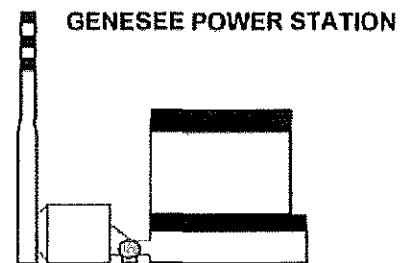


**Air Emission Test  
for  
EU-BOILER**

**Genesee Power Station  
Limited Partnership  
G-5310 North Dort Highway  
Flint, Michigan**



**Renewable Operating Permit N3570-2012  
State Registration No. N3570**

**Prepared for  
Genesee Power Station Limited Partnership  
Flint, Michigan**

Bureau Veritas Project No. 11016-000080.00  
August 22, 2016

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## Executive Summary

Genesee Power Station Limited Partnership retained Bureau Veritas North America, Inc. to perform air emissions testing at the Genesee Power Station renewable energy power plant in Flint, Michigan. Air emissions from the boiler exhaust (Emission Unit ID: EU-BOILER) were tested from exhaust stack SVBOILER. Genesee Power Station provides electricity to the Midwest Independent Transmission Operator (MISO). Genesee Power Station can produce up to approximately 35 megawatt-hours of electricity.

The purpose of the testing was to:

- Measure hydrogen chloride (HCl), mercury (Hg), and filterable particulate matter (PM) concentrations and mass emission rates.
- Evaluate compliance with (1) Michigan Department of Environmental Quality (MDEQ) Renewable Operating Permit (ROP) MI-ROP-N3570-2012, dated August 24, 2012, and (2) 40 CFR Part 63, Subpart DDDDD, “National Emission Standards for Hazardous Air Pollution for Major Sources: Industrial, Commercial, and Institutional Boilers and Process Heaters.”

The testing followed United States Environmental Protection Agency (USEPA) Reference Methods 1, 2, 3A, 4, 5, 19, 26A, 29. Three 120-minute test runs were completed to measure PM and Hg concentrations and mass emission rates, and three 60-minute test runs were completed to measure HCl concentrations and mass emission rates.

Detailed results are presented in Tables 1 and 2 after the Tables Tab of this report. The following table summarizes the results of the testing conducted on July 19 and 20, 2016.



### EU-BOILER Air Emissions Test Results

Parameter	Units	Run 1	Run 2	Run 3	Average Result	Permit Limit	40 CFR Part 63 Subpart DDDDD Emission Limits
Filterable Particulate Matter (PM)	lb/hr	0.63	0.54	0.56	0.57	15.7	—
	lb/MMBtu	0.0012	0.0010	0.0011	0.0011	0.03	0.037
Mercury (Hg)	lb/hr	0.00016	0.00024	0.00019	0.00020	0.0047	—
	lb/MMBtu	$3.1 \times 10^{-7}$	$4.5 \times 10^{-7}$	$3.6 \times 10^{-7}$	$3.7 \times 10^{-7}$	$9 \times 10^{-6}$	$5.7 \times 10^{-6}$
Hydrogen Chloride (HCl)	lb/hr	8.5	3.2	3.9	5.2	47.1	—
	lb/MMBtu	0.016	0.0061	0.0079	0.010	0.09	0.022

lb/hr: pound per hour

lb/MMBtu: pound per million British thermal unit

The results of the testing indicate compliance with the applicable EU-BOILER permit limits listed in the table.



# 1.0 Introduction

## 1.1 Summary of Test Program

Genesee Power Station Limited Partnership retained Bureau Veritas North America, Inc. to perform air emissions testing at the Genesee Power Station renewable energy plant in Flint, Michigan. Air emissions from the boiler exhaust (Emission Unit ID: EU-BOILER) were tested at the exhaust stack SVBOILER. Genesee Power Station provides electricity to the Midwest Independent Transmission Operator (MISO). Genesee Power Station can produce up to approximately 35 megawatt-hours of electricity.

The purpose of the testing was to:

- Measure hydrogen chloride (HCl), mercury (Hg), and filterable particulate matter (PM) concentrations and mass emission rates.
- Evaluate compliance with (1) Michigan Department of Environmental Quality (MDEQ) Renewable Operating Permit (ROP) MI-ROP-N3570-2012, dated August 24, 2012, and (2) 40 CFR Part 63, Subpart DDDDD, "National Emission Standards for Hazardous Air Pollution for Major Sources: Industrial, Commercial, and Institutional Boilers and Process Heaters."

The Intent-to-Test Plan was submitted to MDEQ on March 30, 2016, and approved on May 3, 2016. Tire-derived fuel (TDF) and wood biomass were used during the testing. This report summarizes the results of the testing performed on July 19 and 20, 2016 (see Table 1-1).

**Table 1-1**  
**Source Tested, Parameters, and Test Dates**

Source	Parameter	Test Date
EU-BOILER Exhaust	Mercury (Hg)	July 19, 2016
	Filterable particulate matter (PM)	July 19, 2016
	Hydrogen chloride (HCl)	July 19 and 20, 2016



## 1.2 Key Personnel

Key personnel involved in this test program are listed in Table 1-2. Mr. Kenneth A. DesJardins, General Manager, and Mr. Mitchell Hefner, Environmental Health and Safety Technician, with Genesee Power Station, provided process coordination and arranged for facility operating parameters to be recorded. The testing was coordinated with Mr. David Patterson, Environmental Quality Analyst with MDEQ.

**Table 1-2  
Key Personnel**

<b>Genesee Power Station</b>	<b>Bureau Veritas North America, Inc.</b>
Kenneth A. DesJardins General Manager <b>Genesee Power Station Limited Partnership</b> 5315 Energy Drive Flint, Michigan 48505 Telephone: 810.785.4144 x2222 Facsimile: 810.785.7836 ken.desjardins@cmsenergy.com  Mitchell R. Hefner Environmental Health and Safety Technician <b>Genesee Power Station Limited Partnership</b> G-5310 North Dort Highway Flint, Michigan 48505 Telephone: 810.785.4144 x 224 Facsimile: 810.785.7836 michell.hefner@cmsenergy.com	Brian P. Young Senior Project Manager <b>Bureau Veritas North America, Inc.</b> 22345 Roethel Drive Novi, Michigan 48375 Telephone: 248.344.3020 Facsimile: 248.344.2656 brian.young@us.bureauveritas.com
<b>Michigan Department of Environmental Quality</b>	
David Patterson Environmental Quality Analyst <b>Michigan Department of Environmental Quality</b> Air Quality Division—Technical Programs Unit Constitution Hall 2 <sup>nd</sup> Floor South Tower 525 West Allegan Street Lansing, Michigan 48909 Telephone: 517.284.6782 Facsimile: 517.355.3122 pattersond2@michigan.gov	Julie Brunner Senior Environmental Engineer <b>Michigan Department of Environmental Quality</b> Air Quality Division—Technical Programs Unit Constitution Hall 2 <sup>nd</sup> Floor South Tower 525 West Allegan Street Lansing, Michigan 48909 Telephone: 517.284.6789 Facsimile: 517.355.3122 brunnerj1@michigan.gov

## 2.0 Source and Sampling Locations

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### 2.1 Process Description

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Genesee Power Station operates a renewable energy power plant that can produce up to 35 megawatts of electricity using (1) an ABB Combustion Engineering VU-40 traveling-grate-spreader-stoker boiler rated at 523 million British thermal units per hour (MMBtu/hr) and (2) an ABB single-flow condensing turbine coupled to an ABB synchronous generator unit. The power plant has been in operation since 1995 and is permitted to fire wood biomass, TDF (up to 20 tons per day), and natural gas for startup.

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During testing, the boiler was fired with wood biomass and TDF.

The wood biomass is transported to the Genesee Power Station via trucks and unloaded into the 7-acre wood yard using a truck tipper (Figure 2-1). The wood biomass is stored in piles that are rotated using front-end loaders to prevent decay, achieve uniform moisture content, and prevent pile fires. Once the wood has achieved the desired characteristics, front-end loaders load wood into a hopper that conveys the wood to the boiler feeders.



**Figure 2-1. Wood biomass unloading**

Wood is gravity-fed into the feeders and introduced into the boiler at injection points. As the wood and air enter the boiler, the wood rapidly ignites and is combusted, producing heat.

The heat generated increases the temperature of water-filled tubes inside the boiler and produces steam. The steam in the tubes rises and enters a boiler steam drum, where liquid water and vapor are separated. The liquid in the boiler drum is recycled into the boiler tubes for re-heating, while the steam from the drum is sent through tubes positioned in the location of the boiler with the highest temperature for superheating. The high-pressure, superheated steam rotates a turning gear for a turbine-generator unit to generate electricity. After propelling the turning gear, the steam is (1) directed into the boiler or (2) passed through a condenser to be recaptured as liquid and recycled into the boiler.

