendix 7E & I Start Up Check ListAppendix 8CEMS Start Up Check List

### 4.0 Deleted

### 5.0 Standard Operating Procedure Steps:

### 5.1 PREREQUISITES:

5.2 Cooling Tower Valve alignment as required by seasonal conditions of ambient air temperature.

5.2.1 Wet Mode5.2.2 Wet I Dry Mode5.2.3 Dry Mode

- 5.3 Circulating Water System in service.
- 5.4 Closed Cooling Water System in service.

Exhibit A

- 5.5 Service Air System in Service supplying 80-100 psi.
- 5.6 Instrument Air System in Service supplying 80-100 psi.
- 5.7 Service Water System in Service supplying 80-100 psi.
- 5.8 Availability of demineralized water and make up storage water supply (fifteen feet in both the demineralized water and condensate storage tanks).
- 5.9 Availability of #2 Fuel Oil and RDF.
- 5.10 Availability of Pebble Lime for Slaker operation.
- 5.11 Check Clearance Log for Active Tag Outs.
- 5.12 Condensate System in service.
  - 5.12.1. Condensate Hot well at normal operating level.
  - 5.12.2. Deaerator at normal operating level.
- 5.13 PREPARING STEAM GENERATOR FOR LIGHT-OFF:
- 5.14 Establish communications with Boiler Operator to prepare boiler for startup.
- 5.15 Verify all boiler vents and drains are in their start-up alignment positions.
  - 5.15.1 Secondary super heater outlet vents open.
  - 5.15.2 Primary super heater outlet vents open.
  - 5.15.3 Intermediate Crossover vents open.
  - 5.15.4 Align main and non-return valves into open position.
- 5.16 Verify bag house compartment dampers are operational and aligned for startup.
  - 5.16.1 Compartments A, B, F & G "on line".
  - 5.16.2 Compartments H, J, K, C, D, E "isolated".
  - 5.16.3 The compartment inlet and outlet dampers should fail "open" on loss of power or air.
  - 5.16.4 Bypass dampers "closed".
  - 5.16.5 The bypass dampers are "welded" and blocked closed.
  - 5.16.6 All interlocks which could result in automatic operation of the bypass damper have been eliminated.
- 5.17 Verify drum level is at a -2" below normal.
- 5.18 Start ID fan.
  - 5.18.1 Perform prestart inspections.
  - 5.18.2 Perform running inspections.
  - 5.18.3 Decrease furnace pressure to -0.05 by opening ID fan damper. Place damper in Auto.

J.17 Statt Dial	5.19	Start	FD	fan
-----------------	------	-------	----	-----

- 5.19.1 Perform prestart inspections.
- 5.19.2 Perform running inspections.
- 5.19.3 Increase air heater outlet pressure to 4-7" w.g. and place damper in Auto

### 5.20 Purge boiler.

- 5.20.1 Place wind box dampers at or above 93% open.
- 5.20.2 Ensure O.F.A. damper are closed.
- 5.20.3 Start purge, air flow >30%.
- 5.20.4 When purge is complete reset MFR.

### 5.21 Boiler Light Off:

5.21.1 Ensure an operator is on station to observe light off and check for fuel leaks at the ignitors.

5.21.2Initiate ignitor light off and record time in log.

5.22 If desired, place oil guns in service:

5.22.1 Ensure an operator is on station to observe light off and check for fuel leaks at the Oil Guns

5.22.2 Adjust wind box dampers to 8% open.

5.22.3 Initiate oil gun light off

- 5.23 Perform Oil Gun/ Ignitor Interlock Test
- 5.24 Adjust firing rate to ensure that warm-up rates are not exceeded.
  - 5.24.1 Gas exit temperatures not to exceed 900° F.
  - 5.24.2 Saturated steam temperature rise not to exceed 100° F.
- 5.25 As pressure increases throttle vents and drains. Do not close secondary super heater outlet vent until Electromatic Relief Valve (ERV) is open to ensure adequate flow through Super heater.
- 5.26 At 25 psi perform the following
  5.26.1 Close drum Vent
  5.26.2 Close Intermediate Crossover vents
  5.26.3 Open Electromatic Relief Valve (ERV)
  5.26.4 Close Secondary super heater outlet vents.
- 5.27 Install SDA Spray Machine IAW SOP 1029

Exhibit A

5.28	When drum pressure reaches 200 psi, blow down the:
	<ul><li>5.28.1 Gage glasses</li><li>5.28.2 Water columns</li><li>5.28.3 Remote level indicators</li></ul>
5.29	When Water level no longer increases due to swelling align feedwater start-up Valve for use up to 148,000 lbs/hour
5.30	Roll turbine generator as soon as minimum steam temperature and pressure are reached.
	<ul><li>5.31.1 Consult turbine start up chart.</li><li>5.31.2 Omit this step if process steam line is to be placed into service first.</li></ul>
5.31	Turbine Start-up valve alignment. Go to step 5.69 if Turbine is in service.
5.32	Steam generator outlet free blows.
5.33	Main stream line drains to blow down tank.
	<ul><li>5.34.1 Verify drains alignment to blow down tank.</li><li>5.34.2 Open SGG-BV-23 and SGG-BV-24.</li></ul>
5.34	Open turbine isolation valve SGG-BV-25.
5.35	Open steam seal isolation valves.
5.36	Verify EHC system is in service.
	5.36.1 Check auto starts on pumps.
5.37	Verify turbine lube oil system is in service.
	5.37.1 Check auto starts on pumps.
5.38	Reset turbine stop valves by.
	<ul><li>5.39.1 Test turbine stop valves by tripping and resetting several times.</li><li>5.39.2 Allow turbine chest to warm up.</li></ul>
5.39	Place turbine on turning gear.
	5.40.1 Four hour minimum when taking off turning gear before turbine can be rolled.
5.40	Startup turbine generator following General Electric instructions.
	5.41.1 GEL-81479 and GEK-96801.
5.41	Process Steam Line Warm-up and Operation:
	Page 4 of 26

5.42 Notify Detroit Edison Beacon Heating Plant by phone that the process steam line is being warmed up. Beacon control room- 963-3707. Shift supervisor's office- 963-3287.

Make sure that we call the following entities when the turbine generator is coming online.

Michigan Electric Coordinated Systems Balancing Authority: Call this number first > (248) 380-2932 or (248) 380-2931

Midwest Independent Transmission System Operator Reliability Coordinator: (317) 249-5030

ITC Transmission Transmission Operators Control Room: (248) 380-2903

- 5.43 Valve TEG-BV-14 and bypass BV-3007 closed.
- 5.44 Check level switches LS-40, and LS-26 is valved in and operational.
- 5.45 Check flow transmitters PT-29, PT-7, PT-8, and PT-10 are valved in and operational.
- 5.46 Check flow transmitters FT-82, FT-87, and FT-81 are valved and operational.
- 5.47 Check extraction traps and drains 1-603, 5-603, 7-603, 9-603, 10-603, and 4-603 are valved and operational.
- 5.48 Open steam line drain in metering pit.
- 5.49 Open isolation valves TEG-BV-10 and TEG-BV-20.

5.49.1 Stroke ACV-6 prior to opening BV-1 0.

- 5.50 Open desuperheater spray isolation valves.
- 5.51 Open turbine bypass isolation valves.

5.51.1 Stroke SGG-ACV-18 prior to opening valves.
5.51.2 SGG-BV-16.
5.51.3 SGG-BV-17.
5.51.4 SGG-BV-19.

5.52 Open TEG-MBV-13 process steam line isolation valve (this valve closes automatically under the following conditions):

5.52.1 Outlet temperature 520° F for 30 seconds.

5.52.2 Outlet temperature of 550° F instantly.

5.52.3 Outlet drains pot level high.

5.53 Crack open SGG-ACV-18 until flow is established (Manual operation at this time is 3% - 5% open)

Exhibit A

	5.54.1 Automatically closes when TEG-MBV-13 trips closed.
5.54	Verify process steam dump valve TEG-ACV-6 to the condenser is operational and in manual control at 20% open.
	5.54.1 Automatically opens to 20% when steam flow is below 60 klbh.
5.55	Allow the line to warm slowly, making checks on all drains often.
5.56	Raise steam pressure and temperature as drain become free of condensate.
5.57	As the steam temperature reaches 400 F places the attemperator in service using ACV-32.
5.58	When temperature is stable place in automatic and slowly raises set point to 460 f.
5.59	Raise steam pressure to 200 PSI.
5.60	Check steam line drains for condensate.
5.61	Once drains are dry DECO is to be notified to witness steam quality.
5.62	When contacted by DECO that steam quality has been accepted, note time and contact person in the Shift Supervisor log.
	5.62.1 Ensure that Beacon Heating supervisor has been notified.
5.63	Start opening TEG-BV-14 bypass BV-3007 valve.
	<ul><li>5.63.1 Equalize line pressure acrossBV-14 before opening valve.</li><li>5.63.2 Drain valve in metering pit can be closed at this time.</li></ul>
5.64	Slowly open BV-14.
5.65	Continue to open ACV-18 until export steam flow is above 80 klbh and flow is stable.
5.66	Slowly start closing ACV-6 and place into automatic when fully closed.
	5.66.1 Manual closing operation is over ridden if export flow is below 60 klbh m1mmum.
5.67	ACV-18 can now be place into automatic.
5.68	Turbine generator can 'now be started or placed into turbine extraction flow if already service.
5.69	RDF Firing Pre-requisitions for Start-up:
	<ul> <li>5.70.1 Oil Fires is boiler.</li> <li>5.70.2 Lime addition available.</li> <li>5.70.3 Bag house in service.</li> <li>5.70.4 Water wall temperature above 200 F.</li> </ul>
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5.70.5 Bag house inlet above 250 F. 5.70.6 Boiler bank inlet temperature above 850 F. 5.70.7 Boiler furnace temperature 1800 F, 1 second above the grate level. 5.71 Start fabric filter reverse air fan when the fabric filter outlet temperature reaches 230 F. 5.71.1. Reverse air for cleaning bag house compartments. 5.72 Place atomizer feed control in auto and adjusts until an outlet temperature of 280 F is obtained. 5.72.1 Lime slurry feed for S02. 5.72.2 Dilution water feed for temperature control 5.73 Continue firing the boiler on fuel oil until an SDA inlet temperature of 280 F is obtained. 5.74 Initiate solid fuel firing and place remaining bag house compartments used during Start up. 5.74.1 First 4 compartments are sacrificial compartments used during start-up. 5.74.2 Furnace temperature above 1800 F. 5.74.3 Start RDF feed to metering bin. 5.74.5 Start PDA fan. 5.74.6 Start augers. 5.75 Remove oil fires when the following conditions are met: 5.76.1 Steam flow above 150 klbh for over five minutes. 5.76.2 Auger speed above 15%. 5.76.3 Furnace temperature above 1800 F. 5.77 Place combustion control loops in auto: 5.77.1 Under grate air in local/auto. 5.77.2 Auger control in auto. 5.77.3 Steam flow master at 0% output place in auto. 5.77.4 Under grate air in remote/auto. 5.77.5 Feed water in 3-element control above 100 klbh. 5.77.6 Adjust fuel to air ratio by placing bias in under grate and or auger master. 5.77.7 Put desuperheaters in Auto. 5.78 Completed Start Up check sheets appendix 1-9 turned attached to completed Start Up procedure and returned to Shift Supervisor. 5.79 Shift Supervisor retains Start Up check sheets appendix 1-9 along with completed Start Up procedure to review according to continuous improvement policies.

