
Regulatory Information

Permit No. Michigan Department of Environment, Great Lakes, and Energy (EGLE) Permit No. MI-ROP-N5940-2019A

Source Information

<i>Source Name</i>	<i>Source ID</i>	<i>Target Parameters</i>
Wood Fuel Boiler 2	EU-WOODBOILER2	PM, CO, benzo (a) pyrene

Contact Information

<i>Test Location</i>	<i>Test Company</i>	<i>Analytical Laboratories</i>
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Alliance Technical Group, LLC (Alliance) has completed the source testing as described in this report. Results apply only to the source(s) tested and operating condition(s) for the specific test date(s) and time(s) identified within this report. All results are intended to be considered in their entirety, and Alliance is not responsible for use of less than the complete test report without written consent. This report shall not be reproduced in full or in part without written approval from the customer.

To the best of my knowledge and abilities, all information, facts and test data are correct. Data presented in this report has been checked for completeness and is accurate, error-free and legible. Onsite testing was conducted in accordance with approved internal Standard Operating Procedures. Any deviations or problems are detailed in the relevant sections in the test report.

This report is only considered valid once an authorized representative of Alliance has signed in the space provided below; any other version is considered draft. This document was prepared in portable document format (.pdf) and contains pages as identified in the bottom footer of this document.



Edward "EJ" Juers
Alliance Technical Group, LLC

02/28/2024

Date

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1.0 Introduction

Alliance Technical Group, LLC (Alliance) was retained by PotlatchDeltic Corporation (PotlatchDeltic) to conduct compliance testing at the Gwinn Sawmill in Gwinn, Michigan. The facility operates under the Michigan Department of Environment, Great Lakes, and Energy (EGLE) Permit No. MI-ROP-N5940-2019A. Testing was conducted to determine the emission rates of particulate matter (PM), carbon monoxide (CO) and benzo (a) pyrene from the exhaust of Wood Fuel Boiler No. 2.

1.1 Facility Description

The PotlatchDeltic Corporation owns and operates the Wood Fuel Boiler. No 2 at the Gwinn Sawmill. The Wood Fuel Boiler 2 is a Hurst and Welding Co. Inc. Model No. HYB-4000-150-WF (SN. No. HYB3948-300-1). It has a capacity of 28.7 MMBtu/hr and is controlled by a primary and secondary multiclone.

1.2 Project Team

Personnel involved in this project are identified in the following table.

Table 1-1: Project Team

Facility Personnel	
	Amy Benson
Alliance Personnel	Ryan Schuth Corbin Godfrey Colin Kelly Leo Peters

1.3 Site Specific Test Plan & Notification

Testing was conducted in accordance with the Site-Specific Test Plan (SSTP) approved by EGLE.

2.0 Summary of Results

Alliance conducted compliance testing at the PotlatchDeltic facility in Gwinn, MI January 16-17, 2024. Testing consisted of determining the emission rates of PM, CO and benzo (a) pyrene from the exhaust of Wood Fuel Boiler No. 2.

Tables 2-1 and 2-2 provide a summary of the emission testing results with comparisons to the applicable Michigan EGLE permit limits. Any difference between the summary results listed in the following tables and the detailed results contained in appendices is due to rounding for presentation.

Table 2-1: Summary of Results - PM and Gases

Run Number	Run 1	Run 2	Run 3	Average
Date	1/16/24	1/16/24	1/17/24	--
Filterable Particulate Matter Data				
Concentration, grain/dscf	0.17	0.13	0.16	0.15
Emission Rate, lb/hr	8.7	6.8	8.3	8.0
Permit Limit, lb/hr	--	--	--	5.7
Percent of Limit, %	--	--	--	> 100
Emission Rate, ton/yr	38.2	30.0	36.5	34.9
Permit Limit, ton/yr	--	--	--	25.1
Percent of Limit, %	--	--	--	> 100
Emission Factor, lb/MMBtu	0.36	0.28	0.35	0.33
Permit Limit, lb/MMBtu	--	--	--	0.2
Percent of Limit, %	--	--	--	> 100
Carbon Monoxide Data				
Emission Rate, lb/hr	7.4	5.1	10.6	7.7
Permit Limit, lb/hr	--	--	--	14.35
Percent of Limit, %	--	--	--	54
Emission Rate, ton/yr	32.5	22.2	46.5	33.7
Permit Limit, ton/yr	--	--	--	62.85
Percent of Limit, %	--	--	--	54
Emission Factor, lb/MMBtu	0.30	0.21	0.45	0.32
Permit Limit, lb/MMBtu	--	--	--	0.50
Percent of Limit, %	--	--	--	64

Table 2-2: Summary of Results - Benzo[a]pyrene

Run Number	Run 1	Run 2	Run 3	Average
Date	1/16/24	1/16/24	1/17/24	--
Benzo[a]pyrene Data				
Concentration, ug/dscm	0.036	0.0053	0.23	0.092
Permit Limit, ug/dscm	--	--	--	9.7
Percent of Limit, %	--	--	--	1
Emission Rate, lb/hr	8.1E-07	1.2E-07	5.2E-06	2.0E-06
Permit Limit, lb/hr	--	--	--	0.0006
Percent of Limit, %	--	--	--	< 1
Emission Rate, ton/yr	3.5E-06	5.1E-07	2.3E-05	8.9E-06
Permit Limit, ton/yr	--	--	--	0.0027
Percent of Limit, %	--	--	--	< 1

3.0 Testing Methodology

The emission testing program was conducted in accordance with the test methods listed in Table 3-1. Method descriptions are provided below while quality assurance/quality control data is provided in Appendix D.

Table 3-1: Source Testing Methodology

Parameter	U.S. EPA Reference Test Methods	Notes/Remarks
Volumetric Flow Rate	1 & 2	Full Velocity Traverses
Oxygen/Carbon Dioxide	3A	Instrumental Analysis
Moisture Content	4	Gravimetric Analysis
Particulate Matter	5	Isokinetic Sampling
Carbon Monoxide	10	Instrumental Analysis
Mass Emission Factors	19	Fuel Factors/Heat Inputs
Benzo (a) Pyrene	SW 846-0010	Isokinetic Sampling

3.1 U.S. EPA Reference Test Methods 1 and 2 – Sampling/Traverse Points and Volumetric Flow Rate

The sampling location and number of traverse (sampling) points were selected in accordance with U.S. EPA Reference Test Method 1. To determine the minimum number of traverse points, the upstream and downstream distances were equated into equivalent diameters and compared to Figure 1-1 in U.S. EPA Reference Test Method 1.

Full velocity traverses were conducted in accordance with U.S. EPA Reference Test Method 2 to determine the average stack gas velocity pressure, static pressure and temperature. The velocity and static pressure measurement system consisted of a pitot tube and inclined manometer. The stack gas temperature was measured with a K-type thermocouple and pyrometer.

Stack gas velocity pressure and temperature readings were recorded during each test run. The data collected was utilized to calculate the volumetric flow rate in accordance with U.S. EPA Reference Test Method 2.

3.2 U.S. EPA Reference Test Method 3A – Oxygen/Carbon Dioxide

The oxygen (O_2) and carbon dioxide (CO_2) testing was conducted in accordance with U.S. EPA Reference Test Method 3A. Data was collected online and reported in one-minute averages. The sampling system consisted of a stainless-steel probe, Teflon sample line(s), gas conditioning system and the identified gas analyzer. The gas conditioning system was a non-contact condenser used to remove moisture from the stack gas. If an unheated Teflon sample line was used, then a portable non-contact condenser was placed in the system directly after the probe. Otherwise, a heated Teflon sample line was used. The quality control measures are described in Section 3.8.

3.3 U.S. EPA Reference Test Method 4 – Moisture Content

The stack gas moisture content (BWS) was determined in accordance with U.S. EPA Reference Test Method 4. The gas conditioning train consisted of a series of chilled impingers. Prior to testing, each impinger was filled with a known quantity of water or silica gel. Each impinger was analyzed gravimetrically before and after each test run on the same balance to determine the amount of moisture condensed.

3.4 U.S. EPA Reference Test Method 5 – Particulate Matter

The filterable particulate matter testing was conducted accordance with U.S. EPA Reference Test Method 5. The complete sampling system consisted of a stainless-steel nozzle, heated glass-lined probe, pre-weighed heated quartz filter, gas conditioning train, pump and calibrated dry gas meter. The gas conditioning train consisted of four (4) chilled impingers – the first and second containing 100 mL of H₂O, an empty third impinger and the fourth containing 200-300 grams of silica gel. The probe liner and filter heating systems were maintained at a temperature of 120 ± 14°C (248 ±25°F) and the impinger temperature was maintained at 20°C (68°F) or less throughout the testing.

Following the completion of each test run, the sampling train was leak checked at a vacuum pressure greater than or equal to the highest vacuum pressure observed during the run, and the contents of the impingers were measured for moisture gain. The probe was rinsed and brushed three (3) times and nozzle was rinsed and brushed six (6) times with acetone to remove any adhering particulate matter. This rinse was recovered in container 2. The front half of the filter holder was rinsed three (3) times with acetone and this rinse was added to container 2. The pre-weighed quartz filter was carefully removed and placed in container 1. All containers were sealed, labeled and liquid levels marked for transport to the identified laboratory.

3.5 U.S. EPA Reference Test Method 10 – Carbon Monoxide

The carbon monoxide (CO) testing was conducted in accordance with U.S. EPA Reference Test Method 10. Data was collected online and reported in one-minute averages. The sampling system consisted of a stainless-steel probe, Teflon sample line(s), gas conditioning system, and the identified gas analyzer. The gas conditioning system was a non-contact condenser used to remove moisture from the gas. If an unheated Teflon sample line was used, then a portable non-contact condenser was placed in the system directly after the probe. Otherwise, a heated Teflon sample line was used. The quality control measures are described in Section 3.8.

3.6 U.S. EPA Reference Test Method 19 – Mass Emission Factors

The pollutant concentrations were converted to mass emission factors (lb/MMBtu) using procedures outlined in U.S. EPA Reference Test Method 19. The published dry O₂, wet O₂ or CO₂ based fuel factor (F-Factor) of 9,600 dscf/MMBtu for wood bark was used in the calculations.

3.7 SW-846 Test Method 0010 – Benzo (a) Pyrene

The benzo (a) pyrene testing was conducted in accordance with SW-846 Test Method 0010. The sampling system consisted of a stainless steel or glass nozzle, heated glass or quartz-lined probe, glass filter holder with pre-cleaned glass-fiber filter, condenser coil, XAD sorbent module, gas conditioning train, pump and calibrated dry gas meter. The gas conditioning system consisted of four (4) chilled impingers. The first impinger was empty. The next two (2) impingers each contained 100 mL of water. The fourth impinger was charged with 200-300 grams of silica gel. The probe liner and filter heating systems were maintained at a temperature of 120 ± 14°C (248 ±25°F), and the impinger temperature was maintained below at 20°C (68°F) or less throughout testing.

All glassware leading to the XAD adsorbing resin trap was cleaned and sealed before mobilizing to the site. The sampling train was assembled in the sample recovery area. The pre-cleaned quartz filter was placed in a glass filter holder with a Teflon filter support and connected to the condenser coil. All open ends of the sampling train were sealed with Teflon tape prior to complete assembly at the sampling location.