The ash from the combustion of wood biomass falls to the bottom of the boiler onto a sloped grate. The sloped grate vibrates at set intervals to migrate the ash into a water trough. A screw conveyor moves the ash from the water trough into a storage bin; the ash is sent to a landfill.



The boiler combustion air (flue gas) that is used to heat the boiler tubes, the boiler drum, and superheater is ducted through an economizer, which pre-heats new boiler feed water that is continually added to the system. The flue gas is also used to pre-heat combustion air (blown in with the wood biomass) prior to being ducted into a mechanical multi-clone separator and electrostatic precipitator (ESP). Fly ash is then disposed of to a landfill.

The electricity production rate recorded during testing is presented in Table 2-1.

**Table 2-1  
Electrical Generation During Testing**

<b>Run</b>	<b>Electricity Generation (megawatt)</b>
<b>Methods 5 and 29</b>	
1	35
2	35
3	35
<b>Method 26A</b>	
1	35
2	35
3	36
<b>Average</b>	<b>35</b>

Genesee Power Station personnel recorded operating parameters during the emission testing. The recorded operating parameters provided to Bureau Veritas are included in Appendix F.

## 2.2 Control Equipment

A selective non-catalytic reduction (SNCR) system is used to reduce nitrogen oxide emissions. The SNCR system injects a mist of blended urea and water into the upper sections of the boiler furnace to reduce nitrogen oxide emissions to nitrogen, carbon dioxide, and water. As the flue gas exits the furnace, particles are captured in a series of multi-cyclones.

Cyclones use centrifugal force to remove particles from the gas stream. Particles enter at a high velocity and travel along the cyclone body where the centrifugal force and gravity cause the particles to travel down tapered walls and into a hopper at the bottom. The treated gas exits a tube at the top of the cyclone. Multi-cyclones are used in series to improve particle collection efficiency. Additional particulate matter removal occurs in the ESP (Figure 2-2).

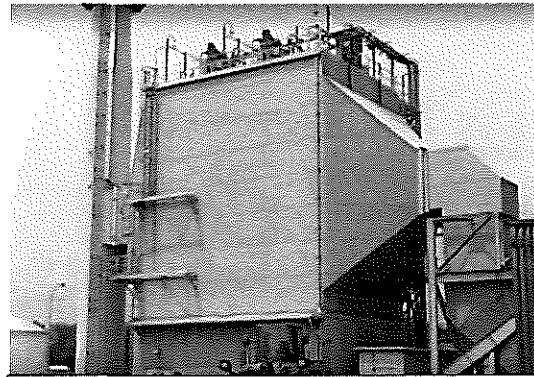


Figure 2-2. ESP

The ESP applies a voltage to generate an electrostatic charge on rows of vertically hung collection plates, which attract particulate matter in the flue. By using a series of plate rappers, the particulate matter is released from the plates and collected at the bottom of the ESP in a hopper. The collected fly ash is pneumatically conveyed to a storage bin; the ash is sent to a landfill. After the air passes through the ESP it is ducted through an induced draft fan that exhaust the flue gas through a 94-inch-diameter, 220-foot-tall stack.

## 2.3 Operating Parameters

Operating parameters for the wood-waste boiler pollution control equipment are monitored by operators in the control room. Continuous emissions monitoring systems (CEMS) are used to monitor select flue gas exhaust parameters to evaluate permit compliance. Operating parameters recorded by CEMS for EU-BOILER include the following:

- Opacity (%)
- Flowrate (kscfm = 1,000s of scfm)
- Sulfur dioxide, SO<sub>2</sub> (ppmvd)
- Oxides of nitrogen, NO<sub>x</sub> (ppmvd)
- Oxygen, O<sub>2</sub> (% , dry)
- Carbon monoxide, CO (ppmvd)





Process data recorded during testing are included in Appendix F. Genesee Power Station informed Bureau Veritas that the clock times of the process data in the printed copy provided by Genesee Power Station are one hour earlier than the actual times of the data recording.

## 2.4 Materials Processed During Tests

The facility typically processes wood biomass, but is also capable of combusting a blend of wood biomass and TDF. Wood biomass is mixed in the wood yard prior to being combusted in the boiler. Air emissions from the fire of the wood biomass and TDF were tested during this study. In addition, Genesee Power Station personnel collected samples of the fuel for analysis. Analytical results of the fuel analysis are included in Appendix F.

## 2.5 Rated Capacity of Process

The boiler is nominally rated at 523 MMBtu/hr and the turbine generator can produce approximately 35 megawatts of electricity.

The power station has the ability to produce approximately 290,000 megawatt-hours annually.

## 2.6 Flue Gas Sampling Location

A description of the source tested is presented in Table 2-3.

**Table 2-2  
Emission Unit Identification**

Emission Unit ID	Emission Unit Description	Stack Identification
EU-BOILER	35-MW electric generation group consists of the wood waste boiler, a selective non-catalytic reduction (SNCR) system, a mechanical multi-clone separator (MMS), and an electrostatic precipitator (ESP). The boiler has a spreader-stoker design and is rated at 523 MMBtu/hr, and able to produce 345,000 pounds of steam per hour.	SVBOILER

A description of the flue gas sampling location is presented in Section 2.6.1.



---

### 2.6.1 EU-BOILER Exhaust

The EU-BOILER exhaust stack is 94 inches in diameter and has four 6.5-inch-diameter sampling ports. Only two ports (located 90° apart) were necessary to conduct the testing. Twelve traverse points for each of the two sampling ports were used to measure stack gas velocity, pollutant concentrations, and mass emission rates. The ports are located:

- Approximately 158 feet (20 duct diameters) from the nearest downstream disturbance (exhaust to atmosphere).
- Approximately 48 feet (6 duct diameters) from the nearest upstream disturbance (duct confluence where flue gas enters exhaust stack).

The sampling ports are accessible via a ladder and a platform on the stack.

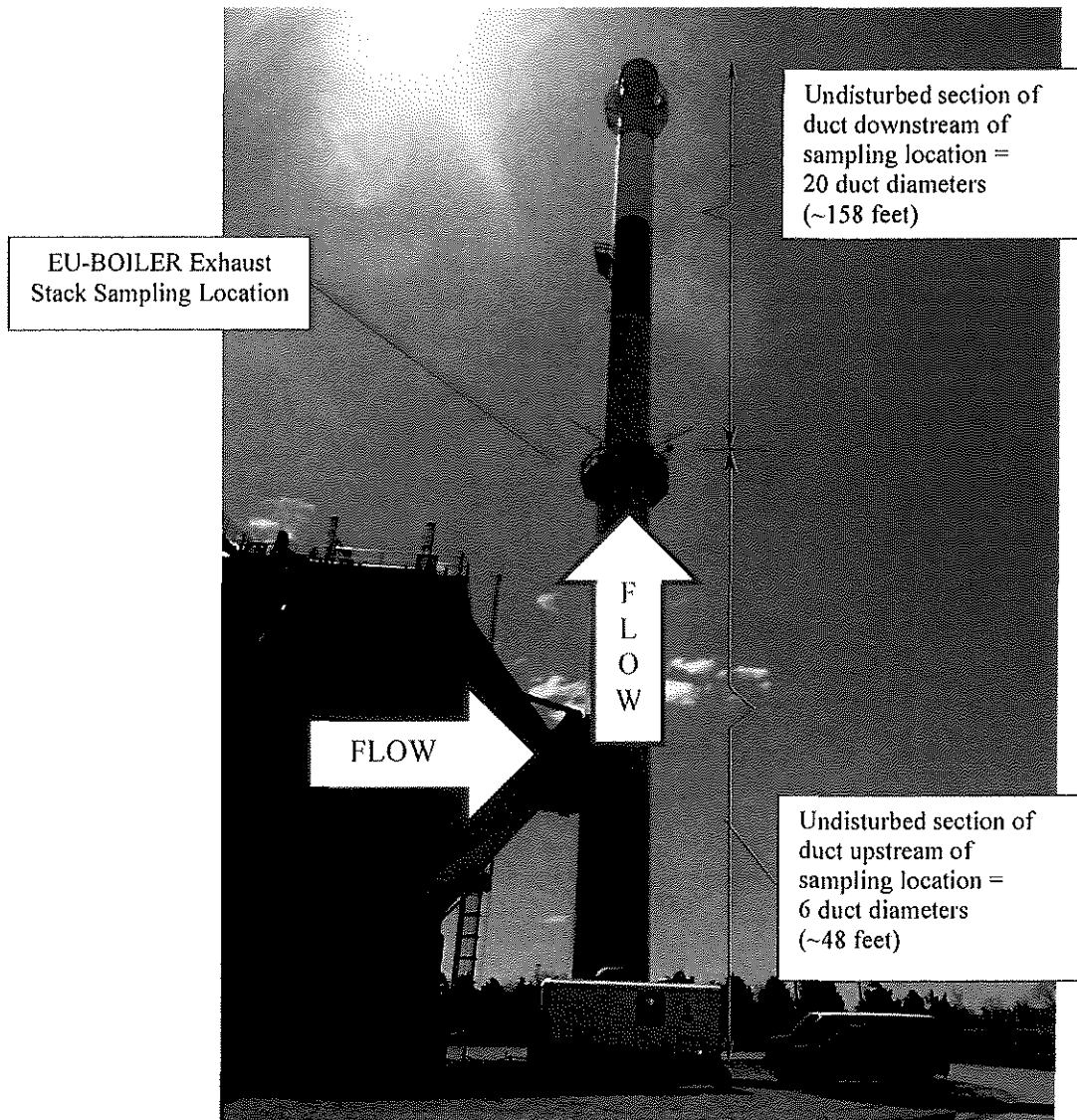
Figure 2-3 presents an aerial photograph of the EU-BOILER exhaust stack at the Genesee Power Station facility. Figure 2-4 is a photograph of the EU-BOILER exhaust sampling location. Figure 1 in the Appendix depicts the EU-BOILER sampling and traverse point locations.