RDF Boiler Start-Up Appendix 1 Turbine Operator Start Up Check List	0
Building Roof	<b>Operator Initials</b>
Verify vent is closed on Steam Supply to Spray Water Condenser expansion loop	
8th Floor Boiler Roof	
Verify the following:	
Check Drum Pressure sensor supply root valve open (at drum vent)	-
Check Soot Blowing Steam Supply valve closed	
Verify air supply to Sootblowing Steam Supply valve ACV open	
Open High Point valves (guarding and blowing)	
Open Superheater intermediate vent valves (guarding and blowing)	L
Check ERV isolation valve open	
Check ERV air supply aligned	
Check Superheater outlet safety valve gag is removed	
Check free blow drain closed (Between Main Steam Stop and Main Steam Automatic Non-return)	x:
Open Main Steam Stop valve	
Open Main Steam Automatic Non-return valve	
North side of Boiler	
Verify the following:	
Check the Economizer vent valves closed (guarding and blowing)	
Check Chemical Feed supply valves open (2 block valves)	
Check Chemical Feed to Steam Drum valves open (2 block valves)	
Check FWA PT supply valves open (2 block valves)	
Check feedwater line drains are closed	
Page 8 of 26	

(From the Economizer outlet to the Feedwater ACVs)	
Check the Spray Water Condenser drains closed	
(2 valves on each drain)	
Feedwater Start up ACV Outlet valve open	
Air supply aligned	
North side of Steam Drum	
Check Drum Level Transmitter Upper and Lower root valves open (From Steam Drum)	
Check Continues Blow Down Root valve closed	
Check CBD valve closed	
Check Water Column upper and lower isolation valves open	
Check Gauge Glass upper and lower isolation valves open	
Check Water Column drain root valve open	
Check Gauge Glass drain root valve open	
Open Primary Superheater drain (2 valves)	
Open Secondary Superheater drain (2 valves)	
Verify Steam Drum door is secure	
Verify the Steam Drum safety valve gag has been removed	
West side of Boiler	
Check Main Stream Flow Transmitter root valve is open (on Main Steam Line)	
Verify Penthouse door is in place	
South side of Steam Drum	
Verify the follow on the Desuperheater ACV station:	
Inlet valve open	
Outlet valve open	

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Air supply	
Vent/drain closed	
Verify the Steam Drum south door in place	
Verify the Steam Drum Safety Valve gags have been remove (2 safety valves)	
Check Water Column upper and lower isolation valves open	
Check Gauge Glass upper and lower isolation valves open	
Check Water Column drain root valve open	
Check Gauge Glass drain root valve open	
Check Eye High upper and lower isolation valves open	
Check Eye High drain root valve open	
Check the Sootblowing Wizard pressure sensing line root valve line is open	
Verify the air supply to the Sootblowing Wizard	
8th floor East side of Boiler at TAH	
Verify the Upper TAH door is on (Gas side)	
7 ½ Floor North side of Boiler	
Check Continuous Blow Down to Flash Tank isolation valve closed	
7th floor North	
Check IR camera in place (mounted in SH Door)	
Verify Air supply to IR camera	
Verify Superheater access doors in place (3 doors)	
Verify Gen Bank "crotch" access door in place	
7th floor East side of Boiler	
Verify TAH doors in place (5 doors)	
6th floor North side of Boiler	
Verify Economizer inlet door in place	

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# Exhibit A

Verify North Mud Drum door in secure	
Verify Dance Floor access door in place (Note: this door is on the South side for unit 12 and Unit 13)	
6th Floor West side of Boiler	
Verify inspection port doors closed (4 doors)	
At the furnace camera station verify the following:	
Purge Air supply valve open	·
Cooling air supply aligned and air present	
Check insertion control air supply aligned and air present	
Check IR camera air supply root valve open	
6th Floor South of Boiler	
Verify South Mud drum door secure	
5th Floor North side of Boiler	
Check Economizer drain closed (2 valves)	
Check Sparging Steam to Economizer inlet isolated (2 valves)	
Check North Mud Drum Blowdown valves closed (2 valves)	
Verify dance floor beams retracted (7 beams)	
Verify beam penetration doors closed (7 doors)	
5th Floor West of Boiler	· ·
Verify inspection doors closed (7 doors)	
5th Floor East of Boiler	
Verify Economizer doors in place (4 doors)	
Verify TAH doors in place (4 doors)	
4th Floor North of Boiler	
Verify Economizer Hopper inspection door in place	

## 4th Floor South of Boiler

Verify Econ/TAH cross over door in place (Note: this door is on the North side on Unit 12 and Unit 13)

## **Ground Floor 4160v Room**

Check closed FD high and low speed breaks closed

Check Closed ID fan breaker

Appendix 2 Unit Start Up Grate Operator Walk Down	<b>Operator's Initials</b>
Verify the following at each:	
Ring wall drains closed Sparging Steam closed Igniter air aligned Drum pressure gage aligned Condensate fill closed	
Verify the following at each:	
Start SSC Check hyd unit gages No leaks on Hyd. Unit Check for bad flights Check clinker switch Check vibrator underneath SSC (underneath SSC incline)	
Verify the following at each:	
Grate doors closed, (use steel wool to seal gaps if possible) Grate glass cleaned or replace Start Grates Check oil level Check speed Check limit torque setting Check Back stops Check Sifting hopper from grate level Inspect grate bars as they rotate around Check SSC from grate level hoppers	
Verify the following at each:	
Start all Sifting Screws Check trough and Flights on screw Check bearing, Chain and Chain guard (grease if needed) Open & closed then set dampers, proof of operation	y
Verify the following at each:	
SSC seal and service water aligned Seal trough filled	
Verify the following at each:	
Start Sifting hopper screw Check shaft for rotation	
Page 13 of 26	

OFA operation, stroke damper UFA operation, Stroke damper North UGD, Stroke damper South UGD, Stroke damper

Appendix 3 Unit Start Up	<b>Operator's Initials</b>
Ash Operator Walk Down Baghouse Penthouse	
Verify the following at each Baghouse Compart damper set:	
Air supply to Outlet damper open Air supply to Reverse Air damper open Air supply to Sonic Air Horn open Inline lubricator oil level 1/2-3/4 Inline moisture separator drained	
Verify the following at the RA Recirc damper (near F compartment):	
Air supply to RA Recirc. damper open Inline lubricator oil level Inline moisture separator drained Baghouse upper catwalk	
Verify the following at each of the Baghouse compartments:	
Both upper doors are closed tight	
Verify the air supply to the Reverse Air Fan inlet damper:	
Baghouse lower catwalk	
Verify the following at each of the Baghouse compartments:	
Both lower doors are closed tight Inside Baghouse Hopper area On catwalk	
Verify the following at each of the Baghouse hopper:	
Air supply to Inlet damper Inline lubricator oil level Inline moisture separator drained On ground floor	
Verify the following at each of the Baghouse hopper:	
D Door is closed tight Poke hole cap in place Plate covers in place (upper and lower)	
Page 15 of 26	

Air supply to double dumps open (upper and lower) ID fan	
Verify the follow at the fan OB bearing:	
Oil level ECB inlet valve open ECB outlet valve open	
Verify the follow at the fan IB bearing:	
Oil level ECB inlet valve open ECB outlet valve open	
Verify the ID Fan inspection door is in place	. <u></u> ,
ID fan controller: Verify the damper controller air supply is aligned and >75psi Verify the damper controller is in automatic with the air cylinder needle valve closed	

If the damper is not in automatic, contact the Control Room to coordinate placing the ID fan into automatic.

FD fan Verify the follow at the fan OB bearing:

Oil level ECB inlet valve open ECB outlet valve open		
Verify the follow at the fan IB bearing:		
Oil level ECB inlet valve open ECB outlet valve open Verify the FD Fan inspection door is in place		
FD fan controller:		

If the damper is not in automatic, contact the Control Room to coordinate placing the FD fan into automatic.

Pugmill MCC building

Verify the following for each of the Baghouse hoppers:

Hopper heater breaker is closed Hopper vibrator breaker is closed

TAH hopper room

Verify the following at the TAH hopper:

D Door is closed tight Poke hole cap in place Platco covers in place (upper and lower) Air supply to double dumps open (upper and lower)

	(e)
Appendix 4 Unit Start Up	Operator's Initials
Slaker Operator Walk Down List 8Th Floor SDA Penthouse	
Verify a clean Spray Machine is available for service	
Spray Machine lube oil reservoir: Verify oil temp>80 deg deg F. If low- turn on/up lube oil heater	
Verify Lube oil tank level is sufficient	
Verify Slurry strainer is clean	
Verify Dilution Water head tank is overflowing	
Verify Dilution Water control valve is in neutral position	
Verify isolation valve between the Dilution Water head tank and control valve is closed	
Verify Slurry head tank is overflowing	
Verify Slurry control valve is in neutral position	
Verify isolation valve between Slurry head tank and control valve is closed	
Verify the SDA inlet door is in place (under SDA floor)	
Verify the SDA midlevel door is in place	
Verify the SDA outlet door is in place	
Ground floor Pugmill MCC	
Verify the Spray Machine breaker is closed	
Verify the Spray Machine lube oil break is closed	

Appendix 5 Unit Start Up	<b>Operator's Initials</b>
Auger Operator Walk Down	
Verify the following at each:	
6 <sup>th</sup>	
Visually inspect I-bolt to distribution spout Check bearing for distribution spout	
$5^{ m th}$	
Check Hydraulic lines to distribution spout Check Hydraulic motor and gages Check camera and housing	
4 <sup>th</sup>	
Check distribution spout travel Check Auger flights Check Auger pull cord Check auger drives and idler, valves open Check auger dischargebearing, speed sensor, E- Stop Check motor, gages and oil reservoir and cooling water Check auto/ hand switch and control power	
3rd	
Check economizer double dumps and put I/S Stroke OFA dampers upper, lowers and modulating Oil tilts @ zero 3&4 and 7&8 windbox ask CRO Insure igniter fan I/S Insure oil and air line for igniters	
Insure oil and air for oil guns are aligned Make sure limits are made on oil train Clean igniter and oil guns put in remote Discharger roller I/S Check plug chute detectors	
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Appendix 6 Unit Start Up Operator Walk Down List DOORS 8 <sup>th</sup>	Operator's Initials
Floor Boiler Penthouse 2 doors Steam drums north & south	
7 <sup>th</sup> 4 doors north side, Superheat and Gen. bank	
6 <sup>th</sup> Mud Drum, north and south side Economizer lanes door Dance floor door 6 View port doors Diverter gate	
6 <sup>th</sup> Outside 2 door on FD outlet ductwork	
<ul> <li>5<sup>th</sup></li> <li>6 View port doors, exterior</li> <li>6 View port doors, interior</li> <li>4 Doors Economizer lanes</li> <li>Distribution spouts cover and doors</li> </ul>	
4 <sup>th</sup> Auger discharge doors Metering bin doors Crossover door Economizer hopper door	
<b>3<sup>rd</sup></b> Plug chute small and large access doors Igniter inspection door Economizer Platco's	
2 <sup>nd</sup> Grate doors Grate inspection doors Grate inspection view port	

### Basement SSC doors (2)

FD ductwork doors (2) Shifting hopper covers

# TAH

10 doors "D "door on TAH hopper in TAH room

# SDA & Baghouse

Inlet door, (underneath SDA room ) Midway door Outlet door Thimble sheet and Outlet damper ... 40 doors Baghouse "D" door on all compartments Baghouse Platco covers's **Appendix 6 Maintenance Checklist** 

Action	Complete?	Initials
Remove grate level 3 front doors		
Remove 6 and 7th floor doors		
Ops run grates off		
Install 2nd floor picks and boards		
Install danger tape over opening		
Install dance floor beams		
Install dance floor ops to sniff 6th floor door		
Throw first half of boards in		
Entry guy wears harness		
Hole watch at door		
Entry lines up boards		
Hole watch hands entry remaining boards		
Deklincker boiler Maint. Supervisor		
Must have hole watch on grate level		
Wash down entire boiler from grate level		
Do a internal and external grate inspection		
Internal remove bars and enter belly of grates from rear		
Hole watch and grates locked out		
Inspect back stops and repairs		
Trajectory chutes 2 guys' inspection and set gaps 3/8		
One guy in boiler on 6 ft. ladder second outside doing adjustments		
Remove under grate doors n/s		
Board out over dampers and install board to reach zone dampers		
Hole watch and a guy stroking zone dampers from outside		
Remove zone dampers if coffins are plugged		
Inspect over fire and under fire dampers		
Inspect SSC- bearings, chain, tail drum, head drum, flights and tension		
Metering bin-inspect couplings, bearings, augers and pumps		
Board out top if entering bin, hole watch		
Make sure bin is run out		
Inspect and clean all spray machines as needed	· · · ·	
Run and inspect all ash conveyors-check for ash leaking out		
Cycle all double dumps-bag house		
Inspect all iks and g9b-repair as needed		
Install picks and boards in super heats do repairs as needed		10
Hole watch stationed outside 7th floor		
Work orders required for all jobs		

Exhibit A

Ap	pend	lix 7	E&I
-			

7 E&I			
	E&I Check Lis	t for Boiler 11 Startup	
ERS			
Description	Cal Range	Location	Checked By: (initials print
FF Outlet Press	(-30" to 0" H2O)	Inside upper level of bag house	
SDA Outlet Press	(-30" to 0" H2O)	SDA Platform	
TAH Gas outlet press	(-15" to 0" H2O)	SDA Platform	
Econ Feedwater Inlet flow	(0" to 71" H2O)	8th FL NE corner Bir	
Econ Feedwater Inlet Press	(0-1400 PSI)	8th FL NE corner Bir	
Main Stm Press	(0 - 1000 PSI	8th FL W side Bir	
Main Stm Flow	(0" to 424" H2O)	8th FL W side Bir	
Boiler Gas Outlet Press	(-15" to +5" H2O)	7.5 FL E. side Blr	
Drum Level	(-36" to -16" H2O)	7.5 FL N side Bir	
Furnace Press	(+5" to +5" H2O)	7 FLS side Bir	
Furnace Press	(-5" to +5: H2O)	7 FLN side Bir	
TAH AIR OUTLET PRESS	(0" to 30" H2O)	15T FL SE Comer Bir 12 ductwork	
TOTAL AIR FLOW	(0" to 5" H2O)	1ST FL SE Corner Bir 12 ductwork	
	ERS	E&I Check LisERSDescription FF Outlet PressFF Outlet PressC-30" to 0" H2O)SDA Outlet Press(-30" to 0" H2O)TAH Gas outlet press(-15" to 0" H2O)Econ Feedwater Inlet flow(0" to 71" H2O)Econ Feedwater Inlet Press(0-1400 PSI)Main Stm Press(0-1000 PSIMain Stm Flow(0" to 424" H2O)Boiler Gas Outlet Press(-15" to +5" H2O)Furnace Press(-5" to +5" H2O)Furnace Press(-5" to +5" H2O)TAH AIR OUTLET PRESS(0" to 30" H2O)	E&I Check List for Boiler 11 StartupERSCal Range (-30" to 0" H2O)Location Inside upper level of bag houseSDA Outlet Press(-30" to 0" H2O)SDA PlatformTAH Gas outlet press(-15" to 0" H2O)SDA PlatformTAH Gas outlet press(-15" to 0" H2O)SDA PlatformEcon Feedwater Inlet flow(0" to 71" H2O)8th FL NE corner BlrEcon Feedwater Inlet Press(0-1400 PSI)8th FL NE corner BlrMain Stm Press(0-1000 PSI)8th FL W side BirMain Stm Flow(0" to 424" H2O)8th FL W side BirBoiler Gas Outlet Press(-15" to +5" H2O)7.5 FL E. side BirFurnace Press(-5" to +5" H2O)7 FL S side BirFurnace Press(-5" to +5" H2O)7 FL S side BirTAH AIR OUTLET PRESS(0" to 30" H2O)15T FL SE Corner Bir 12 ductwork

# CONTROL VALVES

. . .