Following the completion of each test run, the sampling train was leak checked at vacuum pressure greater than or equal to the highest vacuum pressure observed during the run. The XAD sorbent module was sealed on both ends and placed on ice. The filter was removed from the filter holder and placed in container 1. The nozzle, probe liner and front half of the filter holder were triple-rinsed and brushed with methanol/methylene chloride (1:1 v/v), and these rinses were recovered in container 2. The contents of the impingers were measured for moisture gain along with any moisture collected in the back half of the filter housing and the gas-conditioning section of the organic module. The impinger contents and condensate were then transferred to container 3. The back half of the filter holder and coil condenser glassware were triple-rinsed with methanol/methylene chloride and recovered in container 4. All samples were sealed, labeled and liquid levels marked for transport to the identified laboratory for analysis.

3.8 Quality Assurance/Quality Control – U.S. EPA Reference Test Methods 3A and 10

Cylinder calibration gases used met EPA Protocol 1 (+/- 2%) standards. Copies of all calibration gas certificates can be found in the Quality Assurance/Quality Control Appendix.

Low Level gas was introduced directly to the analyzer. After adjusting the analyzer to the Low-Level gas concentration and once the analyzer reading was stable, the analyzer value was recorded. This process was repeated for the High-Level gas. For the Calibration Error Test, Low, Mid, and High-Level calibration gases were sequentially introduced directly to the analyzer. All values were within 2.0 percent of the Calibration Span or 0.5 ppmv/% absolute difference.

High or Mid-Level gas (whichever was closer to the stack gas concentration) was introduced at the probe and the time required for the analyzer reading to reach 95 percent or 0.5 ppmv/% (whichever was less restrictive) of the gas concentration was recorded. The analyzer reading was observed until it reached a stable value, and this value was recorded. Next, Low-Level gas was introduced at the probe and the time required for the analyzer reading to decrease to a value within 5.0 percent or 0.5 ppmv/% (whichever was less restrictive) was recorded. If the Low-Level gas was zero gas, the response was 0.5 ppmv/% or 5.0 percent of the upscale gas concentration (whichever was less restrictive). The analyzer reading was observed until it reached a stable value, and this value was recorded. The measurement system response time and initial system bias were determined from these data. The System Bias was within 5.0 percent of the Calibration Span or 0.5 ppmv/% absolute difference.

High or Mid-Level gas (whichever was closer to the stack gas concentration) was introduced at the probe. After the analyzer response was stable, the value was recorded. Next, Low-Level gas was introduced at the probe, and the analyzer value recorded once it reached a stable response. The System Bias was within 5.0 percent of the Calibration Span or 0.5 ppmv/% absolute difference or the data was invalidated, and the Calibration Error Test and System Bias were repeated.

Drift between pre- and post-run System Bias was within 3 percent of the Calibration Span or 0.5 ppmv/% absolute difference. If the drift exceeded 3 percent or 0.5 ppmv%, the Calibration Error Test and System Bias were repeated.

To determine the number of sampling points, a gas stratification check was conducted prior to initiating testing. The pollutant concentrations were measured at three points (16.7, 50.0 and 83.3 percent of the measurement line). Each traverse point was sampled for a minimum of twice the system response time.

If the pollutant concentration at each traverse point did not differ more than 5 percent or 0.5 ppmv/0.3% (whichever was less restrictive) of the average pollutant concentration, then single point sampling was conducted during the test

runs. If the pollutant concentration did not meet these specifications but differed less than 10 percent or 1.0 ppmv/0.5% from the average concentration, then three (3) point sampling was conducted (stacks less than 7.8 feet in diameter - 16.7, 50.0 and 83.3 percent of the measurement line; stacks greater than 7.8 feet in diameter – 0.4, 1.0, and 2.0 meters from the stack wall). If the pollutant concentration differed by more than 10 percent or 1.0 ppmv/0.5% from the average concentration, then sampling was conducted at a minimum of twelve (12) traverse points. Copies of stratification check data can be found in the Quality Assurance/Quality Control Appendix.

A Data Acquisition System with battery backup was used to record the instrument response in one (1) minute averages. The data was continuously stored as a *.CSV file in Excel format on the hard drive of a computer. At the completion of testing, the data was also saved to the Alliance server. All data was reviewed by the Field Team Leader before leaving the facility. Once arriving at Alliance's office, all written and electronic data was relinquished to the report coordinator and then a final review was performed by the Project Manager.

Location: PotlatchDeltic / Gwinn Sawmill - Gwinn, MI

Source: Boiler No. 2

Project No.: AST-2024-0207

Run No.: 1

Parameter: Benzo[a]Pyrene

Meter Pressure (Pm), in. Hg

$$P_m = P_b + \frac{\Delta H}{136}$$

where,

Pb	28.55	= barometric pressure, in. Hg
ΔH	1.315	= pressure differential of orifice, in. H ₂ O
Pm	28.65	= in. Hg

Absolute Stack Gas Pressure (Ps), in. Hg

$$P_s = P_b + \frac{P_g}{136}$$

where,

Pb	28.55	= barometric pressure, in. Hg
Pg	-0.44	= static pressure, in. H ₂ O
Ps	28.52	= in. Hg

Standard Meter Volume (Vmstd), dscf

$$V_{mstd} = \frac{17.636 \times Y \times V_m \times P_m}{T_m}$$

where,

Y	1.001	= meter correction factor
V _m	37.440	= meter volume, cf
P _m	28.65	= absolute meter pressure, in. Hg
T _m	532.2	= absolute meter temperature, °R
V _{mstd}	35.579	= dscf

Standard Wet Volume (Vwstd), scf

$$V_{wstd} = 0.04716 \times V_{lc}$$

where,

V _{lc}	157.7	= weight of H ₂ O collected, g
V _{wstd}	7.437	= scf

Moisture Fraction (BWSsat), dimensionless (theoretical at saturated conditions)

$$BWS_{sat} = \frac{10^{6.37 - (\frac{2,827}{T_s + 365})}}{P_s}$$

where,

T _s	373.1	= stack temperature, °F
P _s	28.52	= absolute stack gas pressure, in. Hg
BWS _{sat}	12.072	= dimensionless

Moisture Fraction (BWS), dimensionless (measured)

$$BWS = \frac{V_{wstd}}{(V_{wstd} + V_{mstd})}$$

where,

V _{wstd}	7.437	= standard wet volume, scf
V _{mstd}	35.579	= standard meter volume, dscf
BWS	0.173	= dimensionless

Moisture Fraction (BWS), dimensionless

$$BWS = BWS_{msd} \text{ unless } BWS_{sat} < BWS_{msd}$$

where,

BWS _{sat}	12.072	= moisture fraction (theoretical at saturated conditions)
BWS _{msd}	0.173	= moisture fraction (measured)
BWS	0.173	

Location: PotlatchDeltic / Gwinn Sawmill - Gwinn, MI

Source: Boiler No. 2

Project No.: AST-2024-0207

Run No.: 1

Parameter: Benzo[a]Pyrene

Molecular Weight (DRY) (Md), lb/lb-mole

$$Md = (0.44 \times \% CO_2) + (0.32 \times \% O_2) + (0.28 (100 - \% CO_2 - \% O_2))$$

where,

CO_2	13.9	= carbon dioxide concentration, %
O_2	7.4	= oxygen concentration, %
Md	30.52	= lb/lb mol

Molecular Weight (WET) (Ms), lb/lb-mole

$$Ms = Md (1 - BWS) + 18.015 (BWS)$$

where,

Md	30.52	= molecular weight (DRY), lb/lb mol
BWS	0.173	= moisture fraction, dimensionless
Ms	28.36	= lb/lb mol

Average Velocity (Vs), ft/sec

$$Vs = 85.49 \times Cp \times (\Delta P^{1/2})_{avg} \times \sqrt{\frac{Ts}{Ps \times Ms}}$$

where,

Cp	0.840	= pitot tube coefficient
$\Delta P^{1/2}$	0.578	= velocity head of stack gas, (in. H ₂ O) ^{1/2}
Ts	832.7	= absolute stack temperature, °R
Ps	28.52	= absolute stack gas pressure, in. Hg
Ms	28.36	= molecular weight of stack gas, lb/lb mol
Vs	42.1	= ft/sec

Average Stack Gas Flow at Stack Conditions (Qa), acfm

$$Qa = 60 \times Vs \times As$$

where,

Vs	42.1	= stack gas velocity, ft/sec
As	4.75	= cross-sectional area of stack, ft ²
Qa	12,002	= acfm

Average Stack Gas Flow at Standard Conditions (Qs), dscfm

$$Qs = 17.636 \times Qa \times (1 - BWS) \times \frac{Ps}{Ts}$$

where,

Qa	12,002	= average stack gas flow at stack conditions, acfm
BWS	0.173	= moisture fraction, dimensionless
Ps	28.52	= absolute stack gas pressure, in. Hg
Ts	832.7	= absolute stack temperature, °R
Qs	5,996	= dscfm

Dry Gas Meter Calibration Check (Yqa), dimensionless

$$Yqa = \frac{Y - \left(\frac{\theta}{Vm} \sqrt{\frac{0.0319 \times Tm \times 29}{\Delta H @ \times \left(Pb + \frac{\Delta H avg.}{13.6} \right) \times Md}} \sqrt{\Delta H avg.} \right)}{100}$$

where,

Y	1.001	= meter correction factor, dimensionless
θ	60	= run time, min.
Vm	37.44	= total meter volume, dcf
Tm	532.2	= absolute meter temperature, °R
$\Delta H @$	1.806	= orifice meter calibration coefficient, in. H ₂ O
Pb	28.55	= barometric pressure, in. Hg
$\Delta H avg.$	1.315	= average pressure differential of orifice, in H ₂ O
Md	30.52	= molecular weight (DRY), lb/lb mol
$(\Delta H)^{1/2}$	1.142	= average squareroot pressure differential of orifice, (in. H ₂ O) ^{1/2}
Yqa	-2.1	= percent

Location: PotlatchDeltic / Gwinn Sawmill - Gwinn, MI

Source: Boiler No. 2

Project No.: AST-2024-0207

Run No.: 1

Parameter: Benzo[a]Pyrene

Volume of Nozzle (Vn), ft³

$$V_n = \frac{T_s}{P_s} \left(0.002669 \times V_{lc} + \frac{V_m \times P_m \times Y}{T_m} \right)$$

where,

T _s	832.7	= absolute stack temperature, °R
P _s	28.52	= absolute stack gas pressure, in. Hg
V _{lc}	157.7	= volume of H ₂ O collected, ml
V _m	37.440	= meter volume, cf
P _m	28.65	= absolute meter pressure, in. Hg
Y	1.001	= meter correction factor, unitless
T _m	532.2	= absolute meter temperature, °R
V _n	71.199	= volume of nozzle, ft ³

Isokinetic Sampling Rate (I), %

$$I = \left(\frac{V_n}{\theta \times 60 \times A_n \times V_s} \right) \times 100$$

where,

V _n	71.199	= nozzle volume, ft ³
θ	60.0	= run time, minutes
A _n	0.00049	= area of nozzle, ft ²
V _s	42.1	= average velocity, ft/sec
I	95.6	= %