Figure 2-3. Aerial Photograph of EU-BOILER Exhaust Stack



Google earth    feet 100    meters 40

Figure 2-4. EU-BOILER Photograph





## 3.0 Summary and Discussion of Results

### 3.1 Objective and Test Matrix

The objective of the testing was to evaluate compliance with applicable emission limits in MDEQ ROP MI-ROP-N3570-2012, dated August 24, 2012, and 40 CFR Part 63, Subpart DDDDD, "National Emission Standards for Hazardous Air Pollutants for Major Sources: Industrial, Commercial, and Institutional Boilers and Process Heaters."

Table 3-1 summarizes the sampling and analytical matrix.

**Table 3-1  
Test Matrix**

Sampling Location	Test Date (2016)	Test Run	Start Time	Stop Time	Sample/ Type of Pollutant	Sampling Method	No. of Test Runs and Duration	Analytical Method	Analytical Laboratory
EU-BOILER Exhaust	July 19	<b>Method 29</b>							
		1	8:55	11:00	Sample location, volumetric flowrate, molecular weight, PM, Hg	1, 2, 3A, 4, 5, 19, and 29	Three 120-minute test runs	Field measurement; Instrument paramagnetic analysis; gravimetric; cold vapor atomic absorption; inductively coupled plasma mass spectrometry	Maxxam Analytics
		2	11:30	13:35					
	3	14:20	16:25						
	<b>Method 26A</b>								
	July 20	1	16:50	17:53	Sample location, volumetric flowrate, molecular weight, HCl	1, 2, 3A, 4, 19, and 26A	Three 60-minute test runs	Field measurement; Instrument paramagnetic and infrared analysis; gravimetric; ion chromatography	Maxxam Analytics
2		9:00	10:04						
3		10:20	11:23						

### 3.2 Field Test Changes and Issues

Field test changes were not required to complete the emissions testing. Communication between Genesee Power Station and Bureau Veritas allowed the testing to be performed in accordance with established requirements.



### 3.3 Results

The results of the testing, compared to the applicable emission limits, are summarized in Table 3-2. Detailed results are presented in Tables 1 and 2 after the Table Tab of this report. Sample calculations are presented in Appendix B.

**Table 3-2  
Summary of EU-BOILER Air Emission Test Results**

Parameter	Units	Run 1	Run 2	Run 3	Average Result	Permit Limit	40 CFR Part 63 Subpart DDDDD Emission Limits
Filterable Particulate Matter (PM)	lb/hr	0.63	0.54	0.56	0.57	15.7	—
	lb/MMBtu	0.0012	0.0010	0.0011	0.0011	0.03	0.037
Mercury (Hg)	lb/hr	0.00016	0.00024	0.00019	0.00020	0.0047	—
	lb/MMBtu	$3.1 \times 10^{-7}$	$4.5 \times 10^{-7}$	$3.6 \times 10^{-7}$	$3.7 \times 10^{-7}$	$9 \times 10^{-6}$	$5.7 \times 10^{-6}$
Hydrogen Chloride (HCl)	lb/hr	8.5	3.2	3.9	5.2	47.1	—
	lb/MMBtu	0.016	0.0061	0.0079	0.010	0.09	0.022

lb/hr: pound per hour

lb/MMBtu: pound per million British thermal unit

The results of the testing indicate compliance with the applicable EU-BOILER permit limits listed in the table.



## 4.0 Sampling and Analytical Procedures

### 4.1 Test Methods

Bureau Veritas measured emissions in accordance with the procedures specified in the United States Environmental Protection Agency (USEPA) Standards of Performance for New Stationary Sources. Bureau Veritas used methods presented in Table 4-1.

**Table 4-1  
Sampling Methods**

Parameter	Source	USEPA Reference	
	Exhaust of EU-BOILER	Method	Title
Sampling ports and traverse points	•	1	Sample and Velocity Traverses for Stationary Sources
Velocity and flowrate	•	2	Determination of Stack Gas Velocity and Volumetric Flow Rate (Type S Pitot Tube)
Oxygen (O <sub>2</sub> ), carbon dioxide (CO <sub>2</sub> ), molecular weight	•	3A	Determination of Oxygen and Carbon Dioxide Concentrations in Emissions from Stationary Sources (Instrument Analyzer Procedure)
Moisture content	•	4	Determination of Moisture Content in Stack Gases
Filterable PM	•	5	Determination of Particulate Matter Emissions from Stationary Sources
Emission rate in lb/MMBtu	•	19	Determination of Sulfur Dioxide Removal Efficiency, Particulate Matter, Sulfur Dioxide, and Nitrogen Oxide Emission Rates
Hydrogen chloride (HCl)	•	26A	Determination of Hydrogen Halide and Halogen Emissions from Stationary Sources Isokinetic Method
Mercury (Hg)	•	29	Determination of Metals Emissions from Stationary Sources

• Denotes a test parameter to be tested

#### 4.1.1 Volumetric Flowrate (USEPA Methods 1 and 2)

USEPA Method 1, "Sample and Velocity Traverses for Stationary Sources," from the Code of Federal Regulations, Title 40, Part 60 (40 CFR 60), Appendix A, was used to evaluate the sampling location and the number of traverse points for the measurement of velocity profiles. Figure 1 (see Figures Tab) depicts the sampling location and traverse points. Details of the sampling location and number of traverse points are presented in the Table 4-2.



Table 4-2

Sampling Location and Number of Traverse Points

Sampling Location	Duct Diameter (inch)	Distance from Ports to Upstream Flow Disturbance (diameter)	Distance from Ports to Downstream Flow Disturbances (diameter)	Number of Ports used	Traverse Points per Port	Total Points
EU-BOILER Exhaust	94	6	20	2	12	24

Method 2, "Determination of Stack Gas Velocity and Volumetric Flow Rate (Type S Pitot Tube)," was used to measure flue gas velocity and calculate volumetric flowrate. An S-type Pitot tube and thermocouple assembly connected to an oil-filled manometer and thermometer was used. Because the dimensions of Bureau Veritas' Pitot tube met the requirements outlined in Method 2, Section 10.0, a baseline Pitot tube coefficient of 0.84 (dimensionless) was assigned.

**Cyclonic Flow Check.** Bureau Veritas evaluated whether cyclonic flow was present at the sampling location.

Cyclonic flow is defined as a flow condition with an average null angle greater than 20°. The direction of flow can be determined by aligning the Pitot tube to obtain zero (null) velocity head readings—the direction would be parallel to the Pitot tube face openings or perpendicular to the null position. By measuring the angle of the Pitot tube face openings in relation to the stack wall when a null angle is obtained, the direction of flow is measured. If the absolute average of the flow direction angles is greater than 20°, the flue gas flow is considered to be cyclonic at that sampling location and an alternative location should be used.

The measured traverse point flue gas velocity null angle was 5° at the EU-BOILER exhaust sampling location. The measurements indicate the absence of cyclonic flow at the sampling location.

The Pitot tube inspection and calibration sheet is included in Appendix A. Field data sheets are included in Appendix C. Computer-generated field data sheets are included in Appendix D.

#### 4.1.2 Molecular Weight (USEPA Method 3A)

USEPA Method 3A, "Determination of Oxygen and Carbon Dioxide Concentrations in Emissions from Stationary Sources (Instrument Analyzer Procedure)," was used to measure the oxygen (O<sub>2</sub>) and carbon dioxide (CO<sub>2</sub>) concentrations of the flue gas. These concentrations were





measured in order to calculate an emission rate in pounds of pollutant per million British thermal units (lb/MMBtu).

Figure 2 depicts the USEPA Method 3A sampling train.

Sampling for O<sub>2</sub> and CO<sub>2</sub> consists of extracting the flue gas from the stack through:

- A stainless-steel probe.
- Heated Teflon® sample line to prevent condensation.
- A chilled Teflon condenser with peristaltic pump to remove moisture from the sampled gas stream prior to entering the analyzer.
- A Teledyne® paramagnetic O<sub>2</sub> and CO<sub>2</sub> gas analyzer.