Tag Number	Description	Cal Range	Location	Checked By: (initials print)
1CCC-ACV2008	SDA DILUTION WATER VLV	0-100%	SDA PLATFORM	
1CCC-ACV2028	SDA SLURRY VLV	0-100%	SDA PLATFORM	
11FWA-ACV0095	MAIN FEEDWATER VLV	0-100%	8th FL N Side Bir 12	
11FWA-ACV157	START-UP FEEDWATER VLV	0-100%	8th FLN Side Bir 12	
15GF-ACV0032	DESUPERHEATER SUPPLY VLV	0-100%	8th FLN Side Bir 12	
15G1-ACV0002	SOOT BLWR STM SUPPLY VLV	0-100%	Top of Bir 12	
1FOB-ACV0092	FUEL OIL SUPPLY VLV	0-100%	3rd Fl N side Bir 12	
BOILER I/P C	ONVERTERS			
15GB-5GC0003	WINDBOX CTRL-F	4-20ma = 0-100%	3rd FL S Side Blr 12	
15G8-5GC0004	WINDBOX CTRL - R	4-20ma = 0-100%	3rd FL 5 Side Blr 12	

		E&I Check Lis	t for Boiler 12 Startup	
TRANSMITTE	RS			
			1	Checked By: (initials print)
Tag Number PI2040	Description FF Outlet Press	Cal Range (-30" to 0" H2O)	Location Inside upper level of bag house	
PI2001	SDA Outlet Press	(-30" to 0" H2O)	SDA Platform	
125GA-PT2006	TAH Gas outlet press	(-15" to 0" H2O)	SDA Platform	
12FWA-FT0028	Econ Feedwater Inlet flow	(0" to 71" H2O)	8th FL NE comer Bir	
12FWA-PT0076	Econ Feedwater Inlet Press	(0 -1400 PSI)	8th FL NE corner Bir	
125GG-PT0002	Main Stm Press	(0 - 1000 PS)	8th FL W side Bir	
125GG-FT0002	Main Stm Flow	(0" to 424" H2O)	8th FL W side Blr	
125GA-PT0063	Boiler Gas Outlet Press	(-15" to +5" H2O)	7.5 FL E. side Blr	
125GF-LT00026	Drum Level	(-36" to -16" H2O)	7.5 FL N side Bir	
125GA-PT0036	Furnace Press	(-5" to +5" H2O)	7 FLS side Bir	
125GA-PT0039	Furnace Press	(-5" to +5: H2O)	7 FLN side Bir	
25GB-PT2004	TAH AIR OUTLET PRESS	(0" to 30" H2O)	1ST FL SE Comer Bir 12 ductwork	
25GB-PT0049	TOTAL AIR FLOW	(0" to 5" H2O)	1ST FL SE Corner Bir 12 ductwork	
CONTROL VA	LVES			
Tag Number 2CCC-ACV2008	Description SDA DILUTION WATER VLV	<u>Cal Range</u> 0-100%	Location SDA PLATFORM	<u>Checked By: (initials print</u>
2CCC-ACV2028	SDA SLURRY VLV	0-100%	SDA PLATFORM	
12FWA-ACV0095	MAIN FEEDWATER VLV	0-100%	8th FL N Side Bir 12	
12FWA-ACV157	START-UP FEEDWATER VLV	0-100%	8th FLN Side Bir 12	
1SGF-ACV0032	DESUPERHEATER SUPPLY VLV	0-100%	8th FL N Side Bir 12	
25G1-ACV0002	SOOT BLWR STM SUPPLY VLV	0-100%	Top of Bir 12	
2FOB-ACV0092	FUEL OIL SUPPLY VLV	0-100%	3rd Fl N side Bir 12	
	ONVERTERS			
BOILER I/P C	CALA A PLAT PLAN			
BOILER I/P C	WINDBOX CTRL+F	4-20ma = 0-100%	3rd FLS Side Bir 12	

AQD No. 6-2017

# Exhibit A

		E&I Check Lis	st for Boiler 13 Startup	
TRANSMITTE	RS			
Taa Number	Description	Cal Range	Location	Checked By: linitials printl
FIZ:40	FF OLT ET F'ELL	-30 to 0 F20:	Instal Local avail of cagnolise	
F12001	504 0.1 61 F1833	,-30 to 0 F201	SDAF ITCIM	
1253A-FT2006	TAP SE LLE ELC'EN	,-15 t: 0 +20;	504 F #****	
12FWA-FT3025	Ear Feedwatenin et fick	,0 11 71 H2O	Etr fL h E II mer 5 -	
12FWA-FT0075	EII'r feeddaler i'r el Press	.0 -1400 FSI	Btr FL N Ecorrer B *	
12555-FTXX22	hts = 31 = F122	,0 - 1000 FSI	BIT PL WE DE B *	
12555-FT0002	Na - St - Fow	10 to 424 H20	Etr FL'Walte Bir	
1252-4729	5: 1'GEL D.T ETF'EII	-15 1: -E +20	75 FLE 2 28 6 *	
12537-17030-25	D" Leve	36 11 -15 F20	7.5 FL R. 2 28 5 *	
12554-FT3056	F	5 t2 -5 F20:	TRUSS DE B T	
12534-FT003F	F.***** F*111	5 12 -5: +20	77LN 3 285 *	
2595-FT204	TAH AIR OUTLET FREES	,0 to 30 H2C	15T FL SE Comer 5 1202 2407	
2595-FT0042	TOTAL AIR FLOW	.0 to 5 F20	15T FL 5E Corner 5 11202 I 4019	
CONTROL VA	LVES			
Tas Number	Description	Cal Banze	Location	Checked By: linitials print!
200-40-20-2	SD4 DILUTION WATER VEH	0-100%	SD2 FLATFORIA	
30 00-4 0 120-25	SEA SLURRY VLV	0-12099	SD4 FLATFORM	
12FW4-4CV0098	MAIN FEEDWATER THE	0-1004	81" FL N S 28 5 12	
12FWA-4CV187	START-UP FEEDWATER THE	0-120H	81- PL 1: 5 38 5 12	
15GR-400-063	DES JEERHEATER, SJEFLY VLV	0-100%	51" FL % 5 35 5 * 12	
2561-400002	SOCT BLAR STRASJEFULVUV	0-1205	T12 2° 5 * 12	
28.06-140 10092	FJEL CILSJFFLY VLV	0-1205	3'2 F 1. J 28 5 12	
	ONNESTER			
BOILER I/P CI	WINDSOK CTRL-F	4-20 mg = 0-100%	312 RL 5 5 18 5 * 12	
12/4 0+2 (4/14/14)	WIDEDER SINS * P	and a stratter	a - 11 2 3 38 9 1 22	
1555-5520204	WINDSOX CTRL-R	4-20ma = 0-100 <del>21</del>	312 FL 5 5 28 6 1 12	

Appendix 8 CEMS Checklist

	MON	TUES	WED	THURS	FRI			DATE:		1	1	
	1	i				Cal Gas Press.	MON	TUE	WED	THUR	FAI	CA
Check Gas Bottles						1)N2/02						1
Check System pressures and vacuums		-				2) SO2/NO/CO						
Check Sample Gas Flows						3) 02/CO/CO2						
Theck Analyzer Alsime						4) N2						
Check Computer Is on Line						5) 502						
Check Dally Cal Drifts of OOC Conditions	1		:			6) 02						
INITIAL	s											
1.1		ουτι	1	1	INLET			-				
GAS ANALYZERS	18	OUTL 12	ET 13		INLET	13			INLET			1
GAS ANALYZERS HECK CAL CAS FLOW (STEADY FLOW FLOW FLOW RATE)	11	T	1	1			UNITS		11	12	1:	2
HECK GAL GAS FLOW (STEADY FLOW FLOW RATE) HECK SYSTEM PARAMETERS (PRESSURE VACCUM)	11	T	1	1				VOLTAGE	11		1:	3
HECK CAL GAS FLOW (STEADY FLOW FLOW RATE)	18	T	1	1			SC2 LAMP	VOLTAGE	DUTLE	г		3
HECK GAL GAS FLOW (STEADY FLOW FLOW RATE) HECK SYSTEM PARAMETERS (PRESSURE VACCUM)	11	T	1	1			SO2 LAMP	VOLTAGE	11			
HECK GAL GAS FLOW (STEADY FLOW FLOW RATE) HECK SYSTEM PARAMETERS (PRESSURE VACCUM)	18	T	1	1			SO2 LAMP	VOLTAGE	DUTLE	г		
HECK GAL GAS FLOW (STEADY FLOW FLOW RATE) HECK SYSTEM PARAMETERS (PRESSURE VACCUM)	11	T	1	1			SO2 LAMP	VOLTAGE	DUTLE	г		
HECK CAL GAS FLOW (STEADY FLOW FLOW RATE) HECK SYSTEM PARAMETERS (PRESSURE VACCUM) HECK SO2 MONITOR LAMP VOLTAGE (~165 VDC.STABLE)		12		1			SO2 LAMP	VOLTAGE	DUTLE	г		
HECK GAL GAS FLOW (STEADY FLOW FLOW RATE) HECK SYSTEM PARAMETERS (PRESSURE VACCUM)	11	T	1	1			SO2 LAMP	VOLTAGE	DUTLE	г		

Exhibit A

-

# Boiler Shutdown Standard Operating Procedures

## SOP-1022

#### 1.0 Purpose:

To provide a procedure to ensure proper shutdown of the boiler. Each boiler is shutdown at least every 42 days but, in general, it is done on a more frequent basis.

### 2.0 Scope:

Detroit Renewable Power – Power Block

### 3.0 Responsibilities:

Department Manager or designee is responsible for implementing and maintaining this procedure.

Department Supervisor(s) and Control Room operators (CRO) are responsible for adhering to this procedure.

#### 4.0 Definitions: None

### 5.0 Safety and Environmental Information:

You must wear proper Personal Protective Equipment, which consists of:

- 5.1 Approved hard hat that meets all ANSI/ISEA Z89. 1 Type 1 standard and Class E certification standard are located inside employee's hard hat.
- 5.2 Safety Glasses/Face shield Approved by ANSI with the designation stamped or molded on the glasses saying Z-87 which have been tested and have been approved to wear in industry.
- 5.3 The following specifications are the minimum requirements for protective work boot.
  - 5.3.1 Leather upper material
  - 5.3.2 Minimum 6" boot height
  - 5.3.3 No deep cleats in the sole
  - 5.3.4 Semi-lug sole for traction
  - 5.3.5 High density sole
  - 5.3.6 Composite or steel toe

- 5.4 Long sleeved shirt and long pants to keep ash off of your body.
- 5.5 Hearing protection may be necessary but not required.
- 5.6 Leather gloves may be required. Use our standard leather glove (grey with cuff) should be available.
- 5.7 Before starting, or shutting down follow Safety Procedure # 15 Lockout Tagout which can be viewed in the Safety Manager's office or on the S drive.

### 6.0 Standard Operating Procedures Steps:

6.1 Notify Beacon Control to coordinate boiler shut down vs. steam demand.

- 6.1.1 Make sure that we call the following entities when the turbine generator is coming offline.
- 6.1.2 Michigan Electric Coordinated Systems Balancing Authority: Call this number first > (248) 380-2932 or (248) 380-2931
- 6.1.3 Midwest Independent Transmission System Operator Reliability Coordinator: (317) 249-5030
- 6.1.4 ITC Transmission

Transmission Operators Control Room: (248) 380-2903

- 6.2 Reduce Boiler Main Steam set point to approximately 250klb/hr.
- 6.3 Stop feeding Metering bin to allow to run empty.
- 6.4 Start igniters and oil guns.
- 6.5 As metering bin runs low, place Combustion Control loop in manual from auto.
- 6.6 Adjust oil firing rate to maintain stable boiler conditions while metering bin runs completely empty.
- 6.7 When metering bin is empty:
  - a. Stop Augers.
    - i. Toggle CEMS input to off line.
    - ii. Record auger stop time as "RDF Out".
  - b. Open Superheater drains by turning two (2) rotations.
  - c. Isolated slurry to Spray Machine.
  - d. Stop PDA fan.
  - e. Isolate all make up water to SSC.
- 6.8 Reduce oil firing rate.
- 6.9 Align the Start Up Feedwater ACV and place in service (recommended below100Klb/hr.).
- 6.10 Isolate Main Feedwater ACV.
- 6.11 Stop oil guns and allow to purge.
- 6.12 Stop igniters (Boiler will trip. First Out: loss of all fuel).
- 6.13 Record MFT time as "Oil Out".
- 6.14 Clean Baghouse (two [2] times).
- 6.15 Continue to run the bottom ash screws and Grates until the boiler is cool.
- 6.16 Stop and remove Spray Machine when SDA outlet temp is below approximately 300 degrees.