Benzo[a]pyrene Concentration (C_{C20H12}), ug/dscm

$$C_{C20H12} = \frac{M_{C20H12} \times 35.313}{Vmstd}$$

where,

M _{C20H12}	0.04	= benzo[a]pyrene mass, ug
V _{mstd}	35.579	= standard meter volume, dscf
C _{C20H12}	0.036	= ug/dscm

Benzo[a]pyrene Emission Rate (ER_{C20H12}), lb/hr

$$ER_{C20H12} = \frac{M_{C20H12} \times Q_s \times 60}{Vmstd \times 4.54E + 08}$$

where,

M _{C20H12}	0.0	= benzo[a]pyrene mass, ug
Q _s	5.996	= average stack gas flow at standard conditions, dscfm
V _{mstd}	35.579	= standard meter volume, dscf
ER _{C20H12}	8.1E-07	= lb/hr

Benzo[a]pyrene Emission Rate (ER_{C20H12}), ton/yr

$$ER_{C20H12TPY} = \frac{ER_{C20H12} \times 8,760 \frac{hr}{yr}}{2.0E + 02}$$

where,

ER _{C20H12}	8.1E-07	= benzo[a]pyrene emission rate, lb/hr
ER _{C20H12TPY}	3.5E-06	= ton/yr

Location: PotlatchDeltic / Gwinn Sawmill - Gwinn, MI

Source: Boiler No. 2

Project No.: AST-2024-0207

Run No.: 1

Parameter: PM

Meter Pressure (Pm), in. Hg

$$P_m = P_b + \frac{\Delta H}{13.6}$$

where,

P_b	<u>28.55</u>	= barometric pressure, in. Hg
ΔH	<u>1.251</u>	= pressure differential of orifice, in. H ₂ O
P_m	<u>28.64</u>	= in. Hg

Absolute Stack Gas Pressure (Ps), in. Hg

$$P_s = P_b + \frac{P_g}{13.6}$$

where,

P_b	<u>28.55</u>	= barometric pressure, in. Hg
P_g	<u>-0.44</u>	= static pressure, in. H ₂ O
P_s	<u>28.52</u>	= in. Hg

Standard Meter Volume (Vmstd), dscf

$$V_{mstd} = \frac{17.636 \times Y \times V_m \times P_m}{T_m}$$

where,

Y	<u>0.995</u>	= meter correction factor
V_m	<u>37.420</u>	= meter volume, cf
P_m	<u>28.64</u>	= absolute meter pressure, in. Hg
T_m	<u>528.4</u>	= absolute meter temperature, °R
V_{mstd}	<u>35.595</u>	= dscf

Standard Wet Volume (Vwstd), scf

$$V_{wstd} = 0.04716 \times V_{lc}$$

where,

V_{lc}	<u>161</u>	= weight of H ₂ O collected, g
V_{wstd}	<u>7.593</u>	= scf

Moisture Fraction (BWSsat), dimensionless (theoretical at saturated conditions)

$$BWS_{sat} = \frac{10^{6.37 - \left(\frac{2.827}{T_s + 365} \right)}}{P_s}$$

where,

T_s	<u>371.4</u>	= stack temperature, °F
P_s	<u>28.52</u>	= absolute stack gas pressure, in. Hg
BWS_{sat}	<u>11.828</u>	= dimensionless

Moisture Fraction (BWS), dimensionless (measured)

$$BWS = \frac{V_{wstd}}{(V_{wstd} + V_{mstd})}$$

where,

V_{wstd}	<u>7.593</u>	= standard wet volume, scf
V_{mstd}	<u>35.595</u>	= standard meter volume, dscf
BWS	<u>0.176</u>	= dimensionless

Moisture Fraction (BWS), dimensionless

$$BWS = BWS_{msd} \text{ unless } BWS_{sat} < BWS_{msd}$$

where,

BWS_{sat}	<u>11.828</u>	= moisture fraction (theoretical at saturated conditions)
BWS_{msd}	<u>0.176</u>	= moisture fraction (measured)
BWS	<u>0.176</u>	

Location: PotlatchDeltic / Gwinn Sawmill - Gwinn, MI

Source: Boiler No. 2

Project No.: AST-2024-0207

Run No.: 1

Parameter: PM

Molecular Weight (DRY) (Md), lb/lb-mole

$$Md = (0.44 \times \% CO_2) + (0.32 \times \% O_2) + (0.28 (100 - \% CO_2 - \% O_2))$$

where,

CO_2	<u>13.9</u>	= carbon dioxide concentration, %
O_2	<u>7.4</u>	= oxygen concentration, %
Md	<u>30.52</u>	= lb/lb mol

Molecular Weight (WET) (Ms), lb/lb-mole

$$Ms = Md (1 - BWS) + 18.015 (BWS)$$

where,

Md	<u>30.52</u>	= molecular weight (DRY), lb/lb mol
BWS	<u>0.176</u>	= moisture fraction, dimensionless
Ms	<u>28.32</u>	= lb/lb mol

Average Velocity (Vs), ft/sec

$$Vs = 85.49 \times Cp \times (\Delta P^{1/2})_{avg} \times \sqrt{\frac{Ts}{Ps \times Ms}}$$

where,

Cp	<u>0.840</u>	= pitot tube coefficient
$\Delta P^{1/2}$	<u>0.584</u>	= velocity head of stack gas, (in. H ₂ O) ^{1/2}
Ts	<u>831.0</u>	= absolute stack temperature, °R
Ps	<u>28.52</u>	= absolute stack gas pressure, in. Hg
Ms	<u>28.32</u>	= molecular weight of stack gas, lb/lb mol
Vs	<u>42.5</u>	= ft/sec

Average Stack Gas Flow at Stack Conditions (Qa), acfm

$$Qa = 60 \times Vs \times As$$

where,

Vs	<u>42.5</u>	= stack gas velocity, ft/sec
As	<u>4.75</u>	= cross-sectional area of stack, ft ²
Qa	<u>12,117</u>	= acfm

Average Stack Gas Flow at Standard Conditions (Qs), dscfm

$$Qs = 17.636 \times Qa \times (1 - BWS) \times \frac{Ps}{Ts}$$

where,

Qa	<u>12,117</u>	= average stack gas flow at stack conditions, acfm
BWS	<u>0.176</u>	= moisture fraction, dimensionless
Ps	<u>28.52</u>	= absolute stack gas pressure, in. Hg
Ts	<u>831.0</u>	= absolute stack temperature, °R
Qs	<u>6,044</u>	= dscfm

Dry Gas Meter Calibration Check (Yqa), dimensionless

$$Yqa = \frac{Y - \left(\frac{\theta}{Vm} \sqrt{\frac{0.0319 \times Tm \times 29}{\Delta H@ \times \left(Pb + \frac{\Delta H_{avg.}}{13.6} \right) \times Md}} \sqrt{\Delta H_{avg.}} \right)}{\sqrt{\Delta H_{avg.}}} \times 100$$

where,

Y	<u>0.995</u>	= meter correction factor, dimensionless
θ	<u>60</u>	= run time, min.
Vm	<u>37.42</u>	= total meter volume, dcf
Tm	<u>528.4</u>	= absolute meter temperature, °R
$\Delta H@$	<u>1.764</u>	= orifice meter calibration coefficient, in. H ₂ O
Pb	<u>28.55</u>	= barometric pressure, in. Hg
$\Delta H_{avg.}$	<u>1.251</u>	= average pressure differential of orifice, in H ₂ O
Md	<u>30.52</u>	= molecular weight (DRY), lb/lb mol
$(\Delta H)^{1/2}$	<u>1.112</u>	= average square root pressure differential of orifice, (in. H ₂ O) ^{1/2}
Yqa	<u>-0.9</u>	= percent

Location: PotlatchDeltic / Gwinn Sawmill - Gwinn, MI

Source: Boiler No. 2

Project No.: AST-2024-0207

Run No.: 1

Parameter: PM

Volume of Nozzle (Vn), ft³

$$V_n = \frac{T_s}{P_s} \left(0.002669 \times V_{lc} + \frac{V_m \times P_m \times Y}{T_m} \right)$$

where,

T _s	831.0	= absolute stack temperature, °R
P _s	28.52	= absolute stack gas pressure, in. Hg
V _{lc}	161.0	= volume of H ₂ O collected, ml
V _m	37.420	= meter volume, cf
P _m	28.64	= absolute meter pressure, in. Hg
Y	0.995	= meter correction factor, unitless
T _m	528.4	= absolute meter temperature, °R
V _n	71.337	= volume of nozzle, ft ³

Isokinetic Sampling Rate (I), %

$$I = \left(\frac{V_n}{\theta \times 60 \times A_n \times V_s} \right) \times 100$$

where,

V _n	71.337	= nozzle volume, ft ³
θ	60.0	= run time, minutes
A _n	0.00049	= area of nozzle, ft ²
V _s	42.5	= average velocity, ft/sec
I	95.5	= %

Filterable PM Concentration (C_s), grain/dscf

$$C_s = \frac{M_n \times 0.0154}{V_{mstd}}$$

where,

M _n	388.5	= filterable PM mass, mg
V _{mstd}	35.595	= standard meter volume, dscf
C _s	0.17	= grain/dscf

Filterable PM Emission Rate (PMR), lb/hr

$$PMR = \frac{C_s \times Q_s \times 60}{7.0E + 03}$$

where,

C _s	0.1684	= filterable PM concentration, grain/dscf
Q _s	6,044	= average stack gas flow at standard conditions, dscfm
PMR	8.7	= lb/hr

Filterable PM Emission Rate (ER_{PMTPY}), ton/yr

$$ER_{PMTPY} = \frac{PMR \times 8,760}{20E + 03}$$

where,

PMR	8.73	= filterable PM emission rate, lb/hr
ER _{PMTPY}	38.2	= ton/yr

Filterable PM Emission Factor (EF_{PM O2d}), lb/MMBtu

$$EF_{PM O2d} = \frac{M_n \times F_d}{V_{mstd} \times 4.54E + 05} \times \frac{20.9}{20.9 - O_2}$$

where,

M _n	388.5	= filterable PM mass, mg
F _d	9,600	= oxygen based fuel factor, dscf/MMBtu
V _{mstd}	35.595	= standard meter volume, dscf
O ₂	7.4	= oxygen concentration, %
EF _{PM O2d}	0.36	= lb/MMBtu



Location: PotlatchDeltic / Gwinn Sawmill - Gwinn, MI

Source: Boiler No. 2

Project No.: AST-2024-0207

Run No. /Method Run 1 / Method 3A

O₂ - Outlet Concentration (C_{O₂}), % dry

$$C_{O_2} = (C_{obs} - C_0) \times \left(\frac{C_{MA}}{(C_M - C_0)} \right)$$

where,

C _{obs}	7.3	= average analyzer value during test, % dry
C ₀	0.1	= average of pretest & posttest zero responses, % dry
C _{MA}	11.0	= actual concentration of calibration gas, % dry
C _M	10.9	= average of pretest & posttest calibration responses, % dry
C _{O₂}	7.4	= O ₂ Concentration, % dry

CO₂ - Outlet Concentration (C_{CO₂}), % dry

$$C_{CO_2} = (C_{obs} - C_0) \times \left(\frac{C_{MA}}{(C_M - C_0)} \right)$$

where,

C _{obs}	13.6	= average analyzer value during test, % dry
C ₀	0.1	= average of pretest & posttest zero responses, % dry
C _{MA}	8.4	= actual concentration of calibration gas, % dry
C _M	8.3	= average of pretest & posttest calibration responses, % dry
C _{CO₂}	13.9	= CO ₂ Concentration, % dry