Data was recorded at 1-second intervals on a computer equipped with data acquisition software. Recorded concentrations were reported in 1-minute averages over the duration of each test run.

A calibration error check was performed on each analyzer by introducing zero-, mid-, and high-level calibration gases directly into the analyzer. The calibration error check was performed to evaluate if the analyzers respond to within  $\pm 2\%$  of the calibration span. Prior to each test run, a system-bias test was performed where known concentrations of calibration gases are introduced at the probe tip to measure if the response is within  $\pm 5\%$  of the analyzer calibration span.

Prior to testing, a three-point stratification test was conducted with the sampling probe located along a traverse line passing through the stack cross section's centroid and at points corresponding to 17, 50, and 83% of the stack diameter. The stack gas was sampled for at least twice the response time. If the concentration at each traverse point is no more than (1)  $\pm 5\%$  of the mean concentration or (2)  $\pm 0.5\%$ , whichever is less restrictive, the gas stream can be considered unstratified. Based on the measurements, the gas stream was considered to be unstratified and a single sampling point located near the centroid of the duct was used (all points had a percent difference less than 5%).

At the conclusion of the each test run, an additional system-bias check was performed to evaluate the analyzer drift from pre- and post-test system-bias checks. The acceptable analyzer drift tolerance is  $\pm 3\%$  of the calibration span.

Calibration data along with the USEPA Protocol 1 certification sheets for the calibration gases used are included in Appendix A.

Concentrations of oxygen in the exhaust gas were also measured by the facility's CEMS and averaged over the test periods in order to calculate an emission rate in pounds of HCl per million British thermal unit (lb/MMBtu), if necessary (refer to Section 3.2 for details).



### **4.1.3 Moisture Content (USEPA Method 4)**

Prior to testing, the moisture content was estimated using measurements from previous testing, psychrometric charts, and/or water saturation vapor pressure tables. These data was used in conjunction with preliminary velocity head pressure and temperature data to calculate flue gas velocity, nozzle diameter, and to establish the isokinetic sampling rate for the USEPA Method 5, 26A, and 29 sampling. For each sampling run, moisture content of the flue gases was measured using the reference method outlined in Section 2 of USEPA Method 4, "Determination of Moisture Content in Stack Gases" in conjunction with the performance of USEPA Methods 5, 26A, and 29.

### **4.1.4 Particulate Matter and Mercury (USEPA Methods 5 and 29)**

USEPA Method 5, "Determination of Particulate Matter Emissions from Stationary Sources," and Method 29, "Determination of Metals Emissions from Stationary Sources," were used to measure particulate matter and metals (arsenic, beryllium, cadmium, total chromium, lead, and mercury) emissions. Figure 3 depicts the USEPA Methods 5 and 29 sampling train.

Bureau Veritas' modular isokinetic stack sampling system consists of:

- A borosilicate glass button-hook nozzle.
- A heated ( $248\pm 25^{\circ}\text{F}$ ) borosilicate glass-lined probe.
- A desiccated and pre-weighed 110- or 83-millimeter-diameter quartz fiber filter (manufactured to at least 99.95% efficiency ( $<0.05\%$  penetration) for 0.3-micron dioctyl phthalate smoke particles) in a heated ( $248\pm 25^{\circ}\text{F}$ ) filter box.
- A set of six pre-cleaned impingers in an ice bath with the configuration shown in Table 4-3.
- A sampling line.
- An Environmental Supply® control case equipped with a pump, dry-gas meter, and calibrated orifice.



**Table 4-3**  
**USEPA Methods 5 and 29 Impinger Configuration**

Impinger Order (Upstream to Downstream)	Impinger Type	Impinger Contents	Amount
1	Modified	5% HNO <sub>3</sub> , 10% H <sub>2</sub> O <sub>2</sub>	100 ml
2	Greenburg-Smith	5% HNO <sub>3</sub> , 10% H <sub>2</sub> O <sub>2</sub>	100 ml
3	Modified	Empty	0 ml
4	Modified	Acidified KMnO <sub>4</sub>	100 ml
5	Modified	Acidified KMnO <sub>4</sub>	100 ml
6	Modified	Silica gel desiccant	~200-300 g

Before testing, a preliminary velocity traverse was performed and an ideal nozzle size was calculated. The calculated nozzle size allowed isokinetic sampling at an average rate of 0.75 cfm. Bureau Veritas selected a pre-cleaned borosilicate glass nozzle with an inner diameter that approximates the calculated ideal value. The nozzle inside diameter was measured with calipers across three cross-sectional chords. The nozzle was rinsed and connected to the borosilicate glass-lined sample probe.

The impact and static pressure openings of the Pitot tube were leak-checked at or above a pressure of 3 inches of water for more than 15 seconds. The sampling train was leak-checked by capping the nozzle tip and applying a vacuum of approximately 15 inches of mercury to the sampling train. The dry-gas meter was monitored to measure whether the sample train leak rate was less than 0.02 cfm. If the pre-test leak failed, the sampling train was adjusted until the leak rate was <0.02 cfm. Next, the sampling probe was inserted into the stack through the sampling port to begin sampling.

Ice and water was placed around the impingers and the probe and filter temperatures were allowed to stabilize at  $\geq 248 \pm 25^\circ\text{F}$  before each test run. After the desired operating conditions were coordinated with the facility, testing was initiated.

Stack parameters (e.g., flue velocity, temperature) were monitored to establish the isokinetic sampling rate to within  $\pm 10\%$  for the duration of the test.

At the conclusion of a test run and the post-test leak check, the sampling train was disassembled and the impingers and filter were transported to the recovery area. The filter was recovered using Teflon-lined tweezers and placed in a Petri dish. The Petri dish was immediately labeled and sealed with Teflon tape. The nozzle, probe, and the front half of the filter holder assembly was brushed and, at a minimum, triple-rinsed with acetone to recover particulate matter. The acetone rinses were collected in pre-cleaned sample containers.



Next, the probe nozzle, fittings, probe liner, and front-half of the filter holder were washed and brushed (using a nylon bristle brush) three times with 100 ml of 0.1-N nitric acid (HNO<sub>3</sub>). This rinsate was collected in a 500-ml glass sample container. Following the HNO<sub>3</sub> rinse, the probe nozzle, fittings, probe liner, and front-half of the filter holder were rinsed with HPLC water followed by acetone. The HPLC water and acetone rinses were discarded.

At the end of a test run, the liquid volume collected in each impinger was measured using a graduated cylinder to within ±0.5 milliliters; these volumes measurements were used to calculate the moisture content of the flue gas.

The contents of Impingers 1 and 2 were transferred to two glass sample containers. Impingers 1 and 2, the filter support, the back half of the filter housing, and connecting glassware were thoroughly rinsed with 100 ml of 0.1-N HNO<sub>3</sub>, and the rinsates were added to the sample containers in which the contents of the first two impingers were stored.

The weight of the contents of Impinger 3 was measured and the contents transferred to a glass sample container. This impinger was rinsed with 100 ml of 0.1-N HNO<sub>3</sub>, and the rinsate was added to the glass sample container.

The weight of liquid in Impingers 4 and 5 were measured and the contents transferred to a glass sample container. The impingers and connecting glassware were triple-rinsed with acidified KMnO<sub>4</sub> solution and the rinsate was added to the Impinger 4 and 5 sample containers. Subsequently, these impingers were rinsed with 100 ml of HPLC water, and the rinsate was added to the sample container. Because deposits may still be visible on the impinger surfaces after the water rinse, 25 ml of 8-N hydrochloric acid were used to wash these impingers and connecting glassware. This 8-N hydrochloric acid rinsate was collected in a separate sample container containing 200 ml of water.

The silica gel impinger was weighed as part of the measurement of the flue gas moisture content. All sample containers containing the acetone, 0.1-HNO<sub>3</sub>, HPLC water, 5% HNO<sub>3</sub>/10% H<sub>2</sub>O<sub>2</sub>, acidified KMnO<sub>4</sub>, 8-N hydrochloric acid, and filter blanks were transported by courier to Maxxam Analytics, a Bureau Veritas laboratory, located in Mississauga, Ontario, Canada for analysis.

#### 4.1.5 Emission Rates (USEPA Method 19)

USEPA Method 19, "Determination of Sulfur Dioxide Removal Efficiency and Particulate Matter, Sulfur Dioxide, and Nitrogen Oxide Emission Rates," was used to calculate an emission rate (lb/MMBtu). Oxygen concentrations and F factors (ratios of combustion gas volumes to heat inputs) were used to calculate emission rates using equation 19-1 from the method:

$$E = C_d F_d \frac{20.9}{(20.9 - \%O_{2d})}$$



Where:

- E = Pollutant emission rate (lb/million Btu)
- C<sub>d</sub> = Pollutant concentration, dry basis (lb/dscf)
- F<sub>d</sub> = Volumes of combustion components per unit of heat content, (9,240 dscf/million Btu for wood)
- %O<sub>2d</sub> = Concentration of oxygen on a dry basis (% , dry)

#### 4.1.6 Hydrogen Chloride (USEPA Method 26A)

USEPA Method 26A, "Determination of Hydrogen Halide and Halogen Emissions from Stationary Sources," was used to measure hydrogen chloride emissions. Three 60-minute test runs were performed at the EU-BOILER sampling location. Figure 4 depicts the USEPA Method 26A sampling train.