- 6.17 Continue to run the DF fan for cooling as needed until the Baghouse outlet temperature is 150 degrees.
  - a. After stopping the FD fan, leave the 4 sacrificial baghouse compartments in service while isolating the remaining 6 compartments. (A, B, F, G in) (C, D, H, J, K isolated).
  - b. Stop the reverse Air Fan.
  - c. Turn Off the sonic air horns.
  - d. Place the cleaning cycle from Auto to Manual.
- 6.18 Perform the list of required checks on the "Supervisor Boiler Inspection / Shutdown Checklist"

### SUPERVISOR

# BOILER INSPECTION / SHUTDOWN CHECKLIST

(each boiler is shut down every 42 days, but in general it is more frequent) Date: \_\_\_\_\_ Boiler #\_\_\_\_\_ Initials 1. LO/TO Boiler 2. Have doors removed per door list 3. Remove Spray Machine a. Drain/ Flush Slurry Line b. Spray Machine Cleaned (Maintenance) 4. Confined Space Sheets 5. Gas Path/ Furnace Inspection a. TAH Gas Path b. Economizer Gas Path c. Gen Bank Gas Path d. Furnace Wall Inspection e. Wind box/TOFA Nozzles f. UGA Zone Plenums g. UFA Duct PDA Fan Suction h. Inspect S.D.A Inlet, Vessel & Outlet 6. Bag House Hoppers Clear 7. Economizer Hoppers Clear

14. P.D.A Inspection a. Internal b. External	
15. Sifting Screw Inspection	
16. Sifting Hopper Inspection	
17. Inspect Boiler for Tube Leaks	
<ul><li>18. Grate Inspection (Maintenance)</li><li>a. External (each Shut Down)</li><li>b. Internal (Per schedule)</li></ul>	
19. SSC Inspection (Maintenance)	1.5
20. Verify Damper Operation a. UFA Damper	
b. N. UGA Damper c. S. UGA Damper	
<ul><li>d. OFA Damper</li><li>e. Wind box Dampers (1-8)</li></ul>	2.3 2
f. Upper TOFA (1-8)	
g. Lower TOFA (1-8)	

Supervisors are responsible for the performance or directing of performance of all checks

### SOP-0110 Procedure Title:

#### LOSS of STATION POWER

Following a total loss of station power, the immediate priority is to ensure a safe shutdown of all equipment and to ensure the safety of the Facility personnel.

- A. The following actions will be taken:
  - 1. Immediately check all relays both in the control room and the switchyard
  - 2. Immediately ensure that the DC turbine lube oil pump has started and is maintaining pressure
  - Immediately ensure that the generator breaker is open and open I main and reserve breakers.
  - Immediately check for fire in all fuel-feed systems that were in service and station operator at the diesel fire pump
  - 5. Contact the DTE dispatcher for any information on the cause of the power loss
  - Notify the FAA (1-800-332-5694) that the chimney strobe lights are not operating. Report the stack location as:

Latitude 42° 22 minutes 04 seconds

Longitude 83° 03 minutes 05 seconds

- 7. Notify the MDEQ AQD
- 8. If the cause of the outage has been identified and corrected, re-energize immediately
- If the cause cannot be identified within a short time, contact the appropriate technical support personnel for assistance
- 10. If the power is not restored, isolate all deluge systems and post a fire watch
- 11. Ensure that there is a natural draft through the boilers tripped off line
- 12. If power is not restored within one hour, begin degassing and purging the turbine generator with carbon dioxide.
- 13. If temperature is below freezing, drain any fire protection systems that may have tripped

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- 14. Isolate any air operated control valves that are allowing operating parameters to reach abnormal values
- B. When power is restored:

Once power is restored, place in service the air compressor

- 1. Reset all fire systems
- 2. Refill boilers as per manufacturer's recommendation
- Minimum air flows will be used to purge boilers of gases and particulate to minimize impact on opacity.
- 4. Restart gas generator, as per power manufacturer's recommendations
- 5. Run all ash out of all conveyors systems
- 6. Once all auxiliary systems have been restarted and operating conditions are stabilized, re-initiate fires in the boilers
- 7. Proceed with restart procedure

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#### SOP-0120

#### **Procedure Title:**

### **SDA MALFUNCTIONS**

The Shift Supervisor will be responsible to determine the cause of the problem, rectify the problem and place all systems back in service as soon as possible. The operating SOP is as follows:

- Attempt to re-establish proper SO2 control. If unsuccessful, place the oil guns in service and secure RDF feed to the boiler as quickly as possible
- Secure the RDF feed to the boiler and allow the fuel remaining on the grate to completely burnout.
- 3. If the SO2 is within the air permit limit value, leave the boiler in-service on oil-firing.
- 4. Re-establish RDF fires once proper SO2 control is restored.

### 103116\_SOP-0120 SDA MALFUNCTIONS\_Final 11/1/2016 3:16:00 PM

#### SOP-0130

#### Procedure Title:

#### **BOILER FEED CHUTE PLUG**

Feed chute plug may cause excessive transient CO emissions. In order to compensate for these conditions, the following procedure will be observed:

- 1. If steam flow is affected reduce load.
- 2. Evaluate grate conditions for barren spots or lightly-covered areas.
- 3. Adjust undergrate air dampers to maintain grate temperature.
- 4. Identify the plugged chute and clear it.
- 5. If necessary, adjust TOFA to keep CO within the air permit limit value.
- 6. Adjust grate speed.
- Once grate conditions are stable, adjust the grate speed to maintain proper burnout.
- 8. After fuel-feed is re-established, adjust all parameters to the normal operational settings while maintaining emissions within limits.
- 9. Check the CEM system for possible CO exceedance.

11/1/2016 3:18 PM

### SOP-0140

#### Procedure Title:

#### **RDF Boiler Grate Malfunction**

Boiler grate malfunctions may include drive failure, chain breakage, binding or damage due to high temperatures. The following SOP should be used if the grate malfunctions:

- 1. If steam flow is affected reduce load.
- 2. Immediately shutdown the Auger screws feeding the affected half-of-grate.
- 3. Bias up undergrate air
- 4. If necessary, evenly distribute piled RDF on the grate with appropriate tools.
- 5. Maintain undergrate air flow to keep grate temperatures less than SOOT.
- 6. Concurrent with emergency actions, identify causes for the malfunction.
- 7. Monitor and maintain CO and excess O<sub>2</sub> within normal operating limits.
- Re-establish fuel feed and carefully monitor grate conditions, once the malfunction is corrected.
- 9. If the boiler must be shutdown, follow procedures for RDF BOILER STARTUP/SHUTDOWN.

#### 103116\_SOP-0140 Boiler Grate Malfunction\_Final

11/1/2016 3:19 PM

#### SOP-0150

#### **Procedure Title**

#### **RESPONSE TO CARBON MONOXIDE (CO) EXCURSION**

Anytime CO emissions are above the permit limit, immediate action must be taken to reduce them to normal levels. If CO levels cannot be reduced to permitted levels in one hour, the Operations Supervisor must be notified. Unit load must be reduced or the unit removed from service, as necessary to prevent exceeding the hourly or the 24 hour average permit limit for CO emissions.

In the event that the CEM CO monitor indicates an increasing trend or an alarm condition is reached:

- 1. Verify whether a substantial increase in fuel moisture content is occurring as indicated by:
  - Auger Speed is increasing.
  - Verbal communication with the Waste Processing Loader Operator.
  - Visual inspection of the refuse fire. (Unburned fuel at grate discharge, fuel not reaching back of grate.)

If wet refuse is causing the increase in CO, take action to:

- Immediately reduce load.
- Instruct the loader operator to mix a more homogeneous blend of wet and dry fuel.
- Increase the pneumatic distribution air by opening each of the seven manually controlled dampers, ensuring that the fuel is being delivered to the charging zone of the grate
- Reduce bed thickness by increasing the speed of the grates 10 15%.
- Place burner tilts at 30 ° down to increase fuel bed agitation,
- Adjust fuel/air ratio by decreasing the auger bias,
- Increase overfire air by raising the air heater outlet duct pressure set point.
- 2. In addition to items listed in #1 above, verify whether a fuel overfeed situation exists as indicated by:
  - Furnace O<sub>2</sub> continues dropping below the normal operating range of 5 to 7%.

If a fuel overfeed situation exists, take action to:

- Decrease the Auger bias.
- Increase the grate speeds 10-15%.
- Maintain these settings until fuel feed and combustion return to acceptable levels.
- Adjust settings to insure complete combustion.
- Adjust grate speed to maintain a 4 to 6 inch bed depth.
- Adjust pneumatic distribution air to maintain fuel delivery to the grate charging zone.
- Adjust auger bias to maintain an O<sub>2</sub> range of 5 to 7%.
- 3. Verify whether a severe fuel overfeed situation exists as indicated by (in addition to items listed in #1 and #2 above):
  - Furnace flue gas temperature decreasing below 1810°F, approaching the permit limit of 1800°F; requiring that oil burners be placed in service,
  - Annunciation on the Taylor DCS alarm screen occurring as process O<sub>2</sub> falls below 5% or raises above 7%.

Actions to correct a severe refuse overfeed are as follows:

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- Place the underfire air dampers in local/auto control and increase the amount of undergrate air by 5 %.
- Decrease auger bias by 10 to 15%.
- Increase the grate speeds by 10 to 15% to thin out fuel bed.
- Place the oil burners in service as necessary to maintain a <u>minimum</u> of 1800°F flue gas temperature leaving the furnace.
- As the fuel bed returns to normal, place the undergrate air control back to remote auto
- Take oil burners out of service as temperatures are stabilized at or above 1810°F.
- Verify that no ingress of fugitive air is occurring at the ash discharger(s) or any other furnace opening upstream of the O<sub>2</sub> probe as would be indicated by:
  - ID Fan amps increasing and furnace draft becoming unsteady, sporadically going on positive pressure,
  - ID fan damper at 100% or above normal.

If loss of atmospheric seal occurs, take the following action:

- Identify and begin restoring the atmospheric seal, reduce load as necessary to stabilize boiler draft.
- Determine the degree of overfeed which has caused the CO to increase and follow the appropriate corrective action as indicated in item 1.
- 5. Verify that the soot blowers are not in operation and that a soot blower poppet valve has not stuck open. These may cause the following:
  - May cause a CO spike or repeated spiking.
  - Soot blowing increases loading on the ID fan. It is possible for this loading to cause the boiler draft to become unsteady causing sporadically positive pressures in the furnace.
  - ID fan damper near 100% open (or above normal damper opening) during soot blowing operation.

If malfunctioning soot blowers or sporadically positive pressures in the furnace are the cause of the CO problem, take the following action:

- Isolate soot blowing steam block valve to ensure no steam is entering boiler through the soot blowers.
- Reduce load on the boiler until the ID fan damper can control the boiler draft,
- Insure that the air preheater is clean, soot blow if needed.

6. Verify that the CO reading on the CEM monitor is correct as indicated by:

- Comparing current CO readings with visual observations of the refuse fire on the stoker.
- Access the group trend for emissions on the Taylor MOD-300 and review these trends.
- Reviewing the Daily Calibration Report printout status. Report is recorded every day on the senior operators log at 0800.
- If the continuous emission monitor is suspected or found to be faulty, immediately notify E&I department so that repairs can be made.

103116\_SOP-0150 RESPONSE TO CARBON MONOXIDE (CO) EXCURSION\_Final

Procedure Title

SOP for High SO<sub>2</sub>

This procedure covers the actions to be taken to respond to a high SO<sub>2</sub> condition and prevent an excursion. The SO<sub>2</sub> (stack) rate (ppm) should be closely monitored. If the SO<sub>2</sub> (stack) exceeds the normal operating range, the shift supervisor must be immediately notified. The boiler load must be reduced and if necessary, taken off line to prevent the unit from exceeding the SO<sub>2</sub> permit limit.

In the event that the SO<sub>2</sub> (stack) monitor indicates an increasing trend or an alarm condition is reached:

1. Verify that the atomizer is running. Restart the machine if necessary.

2. Verify proper lime slurry flow is being supplied to the Spray Dryer Atomizer (SDA) via Lime Slurry head tank.

- Normal slurry flow is indicated on the Control Room CRT, varying between 3 and 30 gallons per minute (gpm),
- SDA outlet temperature is being maintained at setpoint (285°F) and "Spray Dryer Absorber Temp High" alarm has not activated.

If no slurry flow or poor flow is being supplied to the Spray Dryer Atomizer head tank, take action to:

- Verify that the Additive feed pump is operating properly. Restart pump or switch over to standby pump if necessary.
- Verify proper Additive feed pump flow by checking the recirculation flow back to the tank. If necessary, flush the loop or start a second pump.
- Verify that the atomizer slurry inlet strainer is clear of all material. Clean the strainer if necessary.
- Verify that Additive Feed Isolation Block Valve is open. Reopen if necessary.
- Verify that the Additive Flow Control Valve's actual position matches temperature controller's indication. Stroke
  valve through its range. Verify that valve is opening properly.
- Verify that the atomizer wheel nozzles are clear. Clean nozzles if necessary. High vibration may indicate plugged nozzles.

If control over SDA SO<sub>2</sub> emissions cannot be regained within one hour, the boiler load must be reduced, and if necessary, taken off line to prevent the unit from exceeding the SO<sub>2</sub> permit limit.