Location: PotlatchDeltic / Gwinn Sawmill - Gwinn, MI

Source: Boiler No. 2

Project No.: AST-2024-0207

Run No. /Method Run 1 / Method 10

CO - Outlet Concentration (C_{CO}), ppmvd

$$C_{CO} = (C_{obs} - C_0) \times \left(\frac{C_{MA}}{C_M - C_0} \right)$$

where,

C_{obs}	278.7	= average analyzer value during test, ppmvd
C_0	0.4	= average of pretest & posttest zero responses, ppmvd
C_{MA}	257.0	= actual concentration of calibration gas, ppmvd
C_M	254.8	= average of pretest & posttest calibration responses, ppmvd
C_{CO}	281.1	= CO Concentration, ppmvd

CO - Outlet Concentration ($C<COc3>$), ppmvd @ 3% O₂

$$C<COc3> = C<CO> \times \left(\frac{20.9 - 3}{20.9 - O_2} \right)$$

where,

C_{CO}	281.1	= CO - Outlet Concentration, ppmvd
O_2	7.4	= oxygen concentration, %
$C<COc3>$	371.5	= ppmvd @3% O ₂

CO - Outlet Emission Rate (ER_{CO}), lb/hr

$$ER_{CO} = \frac{C_{CO} \times MW \times Q_s \times 60 \frac{\text{min}}{\text{hr}} \times 28.32 \frac{\text{L}}{\text{min}}}{24.04 \frac{\text{L}}{\text{a-mole}} \times 1.0E06 \times 453.592 \frac{\text{g}}{\text{lb}}} \frac{\text{g}}{\text{hr}}$$

where,

C_{CO}	281.1	= CO - Outlet Concentration, ppmvd
MW	28.01	= CO molecular weight, g/g-mole
Q_s	6,044	= stack gas volumetric flow rate at standard conditions, dscfm
ER_{CO}	7.4	= lb/hr

CO - Outlet Emission Rate (ER_{COTPD}), ton/day

$$ER_{COTPD} = \frac{C_{CO}}{2,000 \frac{\text{lb}}{\text{ton}} \times 24 \frac{\text{hr}}{\text{day}}}$$

where,

ER_{CO}	7.42	= CO - Outlet Emission Rate, lb/hr
ER_{COTPY}	0.089	= ton/day

CO - Outlet Emission Rate (ER_{COTPY}), ton/yr

$$ER_{COTPY} = \frac{ER_{CO} \times 8,760 \frac{\text{hr}}{\text{yr}}}{2,000 \frac{\text{lb}}{\text{ton}}}$$

where,

ER_{CO}	7.42	= CO - Outlet Emission Rate, lb/hr
ER_{COTPY}	32.5	= ton/yr

CO - Outlet Emission Factor (EF_{COO,d}), lb/MMBtu

$$EF_{COO,d} = ER_{CO} \times K \times F_d \times \left(\frac{20.9}{20.9 - C_{O_2}} \right)$$

where,

C_{CO}	281.1	= CO - Outlet Concentration, ppmvd
K	7.27456E-08	= constant, lb/dscf · ppmvd
F_d	9,600	= fuel factor, dscf/MMBtu
C_{O_2}	7.354722852	= oxygen concentration, %
$EF_{COO,d}$	0.30	= lb/MMBtu

Location PotlatchDeltic / Gwinn Sawmill - Gwinn, MI

Source Boiler No. 2

Project No. AST-2024-0207

Parameter PM

Run Number		Run 1	Run 2	Run 3	Average
Date		1/16/24	1/16/24	1/17/24	--
Start Time		13:25	15:45	11:10	--
Stop Time		14:28	16:48	12:13	--
Run Time, min	(θ)	60.0	60.0	60.0	60.0
INPUT DATA					
Fuel Factor (O2 dry), dscf/MMBtu	(Fd)	9,600	9,600	9,600	9,600
Barometric Pressure, in. Hg	(Pb)	28.55	28.55	28.40	28.50
Meter Correction Factor	(Y)	0.995	0.995	0.995	0.995
Orifice Calibration Value	(ΔH @)	1.764	1.764	1.764	1.764
Meter Volume, ft ³	(Vm)	37.420	39.000	39.080	38.500
Meter Temperature, °F	(Tm)	68.7	72.0	71.8	70.8
Meter Temperature, °R	(Tm)	528.4	531.6	531.5	530.5
Meter Orifice Pressure, in. WC	(ΔH)	1.251	1.344	1.383	1.326
Volume H ₂ O Collected, mL	(Vlc)	161.0	151.6	149.2	153.9
Nozzle Diameter, in	(Dn)	0.299	0.299	0.299	0.299
Area of Nozzle, ft ²	(An)	0.0005	0.0005	0.0005	0.0005
Filterable PM Mass, mg	(Mn)	388.5	311.9	376.3	358.9
ISOKINETIC DATA					
Standard Meter Volume, ft ³	(Vmstd)	35.595	36.880	36.776	36.417
Standard Water Volume, ft ³	(Vwstd)	7.593	7.149	7.036	7.259
Moisture Fraction Measured	(BWSmsd)	0.176	0.162	0.161	0.166
Moisture Fraction @ Saturation	(BWSSat)	11.828	12.195	10.300	11.441
Moisture Fraction	(BWS)	0.176	0.162	0.161	0.166
Meter Pressure, in Hg	(Pm)	28.64	28.65	28.50	28.60
Volume at Nozzle, ft ³	(Vn)	71.337	72.952	71.725	72.00
Isokinetic Sampling Rate, (%)	(I)	95.5	97.8	96.8	96.7
DGM Calibration Check Value, (+/- 5%)	(Y _{qa})	-0.9	-0.6	-2.1	-1.2
EMISSION CALCULATIONS					
Filterable PM Concentration, grain/dscf	(C _s)	0.17	0.13	0.16	0.15
Filterable PM Emission Rate, lb/hr	(PMR)	8.7	6.8	8.3	8.0
Filterable PM Emission Rate, ton/yr	(ER _{FPM})	38.2	30.0	36.5	34.9
Filterable PM Emission Factor, lb/MMBtu (O ₂)	(EF _{PM O2d})	0.36	0.28	0.35	0.33

Location PotlatchDeltic / Gwinn Sawmill - Gwinn, MI

Source Boiler No. 2

Project No. AST-2024-0207

Run Number		Run 1	Run 2	Run 3	Average
Date		1/16/24	1/16/24	1/17/24	--
Start Time		13:25	15:45	11:10	--
Stop Time		14:25	16:45	12:10	--
Source Data					
Fuel Factor (O2 dry), dscf/MMBtu	Fd	9,600	9,600	9,600	9,600
Input Data - Outlet					
Volumetric Flow Rate (M1-4), dscfm	Qs	6,044	6,115	6,161	6,107
Calculated Data - Outlet					
O ₂ Concentration, % dry	C _{O₂}	7.4	7.6	8.0	7.7
CO ₂ Concentration, % dry	C _{CO₂}	13.9	13.2	13.6	13.6
CO Concentration, ppmvd	C _{CO}	281.1	190.2	394.6	288.7
CO Concentration, ppmvd @ 3 % O ₂	C _{CO₂3}	371.5	256.5	547.0	391.7
CO Emission Rate, lb/hr	ER _{CO}	7.4	5.1	10.6	7.7
CO Emission Rate, ton/day	ER _{COTPD}	0.089	0.061	0.13	0.092
CO Emission Rate, ton/yr	ER _{COTPY}	32.5	22.2	46.5	33.7
CO Emission Factor, lb/MMBtu (O2d)	EF _{CO O₂d}	0.30	0.21	0.45	0.32

Location PotlatchDeltic / Gwinn Sawmill - Gwinn, MI

Source Boiler No. 2

Project No. AST-2024-0207

Parameter Benzo[a]Pyrene

Run Number		Run 1	Run 2	Run 3	Average
Date		1/16/23	1/16/24	1/17/24	--
Start Time		13:25	15:45	11:10	--
Stop Time		14:28	16:48	12:13	--
Run Time, min	(θ)	60.0	60.0	60.0	60.0
INPUT DATA					
Barometric Pressure, in. Hg	(Pb)	28.55	28.55	28.40	28.50
Meter Correction Factor	(Y)	1.001	1.001	1.001	1.001
Orifice Calibration Value	(ΔH @)	1.806	1.806	1.806	1.806
Meter Volume, ft ³	(Vm)	37.440	37.650	38.300	37.797
Meter Temperature, °F	(Tm)	72.5	71.5	75.3	73.1
Meter Temperature, °R	(Tm)	532.2	531.2	535.0	532.8
Meter Orifice Pressure, in. WC	(ΔH)	1.315	1.305	1.365	1.328
Volume H ₂ O Collected, mL	(Vlc)	157.7	143.1	139.8	146.9
Nozzle Diameter, in	(Dn)	0.300	0.300	0.300	0.300
Area of Nozzle, ft ²	(An)	0.0005	0.0005	0.0005	0.0005
Benzo[a]pyrene Mass, ug	(M _{C₂₀H₁₂})	0.0362	0.00535	0.239	0.0935
ISOKINETIC DATA					
Standard Meter Volume, ft ³	(Vmstd)	35.579	35.845	36.021	35.815
Standard Water Volume, ft ³	(Vwstd)	7.437	6.749	6.593	6.926
Moisture Fraction Measured	(BWSmsd)	0.173	0.158	0.155	0.162
Moisture Fraction @ Saturation	(BWSsat)	12.072	12.482	10.461	11.672
Moisture Fraction	(BWS)	0.173	0.158	0.155	0.162
Meter Pressure, in Hg	(Pm)	28.65	28.65	28.50	28.60
Volume at Nozzle, ft ³	(Vn)	71.199	70.739	69.870	70.60
Isokinetic Sampling Rate, (%)	(I)	95.6	97.6	97.9	97.0
DGM Calibration Check Value, (+/- 5%)	(Y _{qa})	-2.1	-1.2	-2.3	-1.9
EMISSION CALCULATIONS					
Benzo[a]pyrene Concentration, ug/dscm	(C _{C₂₀H₁₂})	0.036	0.0053	0.23	0.092
Benzo[a]pyrene Emission Rate, lb/hr	(ER _{C₂₀H₁₂})	8.1E-07	1.2E-07	5.2E-06	2.0E-06
Benzo[a]pyrene Emission Rate, ton/yr	(ER _{C₂₀H₁₂})	3.5E-06	5.1E-07	2.3E-05	8.9E-06

Italicized values were 'J' flagged by the lab as Result is less than the RL but greater than or equal to the MDL and the concentration is an approximate value.