Bureau Veritas' modular isokinetic stack sampling system consists of:

- A borosilicate glass button-hook nozzle.
- A heated borosilicate glass-lined probe maintained at a temperature greater than 248°F.
- A desiccated and an untarred 83-millimeter-diameter filter in a filter box maintained at a temperature above 248°F.
- A set of five pre-cleaned impingers with the configuration shown in Table 4-4.
- A sampling line.
- An Environmental Supply® control case equipped with a pump, dry-gas meter, and calibrated orifice.

**Table 4-4  
Method 26A Impinger Configuration**

Impinger Order (Upstream to Downstream)	Impinger Type	Impinger Contents	Amount (gram)
1	Greenburg-Smith	0.1N H <sub>2</sub> SO <sub>4</sub>	100
2	Greenburg-Smith	0.1N H <sub>2</sub> SO <sub>4</sub>	100
3	Modified	0.1N NaOH	100
4	Modified	0.1N NaOH	100
5	Modified	Silica gel desiccant	~200-300



Before testing, a preliminary velocity traverse was performed and a nozzle size was calculated that would allow isokinetic sampling at an average rate of 0.75 cfm. Bureau Veritas selected a pre-cleaned borosilicate glass nozzle that had an inner diameter that approximated the calculated ideal value. The nozzle was measured with calipers across three cross-sectional chords to evaluate the inside diameter; rinsed and brushed with Type 3 deionized water and proof-rinsed with 0.1N H<sub>2</sub>SO<sub>4</sub>; and connected to the borosilicate glass-lined sample probe.

The impact and static pressure openings of the Pitot tube were leak-checked at or above a velocity head of 3.0 inches of water for more than 15 seconds. The sampling train was leak-checked by capping the nozzle tip and applying a vacuum of approximately 15 inches of mercury to the sampling train. The dry-gas meter was monitored for approximately 1 minute to measure that the sample train leakage rate was less than 0.02 cubic foot per minute (cfm). The sample probe was then inserted into the sampling port to begin sampling.

Ice was placed around the impingers and the probe, and filter temperatures were allowed to stabilize to a temperature above 248°F before sampling. After the desired operating conditions were coordinated with the facility, testing was initiated.

Stack parameters (e.g., flue velocity, temperature) were monitored to establish the isokinetic sampling rate within ±10 % for the duration of the test. Each of the 12 traverse points were sampled at 2.5-minute intervals.

At the conclusion of a test run and the post-test leak check, the sampling train was disassembled and the impingers and filter housing were transported to the recovery trailer. The filter was removed from the filter housing and discarded. The nozzle and probe liner, and the front half of the filter housing were rinsed with deionized water to remove any existing particulate matter. The deionized water rinses were discarded.

At the end of a test run, the liquid volume collected in each impinger, including the silica gel impinger, was measured using an electronic scale; these volumes were used to calculate the moisture content of the flue gas. The contents of Impingers 1 and 2, back half of the filter housing and connecting glassware were placed in a 500 ml polyethylene bottle with a Teflon cap screw liner. The described glassware was rinsed three times with deionized water and the rinsate was placed in that same sample container. The sample container was labeled as 0.1N H<sub>2</sub>SO<sub>4</sub>/DI, marked at the liquid level, and sealed.

The volume of the contents of Impinger 4 and 5, and all connecting glassware were emptied into a polyethylene bottle with a Teflon screw cap liner. The described glassware was rinsed three times with deionized water and the rinsate was placed in the same polyethylene bottle. This sample container was labeled as 0.1N NaOH/DI, marked at the liquid level, and sealed.

All sample containers, including blanks of water, 0.1N H<sub>2</sub>SO<sub>4</sub>, and 0.1N NaOH were sent by courier to Maxxam Analytics, a Bureau Veritas laboratory, located in Mississauga, Ontario, Canada for analysis.



## 4.2 Procedures for Obtaining Process Data

Process data were recorded by Genesee Power Station personnel. Refer to Section 2.1 and 2.2 for discussions of process and control device data and Appendix F for the operating parameters recorded during testing.

## 4.3 Sampling Identification and Custody

Mr. Li Wu, with Bureau Veritas, was responsible for the handling and procurement of the data collected in the field. Mr. Wu ensured the data sheets were accounted for and completed.

Recovery and analytical procedures were applicable to the sampling methods used in this test program. Sampling and recovery procedures were described previously Section 4.0.

Applicable Chain of Custody procedures followed guidelines outlined within ASTM D4840-99 (Reapproved 2010), "Standard Guide for Sample Chain-of-Custody Procedures."

For each sample collected (i.e., impinger, sorbent tube) sample identification and custody procedures were completed as follows:

- Containers were sealed to prevent contamination.
- Containers were labeled with test number, location, and test date.
- Containers were stored in a cooler.
- Samples were logged using guidelines outlined in ASTM D4840-99 (Reapproved 2010), "Standard Guide for Sample Chain-of-Custody Procedures."
- Samples were delivered to the laboratory.

Chains of custody and laboratory analytical results are included in Appendix E.



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## 5.0 QA/QC Activities

Equipment used in this test program passed quality assurance/quality control (QA/QC) procedures. Refer to Appendix A for equipment calibrations and inspection sheets. Field data sheets are presented in Appendix C. Computer-generated data sheets are presented within Appendix D.

### 5.1 Pretest QA/QC Activities

Before testing, the sampling equipment was cleaned, inspected, and calibrated according to procedures outlined in the applicable USEPA sampling method and USEPA's "Quality Assurance Handbook for Air Pollution Measurement Systems: Volume III, Stationary Source-Specific Methods."

### 5.2 QA/QC Audits

The results of select sampling and equipment QA/QC audits and the acceptable tolerance are presented in the following sections. Analyzer calibration and gas certification sheets are present in Appendix A.

#### 5.2.1 Sampling Train QA/QC Audits

The sampling train described in Section 4.1 was audited for measurement accuracy and data reliability. Table 5-1 summarizes the QA/QC audits conducted for the Methods 5, 26A, and 29 sampling trains.





**Table 5-1  
Methods 26A and 29 Sampling Train QA/QC Audits**

Parameter	Run 1	Run 2	Run 3	Method Requirement	Comment
<b>Method 26A</b>					
Sampling train leak check Post-test	0 ft <sup>3</sup> for 1 min at 15 in Hg	0 ft <sup>3</sup> for 1 min at 15 in Hg	0 ft <sup>3</sup> for 1 min at 12 in Hg	<0.020 ft <sup>3</sup> for 1 minute at ≥ sample vacuum recorded during test	Valid
Sampling vacuum (in Hg)	4 to 9	5 to 7	7 to 9		
<b>Methods 5 and 29</b>					
Sampling train leak check Post-test	0.005 ft <sup>3</sup> for 1 min at 10 in Hg	0 ft <sup>3</sup> for 1 min at 11 in Hg	0.003 ft <sup>3</sup> for 1 min at 10 in Hg	<0.020 ft <sup>3</sup> for 1 minute at ≥ sample vacuum recorded during test	Valid
Sampling vacuum (in Hg)	2 to 3	3 to 6	2 to 3		

### 5.2.2 Instrument Analyzer QA/QC Audits

The instrument sampling trains described in Section 4.1 were audited for measurement accuracy and data reliability. The analyzers passed the applicable calibration criteria. Table 5-2 summarizes gas cylinders used during this test program. Refer to Appendix A for additional calibration data.

**Table 5-2  
Calibration Gas Cylinder Information**

Parameter	Gas Vendor	Cylinder Serial Number	Cylinder Value	Expiration Date
Carbon dioxide (CO <sub>2</sub> ) Oxygen (O <sub>2</sub> ) Nitrogen (N)	Airgas	CC3829B	19.78% (CO <sub>2</sub> ) 19.94% (O <sub>2</sub> ) Balance (N)	6/2/24
		CC465807	11.09% (CO <sub>2</sub> ) 11.04% (O <sub>2</sub> ) Balance (N)	6/8/24
Nitrogen (N)	Airgas	CC183736	99.9995%	11/2/23



### 5.2.3 Dry-Gas Meter QA/QC Audits

Table 5-3 summarizes the dry-gas meter calibration checks in comparison to the acceptable USEPA tolerance. Refer to Appendix A for DGM calibrations.