- 3. Verify whether the slurry supply to the SDA has low lime density as indicated by:
  - Proper temperature control but poor SO<sub>2</sub> reduction.
  - Both online boilers indicating high SO2 outlet problems. Take manual samples of slurry from additive feed sample port. Check the specific gravity of the sample.
  - Normal slurry from the storage tank will contain around 22% solids. Normal slurry supplied to the SDA will vary from 11% to 22% solids.
- 4. If low slurry density is found on the additive feed pump discharge, take the following action:
  - Verify that the additive transfer pump is in operation. Restart pump or switch over to the standby pump if necessary.
  - Verify proper additive transfer pump flow. If necessary, flush the loop or start a second pump.
  - Verify that the SO<sub>2</sub> Control Valve's actual position matches controller's indication. Stroke valve through its range. Verify that valve is opening properly.

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5. If one additive transfer pump cannot provide proper flow; determine cause of problem and correct or notify maintenance of the necessary repair. Acid clean the additive transfer pump if necessary.

If a low slurry density is found in the additive storage tank, take the following action:

- Verify that the additive storage tank mixer is operating properly. If the mixer is not running, the slurry will concentrate at the bottom of the tank. Once the high solids slurry is used up, only low density slurry will remain in the tank.
- Restart or repair the mixer as necessary. If the mixer cannot be quickly repaired, ensure proper agitation with compressed air.
- Start the slaker. Verify proper slaking temperature 170°F. Test slaker outlet density. If density is low, adjust slaker settings as required.
  - If problems are found with the lime slurry, check quality of the lime for proper CaO content.
  - If control over slurry density cannot be regained within one hour, the boiler load must be reduced, and if necessary, taken off line to maintain proper SO<sub>2</sub> limit.
- 7. Verify that the waste processing tipping floor operator is locating and removing items known to produce excessive amounts of SO<sub>2</sub> during combustion, e.g. sheetrock
- 8. Ensure that the waste processing is feeding a homogeneous blend of RDF onto the boiler feed conveyor belt.
- 9. Verify that flue gas inlet conditions are suitable for optimum SO<sub>2</sub> absorption in the reactor. SDA inlet temperature should be maintained between 400 and 450°F.
  - If the inlet temperature is too high, SO<sub>2</sub> will not be absorbed because the particles dry too quickly. Maximum temperature allowed is \*\*\*520°F\*\*\*. Blow soot and if necessary reduce load until temperature is brought back into design.
  - If the inlet temperature is too low, lime particles will not react properly with the SO<sub>2</sub>. Minimum inlet temperature allowed is \*\*\*350°F\*\*\*. Increase load and/or place auxiliary burners in service to bring the inlet temperature back up to design.
  - Check for abnormally high SO<sub>2</sub> inlet conditions.

10. Verify that the SO<sub>2</sub> reading on the CEM monitor is correct as indicated by:

- Comparing current SO<sub>2</sub> readings with visual observations of the refuse fire on the stoker.
- Access the group trend for emissions on the Taylor MOD-300 and review these trends.
- Reviewing the Daily Calibration Report printout status. Report is recorded every day on the senior operators log at 0700.
- Review the Daily Report by accessing the HOURLY OUTLET DATA on the Trace Data Explorer generation by the DAU number for the boiler experiencing the SO<sub>2</sub> excursions and reviewing the hourly SO<sub>2</sub> readings as an indication as to whether the monitor has been tracking SO<sub>2</sub> emissions in a steady or very erratic manner.
- 11. If the continuous emission monitor is suspected or found to be faulty, immediately notify CEM coordinator E&I so that repairs can be made.

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#### SOP-0170

#### **Procedure Title**

#### SOP for High NO<sub>x</sub>

Anytime NOX emissions are above the permit limit, immediate action must be taken to reduce them to normal levels. If NOX levels cannot be reduced to permitted levels in one hour, the Operations Supervisor must be notified. Unit load must be reduced or the unit removed from service, as necessary to prevent exceeding the 2nd 1 hour average permit limit for NOX emissions.

In the event that the CEM NOX monitor indicates an increasing trend or an alarm condition is reached:

- 1. Verify whether an oversupply of excess air is present in the furnace, as indicated by:
  - A substantial increase in the opening of underfire and/or overfire air dampers,
  - Increased pressure drops throughout the furnace flue gas path.
  - The ID fan damper position continuously running at or near the end of its effective operating range, o
  - Furnace draft becoming unstable due to an imbalance of combustion air or loss of atmospheric seal on the furnace.

If too much excess air is causing the increase in NOX, take action to:

- Reduce the combustion air temperature if fuel is dryer than normal and high in BTU.
- Reduce the underfire and/or overfire air by increasing auger bias 2-10%. This should ensure good combustion and reduce NOX levels,
- Identify and reestablish furnace atmospheric seal and/or determine and correct the deficiency causing the ID fan dampers to run at the end of their effective range,
- Reduce load if overall fuel moisture is too high to ensure complete combustion while running unit at full load.
- Verify whether a substantial increase in organic/vegetable matter such as brush, undergrowth, grass clippings, leaves and/or food waste is being fed to the furnace, as indicated by:
  - Auger increasing dramatically above the proportion run time setting as a result of the sudden increase in refuse moisture
  - Furnace flue gas temperature decreasing
  - Boiler steam flow rate steadily decreasing

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- Verbal communication with the Waste Processing Loader Operator
- Visual inspection of the fire.

If an increase in organic/vegetable matter is found to be causing the increase in NO<sub>x</sub>, take action to notify the Waste Processing Loader Operator to mix a more homogenous blend of wet and dry refuse and maximize the combustion air temperature.

- 3. Verify that the stoker refuse bed condition is not contributing to the formation of NO<sub>x</sub> as indicated by:
- The grate fuel bed being a uniform and correct thickness across the width of each undergrate air zone
- There being no thick patches of partially burning fuel where unconsumed oxygen can react with nitrogen to form nitrogen oxides (NO<sub>x</sub>).

If the refuse bed condition is causing the increase in NO<sub>x</sub>, take action to:

- Notify the Waste Processing Loader Operator to mix a more homogenous blend of wet and dry fuel.
- Maximize the combustion air temperature.
- Reduce load as necessary to ensure complete combustion and <u>minimize</u> the formation of NO<sub>x</sub>.

If the continuous emission monitor is suspected or found to be faulty, immediately notify CEM coordinator or E&I department so that repairs can be made.

#### 103116\_SOP-0170 SOP for High NOx\_Final

SOP-0180

Procedure Title

#### **SOP for High Opacity**

(Fabric Filter)

Anytime Opacity emissions are above the permit limit, immediate action must be taken to reduce them to normal levels. If Opacity emissions exceed 10.0% unit load must be reduced or the unit removed from service, as necessary to prevent exceeding the 6 minute average permit limit for Opacity Emissions.

 Immediately notify the shift supervisor and begin taking steps to identify and correct the cause of the opacity excursion.

Note: Most often a <u>gradual</u> increase in opacity will be observed if the cause is a small leak(s) in one or two filter bags or a gradual dirtying of the optics on the opacity monitor itself. Likewise, a small <u>momentary</u> spike in opacity between 8 and 26%, immediately after cleaning of a compartment(s) is generally an indication of a leaking bag in that compartment. A <u>guick</u> increase in opacity could be an indication that the bypass damper has opened or a bag has come unseated. A large <u>sustained</u> increase in opacity may be an indication of a malfunction occurring in the opacity monitor itself. A visual inspection of the gas plume exiting the stack together with additional instrument indications may signify that a multiple bag or catastrophic failure such as a fire is occurring. All of these conditions require immediate action in order to prevent, or minimize, a reportable opacity excursion from occurring and to prevent, or minimize, damage to equipment and danger to personnel.

- 2. Verify which (if any) compartments) have leaking bag(s) by performing the following:
  - Call-up on the Taylor DCS process control screen "Baghouse Overview "(compartments 1-10) of the unit experiencing the opacity excursion, If the baghouse is being cleaned using off-line cleaning, close the outlet damper on the compartment which had last finished cleaning prior to the increase in opacity, by issuing an ISOLATE command,
  - Access the group trend for emissions on the Taylor MOD-300 and review these trends (has real time opacity indication and updates every 10 seconds).
  - Check to see if a noticeable decrease in opacity occurs. Reopen the compartment outlet damper. If the leaking bag(s) is located in the compartment opacity will again increase as seen on the CEM monitor.

Note: It is possible that two or more compartments have leaking bag(s), causing the high opacity. If opacity does not return to its pre-aiann level when a compartment containing a

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leaking bag is located and isolated, a second check of all remaining compartments should be made.

- 3. Once the leaking compartment(s) is located, it should be:
  - Injected with leak detection powder.
  - Tagged and locked out.
  - The cover removed and the damaged/unseated bag(s) identified and replaced.
  - The tube sheet vacuumed and all bags inspected for fly ash buildup in them. Any fly ash in the bags must be vacuumed out to prevent damaging the fabric.

Note: If the leaks at this point are minor i.e. < 5% and the compartmest(s) can be isolated without the need to reduce load on the unit, it is advisable to postpone the inspection until after dark. The leak detection powder is most visible in ultraviolet light, with little or no sunlight interference.

- When the bag(s) have been replaced a <u>bag replacement form</u> must be completed. This form details the cause of the failure/unseating, together with the action which should be taken to make corrections and to prevent any further recurrence.
- Verify that the following parameters are within a normal operating range and are not indirectly causing high opacity:
  - Furnace draft is stable at approximately -0.005"WG. Large pressure fluctuations in the furnace and baghouse may cause fly ash to "bleed" through the filter bag fabric or cause the fabric to tear
  - Baghouse inlet temperature is below 350°F. High inlet temperatures (above 400°F) may damage or cause bags to fail
  - Furnace O<sub>2</sub> is between 8-9%. Large amounts of excess air may cause fly ash to "bleed" through the filter bag fabric or cause the fabric to tear,
  - Differential pressure across the baghouse is running between 5 and 7"WG.
  - Excessive cleaning can clean off the buildup of filter cake on the filter bag allowing fly ash to "bleed" through the filter bag.
  - Insufficient cleaning allows the filter cake to become excessively thick and creates a much greater
  - Restriction to gas flow which can cause the filter bag fabric to tear. (High compartment differential pressure and no High Hopper Level alarms indicate plugged or blinded filter bags.)
  - Differential pressures on each baghouse compartment are running between 5 and 7"inches WC. Large differences in pressure between compartments indicate problems which left uncorrected can or may cause overloading of compartments a with lower differential pressure. (Use sonic horns to clear the compartments of the high differences in pressure.)
  - All fly ash hoppers are empty or flowing. Plugged fly ash hoppers increase flue gas velocities and particulate carryover which increase the particulate loading in the baghouse.

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- No casing air leaks or other routes of fugitive air ingress i.e. loose or missing screw conveyor covers, hopper inspection pipe caps, which can overload the baghouse.
- If no leaks can be identified, verify that the Opacity reading on the CEM monitor is correct as indicated by:
  - Having an EPA Method 9 certified smoke reader, if available and weather permits, determine what actual stack opacity emissions are for the unit in question.
  - Reviewing the Daily Calibration Report printout status. Report is recorded every day on the senior operators log at 1900,
  - Review the Daily Report by accessing the HOURLY OUTLET DATA on the Trace Date Explorer generation by the DAU number for the boiler experiencing the opacity excursions and reviewing the hourly opacity readings as an indication as to whether the monitor has been tracking opacity emissions in a steady or very erratic manner.
  - If the continuous emission monitor is suspected or found to be faulty, immediately notify E&I so that repairs can be made.

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### PREVENTIVE MAINTENANCE INSPECTION SCHEDULE – Schedule 0001

### 1. CEMS PREVENTIVE MAINTENANCE INSPECTION SCHEDULE

Item	Description of Inspections	Frequency of Checks	Responsible Supervisor	
1	CHECK CAL GAS BOTTLES (PRESSURE,	DAILY	E&I Group	
	CONNECTIONS, LEAKS)		1	
2	CHECK SYSTEM PARAMETERS (PRESSURES,	DAILY	E&I Group	
	VACUUM, TEMPS.)			
3	CHECK SAMPLE GAS FLOW (STEADY FLOW,	DAILY	E&I Group	
	FLOW RATE)			
4	CHECK ANALYZERS (ALARMS, INDICATIONS)	DAILY	E&I Group	
7	CHECK DAILY CAL DRIFT RESULTS FOR OOC	DAILY	E&I Group	
	CONDITIONS			Note that all of the CEMS checks are completed
11	GAS ANALYZERS a. OBSERVE COMPLETE CALIBRATION CYCLE. 1- CHECK CAL GAS FLOW (STEADY FLOW, FLOW RATES). 2-CHECK SYSTEM PARAMETERS (PRESSURES, VACUUM),	WEEKLY	E&I Group	and documented by the E&I Group separate from this log.
13	CHANGE OUTLET PROBE FILTER	ANNUALLY	E&I Group	-
14	REBUILD METERING PUMPS	BI - MONTHLY	E&I Group	
15	CHECK/REPLACE CEM TRAILER AIR FILTER	MONTHLY	E&I Group	
17	CALIBRATION GAS AUDIT TESTING	QUARTERLY	E&I Group	1
18	REPLACE OPACITY BLOWER FILTERS	QUARTERLY	E&I Group	]
20	REPLACE TRANSPORT PUMP DIAPHRAGMS	SEMI ANNUALLY	E&I Group	1