Location PotlatchDeltic / Gwinn Sawmill - Gwinn, MI

Source Boiler No. 2

Project No. AST-2024-0207

Parameter Benzo[a]Pyrene

Run Number	Run 1	Run 2	Run 3	Average
Date	1/16/23	1/16/24	1/17/24	--
Start Time	13:25	15:45	11:10	--
Stop Time	14:28	16:48	12:13	--
Run Time, min	60.0	60.0	60.0	60.0
VELOCITY HEAD, in. WC				
Point 1	0.23	0.25	0.24	0.24
Point 2	0.25	0.27	0.26	0.26
Point 3	0.28	0.36	0.26	0.30
Point 4	0.30	0.35	0.30	0.32
Point 5	0.39	0.40	0.35	0.38
Point 6	0.38	0.39	0.37	0.38
Point 7	0.36	0.33	0.35	0.35
Point 8	0.36	0.34	0.33	0.34
Point 9	0.34	0.29	0.30	0.31
Point 10	0.37	0.28	0.33	0.33
Point 11	0.27	0.27	0.29	0.28
Point 12	0.27	0.25	0.28	0.27
Point 13	0.30	0.37	0.37	0.35
Point 14	0.40	0.36	0.37	0.38
Point 15	0.43	0.41	0.39	0.41
Point 16	0.44	0.30	0.40	0.38
Point 17	0.33	0.29	0.32	0.31
Point 18	0.32	0.30	0.25	0.29
Point 19	0.38	0.27	0.25	0.30
Point 20	0.34	0.30	0.28	0.31
CALCULATED DATA				
Square Root of ΔP , (in. WC) ^{1/2}	(ΔP)	0.578	0.563	0.559
Pitot Tube Coefficient	(C_p)	0.840	0.840	0.840
Barometric Pressure, in. Hg	(P_b)	28.55	28.55	28.40
Static Pressure, in. WC	(P_g)	-0.44	-0.44	-0.44
Stack Pressure, in. Hg	(P_s)	28.52	28.52	28.37
Stack Cross-sectional Area, ft ²	(A_s)	4.75	4.75	4.75
Temperature, °F	(T_s)	373.1	375.9	360.9
Temperature, °R	(T_s)	832.7	835.5	820.5
Moisture Fraction Measured	(BW_{Smsd})	0.173	0.158	0.155
Moisture Fraction @ Saturation	(BW_{Ssat})	12.072	12.482	10.461
Moisture Fraction	(BWS)	0.173	0.158	0.155
O ₂ Concentration, %	(O ₂)	7.35	7.62	7.98
CO ₂ Concentration, %	(CO ₂)	13.92	13.24	13.64
Molecular Weight, lb/lb-mole (dry)	(M_d)	30.52	30.42	30.50
Molecular Weight, lb/lb-mole (wet)	(M_s)	28.36	28.46	28.57
Velocity, ft/sec	(V_s)	42.1	41.0	40.4
VOLUMETRIC FLOW RATE				
At Stack Conditions, acfm	(Q_a)	12,002	11,686	11,505
At Standard Conditions, scfm	(Q_{sw})	7,249	7,034	7,015
At Standard Conditions, dscfm	(Q_s)	5,996	5,920	5,929

Method 1 Data

Location PotlatchDeltic / Gwinn Sawmill - Gwinn, MI

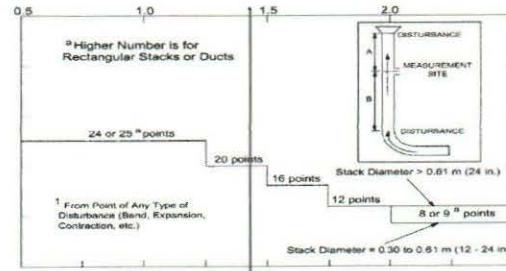
Source Boiler No. 2

Project No. AST-2024-0207

Date: 01/15/24

Stack Parameters

Duct Orientation:	Vertical
Duct Design:	Circular
Distance from Far Wall to Outside of Port:	34.00 in
Nipple Length:	4.50 in
Depth of Duct:	29.50 in
Cross Sectional Area of Duct:	4.75 ft ²
No. of Test Ports:	2
Distance A:	15.0 ft
Distance A Duct Diameters:	6.1 (must be ≥ 0.5)
Distance B:	14.0 ft
Distance B Duct Diameters:	5.7 (must be ≥ 2)
Minimum Number of Traverse Points:	20
Actual Number of Traverse Points:	20
Number of Readings per Point:	1
Measurer (Initial and Date):	COG 1/15/24
Reviewer (Initial and Date):	CRK 1/15/24



CIRCULAR DUCT

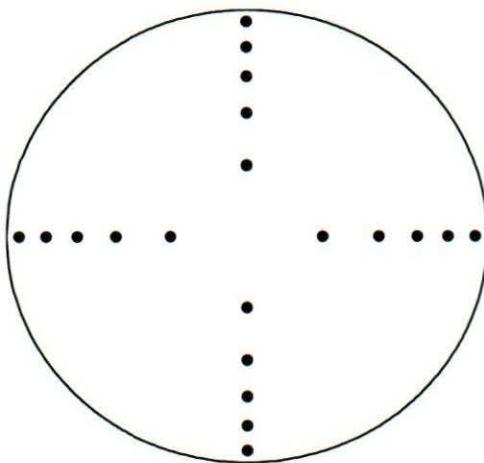
	LOCATION OF TRAVERSE POINTS Number of traverse points on a diameter											
	2	3	4	5	6	7	8	9	10	11	12	
1	14.6	--	6.7	--	4.4	--	3.2	--	2.6	--	2.1	
2	85.4	--	25.0	--	14.6	--	10.5	--	8.2	--	6.7	
3	--	--	75.0	--	29.6	--	19.4	--	14.6	--	11.8	
4	--	--	93.3	--	70.4	--	32.3	--	22.6	--	17.7	
5	--	--	--	--	85.4	--	67.7	--	34.2	--	25.0	
6	--	--	--	--	95.6	--	80.6	--	65.8	--	35.6	
7	--	--	--	--	--	--	89.5	--	77.4	--	64.4	
8	--	--	--	--	--	--	96.8	--	85.4	--	75.0	
9	--	--	--	--	--	--	--	--	91.8	--	82.3	
10	--	--	--	--	--	--	--	--	97.4	--	88.2	
11	--	--	--	--	--	--	--	--	--	--	93.3	
12	--	--	--	--	--	--	--	--	--	--	97.9	

*Percent of stack diameter from inside wall to traverse point.

Stack Diagram
A = 15 ft.
B = 14 ft.
Depth of Duct = 29.5 in.

Traverse Point	% of Diameter	Distance from inside wall	Distance from outside of port
1	2.6	1.00	5 1/2
2	8.2	2.42	6 15/16
3	14.6	4.31	8 13/16
4	22.6	6.67	11 3/16
5	34.2	10.09	14 9/16
6	65.8	19.41	23 15/16
7	77.4	22.83	27 5/16
8	85.4	25.19	29 11/16
9	91.8	27.08	31 9/16
10	97.4	28.50	33
11	--	--	--
12	--	--	--

Cross Sectional Area





Cyclonic Flow Check

Location PotlatchDeltic / Gwinn Sawmill - Gwinn, MI

Source Boiler No. 2

Project No. AST-2024-0207

Date 01/16/23

Sample Point	Angle ($\Delta P=0$)
1	5
2	0
3	0
4	0
5	0
6	0
7	0
8	0
9	0
10	0
11	0
12	0
13	0
14	0
15	0
16	0
17	0
18	0
19	0
20	0
Average	0

Location PotlatchDeltic / Gwinn Sawmill - Gwinn, MI

Source Boiler No. 2

Project No. AST-2024-0207

Parameter Benzo[a]Pyrene

Analysis Gravimetric

Run 1	Date: 1/16/23					
Impinger No.	1	2	3	4	5	Total
Contents	XAD Trap	Empty	H2O	H2O	Silica	--
Initial Mass, g	320.0	513.2	738.6	748.7	1529.6	3850.1
Final Mass, g	331.2	634.6	753.8	737.7	1550.5	4007.8
Gain	11.2	121.4	15.2	-11.0	20.9	157.7
Run 2	Date: 1/16/24					
Impinger No.	1	2	3	4	5	Total
Contents	XAD Trap	Empty	H2O	H2O	Silica	--
Initial Mass, g	316.0	492.5	725.5	663.5	1542.5	3740.0
Final Mass, g	326.4	605.7	726.7	663.3	1561.0	3883.1
Gain	10.4	113.2	1.2	-0.2	18.5	143.1
Run 3	Date: 1/17/24					
Impinger No.	1	2	3	4	5	Total
Contents	XAD Trap	Empty	H2O	H2O	Silica	--
Initial Mass, g	314.3	513.2	746.0	742.4	1580.5	3896.4
Final Mass, g	328.9	625.0	744.6	740.2	1597.5	4036.2
Gain	14.6	111.8	-1.4	-2.2	17.0	139.8



Isokinetic Field Data

Location: PotlatchDeltic / Gwinn Sawmill - Gwinn, MI Date: 1/16/23				Run 1	VALID	Start Time: 13:25 End Time: 14:28	Source: Boiler No. 2 Project No.: AST-2024-0207				Parameter: Benzo[a]Pyr.			
STACK DATA (EST)				EQUIPMENT		STACK DATA (EST)	FILTER NO.		STACK DATA (FINAL)		MOIST. DATA			
Moisture: 20.0 % est.	Meter Box ID: 14	Est. Tim: 55 °F	1	Pb: 28.55 in. Hg	Vlc (ml)									
Barometric: 28.55 in. Hg	Y: 1.001	Est. Ts: 369 °F		Pg: -0.44 in. WC	157.7									
Static Press: -0.44 in. WC	ΔH @ (in.WC): 1.806	Est. AP: 0.33 in. WC		O ₂ : 7.35 %	K-FACTOR									
Stack Press: 28.52 in. Hg	Probe ID: 08-04-a2	Est. Dn: 0.293 in.		CO ₂ : 13.92 %	3.764									
CO ₂ : 15.0 %	Liner Material: glass	Target Rate: 0.58 scfm				Check Pt.	Initial	Final	Corr.					
O ₂ : 5.0 %	Pitot ID: 08-04-a2	LEAK CHECK!	Pre	Mid 1	Mid 2	Mid 3	Post							
N ₂ /CO: 80.0 %	Pitot Cp/Type: 0.840 S-type	Leak Rate (cfm): 0.000	--	--	--	--	0.000	Mid 1 (cf)	--					
Md: 30.60 lb/lb-mole	Nozzle ID: al SS	Vacuum (in Hg): 10	--	--	--	--	9	Mid 2 (cf)	--					
Mer: 28.08 lb/lb-mole	Nozzle Dn (in.): 0.300	Pitot Tube:	Pass	--	--	--	Pass	Mid-Point Leak Check Vol (cf):	--					
Sample Pt.	Sample Time (minutes)		Dry Gas Meter Reading (ft ³)	Pitot Tube AP (in WC)	Gas Temperatures (°F)		Orifice Press. ΔH (in. WC)		Pump Vac (in. Hg)	Gas Temperatures (°F)		% ISO	Vs (fps)	
Begin	End				DGM Average	Stack	Amb.	Amb.	Ideal Actual	Probe	Filter	Imp Exit	NA	
Amb.	Amb.									Amb.	Amb.	Amb.	Amb.	
1	0.00	3.00	734.000	0.23	71	357	0.91	0.90	4	255	252	44	na	94.3 34.78
2	3.00	6.00	735.500	0.25	71	367	0.97	1.00	4	255	252	44	na	103.2 36.48
3	6.00	9.00	737.200	0.28	71	371	1.09	1.10	4	255	252	44	na	103.5 38.70
4	9.00	12.00	739.000	0.30	71	372	1.16	1.20	4	255	252	44	na	100.1 40.08
5	12.00	15.00	740.800	0.39	72	373	1.51	1.50	5	255	252	44	na	95.0 45.73
6	15.00	18.00	742.750	0.38	72	375	1.47	1.50	5	255	252	44	na	96.4 45.19
7	18.00	21.00	744.700	0.36	72	374	1.39	1.40	5	255	252	44	na	96.4 43.96
8	21.00	24.00	746.600	0.36	71	373	1.39	1.40	5	255	252	44	na	96.5 43.94
9	24.00	27.00	748.500	0.34	72	373	1.32	1.30	6	255	252	44	na	93.9 42.70
10	27.00	30.00	750.300	0.37	72	375	1.43	1.44	6	255	252	44	na	100.2 44.60
1	30.00	33.00	752.300	0.27	73	373	1.05	1.00	6	255	252	44	na	99.3 38.05
2	33.00	36.00	754.000	0.27	73	374	1.05	1.10	6	254	252	44	na	99.4 38.07
3	36.00	39.00	755.700	0.30	73	374	1.16	1.20	6	254	252	43	na	99.8 40.13
4	39.00	42.00	757.500	0.40	73	377	1.54	1.55	7	254	252	43	na	101.1 46.42
5	42.00	45.00	759.600	0.43	73	377	1.66	1.70	7	254	251	43	na	97.6 48.13
6	45.00	48.00	761.700	0.44	74	377	1.70	1.70	7	254	251	43	na	96.3 48.69
7	48.00	51.00	763.800	0.33	74	375	1.28	1.30	7	254	251	43	na	100.4 42.12
8	51.00	54.00	765.700	0.32	74	375	1.24	1.20	7	254	251	43	na	96.5 41.47
9	54.00	57.00	767.500	0.38	74	375	1.47	1.50	8	254	251	43	na	98.5 45.19
10	57.00	60.00	769.500	0.34	74	374	1.32	1.30	8	254	251	43	na	100.9 42.72
Final DGM: 771.440														
RESULTS	Run Time	Vm	ΔP	Tm	Ts	Max Vac	ΔH	%ISO	BWS	Y _{qs}				
	60.0 min	37.440 ft ³	0.34 in. WC	72.5 °F	373.1 °F	8	1.315 in. WC	95.6	0.173	-2.1				