**Table 5-3  
Dry-gas Meter Calibration QA/QC Audit**

Dry-Gas Meter	Pre-test DGM Calibration Factor (Y) (dimensionless)	Post-Test DGM Calibration Factor (Y) (dimensionless)	Difference Between Pre- and Post-test DGM Calibrations	Acceptable Tolerance	Comment
6	0.954 May 27, 2016	0.960 July 25, 2016	0.006	±0.05	Valid

### 5.2.4 Isokinetic Sampling

Isokinetic sampling, which means collecting flue gas into the sampling nozzle at the velocity equal to that of the flue gas velocity, is a requirement of USEPA Methods 5, 26A, and 29.

Maintaining isokinetic sampling is important because under isokinetic conditions, sample concentrations may be biased depending on the inertial effects of the particles. When flue gas containing small and large particles are collected isokinetically, the small and large particle concentrations are consistent with the flue gas composition. However, in over-isokinetic conditions (200% high sampling flowrate into nozzle), the particulate matter concentrations are biased low, because a greater number of smaller, lighter particles and fewer large, heavier particles will be collected compared to isokinetic conditions. Under-isokinetic sampling (50% low sampling flowrate into nozzle) will bias the results high because a greater number of larger, heavy particles will be collected.

The USEPA Methods 5, 26A, and 29 isokinetic sampling rate for each test run is presented in Table 5-4. The isokinetic sampling rates were within the isokinetic requirement of 100±10% percent.



**Table 5-4  
Summary of Isokinetic Sampling Rates**

Source	Sampling Date 2016	Run	Actual % Isokinetic Sampling Rate	Allowable % Isokinetic Sampling Rate
EU-BOILER	<b>Method 26A</b>			100±10
	May 19	1	101	
	May 20	2	105	
		3	103	
	<b>Methods 5 and 29</b>			
	May 19	1	101	
		2	98	
		3	102	

### 5.2.5 Thermocouple QA/QC Audits

Temperature measured using thermocouples and digital pyrometers were compared to a reference temperature (i.e., ice water bath, boiling water) before and after testing to evaluate accuracy of the equipment. The thermocouples and pyrometers measured temperature within ±1.5% of the reference temperatures and were within USEPA acceptance criteria. Thermocouple calibration sheets are presented in Appendix A.

### 5.2.6 QA/QC Blanks

Reagent and field blanks were analyzed for particulate matter. The results of the blanks are presented in Table 5-5. Analytes of concern were not detected in the reagent and field blanks, with the exception of Blank 3A Hg; mercury was detected at a mass of 0.012 micrograms (µg) in this blank. The mass of mercury detected in the blank was significantly less than the mass detected in the Run 1 through 3 samples.



**Table 5-5  
QA/QC Blanks**

<b>Sample Identification</b>	<b>Result</b>	<b>Comment</b>
M5/29 Filter Blank	0.5 mg	
M5/29 Acetone Blank	0.6 mg	Sample Volume 98 ml
M25/9 Blanks	0.012 µg	Only 3A Hg detected in Method 29 blank
M26A Blanks	Not detected	HCl and Cl not detected in Method 26A blanks

### **5.3 QA/QC Checks for Data Reduction and Validation**

Bureau Veritas validated the computer spreadsheets onsite. The computer spreadsheets were used to evaluate the accuracy of field calculations. The field data sheets were reviewed to evaluate whether data has been recorded appropriately. The computer data sheets were checked against the field data sheets for accuracy during review of the draft report. Sample calculations were performed to check computer spreadsheet computations.

### **5.4 QA/QC Problems**

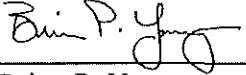
Equipment audits and QA/QC procedures demonstrate sample collection accuracy for the test runs.

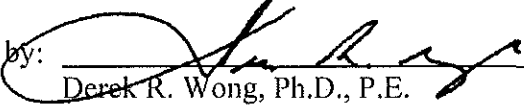


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## 6.0 Limitations

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This report prepared by:   
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**Table 1 - EU-BOILER Exhaust Mercury and Particulate Matter Results**

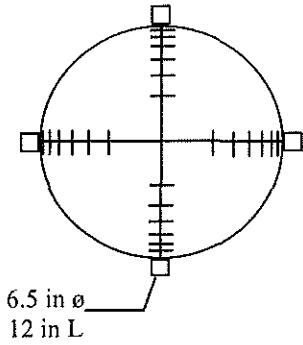
Facility	Genesee Power				
Source Designation	EU-BOILER				
Test Date	Jul 19, 2016	Jul 19, 2016	Jul 19, 2016		
Meter/Nozzle Information	Run 1 - M29	Run 2 - M29	Run 3 - M29	Average	
Meter Temperature, $T_m$	°F	80	84	88	84
Meter Pressure, $P_m$	in Hg	30.58	30.59	30.58	30.58
Measured Sample Volume, $V_m$	ft <sup>3</sup>	137.67	141.46	140.41	139.85
Sample Volume, $V_s$	std ft <sup>3</sup>	131.27	133.81	132.03	132.37
Sample Volume, $V_{s1}$	std m <sup>3</sup>	3.72	3.79	3.74	3.75
Condensate Volume, $V_w$	std ft <sup>3</sup>	26.79	21.11	29.26	25.72
Gas Density, $\rho_g$	std lb/ft <sup>3</sup>	0.0736	0.0748	0.0736	0.0740
Total weight of sampled gas	lb	11.638	11.594	9.992	11.075
Nozzle Size, $A_n$	ft <sup>2</sup>	0.0004461	0.0004461	0.0004461	0.0004461
Isokinetic Variation, I	%	101	98	102	100
<b>Stack Data</b>					
Average Stack Temperature, $T_s$	°F	376	379	379	378
Molecular Weight Stack Gas-dry, $M_d$	lb/lb-mole	30.48	30.54	30.65	30.56
Molecular Weight Stack Gas-wet, $M_w$	lb/lb-mole	28.37	28.83	28.35	28.52
Stack Gas Specific Gravity, $G_s$		0.98	1.00	0.98	0.98
Percent Moisture, $B_w$	%	16.95	13.63	18.14	16.24
Water Vapor Volume (fraction)		0.169	0.136	0.181	0.162
Pressure, $P_s$	in Hg	30.19	30.19	30.19	30.19
Average Stack Velocity, $V_s$	ft/sec	76.60	77.67	77.63	77.30
Area of Stack	ft <sup>2</sup>	48.19	48.19	48.19	48.19
<b>Exhaust Gas Flowrate</b>					
Flowrate	ft <sup>3</sup> /min, actual	221,502	224,585	224,473	223,520
Flowrate	ft <sup>3</sup> /min, standard wet	141,079	142,695	142,610	142,128
Flowrate	ft <sup>3</sup> /min, standard dry	117,170	123,248	116,738	119,052
Flowrate	m <sup>3</sup> /min, standard dry	3,318	3,490	3,306	3,371
<b>Mercury</b>					
<b>Collected Mass</b>					
Mercury	mg	0.0013	0.0020	0.0016	0.0017
<b>Concentration</b>					
Mercury	mg/dscf	0.000010	0.000015	0.000012	0.000012
<b>Mass Emission Rate</b>					
Mercury	lb/MMBtu	0.00000031	0.00000045	0.00000036	0.00000037
Mercury	lb/hr	0.00016	0.00024	0.00019	0.00020
<b>Particulate Matter</b>					
<b>Collected Mass</b>					
Particulate Matter Acetone Wash	mg	5.0	4.1	3.2	4.1
Particulate Matter Filter	mg	<0.30	<0.30	1.60	0.73
Total Filterable Particulate Matter (FPM)	mg	5.3	4.4	4.8	4.8
<b>Concentration</b>					
Particulate Matter (FPM)	mg/dscf	0.040	0.033	0.036	0.037
Particulate Matter (FPM)	grain/dscf	0.00062	0.00051	0.00056	0.00056
<b>Mass Emission Rate</b>					
Particulate Matter (FPM)	lb/MMBtu	0.0012	0.0010	0.0011	0.0011
Particulate Matter (FPM)	lb/hr	0.63	0.54	0.56	0.57