WEEKLY Environm	nental Do	cumentation - must keep for t	ive years			
SDA Preventative Mantenance Weekly Checks for SSM Plan Recordkeeping for the Startup, Shutdown, and Malfunction Plan required by the Consent Judgement (draft) Instructions: 1. Review all listed equipment each week. 2. If issues are observed, initiate necessary actions to determine the cause and correct the issue. (Note the Work Order number if appliable) 3. Submit completed forms to Environmental Manager.						
the man the second s				Comments		
Inspect the following weekly	Date	Name	Signature	below?		
LIME SILO / WASH DOWN		Operations:				
LIME FEED SCREW - NORTH / SCREW INSPECTION		Operations:				
LIME FEED SCREW - SOUTH / SCREW INSPECTION	-10	Operations:				
. GRIT REMOVAL SCREW CONVEYOR / SCREW INSPECTION		Operations:				
DILUTION WATER PUMP A / RECORD INSPECT AND TEST		Operations:				
DILUTION WATER PUMP B / RECORD INSPECT AND TEST		Operations:				
. SPRAY MACHINE / OIL LEVEL AND INSPECT		Operations:				
STANDBY SPRAY MACHINE / OIL LEVEL AND INSPECT		Operations:				
LIME SLURRY FEED PUMP NORTH / INSPECT AND ALTERNATE		Operations:				
0. LIME SLURRY FEED PUMP SOUTH / INSPECT AND ALTERNATE		Operations:	-			
1. NORTH LIME SLAKER / GREASE BEARINGS		Operations:				
2. SOUTH LIME SLAKER / GREASE BEARINGS		Operations:				
.3. LIME SLURRY MIXING & STORAGE TANK / GEARBOX OIL LEVEL THECK		Operations:				
4. STANDBY SPRAY MACHINE / ATOMIZING WHEEL		Maintenance:		ē,		
5. NORTH GRIT SCREEN / ACID WASH AND INSPECT	Page 11 2000	Maintenance:				
.6. SOUTH GRIT SCREEN / ACID WASH AND INSPECT		Operations:				
comments (reference the item):						

Environmental Documentation - must be kept for five years

# Exhibit A

		cumentation - must keep for fi		SSM-Form-01
SDA Preventative Mantenance Monthly Checks for S Recordkeeping for the Startup, Shutdown, and Malfunction Plan re				Revision 11/04/20
Instructions: 1. Review all listed equipment each month. 2. If issues are observed, initiate necessary actions to determine the 3. Submit completed forms to Environmental Manager.	cause and c	orrect the issue. (Note the Work Or	der number if appliable)	
Inspect the following monthly	Date	Name	Signature	Comments below?
1. PENTHOUSE EAST UNIT HEATER / TEST OPERATION		Plant Engineer.		
2. PENTHOUSE WEST UNIT HEATER / TEST OPERATION		Plant Engineer:		
3. ROOF ENCLOSURE EAST VENT FAN / TEST AND ENSURE OPERATION		Operations:		
4. ROOF ENCLOSURE WEST VENT FAN / TEST AND ENSURE DPERATION		Operations:		
5. DILUTION WATER STORAGE TANK & MIXER / RECORD, GREASE AND CLEAN		Maintenance:		
6. SPRAY MACHINE / OIL FILTER CHANGE	74 	Maintenance:	*	
7. DILUTION WATER PUMP A / INSPECTION		Maintenance:		
8. DILUTION WATER PUMP B / INSPECTION		Maintenance:		
9. AQC ELECT/CTRL BDLG WEST UNIT HEATER / INSPECT AND TEST RUN		Plant Engineer:		
10. AQC ELECT/CTRL BDLG WEST UNIT HEATER / DRIVE BELT		Plant Engineer:		
11. LIME FEED SCREW + NORTH / GREASE SHAFT BEARINGS & GEARBOX OIL LEVEL CHECK		Operations:		
12. LIME SILO / GREASE BEARING		Operations:		-
13. GRIT REMOVAL SCREW CONVEYOR / GREASE AND OIL LEVEL CHECK		Operations:		
14. LIME SLURRY FEED PUMP NORTH / GREASE AND INSPECT	.0-	Maintenance:		
15. LIME SLURRY FEED PUMP SOUTH / GREASE AND INSPECT 16. LIME SLURRY MDCING & STORAGE TANK / GREASE AND		Maintenance:		
INSPECT 17. DILUTION WATER STORAGE TANK & MIXER / GREASE AND		Maintenance:		
INSPECT 18. LIME PREP BUILDING PREP HEATER LOWER / ENSURE	-	Maintenance:		
OPERATION 19. LIME PREP BUILDING PREP HEATER UPPER / ENSURE		Operations:		
OPERATION		Operations:		
20. NORTH LIME SLAKER / DRIVE BELT INSPECTION		Maintenance:		
21. SOUTH LIME SLAKER / DRIVE BELT INSPECTION		Maintenance:		
22 LIME SLURRY FEED PUMP NORTH / DRIVE BELT INSPECTION		Maintenance:		
23. LIME SLURRY FEED PUMP SOUTH / DRIVE BELT INSPECTION		Maintenance:		
Comments (reference the item):		produticitante.	1	

Environmental Documentation - must be kept for five years

SEMI-ANNUAL Environmental Documentation - must keep for five years

SDA Preventative Mantenance Semi-annual Checks for SSM Plan

SSM-Form-016 Revision 1 11/04/2016

Recordkeeping for the Startup, Shutdown, and Malfunction Plan required by the Consent Judgement (draft)

Instructions:

1. Review all listed equipment semi-annually

2. If issues are observed, initiate necessary actions to determine the cause and correct the issue. (Note the Work Order number if appliable)

3. Submit completed forms to Environmental Manager.

Inspect the following weekly	Date	Name	Signature	Comments below?
1. DILUTION WATER PUMP A / GEARBOX OIL CHANGE		Maintenance:		
2. DILUTION WATER PUMP B / GEARBOX OIL CHANGE		Maintenance:		
3. LIME FEED SCREW - NORTH / GEARBOX OIL CHANGE		Maintenance:		
4. LIME FEED SCREW - SOUTH / GEARBOX OIL CHANGE		Maintenance:		
5. GRIT REMOVAL SCREW CONVEYOR / GEARBOX OIL CHANGE		Maintenance:		
6. LIME SLURRY MIXING & STORAGE TANK / GEARBOX OIL CHANGE		Maintenance:		
7. SPRAY MACHINE / OIL AND FILTER CHANGE (can be done annually)		Maintenance:		
8. DILUTION WATER STORAGE TANK & MIXER / GEARBOX OIL CHANGE (can be done annually)		Maintenance:		

Comments (reference the item):

SAEnvironmental/Air/ROP/Record keeping for ROP/Record keeping Summary ironmental Documentation - must be kept for five years

# Exhibit A

Baghouse Preventative Mantenance Weekly Check		umentation - must keep for fi Plan		SSM-Form-I Revisio
Recordkeeping for the Startup, Shutdown, and Malfunction Plan				11/04/2
Instructions:				
<ol> <li>Review all listed equipment each week.</li> <li>If issues are observed, initiate necessary actions to determine the second se</li></ol>	he cause and	correct the issue. {Note the Work	Order number if appliable)	
3. Submit completed forms to Environmental Manager.		1		Comments
Inspect the following weekly	Date	Name	Signature	below?
1. BAGHOUSE BYPASS DAMPER A / RECORD, DRAIN AND GREASE		Operations:		
2. BAGHOUSE BYPASS DAMPER B / RECORD, DRAIN AND GREASE		Operations:		
3. A COMP BAGHOUSE INLET DAMPER / RECORD, DRAIN AND GREASE		Operations:		
4. B COMP BAGHOUSE INLET DAMPER / RECORD, DRAIN AND GREASE		Operations:		
S. C COMP BAGHOUSE INLET DAMPER / RECORD, DRAIN AND GREASE		Operations:		
6. D COMP BAGHOUSE INLET DAMPER / RECORD, DRAIN AND GREASE		Operations:		
7. E COMP BAGHOUSE INLET DAMPER / RECORD, DRAIN AND GREASE		Operations:		
8. F COMP BAGHOUSE INLET DAMPER / RECORD, DRAIN AND GREASE		Operations:		
9. G COMP BAGHDUSE INLET DAMPER / RECORD, DRAIN AND GREASE		Operations:		
10. H COMP BAGHOUSE INLET DAMPER / RECORD, DRAIN AND				
GREASE 11. J COMP BAGHOUSE INLET DAMPER / RECORD, DRAIN AND		Operations:		-
GREASE 12. K COMP BAGHOUSE INLET DAMPER / RECORD, DRAIN AND		Operations:		
GREASE 13. A COMP BAGHOUSE OUTLET DAMPER / RECORD. DRAIN AND		Operations:		
GREASE 14. B COMP BAGHOUSE OUTLET DAMPER / RECORD, DRAIN AND		Operations:		_
GREASE 15. C COMP BAGHOUSE OUTLET DAMPER / RECORD, ORAIN AND		Operations:		
GREASE 16. D COMP BAGHOUSE OUTLET DAMPER / RECORD, DRAIN		Operations:		_
AND GREASE 17. E COMP BAGHOUSE OUTLET DAMPER / RECORD, DRAIN AND		Operations:		
GREASE		Operations:		
18. F COMP BAGHOUSE OUTLET DAMPER / RECORD, DRAIN AND GREASE		Operations:		_
19. G COMP BAGHOUSE DUTLET DAMPER / RECORD, DRAIN AND GREASE		Operations:		_
20. H COMP BAGHOUSE OUTLET DAMPER / RECORD, DRAIN AND GREASE		Operations.		
21. J COMP BAGHOUSE OUTLET DAMPER / RECORD, DRAIN AND GREASE		Operations:		
22. K COMP BAGHOUSE OUTLET DAMPER / RECORD, DRAIN AND GREASE		Operations:		
23. A COMP REVERSE AIR DAMPER / RECORD, DRAIN AND GREASE		Operations:		
24 B COMP REVERSE AIR DAMPER / RECORD, DRAIN AND GREASE		Operations:		
25. C COMP REVERSE AIR DAMPER / RECORD, DRAIN AND GREASE		Operations:		
26. D COMP REVERSE AIR DAMPER / RECORD, DRAIN AND GREASE		Operations:		
27. E COMP REVERSE AIR DAMPER / RECORD, DRAIN AND	-			_
GREASE 28. F COMP REVERSE AIR DAMPER / RECORD, DRAIN AND		Operations:		
GREASE 29 G COMP REVERSE AIR DAMPER / RECORD, DRAIN AND		Operations:		-
GREASE 30. H COMP REVERSE AIR DAMPER / RECORD, DRAIN AND		Operations:	- <del> </del> .	-
GREASE 31. J COMP REVERSE AIR DAMPER / RECORD, DRAIN AND		Operations:		_
GREASE 32 K COMP REVERSE AIR DAMPER / RECORD, DRAIN AND		Operations:		
GREASE		Operations:		_
33. FABRIC FILTER / INSPECT AND CLEAN Comments (reference the item):		Operations:		
	1.0	tation - must be kept for five		

MONTHLY Envi	ironmental Do	cumentation - must keep for fi	ive years	
Baghouse Preventative Mantenance Monthly Ch Recordkeeping for the Startup, Shutdown, and Malfunction Pla				SSM-Form-018 Revision 1 11/04/2016
Instructions:				-2
1. Review all listed equipment each month.				
2. If issues are observed, initiate necessary actions to determine	the cause and c	orrect the issue. (Note the Work O	rder number if appliable)	
3. Submit completed forms to Environmental Manager.				
				Comments
Inspect the following monthly	Date	Name	Signature	below?
1. FABRIC FILTER / INSPECT AND CYCLE		Operations:		
2. FABRIC FILTER / INSPECT AND RECORD		Operations:		
3. FABRIC FILTER REVERSE AIR FAN / GREASE BEARINGS		Maintenance:		
4. REVERSE AIR RECIRC DAMPER / GREASE AND INSPECT		Operations:		
Comments (reference the item):				
				1
Environme	ntal Document	tation - must be kept for five y	ears	
entronnie		inter a construction and t		

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### Detroit Renewable Power Boiler Critical Spare Parts List