Isokinetic Field Data

Location: PotlatchDeltic / Gwinn Sawmill - Gwinn, MI				Start Time: 15:45	Source: Boiler No. 2										
Date: 1/16/24 Run 2 VALID				End Time: 16:48	Project No.: AST-2024-0207 Parameter: Benzo[a]Pyr.										
STACK DATA (EST)	EQUIPMENT	STACK DATA (EST)	FILTER NO.	STACK DATA (FINAL)	MOIST. DATA										
Moisture: 17.3 % est.	Meter Box ID: 14	Est. Tm: 73 °F	2	Pb: 28.55 in. Hg	Vlc (ml)										
Barometric: 28.55 in. Hg	Y: 1.001	Est. Ts: 373 °F		Pg: -0.44 in. WC	143.1										
Static Press: -0.44 in. WC	ΔH @ (in.WC): 1.806	Est. ΔP: 0.34 in. WC		O ₂ : 7.62 %	K-FACTOR										
Stack Press: 28.52 in. Hg	Probe ID: 08-04-a2	Est. Dn: 0.284 in.		CO ₂ : 13.24 %	4.09										
CO ₂ : 15.0 %	Liner Material: glass	Target Rate: 0.58 scfm		Check Pt.	Initial	Final	Corr.								
O ₂ : 5.0 %	Pitot ID: 08-04-a2	LEAK CHECK! Pre	Mid 1	Mid 2	Mid 3	Post									
N ₂ /CO: 80.0 %	Pitot Cp/Type: 0.840 S-type	Leak Rate (cfm): 0.000	--	--	--	0.000	Mid 1 (cf)	--							
Md: 30.60 lb/lb-mole	Nozzle ID: al SS	Vacuum (in Hg): 10	--	--	--	8	Mid 2 (cf)	--							
Ms: 28.42 lb/lb-mole	Nozzle Dn (in.): 0.300	Pitot Tube: Pass	--	--	--	Pass	Mid-Point Leak Check Vol (cf):	--							
Sample Pt.	Sample Time (minutes)		Dry Gas Meter Reading (ft ³)	Pitot Tube ΔP (in WC)	Gas Temperatures (°F)		Orifice Press. ΔH (in. WC)	Pump Vac (in. Hg)	Gas Temperatures (°F)				% ISO	V _s (fps)	
Begin	End				DGM Average	Stack Amb.	Ideal	Actual	Probe Amb.	Filter Amb.	Imp Exit Amb.	NA Amb.			
					--	--			--	--	--	--			
1	0.00	3.00	772.000	0.25	71	375	1.02	1.00	4	254	251	44	na	100.9	36.44
2	3.00	6.00	773.700	0.27	70	376	1.10	1.10	4	254	251	44	na	103.1	37.89
3	6.00	9.00	775.500	0.36	70	376	1.46	1.50	4	254	251	44	na	99.3	43.75
4	9.00	12.00	777.500	0.35	70	376	1.42	1.50	4	254	251	44	na	100.7	43.14
5	12.00	15.00	779.500	0.40	70	375	1.62	1.70	4	254	251	44	na	98.9	46.09
6	15.00	18.00	781.600	0.39	70	375	1.58	1.60	5	254	251	44	na	100.1	45.51
7	18.00	21.00	783.700	0.33	70	375	1.34	1.40	5	254	251	44	na	98.4	41.86
8	21.00	24.00	785.600	0.34	70	375	1.38	1.40	5	254	252	44	na	97.0	42.49
9	24.00	27.00	787.500	0.29	70	376	1.18	1.20	5	254	252	44	na	99.5	39.27
10	27.00	30.00	789.300	0.28	71	376	1.14	1.10	5	254	252	44	na	95.4	38.59
1	30.00	33.00	791.000	0.27	71	375	1.10	1.10	6	254	252	44	na	102.8	37.87
2	33.00	36.00	792.800	0.25	72	376	1.02	1.00	6	255	252	44	na	100.8	36.46
3	36.00	39.00	794.500	0.37	72	376	1.51	1.50	6	255	252	44	na	100.0	44.35
4	39.00	42.00	796.550	0.36	72	375	1.47	1.50	6	255	252	44	na	96.4	43.73
5	42.00	45.00	798.500	0.41	73	377	1.67	1.70	6	255	252	44	na	97.2	46.72
6	45.00	48.00	800.600	0.30	73	378	1.22	1.20	6	255	252	44	na	97.4	39.99
7	48.00	51.00	802.400	0.29	73	377	1.18	1.10	7	255	252	44	na	99.0	39.29
8	51.00	54.00	804.200	0.30	74	377	1.23	1.20	7	255	252	44	na	97.1	39.96
9	54.00	57.00	806.000	0.27	74	376	1.11	1.10	7	255	252	44	na	102.3	37.89
10	57.00	60.00	807.800	0.30	74	375	1.23	1.20	7	255	252	44	na	99.7	39.92
Final DGM:				809.650											
RESULTS	Run Time		V _m	ΔP	T _m	T _s	Max Vac	ΔH	%ISO	BWS	Y _{qs}				
	60.0	min	37.650	ft ³	0.32	in. WC	71.5	°F	375.9	°F	7	1,305	in. WC	97.6	0.158



Isokinetic Field Data

Location: PotlatchDeltic / Gwinn Sawmill - Gwinn, MI			Start Time: 11:10		Source: Boiler No. 2										
Date: 1/17/24	Run 3	VALID	End Time: 12:13		Project No.: AST-2024-0207		Parameter: Benzo[a]Pyr.								
STACK DATA (EST)		EQUIPMENT	STACK DATA (EST)		FILTER NO.	STACK DATA (FINAL)									
Moisture: 15.8 % est.	Meter Box ID: 14		Est. Tm: 72 °F	3	Pb: 28.40 in. Hg	Vlc (ml)									
Barometric: 28.55 in Hg	Y: 1.001		Est. Ts: 376 °F		Pg: -0.44 in. WC	139.8									
Static Press: -0.44 in. WC	AH @ (in.WC): 1.806		Est. ΔP: 0.32 in. WC		O ₂ : 7.98 %	K-FACTOR									
Stack Press: 28.52 in. Hg	Probe ID: 08-04-a2		Est. Dn: 0.286 in.		CO ₂ : 13.64 %	4.189									
CO ₂ : 15.0 %	Liner Material: glass		Target Rate: 0.58 scfm		Check Pt.	Initial	Final Corr.								
O ₂ : 5.0 %	Pitot ID: 08-04-a2		LEAK CHECK!	Pre Mid 1 Mid 2 Mid 3 Post	Mid 1 (cf)		--								
N ₂ /CO: 80.0 %	Pitot Cp/Type: 0.840 S-type		Leak Rate (cfm): 0.000	-- -- -- 0.000	Mid 2 (cf)		--								
Md: 30.60 lb/lb-mole	Nozzle ID: al SS		Vacuum (in Hg): 10	-- -- -- 8	Mid 3 (cf)		--								
Ms: 28.61 lb/lb-mole	Nozzle Dn (in.): 0.300		Pitot Tube: Pass	-- -- -- Pass	Mid-Point Leak Check Vol (cf): --										
Sample Pt.	Sample Time (minutes)		Dry Gas Meter Reading (ft ³)	Gas Temperatures (°F)		Orifice Press. ΔH (in. WC)	Pump Vac (in. Hg)	Gas Temperatures (°F)				% ISO	Vs (fps)		
	Begin	End		DGM Average	Stack			Probe	Filter	Imp Exit	NA				
	Amb.	Amb.		Amb.	Amb.			Amb.	Amb.	Amb.	Amb.				
1	0.00	3.00	815.900	0.24	75	356	1.04	1.00	4	256	251	44	na	93.7	35.18
2	3.00	6.00	817.500	0.26	75	356	1.13	1.10	4	256	251	44	na	101.3	36.61
3	6.00	9.00	819.300	0.26	75	358	1.12	1.10	4	256	251	44	na	95.8	36.66
4	9.00	12.00	821.000	0.30	75	357	1.30	1.30	4	256	251	44	na	94.4	39.35
5	12.00	15.00	822.800	0.35	75	357	1.51	1.50	4	256	251	44	na	97.2	42.51
6	15.00	18.00	824.800	0.37	75	360	1.59	1.60	4	256	251	44	na	99.5	43.78
7	18.00	21.00	826.900	0.35	75	360	1.51	1.50	5	256	251	44	na	102.2	42.58
8	21.00	24.00	829.000	0.33	75	363	1.41	1.40	5	256	251	44	na	100.4	41.42
9	24.00	27.00	831.000	0.30	75	365	1.28	1.30	5	256	251	44	na	94.9	39.54
10	27.00	30.00	832.800	0.33	75	366	1.41	1.40	5	256	251	44	na	100.6	41.50
1	30.00	33.00	834.800	0.29	75	365	1.24	1.20	5	256	251	44	na	101.8	38.88
2	33.00	36.00	836.700	0.28	75	365	1.20	1.20	5	256	252	44	na	98.2	38.20
3	36.00	39.00	838.500	0.37	75	364	1.58	1.60	6	255	252	44	na	99.7	43.89
4	39.00	42.00	840.600	0.37	75	365	1.58	1.60	6	255	252	44	na	99.8	43.92
5	42.00	45.00	842.700	0.39	76	362	1.68	1.70	6	255	252	44	na	96.8	45.01
6	45.00	48.00	844.800	0.40	76	361	1.72	2.00	6	255	252	44	na	104.7	45.55
7	48.00	51.00	847.100	0.32	76	361	1.38	1.40	6	255	252	44	na	96.6	40.74
8	51.00	54.00	849.000	0.25	76	359	1.08	1.10	6	255	252	44	na	97.6	35.97
9	54.00	57.00	850.700	0.25	76	358	1.08	1.10	7	255	252	44	na	97.5	35.95
10	57.00	60.00	852.400	0.28	76	359	1.21	1.20	7	255	252	44	na	97.6	38.06
Final DGM: \$854.200															
RESULTS	Run Time		V _m	ΔP	T _m	T _s	Max Vac	ΔH	%ISO	BWS	Y _{qs}				
	60.0	min	38,300	ft ³	0.31	in. WC	75.3	°F	360.9	°F	7	1,365	in. WC	97.9	0.155