**Table 2 - EU-BOILER Exhaust Hydrogen Chloride Results**

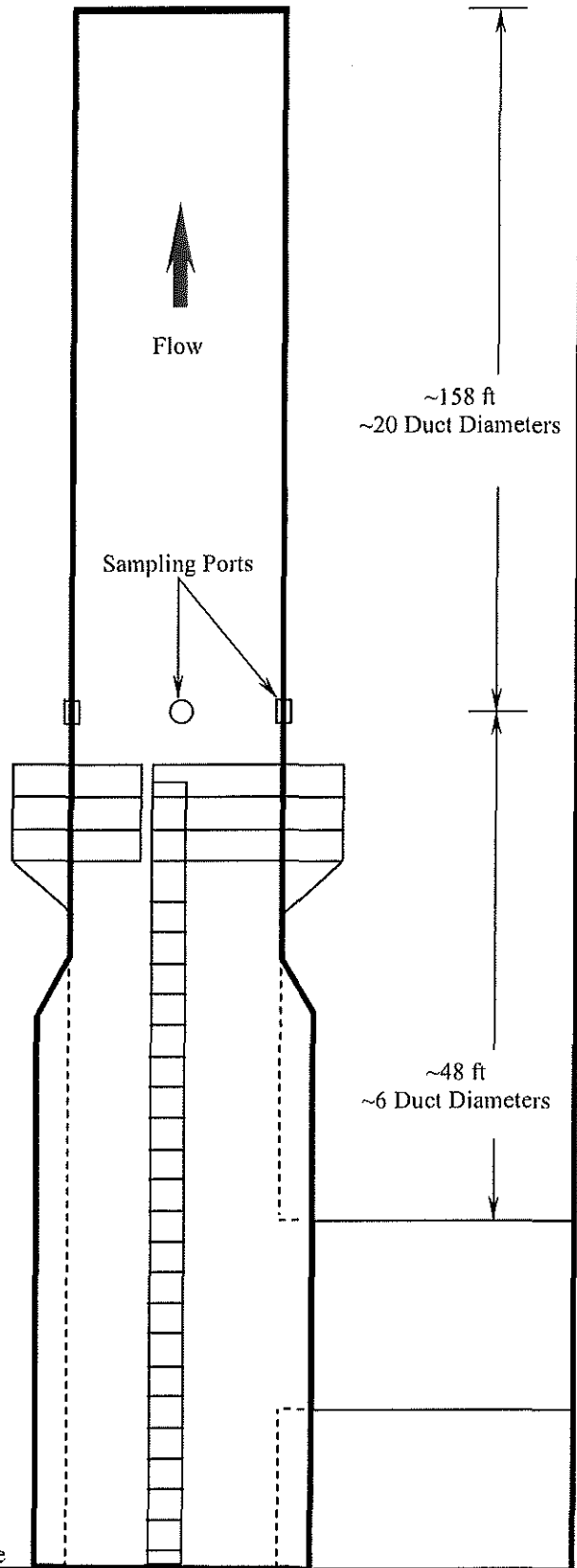
Facility Source Designation Test Date	Genesee Power EU-BOILER			Average	
	Jul 19, 2016	Jul 20, 2016	Jul 20, 2016		
<b>Meter/Nozzle Information</b>					
Meter Temperature, $T_m$	°F	94	72	78	81
Meter Pressure, $P_m$	in Hg	30.58	30.58	30.58	30.58
Measured Sample Volume, $V_m$	ft <sup>3</sup>	69.56	69.49	69.30	69.45
Sample Volume, $V_{m1}$	std ft <sup>3</sup>	64.65	67.27	66.36	66.09
Sample Volume, $V_{m2}$	std m <sup>3</sup>	1.83	1.90	1.88	1.87
Condensate Volume, $V_c$	std ft <sup>3</sup>	15.18	16.18	15.22	15.52
Gas Density, $\rho_g$	std lb/ft <sup>3</sup>	0.0729	0.0729	0.0731	0.0730
Total weight of sampled gas	lb	5.823	6.084	4.986	5.631
Nozzle Size, $A_n$	ft <sup>2</sup>	0.0004461	0.0004461	0.0004461	0.0004461
Isokinetic Variation, $I$	%	101	105	103	103
<b>Stack Data</b>					
Average Stack Temperature, $T_s$	°F	376	378	381	378
Molecular Weight Stack Gas-dry, $M_d$	lb/lb-mole	30.47	30.51	30.48	30.48
Molecular Weight Stack Gas-wet, $M_w$	lb/lb-mole	28.10	28.08	28.15	28.11
Stack Gas Specific Gravity, $G_s$		0.97	0.97	0.97	0.97
Percent Moisture, $B_{w1}$	%	19.01	19.39	18.65	19.02
Water Vapor Volume (fraction)		0.190	0.194	0.187	0.190
Pressure, $P_s$	in Hg	30.19	30.19	30.19	30.19
Average Stack Velocity, $V_s$	ft/sec	77.61	77.79	77.94	77.78
Area of Stack	ft <sup>2</sup>	48.19	48.19	48.19	48.19
<b>Exhaust Gas Flowrate</b>					
Flowrate	ft <sup>3</sup> /min, actual	224,413	224,936	225,369	224,906
Flowrate	ft <sup>3</sup> /min, standard wet	142,955	142,947	142,853	142,918
Flowrate	ft <sup>3</sup> /min, standard dry	115,777	115,228	116,207	115,737
Flowrate	m <sup>3</sup> /min, standard dry	3,278	3,263	3,291	3,277
<b>Hydrogen Chloride</b>					
<b>Collected Mass</b>					
Hydrogen chloride	mg	36	14	17	22
<b>Concentration</b>					
Hydrogen chloride	mg/dscf	0.56	0.21	0.26	0.34
<b>Mass Emission Rate</b>					
Hydrogen chloride	lb/MMBtu	0.016	0.0061	0.0079	0.010
Hydrogen chloride	lb/hr	8.5	3.2	3.9	5.2

94 in Internal Diameter



Traverse Point	Distance from Stack Wall (inch)
1	1.97
2	6.30
3	11.09
4	16.64
5	23.50
6	33.46
7	60.54
8	70.50
9	77.36
10	82.91
11	87.70
12	92.03

Source	Distance from Ports to Nearest Upstream Disturbance	Distance from Ports to Nearest Downstream Disturbance
EU-Boiler Exhaust Stack	~48 (6 Duct Diameters)	~158 (20 Duct Diameters)



Ground Surface

Not to Scale

July 25, 2016

Project No. 11016-000080.00

**EU-BOILER**

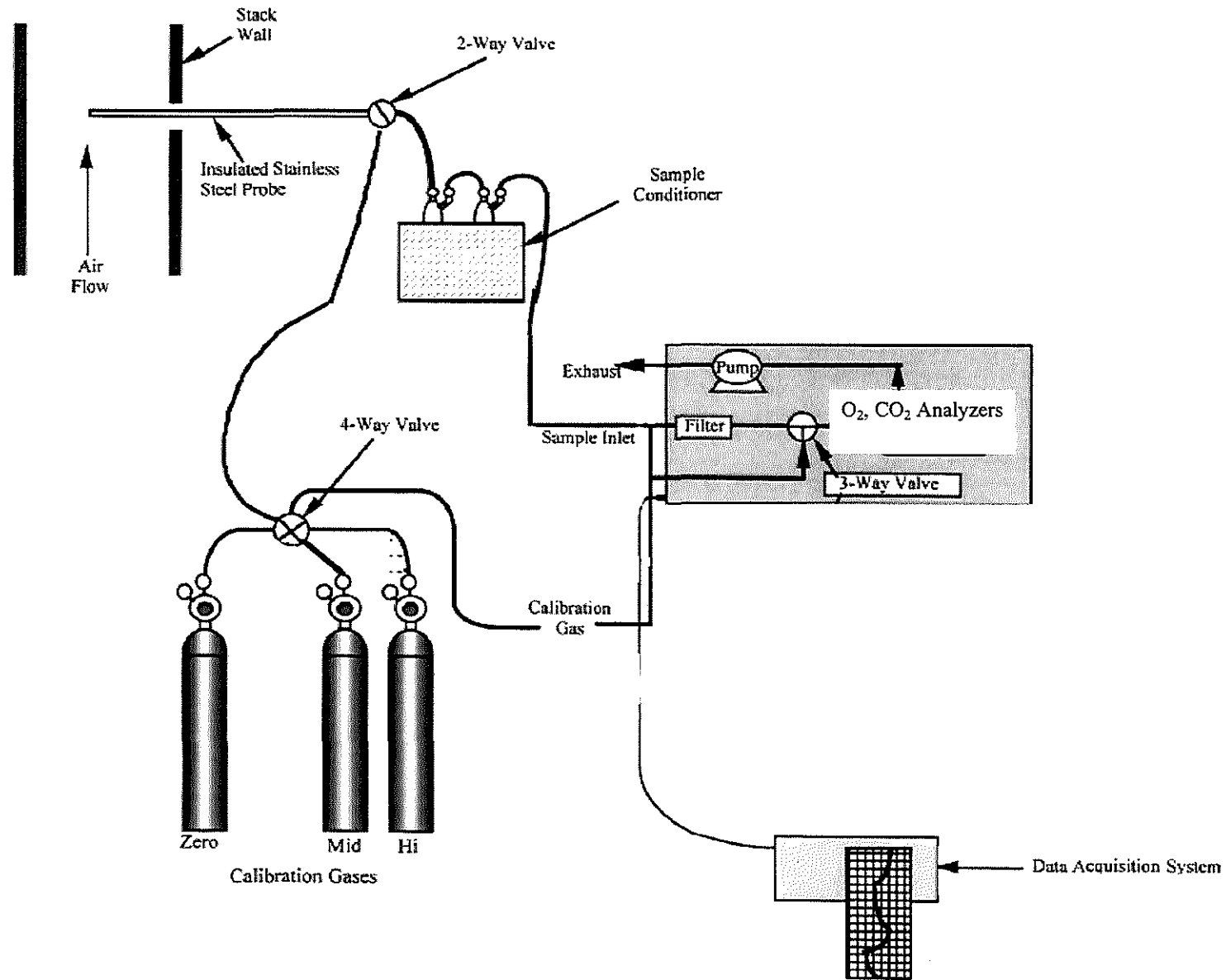
**Sampling Ports and Traverse Point Locations  
Genesee Power Station Limited Partnership**