Item	Description	Critical
658	TROUGH, SIFTING SCREW TROUGH WITHOUT HOLE, 1/4" SA500 (375/425BHN) MATERIAL 62- 1/4" WITH (2) LEG BRACKETS PER DRAWING# 990046	А
666	EDDY PLATE NOZZLE, IGNITOR NOZZLE	A
673	HOSE, HYDRAULIC HOSE, 2-3/4", 18-8 SS ASO 3651	A
674	IGNITOR, SPARK PLUG, # IG-4727-AA	А
675	PLUG, FLAME ROD PLUG, FLAMEROD ASSEMBLY # 1G-6126	А
698	GASKET FOR OIL GUNS,1", CU # 1G-885	А
730	TIP, AIR NOZZLE TIP	А
3262	Chain, Grate Chain Power house Technology brand. 10 pitch sections ( 1each =10 link section) pt# PT2C 7570 - Assy, # 103118	А
6304	DETECTOR, PLUG CHUTE DETECTOR, D220-5-11L-5 SONAC	А
15074	BEARING, FLANGE BLOCK, 2" ID, 4 BOLT, F4B-E-200R, 023103, FOR SIFTING SCREWS	A
27768	AUGER, CONVEYOR, SIFTING SCREW, 5" DIA, 3-1/2" PITCH, 56" LG, 1/4" THK	А
35303	HIGH TEMP INSULATING GASKET/TAPE 2" X 1/8", 100' ROLL	A
35326	GLASS, BOILER SIGHT GLASS, 4-3/4" X 12-1/2" X 7/32",PYREX	A
35327	SHAFT, STUB SHAFT, 1-7/8" DIA FOR SIFTING SCREW CONNECTOR, SEE LONG DESCRIPTION	A
36348	PIN, GRATE BAR COTTER PIN,1-1/4" LG	A
36478	IGNITOR HOSE, HOSE, OIL/AIR, 1/4" ID 18" LG, 1/4" MPT E/E	Α
36718	WRITE OIL GUN LONG PIN REMOVABLE PART	Α
36917	GRATE BAR PIN, 3/4" X 5-3/8" LG,MILD CARBON, 2121CE-3C-608	А
40412	REFRACTORY - RC1118 - 50 LB. PAILS	A
41767	ASSEMBLY, MASTER PIN FOR 698 CHAIN	Α
65279	OVERFIRE AIR CYLINDER, LINEAR ACTUATING, PNEUMATIC, 3/4"-16 TPI FEMALE, V BLOCK, # P1AU- 10A4D-AAA0	A
65848	DRIVE, VARIABLE SPEED, 380V-460VAC 2.1A 3PH 50/60HZ 1.6KVA, # VF515-4007PL	А
66143	GRATE BAR ASSEMBLY, FULLY ASSEMBLED	А

and the second se		AAO SLAKER LOG 1		OG 1	DATE:			
1380 GPM / 1800 RPM								
LOW FLOW ALARM 480 GPM								
1A CONDENSATE PUMP	03:00	07:00	11:00	15:00	19:00	23:00		
DISCHARGE PSI	_							
			1999 AL. 1996-315	C.17				
IB CONDENSATE PUMP						_		
DISCHARGE PSI						1000		
IA CLOSED CYCLE COOLING				6-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1				
DISCHARGE PRESSURE								
OIL LEVEL								
1B CLOSED CYCLE COOLING	_							
DISCHARGE PRESSURE								
OIL LEVEL								
600 GPM/1750 RPM	1							
1A BUILDING HEAT PUMP	-				· · · ·			
DISCHARGE PRESSURE								
SYSTEM TEMPERATURE								
EXSPANSION TANK LEVEL						Badda Bada		
IB BUILDING HEAT PUMP								
DISCHARGE PRESSURE								
DIL LEVEL								
SYSTEM TEMPERATURE					1			
EXSPANSION TANK LEVEL					1.1.1			
IA AIR COMPRESSOR 790 cfm								
I.P. AIR TEMP OUT 180 F MAX				- THE R. L.				
DIL TEMPERATURE 158 F MAX						- 6 - C		
DIL PRESSURE 20 PSIG MIN				II				
DIL LEVEL								
NATER TEMPERATURE								
AIR DISCHARGE TEMPERATURE						-		
AIR FILTER DIFFERENTIAL								
AIR DISCHARGE PSI 100 PSIG								
IB AIR COMPRESSOR 790 cfm				8559				
I.P. AIR TEMP OUT 180 F MAX								
DIL TEMPERATURE 158 F MAX				-				
DIL PRESSURE 20 PSIG MIN		140 M						
DIL LEVEL								
NATER TEMPERATURE								
AIR DISCHARGE TEMPERATURE								
AIR FILTER DIFFERENTIAL								
AIR DISCHARGE PSI 100 PSIG	-					-		
IC AIR COMPRERSSOR (JOY)1025cfm					5			
NJECTION TEMPERATURE 40-60 F								
DISCHARGE AIR TEMPERATURE 100 F								
DISCHARGE AIR PRESSURE 110 PSI								
DIL LEVEL								

DAY SHIFT' SIGNATURE

NIGHT SHIFT 'SIGNATURE:

TA DEMIN BOOSTER PUMP       03.00       07:         DISCHARGE PRESSURE       Image: Constraint of the system of th	11:00	15:00	19.00	23 00
OIL LEVEL       IB DEMIN BOOSTER PUMP       DISCHARGE PRESSURE       OIL LEVEL       B70 GPM / 3560 RPM       L.O. TEMP ALARM 170F TRIP 180F       1A BOILER FEED PUMP       DISCH PSI 1118 PSI       SUCT PSI 145 PSI       LO TEMP 120-140 F       COOLER WATER OUTLET TEMP       LUBE OIL LEVEL CAP 35 GL       LUBE OIL LEVEL       AUXILLIARY LO PMP PSI       SUCT PSI 1118 PSI       SUCT PSI 1118 PSI       BARING OIL LEVEL       AUXILLIARY LO PMP PSI       SUCT PSI 1118 PSI       SUCT ION STRAINER DP       LUBE OIL LEVEL       AUXILLIARY LO PMP PSI       SUCTION STRAINER DP       ID TEMP 120-140 F       COOLER WATER OUNOFF       AUXILLIARY LO PMP PSI       SUCTION STRAINER DP       ID EDILER FEED PUMP       DISCH PSI 1118 PSI       SUCT PSI 145 PSI				
1B DEMIN BOOSTER PUMP         DISCHARGE PRESSURE         OIL LEVEL         870 GPM / 3560 RPM         L.O. TEMP ALARM 170F TRIP 180F         1A BOILER FEED PUMP         DISCH PSI 1118 PSI         SUCT PSI 145 PSI         LO TEMP 120-140 F         COOLER WATER OUTLET TEMP         LUBE OIL LEVEL CAP 35 GL         LUBE OIL LEVEL         AUXILLIARY LO PMP ON/OFF         AUXILLARY LO PMP PSI         SUCT PSI 145 PSI         BOILER FEED PUMP         DISCH PSI 1118 PSI         SUCTION STRAINER DP         1B BOILER FEED PUMP         DISCH PSI 1118 PSI         SUCTION STRAINER DP         1B BOILER FEED PUMP         DISCH PSI 1118 PSI         SUCT PSI 145 PSI         LO TEMP 120-140 F         COOLER WATER OUTLET TEMP         LUBE OIL LEVEL CAP 35 GL         LUBE OIL LEVEL CAP 35 GL         LUBE OIL LEVEL         AUXILLIARY LO PMP ON/OFF         AUXILLIARY LO PMP ON/OFF         DISCH PSI 1118 PSI         SUCT PSI 145 PSI         BEARING OIL LEVEL         AUXILLIARY LO PMP ON/OFF         AUXILLIARY LO PMP ON/OFF         DISCH PSI 1118 PSI         SU				_
DISCHARGE PRESSURE OIL LÉVEL OIL LÉVEL S70 GPM / 3560 RPM L.O. TEMP ALARM 170F TRIP 180F 1 A BOILER FEED PUMP DISCH PSI 1118 PSI SUCT PSI 145 PSI LO TEMP 120-140 F COOLER WATER OUTLET TEMP LUBE OIL LEVEL CAP 35 GL LUBE OIL LEVEL AUXILLIARY LO PMP ON/OFF AUXILLARY LO PMP PSI SUCTION STRAINER DP DISCH PSI 1118 PSI SUCT PSI 145 PSI LO TEMP 120-140 F COOLER WATER OUTLET TEMP LUBE OIL LEVEL CAP 35 GL LUBE OIL EVEL AUXILLARY LO PMP PSI SUCTION STRAINER DP DISCH PSI 1118 PSI SUCT PSI 145 PSI BEARING OIL LEVEL AUXILLARY LO PMP PSI SUCT PSI 145 PSI LO TEMP 120-140 F COOLER WATER OUTLET TEMP LUBE OIL LEVEL AUXILLIARY LO PMP ON/OFF AUXILLIARY LO PMP ON/OFF AUXILLIARY LO PMP PSI SUCT PSI 145 PSI BEARING OIL LEVEL AUXILLIARY LO PMP PSI SUCTION STRAINER DP TO SUCH PSI 1118 PSI SUCTION STRAINER DP TO SUCT PSI 1118 PSI SUCTION STRAINER DP TO SUCT PSI 1118 PSI SUCT PSI 145 PSI LO TEMP 120-140 F COOLER WATER OUTLET TEMP LUBE OIL LEVEL CAP 35 GL		1		
OIL LEVEL  OIL LEVEL  S70 GPM / 3560 RPM  L.O. TEMP ALARM 170F TRIP 180F  1A BOILER FEED PUMP  DISCH PSI 1118 PSI SUCT PSI 145 PSI LO TEMP 120-140 F  COOLER WATER OUTLET TEMP LUBE OIL LEVEL CAP 35 GL  UBE OIL LEVEL AUXILLIARY LO PMP ON/OFF AUXILLARY LO PMP PSI SUCT PSI 1118 PSI SUCT PSI 1118 PSI SUCT PSI 1118 PSI SUCT PSI 145 PSI LO TEMP 120-140 F  COOLER WATER OUTLET TEMP LUBE OIL LEVEL AUXILLIARY LO PMP ON/OFF AUXILLARY LO PMP PSI SUCT PSI 145 PSI SUCT PSI 145 PSI LO TEMP 120-140 F  COOLER WATER OUTLET TEMP LUBE OIL LEVEL AUXILLIARY LO PMP ON/OFF AUXILLARY LO PMP ON/OFF AUXILLARY LO PMP PSI SUCT PSI 145 PSI SUCT PSI 15 PSI BEARING OIL LEVEL AUXILLIARY LO PMP ON/OFF AUXILLIARY LO PMP ON/OFF AUXILLIARY LO PMP PSI SUCTION STRAINER DP  COOLER WATER OUTLET TEMP LUBE OIL LEVEL AUXILLIARY LO PMP PSI SUCT PSI 1118 PS				
870 GPM / 3560 RPM         L.O. TEMP ALARM 170F TRIP 180F         1A BOILER FEED PUMP         DISCH PSI 1118 PSI         SUCT PSI 145 PSI         LO TEMP 120-140 F         COOLER WATER OUTLET TEMP         LUBE OIL LEVEL CAP 35 GL         LUBE OIL LEVEL CAP 35 GL         AUXILLIARY LO PMP ON/OFF         AUXILLARY LO PMP PSI         SUCT PSI 1118 PSI         SUCTION STRAINER DP         1B BOILER FEED PUMP         DISCH PSI 1118 PSI         SUCT PSI 145 PSI         LO TEMP 120-140 F         COOLER WATER OUTLET TEMP         LUBE OIL LEVEL CAP 35 GL         LUBE OIL LEVEL CAP 35 GL         LUBE OIL LEVEL CAP 35 GL         LUBE OIL LEVEL         AUXILLIARY LO PMP ON/OFF         AUXILLIARY LO PMP ON/OFF         AUXILLARY LO PMP ON/OFF         AUXILLIARY LO PMP ON/OFF         AUXILLIARY LO PMP PSI         SUCTION STRAINER DP         1C BOILER FEED PUMP         DISCH PSI 1118 PSI         SUCTION STRAINER DP         1C BOILER FEED PUMP         DISCH PSI 1118 PSI         SUCT PSI 145 PSI         LO TEMP 120-140 F         COOLER WATER OUTLET TEMP         LO TEMP 120-140 F <td></td> <td></td> <td></td> <td></td>				
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1B BOILER FEED PUMP         DISCH PSI 1118 PSI         SUCT PSI 145 PSI         LO TEMP 120-140 F         COOLER WATER OUTLET TEMP         LUBE OIL LEVEL CAP 35 GL         LUBE OIL LEVEL CAP 35 GL         AUXILLIARY LO PMP ON/OFF         AUXILLIARY LO PMP PSI         SUCTION STRAINER DP         DISCH PSI 1118 PSI         SUCT PSI 145 PSI         LO TEMP 120-140 F         COOLER WATER OUTLET TEMP         LUBE OIL LEVEL         AUXILLIARY LO PMP PSI         SUCTION STRAINER DP         10 EON FSI 1118 PSI         SUCT PSI 145 PSI         LO TEMP 120-140 F         COOLER WATER OUTLET TEMP         LUBE OIL LEVEL CAP 35 GL				
DISCH PSI 1118 PSI SUCT PSI 145 PSI LO TEMP 120-140 F COOLER WATER OUTLET TEMP LUBE OIL LEVEL CAP 35 GL LUBE OIL PSI 15 PSI BEARING OIL LEVEL AUXILLIARY LO PMP ON/OFF AUXILLIARY LO PMP PSI SUCTION STRAINER DP 1C BOILER FEED PUMP DISCH PSI 1118 PSI SUCT PSI 145 PSI LO TEMP 120-140 F COOLER WATER OUTLET TEMP LUBE OIL LEVEL CAP 35 GL				
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LUBE OIL PSI 15 PSI         BEARING OIL LEVEL         AUXILLIARY LO PMP ON/OFF         AUXILLIARY LO PMP PSI         SUCTION STRAINER DP         1C BOILER FEED PUMP         DISCH PSI 1118 PSI         SUCT PSI 145 PSI         LO TEMP 120-140 F         COOLER WATER OUTLET TEMP         LUBE OIL LEVEL CAP 35 GL				
BEARING OIL LEVEL AUXILLIARY LO PMP ON/OFF AUXILLIARY LO PMP ON/OFF AUXILLIARY LO PMP PSI SUCTION STRAINER DP IC BOILER FEED PUMP DISCH PSI 1118 PSI SUCT PSI 1118 PSI SUCT PSI 145 PSI LO TEMP 120-140 F COOLER WATER OUTLET TEMP LUBE OIL LEVEL CAP 35 GL				
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SUCTION STRAINER DP				
1C BOILER FEED PUMP         DISCH PSI 1118 PSI         SUCT PSI 145 PSI         LO TEMP 120-140 F         COOLER WATER OUTLET TEMP         LUBE OIL LEVEL CAP 35 GL				
DISCH PSI 1118 PSI SUCT PSI 145 PSI LO TEMP 120-140 F COOLER WATER OUTLET TEMP LUBE OIL LEVEL CAP 35 GL				
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LO TEMP 120-140 F COOLER WATER OUTLET TEMP LUBE OIL LEVEL CAP 35 GL		1.		
COOLER WATER OUTLET TEMP LUBE OIL LEVEL CAP 35 GL				
LUBE OIL LEVEL CAP 35 GL			-	
LUBE OIL PSI 15 PSI				
BEARING OIL LEVEL				
AUXILLIARY LO PMP ON/OFF				
AUXILLART LO PMP PSI		-		
SUCTION STRAINER DP	1			
COMMENTS	COMMENTS			