Location PotlatchDeltic / Gwinn Sawmill - Gwinn, MI

Source Boiler No. 2

Project No. AST-2024-0207

Parameter PM

Run Number	Run 1	Run 2	Run 3	Average
Date	1/16/24	1/16/24	1/17/24	--
Start Time	13:25	15:45	11:10	--
Stop Time	14:28	16:48	12:13	--
Run Time, min	60.0	60.0	60.0	60.0
VELOCITY HEAD, in. WC				
Point 1	0.25	0.23	0.25	0.24
Point 2	0.27	0.26	0.27	0.27
Point 3	0.29	0.28	0.29	0.29
Point 4	0.34	0.32	0.32	0.33
Point 5	0.35	0.34	0.35	0.35
Point 6	0.45	0.47	0.50	0.47
Point 7	0.52	0.53	0.52	0.52
Point 8	0.48	0.50	0.49	0.49
Point 9	0.43	0.38	0.38	0.40
Point 10	0.38	0.35	0.32	0.35
Point 11	0.22	0.22	0.21	0.22
Point 12	0.25	0.24	0.24	0.24
Point 13	0.29	0.28	0.29	0.29
Point 14	0.30	0.32	0.32	0.31
Point 15	0.36	0.34	0.34	0.35
Point 16	0.37	0.39	0.38	0.38
Point 17	0.40	0.40	0.40	0.40
Point 18	0.35	0.36	0.35	0.35
Point 19	0.31	0.34	0.35	0.33
Point 20	0.30	0.35	0.34	0.33
CALCULATED DATA				
Square Root of ΔP , (in. WC) ^{1/2}	(ΔP)	0.584	0.583	0.584
Pitot Tube Coefficient	(C_p)	0.840	0.840	0.840
Barometric Pressure, in. Hg	(P_b)	28.55	28.55	28.40
Static Pressure, in. WC	(P_g)	-0.44	-0.44	-0.44
Stack Pressure, in. Hg	(P_s)	28.52	28.52	28.37
Stack Cross-sectional Area, ft ²	(A_s)	4.75	4.75	4.75
Temperature, °F	(T_s)	371.4	373.9	359.6
Temperature, °R	(T_s)	831.0	833.6	819.3
Moisture Fraction Measured	(BWSmsd)	0.176	0.162	0.161
Moisture Fraction @ Saturation	(BWSSat)	11.828	12.195	10.300
Moisture Fraction	(BWS)	0.176	0.162	0.161
O ₂ Concentration, %	(O ₂)	7.35	7.62	7.98
CO ₂ Concentration, %	(CO ₂)	13.92	13.24	13.64
Molecular Weight, lb/lb-mole (dry)	(M _d)	30.52	30.42	30.50
Molecular Weight, lb/lb-mole (wet)	(M _s)	28.32	28.41	28.50
Velocity, ft/sec	(V _s)	42.5	42.5	42.2
VOLUMETRIC FLOW RATE				
At Stack Conditions, acfm	(Q _a)	12,117	12,099	12,020
At Standard Conditions, scfm	(Q _{sw})	7,333	7,300	7,340
At Standard Conditions, dscfm	(Q _s)	6,044	6,115	6,161
				6,107

Method 1 Data

Location PotlatchDeltic / Gwinn Sawmill - Gwinn, MI

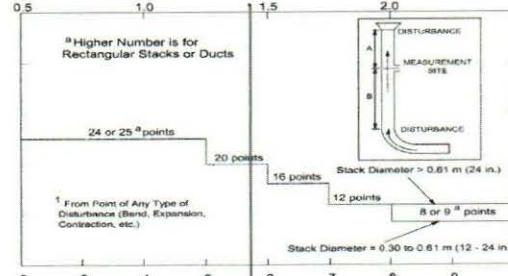
Source Boiler No. 2

Project No. AST-2024-0207

Date: 01/16/24

Stack Parameters

Duct Orientation:	Vertical
Duct Design:	Circular
Distance from Far Wall to Outside of Port:	34.00 in
Nipple Length:	4.50 in
Depth of Duct:	29.50 in
Cross Sectional Area of Duct:	4.75 ft ²
No. of Test Ports:	2
Distance A:	15.0 ft
Distance A Duct Diameters:	6.1 (must be ≥ 0.5)
Distance B:	14.0 ft
Distance B Duct Diameters:	5.7 (must be ≥ 2)
Minimum Number of Traverse Points:	20
Actual Number of Traverse Points:	20
Number of Readings per Point:	1
Measurer (Initial and Date):	COG 1/15
Reviewer (Initial and Date):	RA 1/15



CIRCULAR DUCT

LOCATION OF TRAVERSE POINTS Number of traverse points on a diameter												
	2	3	4	5	6	7	8	9	10	11	12	
1	14.6	--	6.7	--	4.4	--	3.2	--	2.6	--	2.1	
2	85.4	--	25.0	--	14.6	--	10.5	--	8.2	--	6.7	
3	--	--	75.0	--	29.6	--	19.4	--	14.6	--	11.8	
4	--	--	93.3	--	70.4	--	32.3	--	22.6	--	17.7	
5	--	--	--	--	85.4	--	67.7	--	34.2	--	25.0	
6	--	--	--	--	95.6	--	80.6	--	65.8	--	35.6	
7	--	--	--	--	--	--	89.5	--	77.4	--	64.4	
8	--	--	--	--	--	--	96.8	--	85.4	--	75.0	
9	--	--	--	--	--	--	--	--	91.8	--	82.3	
10	--	--	--	--	--	--	--	--	97.4	--	88.2	
11	--	--	--	--	--	--	--	--	--	--	93.3	
12	--	--	--	--	--	--	--	--	--	--	97.9	

*Percent of stack diameter from inside wall to traverse point.

Traverse Point	% of Diameter	Distance from inside wall	Distance from outside of port
1	2.6	1.00	5 1/2
2	8.2	2.42	6 15/16
3	14.6	4.31	8 13/16
4	22.6	6.67	11 3/16
5	34.2	10.09	14 9/16
6	65.8	19.41	23 15/16
7	77.4	22.83	27 5/16
8	85.4	25.19	29 11/16
9	91.8	27.08	31 9/16
10	97.4	28.50	33
11	--	--	--
12	--	--	--

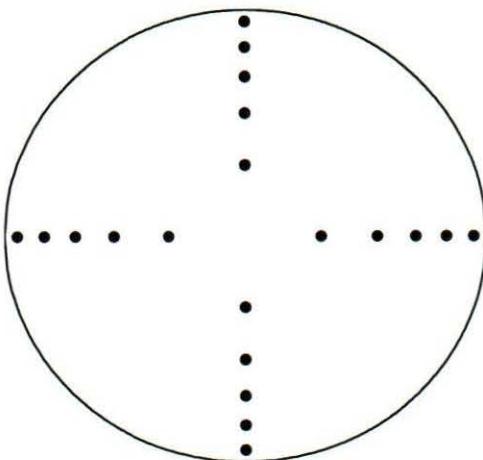
Stack Diagram

A = 15 ft.

B = 14 ft.

Depth of Duct = 29.5 in.

Cross Sectional Area



Downstream Disturbance





Cyclonic Flow Check

Location PotlatchDeltic / Gwinn Sawmill - Gwinn, MI

Source Boiler No. 2

Project No. AST-2024-0207

Date 01/16/24

Sample Point	Angle ($\Delta P=0$)
1	5
2	0
3	0
4	0
5	0
6	0
7	0
8	0
9	0
10	0
11	0
12	0
13	0
14	0
15	0
16	0
17	0
18	0
19	0
20	0
Average	0

Location PotlatchDeltic / Gwinn Sawmill - Gwinn, MI

Source Boiler No. 2

Project No. AST-2024-0207

Parameter PM

Analysis Gravimetric

Run 1		Date: 1/16/24				
Impinger No.	1	2	3	4	Total	
Contents	H2O	H2O	Empty	Silica	--	
Initial Mass, g	488.7	451.1	410.0	1621.0	2970.8	
Final Mass, g	638.1	451.1	410.0	1632.6	3131.8	
Gain	149.4	0.0	0.0	11.6	161.0	
Run 2		Date: 1/16/24				
Impinger No.	1	2	3	4	Total	
Contents	H2O	H2O	Empty	Silica	--	
Initial Mass, g	485.0	451.1	410.0	1632.6	2978.7	
Final Mass, g	622.6	451.1	410.0	1646.6	3130.3	
Gain	137.6	0.0	0.0	14.0	151.6	
Run 3		Date: 1/17/24				
Impinger No.	1	2	3	4	Total	
Contents	H2O	H2O	Empty	Silica	--	
Initial Mass, g	526.3	451.1	410.0	1646.6	3034.0	
Final Mass, g	662.5	451.1	410.0	1659.6	3183.2	
Gain	136.2	0.0	0.0	13.0	149.2	