Figure

**1**





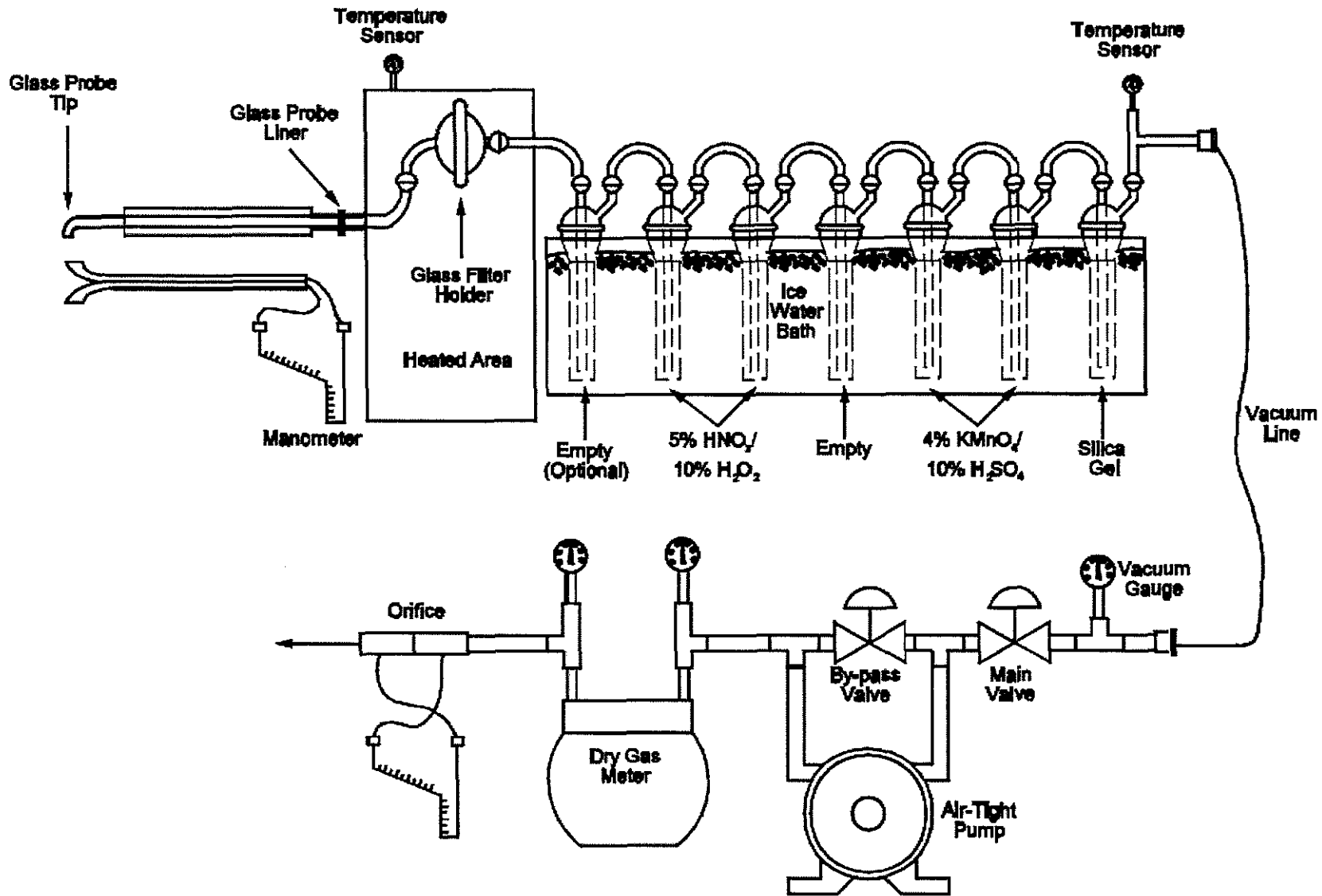
**Figure 2**  
**USEPA Method 3A Sampling Train**



**Genesee Power Station Limited Partnership**  
**Flint, Michigan**

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Last Revision: June 23, 2016



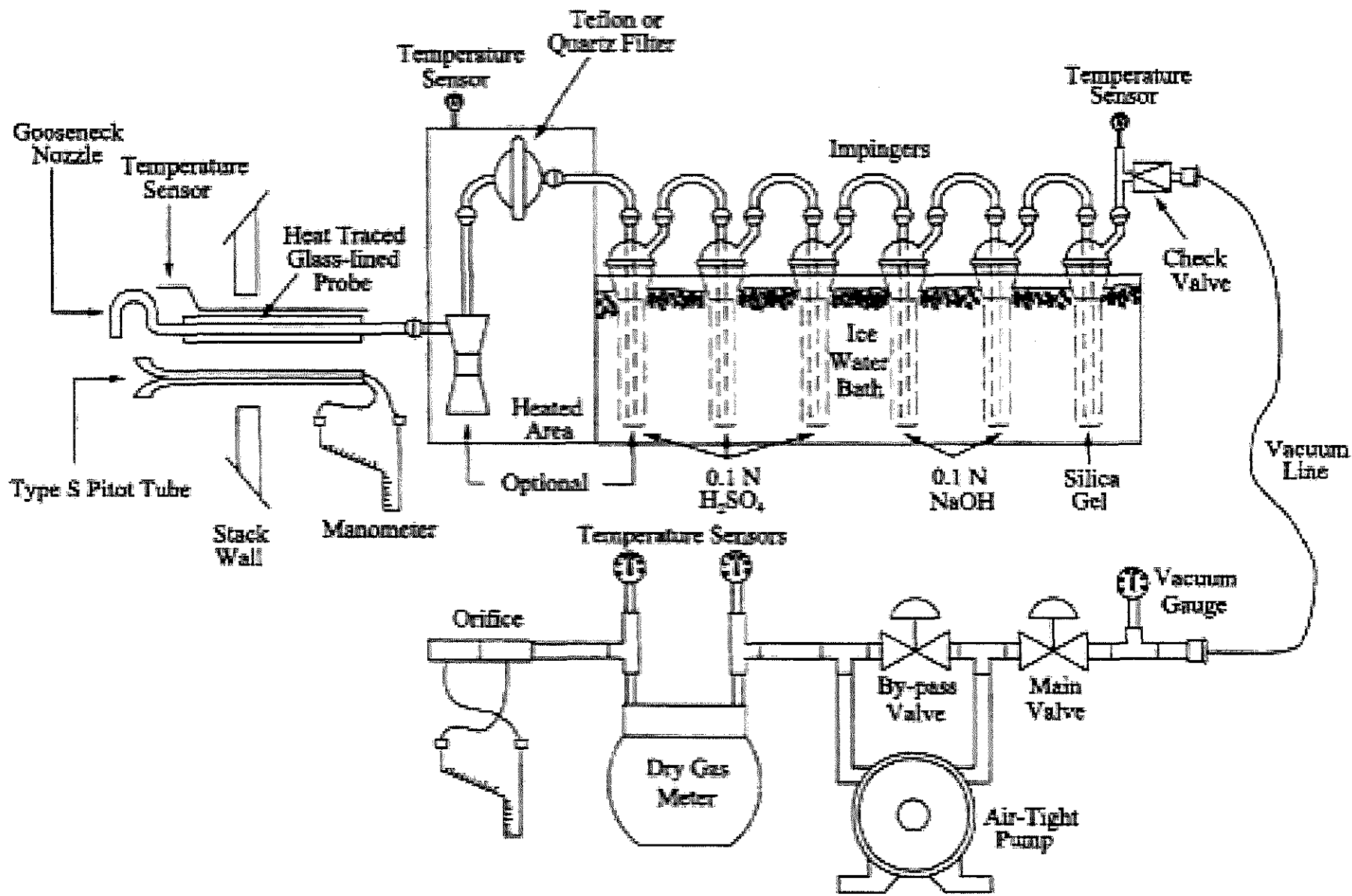
**Figure 3**  
**USEPA Methods 5 and 29 Sampling**  
**Train**



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**Flint, Michigan**

Project No. 11016-00080.00

Last Revision: June 23, 2016



**Figure 4**  
**USEPA Method 26A Sampling**  
**Train**



**Genesee Power Station Limited Partnership**  
**Flint, Michigan**

Project No. 11016-00080.00

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