DAY SHIFT SIGNATURE

11

NIGHT SHIFT SIGNATURE

		AAO	OG 3	DATE:		
17,650 gpm/ 885 rpm 1/2 CAP.	02.00	07.00	44-00	15:00	10-00	22.00
CIRCULATING WATER PUMP IA	03:00	07:00	11:00	15:00	19:00	23:00
DISCHARGE PSI						
SEAL WATER PSI						
CIRCULATING WATER PUMP IB	1					
DISCHARGE PSI						
SEAL WATER PSI					14 m	
UPPER OIL LEVEL						
LOWER OIL LEVEL						
CIRC WATER HEAT EXCHANGER						
EAST DIFF PSI						
WEST DIFF PSI					1	
SERVICE WATER PUMPS						
DISCHARGE PSI						
4001 OIL LEVEL ON/OFF						
4002 OIL LEVEL ON/OFF					•	
4003 OIL LEVEL ON/OFF						
CT VACUUM PMP 1A						
SEAL WATER PSI						
INCHES Hg						
CT VACUUM PMP 1B			L			
SEAL WATER PSI				1		
NCHES Hg.						
15 HP/3535RPM 70 GPM			Long			
FUEL OIL PUMP 1A				1	-	
DISCHARGE PRESSURE 245PSIG					11	
FUEL OIL PUMP 1B						
DISCHARGE PRESSURE 245 PSIG		1910-191-191	1		1	
FUEL OIL TANK LEVEL CAP 500,000						

COMENTS:

NIGHT SHIFT SIGNATURE

COMMENTS:

			AAC	SL/	AKEF	LO	G 4		DAT	E:		
11 SDA PENTHOUSE	03:	00	07:	:00	11:	00	15:	00	19:	00	23	00
OIL SUMP LEVEL 1/2 - 3/4		1 TT		1 Section					5 54	-	1 million	
OIL TEMP. 100 - 140			1		12		A DESCRIPTION OF		-			
SEAL AIR PRESSURE 35 - 45	1			1	10	100			-			1
SEAL AIR CFM 2 - 5						-	1		1	1	1	-
SLURRY HEAD TANK OVERFLOWING	YES	NO	YES	NO	YES	NO	YES	NO	YES	NO	YES	NO
DIL. WATER HEAD TANK OVERFLOWING	YES	NO	YES	NO	YES	NO	YES	NO	YES	NO	YES	NO
12 SDA PENTHOUSE	00:	00	04:	:00	08	00	12:	00	16:	00	20:	:00
DIL SUMP LEVEL 1/2 - 3/4							10		1			
OIL TEMP. 100 - 140				1	10		15		1.00			
SEAL AIR PRESSURE 35 - 45	1000						1000	-				-
SEAL AIR CFM 2-5	1 200						1				1.00	
SLURRY HEAD TANK OVERFLOWING	YES	NO	YES	NO	YES	NO	YES	NO	YES	NO	YES	NO
DIL. WATER HEAD TANK OVERFLOWING	YES	NO	YES	NO	YES	NO	YES	NO	YES	NO	YES	NO
13 SDA PENTHOUSE											1	-
OIL SUMP LEVEL 1/2 - 3/4	1	-			11-4		19-10-1		5			
OIL TEMP. 100 - 140	107-1				10		12					
SEAL AIR PRESSURE 35 - 45		1			1		5.10		1	-		
SEAL AIR CFM 2-5	1		5		-				1000			
SLURRY HEAD TANK OVERFLOWING	YES	NO	YES	NO	YES	NO	YES	NO	YES	NO	YES	NO
DIL. WATER HEAD TANK OVERFLOWING	YES	NO	YES	NO	YES	NO	YES	NO	YES	NO	YES	NO
SLURRY PUMP							6		Contra-		3 T	-
#1 SEAL WATER PRESSURE					12.8		1.000				100.000	200
#1 DISCHARGE PRESSURE	-						-			2.02		
#2 SEAL WATER PRESSURE							and a second sec		-			
#2 DISCHARGE PRESSURE							-		-			
#3 SEAL WATER PRESSURE				incire.								
#3 DISCHARGE PRESSURE					-		12	-				
#4 SEAL WATER PRESSURE		-			1		12				-	1
#4 DISCHARGE PRESSURE					1			-	1	-		1
#5 SEAL WATER PRESSURE												
#5 DISCHARGE PRESSURE					101							
DILUTION WATER PUMP 180 gpm					1		174					
4001 SEAL WATER PSI 85 PSI		1										
4001 DISCH PSI				1								
4001 OIL LEVEL 1/2 - FULL	3			- 15			-					
4002 SEAL WATER PSI 85 PSI												
4002 DISCH PSI		1							1	-		1
4002 OIL LEVEL 1/2 - FULL					1.			_				1
Slurry Specific Gravity				- 19			100		15			1.1

COMMENTS:

COMMENTS:

DAY SHIFT' SIGNATURE:

NIGHT SHIFT 'SIGNATURE:

		AO GRATE	LOG 1		DATE:	
BOILER 11	03 00	07:00	11:00	15:00	19.00	23:00
RIGHT UNDERGRATE AIR DAMPER POSITION						1
LEFT UNDERGRATE AIR DAMPER POSITION						
ZONE 1 N/S PLENUM 15%						
ZONE 2 N/S PLENUM DAMPER 90%		1	1			
ZONE 3 N/S PLENUM DAMPER 90%		1				1
ZONE 4 N/S PLENUM DAMPER 90%		1				1
ZONE 5 N/S PLENUM DAMPER 15-45%						1
11-A GRATE DRIVE % TORQUE SETTING						1
11-B GRATE DRIVE % TORQUE SETTING						1
Grate Speed (Every 2 Hours)					1	
Fuel Bed HeightChecked (Every 2 hours)		1	1		1	
PDA PRESSURE 15-25"						
SSC LEVEL						
SSC HYDRAULIC DRIVE OIL LEVEL		-	1			
SEAL TROUGH LEVEL						
BOILER PRESSURE		-		l		
NORTH GRATE DRIVE LEVEL OIL NORMAL						
SOUTH GRATE DRIVE LEVEL OIL NORMAL						
11 SLOPES CLEANED		1	<u> </u>			
11 HOPPERS BAYS 1 THROUGH 6 CLEAR		1	1	!		L .
Boller 12			1			
RIGHT UNDERGRATE AIR DAMPER POSITION						
LEFT UNDERGRATE AIR DAMPER POSITION						
ZONE 1 N/S PLENUM 15%						
ZONE 2 N/S PLENUM DAMPER 90%						
ZONE 3 N/S PLENUM DAMPER 90%						
ZONE 4 N/S PLENUM DAMPER 90%						
ZONE 5 N/S PLENUM DAMPER 15-45%						
12-A GRATE DRIVE % TORQUE SETTING						
12-B GRATE DRIVE % TORQUE SETTING						
PDA PRESSURE 15-25"		1			1	
Grate Speed (Every 2 Hours)			1		1	
Fuel Bed HeightChecked (Every 2 hours)						
SSC LEVEL				1		
SSC HYDRAULIC DRIVE OIL LEVEL					<u> </u>	
SEAL TROUGH LEVEL		1	1			
BOILER PRESSURE						
NORTH GRATE DRIVE OIL LEVEL NORMAL	16 Te					
SOUTH GRATE DRIVE OIL LEVEL NORMAL		-				
12 SLOPES CLEANED		-		<u> </u>		
12 HOPPERS BAYS 1 THROUGH 6 CLEAR						<u> </u>
BOILER 13						I
		1				
RIGHT UNDERGRATE AIR DAMPER POSITION						
LEFT UNDERGRATE AIR DAMPER POSITION				<u> </u>		
ZONE 1 N/S PLENUM 15%		_				ļ
ZONE 2 N/S PLENUM DAMPER 90%						L
ZONE 3 N/S PLENUM DAMPER 90%					<u> </u>	
ZONE 4 N/S PLENUM DAMPER 90%						
ZONE 5 N/S PLENUM DAMPER 15-45%						
13-A GRATE DRIVE % TORQUE SETTING				-		
13-B GRATE DRIVE % TORQUE SETTING						
PDA PRESSURE 15-25"			_			
Grate Speed (Every 2 Hours)						
Fuel Bed HeightChecked (Every 2 hours)						
SSC LEVEL			7.4572 B. 17.4			1
SSC HYDRAULIC DRIVE OIL LEVEL				-		
SEAL TROUGH LEVEL				<u> </u>		
BOILER PRESSURE		1	1		1	1
		1	1	<u> </u>	1	
NORTH GRATE DRIVE OIL LEVEL NORMAL		1	1	1	1	
NORTH GRATE DRIVE OIL LEVEL NORMAL				-		
SOUTH GRATE DRIVE OIL LEVEL NORMAL SOUTH GRATE DRIVE OIL LEVEL NORMAL 13 SLOPES CLEANED						

AO GRATE LOG 2

DATE:

# 4 FEEDWATER HEATER	03:00	07:00	11:00	15:00	19:00	23 00
FEEDWATER INLET TEMP			Ì		1	
EEDWATER OUTLET TEMP 350F						
EXTRACTION			-			
WATER LEVEL			1			
3 FEEDWATER CAP 18,000 gl.						
PRESSURE 114.5 pslg		1	Ĩ			
VATER LEVEL 80"			<u> </u>			
COND. INLET TEMP			1			
FEEDWATER OUTLET TEMP						
ECTRACTION		1	1			
2 FEEDWATER HEATER						
WATER LEVEL			1			
COND. INLET TEMP 202 F			1			
COND. OUTLET TEMP 274 F					- N.	
EXTRACTION						
1 FEEDWATER HEATER				100		
WATER LEVEL		1	T			
NLET TEMP 120 F		1				
DUTLET TEMP 202 F			1			
EXTRACTION			1			
MAKE UP DA PRESSURE 2.5 PSIA						
GLAND SEAL COND. PUMP 1A ON/OFF						
GLAND SEAL COND. PUMP 1B ON/OFF						
AIR DRYER DEW POINT			1			
COMMENTS		_	COMMENT	S:		
Sector and the		- C				
						(a)
		•				-
	0	-	-		1	

DAY SHIFT SIGNATUE

**NIGHT SHIFT SIGNATURE** 

BOILER #\_\_\_\_

### MICHIGAN WASTE ENERGY

DATE:\_\_

Michigan Waste Energy Control Room Log

	Operator					
	0000	0400	0800	1200	1600	2000
Steam Flow 1000#/hr						
Feedwater Flow 1000#/hr						
Boiler Outlet Steam Temp º F						
Excess O2 %				·	1	
#4 Feedwater Outlet Temp ° F						
Drum Pressure PSIG		- 6			1	_
OFA Damper Position			E.			
Forced Draft Fan Amps						
Induced Draft Fan Amps						
Boiler Outlet Steam Press PSIG					1	
Combustion Air Flow (Total) CFM	Λ				1	
UFA Pressure			13 G <del>E</del> C			
UFA Temperature ° F			- 15			
OFA Pressure						
Furnace Pressure						
Attemporator Outlet Temp ° F						
SDA Differential						
SDA inlet Temp oF						
Econo Gas Outlet Temp ° F						
AH Gas Outlet Temp ° F						
AH Air Inlet Temp ° F						1-
AH Air Outlet Temp ° F						
Roof Temp ° F						
Baghouse DP						
Process Steam Flow						
T/G Megawatts			1.1			

BOILER #\_\_\_\_

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# MICHIGAN WASTE ENERGY

DATE:

	Operator					
	0100	0500	0900	1300	1700	2100
Steam Flow 1000#/hr				[]	·	
Feedwater Flow 1000#/hr						
Boiler Outlet Steam Temp °F		4				
Excess O2 %		-				
#4 Feedwater Outlet Temp ° F						
Drum Pressure PSIG			ei.			
OFA Damper Position						
Forced Draft Fan Amps		<u> </u>		· · · · · · · · · · · · · · · · · · ·		
Induced Draft Fan Amps						
Boiler Outlet Steam Press PSI	G		~~			
Combustion Air Flow (Total) C	FM					
UFA Pressure						
UFA Temperature P F				;	- I H	-
OFA Pressure	2		_	1		
Furnace Pressure	- A.	8			1	
Attemporator Outlet Temp ° F		1				
Opacity %						
PDA Fan On/Off			_			F
Econo Gas Outlet Temp <sup>o</sup> F						
AH Gas Outlet Temp ° F						£
AH Air Inlet Temp <sup>°</sup> F						
AH Air Outlet Temp <sup>©</sup> F						
Grate Temp (Highest) °F	<ul> <li>1</li> </ul>			-		
Baghouse DP						
Process Steam Flow	1	L				
T/G Megawatts						(a
Cameras		1-6-61				