Isokinetic Field Data

Location: PotlatchDeltic / Gwinn Sawmill - Gwinn, MI			Start Time: 13:25		Source: Boiler No. 2											
Date: 1/16/24	Run 1	VALID	End Time: 14:28		Project No.: AST-2024-0207		Parameter: PM									
STACK DATA (EST)		EQUIPMENT		STACK DATA (EST)		FILTER NO.	STACK DATA (FINAL)									
Moisture: 21.0 % est.		Meter Box ID: 17		Est. Tm: 65 °F	2361	Pb: 28.55 in Hg	Vlc (ml)									
Barometric: 28.55 in. Hg		Y: 0.995		Est. Ts: 369 °F		Pg: -0.44 in. WC	161.0									
Static Press: -0.44 in. WC		ΔH @ (in.WC): 1.764		Est. ΔP: 0.33 in. WC		O ₂ : 7.35 %	K-FACTOR									
Stack Press: 28.52 in Hg		Probe ID: 05-04-G1		Est. Dn: 0.278 in.		CO ₂ : 13.92 %	3.618									
CO ₂ : 13.0 %		Liner Material: glass		Target Rate: 0.53 scfm												
O ₂ : 6.0 %		Pitot ID: 05-04-G1		LEAK CHECK! Pre	Mid 1	Mid 2	Mid 3 Post									
N ₂ /CO: 81.0 %		Pitot Cp/Type: 0.840 S-type		Leak Rate (cfm): 0.000	--	--	0.000									
Md: 30.32 lb/lb-mole		Nozzle ID: ss	SS	Vacuum (in Hg): 14	--	--	14									
Ms: 27.73 lb/lb-mole		Nozzle Dn (in.): 0.299		Pitot Tube: Pass	--	--	Pass									
Check Pt. Initial Final Corr.																
Mid 1 (cf)		Mid 2 (cf)		Mid 3 (cf)		Mid-Point Leak Check Vol (cf):										
Sample Pt.	Sample Time (minutes)		Dry Gas Meter Reading (ft ³)	Gas Temperatures (°F)		Orifice Press. ΔH (in. WC)	Pump Vac (in. Hg)	Gas Temperatures (°F)				% ISO	Vs (fps)			
	Begin	End		DGM Average	Stack Amb.			Amb.	Ideal	Actual	Probe Amb.			Filter Amb.	Imp Exit Amb.	NA Amb.
				62	-6						-6			-6	-6	-6
1	0.00	3.00	913.520	0.25	64	350	0.93	0.93	3	245	241	38	-	102.3	36.33	
2	3.00	6.00	915.190	0.27	66	369	0.98	0.98	3	245	241	38	-	101.6	38.20	
3	6.00	9.00	916.900	0.29	66	370	1.05	1.10	3	246	240	40	-	98.7	39.61	
4	9.00	12.00	918.620	0.34	67	372	1.23	1.20	4	246	239	40	-	97.0	42.94	
5	12.00	15.00	920.450	0.35	68	374	1.27	1.30	4	244	239	41	-	98.7	43.62	
6	15.00	18.00	922.340	0.45	68	375	1.63	1.60	5	244	242	41	-	95.4	49.49	
7	18.00	21.00	924.410	0.52	68	375	1.88	1.90	6	243	242	41	-	98.3	53.20	
8	21.00	24.00	926.700	0.48	69	374	1.74	1.70	6	243	244	41	-	100.2	51.08	
9	24.00	27.00	928.950	0.43	69	370	1.57	1.60	6	245	244	41	-	98.1	48.23	
10	27.00	30.00	931.040	0.38	69	371	1.38	1.20	5	245	244	41	-	97.8	45.37	
1	30.00	33.00	933.000	0.22	70	372	0.80	0.80	4	245	244	41	-	102.1	34.54	
2	33.00	36.00	934.560	0.25	70	371	0.91	0.91	5	245	242	41	-	95.1	36.80	
3	36.00	39.00	936.110	0.29	70	371	1.06	1.10	6	245	242	41	-	96.3	39.63	
4	39.00	42.00	937.800	0.30	70	373	1.09	1.10	7	245	242	41	-	98.8	40.36	
5	42.00	45.00	939.560	0.36	70	378	1.30	1.30	8	246	242	41	-	98.2	44.34	
6	45.00	48.00	941.470	0.37	70	377	1.34	1.30	8	246	242	41	-	97.8	44.93	
7	48.00	51.00	943.400	0.40	70	376	1.45	1.50	10	243	242	41	-	98.0	46.69	
8	51.00	54.00	945.410	0.35	70	375	1.27	1.30	10	243	242	41	-	99.4	43.64	
9	54.00	57.00	947.320	0.31	70	368	1.14	1.10	10	241	243	41	-	101.3	40.90	
10	57.00	60.00	949.160	0.30	70	366	1.10	1.10	10	241	243	41	-	99.5	40.19	
Final DGM: 950.940																
RESULTS	Run Time		Vm	ΔP	Tm	Ts	Max Vac	ΔH	%ISO	BWS	Y _{qs}					
	60.0	min	37.420	ft ³	0.35	in. WC	68.7	°F	371.4	°F	10	1.251	in. WC	95.5	0.176	-0.9



Isokinetic Field Data

Location: PotlatchDeltic / Gwinn Sawmill - Gwinn, MI			Start Time: 15:45		Source: Boiler No. 2									
Date: 1/16/24	Run 2	VALID	End Time: 16:48		Project No.: AST-2024-0207		Parameter: PM							
STACK DATA (EST)		EQUIPMENT	STACK DATA (EST)		FILTER NO.	STACK DATA (FINAL)								
Moisture: 18.0 % est.	Meter Box ID: 17	Est. Tm: 69 °F	2362	Pb: 28.55 in. Hg	Vic (ml)									
Barometric: 28.55 in. Hg	Y: 0.995	Est. Ts: 371 °F		Pg: -0.44 in. WC	151.6									
Static Press: -0.44 in. WC	ΔH @ (in.WC): 1.764	Est. ΔP: 0.35 in. WC		O ₂ : 7.62 %	K-FACTOR									
Stack Press: 28.52 in. Hg	Probe ID: 05-04-G1	Est. Dn: 0.271 in.		CO ₂ : 13.24 %	3.86									
CO ₂ : 13.0 %	Liner Material: glass	Target Rate: 0.53 scfm				Check Pt.	Initial Final Corr.							
O ₂ : 6.0 %	Pitot ID: 05-04-G1	LEAK CHECK!	Pre Mid 1 Mid 2 Mid 3 Post			Mid 1 (cf)	--							
N ₂ /CO: 81.0 %	Pitot Cp/Type: 0.840 S-type	Leak Rate (cfm): 0.000 -- -- -- 0.000				Mid 2 (cf)	--							
Md: 30.32 lb/lb-mole	Nozzle ID: ss SS	Vacuum (in Hg): 15 -- -- -- 14				Mid 3 (cf)	--							
Ms: 28.10 lb/lb-mole	Nozzle Dn (in.): 0.299	Pitot Tube: Pass -- -- -- Pass				Mid-Point Leak Check Vol (cf):	--							
Sample Pt.	Sample Time (minutes)		Dry Gas Meter Reading (ft ³)	Pitot Tube ΔP (in WC)	Gas Temperatures (°F)		Orifice Press. ΔH (in. WC)	Pump Vac (in. Hg)	Gas Temperatures (°F)				% ISO	Vs (fps)
	Begin	End			DGM Average	Stack Amb.	Amb.	Amb.	Probe Amb.	Filter Amb.	Imp Exit Amb.	NA Amb.		
1	0.00	3.00	958.700	0.23	70	378	0.89	0.89	2	240	241	40	-	102.2 35.21
2	3.00	6.00	960.340	0.26	71	374	1.01	1.00	2	240	241	41	-	101.6 37.35
3	6.00	9.00	962.080	0.28	71	374	1.08	1.10	2	246	244	42	-	99.6 38.76
4	9.00	12.00	963.850	0.32	72	378	1.24	1.20	3	246	244	42	-	98.5 41.53
5	12.00	15.00	965.720	0.34	72	375	1.32	1.30	4	248	244	42	-	96.9 42.73
6	15.00	18.00	967.620	0.47	72	375	1.82	1.80	6	248	244	42	-	97.8 50.24
7	18.00	21.00	969.870	0.53	72	374	2.05	2.10	7	247	244	42	-	98.6 53.32
8	21.00	24.00	972.280	0.50	72	372	1.94	2.00	7	247	244	42	-	99.7 51.73
9	24.00	27.00	974.650	0.38	72	371	1.48	1.50	6	245	244	42	-	102.1 45.07
10	27.00	30.00	976.770	0.35	72	370	1.36	1.40	6	245	245	42	-	102.3 43.23
1	30.00	33.00	978.810	0.22	72	371	0.86	0.86	4	245	245	42	-	101.7 34.29
2	33.00	36.00	980.420	0.24	72	374	0.93	0.93	5	245	244	42	-	99.4 35.88
3	36.00	39.00	982.060	0.28	72	374	1.09	1.10	6	244	244	42	-	98.3 38.76
4	39.00	42.00	983.810	0.32	72	374	1.24	1.20	6	244	244	42	-	100.4 41.43
5	42.00	45.00	985.720	0.34	72	373	1.32	1.30	7	244	244	42	-	96.3 42.68
6	45.00	48.00	987.610	0.39	72	376	1.51	1.50	8	244	244	42	-	99.7 45.79
7	48.00	51.00	989.700	0.40	72	373	1.55	1.60	9	244	244	42	-	99.7 46.29
8	51.00	54.00	991.820	0.36	73	374	1.40	1.40	9	245	244	42	-	97.5 43.95
9	54.00	57.00	993.790	0.34	73	375	1.32	1.30	9	245	244	42	-	98.3 42.73
10	57.00	60.00	995.720	0.35	73	373	1.36	1.40	10	245	244	42	-	99.3 43.30
Final DGM: 997.700														
RESULTS	Run Time		V _m	A _P	T _m	T _s	Max Vac	ΔH	%ISO	BWS	V _{qs}			
	60.0	min	39.000 ft ³	0.35 in. WC	72.0 °F	373.9 °F	10	1.344 in. WC	97.8	0.162	-0.6			



Isokinetic Field Data

Location: PotlatchDeltic / Gwinn Sawmill - Gwinn, MI Date: 1/17/24 Run 3 VALID				Start Time: 11:10 End Time: 12:13				Source: Boiler No. 2 Project No.: AST-2024-0207 Parameter: PM			
STACK DATA (EST)		EQUIPMENT		STACK DATA (EST)		FILTER NO.		STACK DATA (FINAL)		MOIST. DATA	
Moisture:	18.0 % est.	Meter Box ID:	17	Est. Tm:	72 °F	2363	Pb:	28.40	in Hg	Vlc (ml)	
Barometric:	28.55 in Hg	Y:	0.995	Est. Ts:	374 °F		Pg:	-0.44	in. WC	149.2	
Static Press:	-0.44 in. WC	ΔH @ (in.WC):	1.764	Est. ΔP:	0.35 in. WC		O ₂ :	7.98 %		K-FACTOR	
Stack Press:	28.52 in Hg	Probe ID:	05-04-G1	Est. Dn:	0.270 in.		CO ₂ :	13.64 %		3.875	
CO ₂ :	13.0 %	Liner Material:	glass	Target Rate:	0.53 scfm		Check Pt.	Initial	Final	Corr.	
O ₂ :	6.0 %	Pitot ID:	05-04-G1	LEAK CHECK:	Pre Mid 1 Mid 2 Mid 3 Post		Mid 1 (cf)			--	
N ₂ /CO:	81.0 %	Pitot Cp/Type:	0.840 S-type	Leak Rate (cfm):	0.000	--	Mid 2 (cf)			--	
Md:	30.32 lb/lb-mole	Nozzle ID:	ss	Vacuum (in Hg):	15	--	Mid 3 (cf)			--	
Ms:	28.10 lb/lb-mole	Nozzle Dn (in.):	0.299	Pitot Tube:	Pass	--	Pass	Mid-Point Leak Check Vol (cf):	--		
Sample Pt.	Sample Time (minutes)		Dry Gas Meter Reading (ft ³)	Pitot Tube ΔP (in WC)	Gas Temperatures (°F)		Orifice Press. ΔH (in. WC)		Pump Vac (in. Hg)	Gas Temperatures (°F)	
	Begin	End			DGM	Average	Stack Amb.	Amb.	Amb.	Probe Amb.	Filter Amb.
					--	--	Ideal	Actual	--	--	Imp. Exit
0.23	1	0.00	3.00	2.250	0.25	69	359	0.98	2	246	239
0.26	2	3.00	6.00	4.000	0.27	71	356	1.07	1.10	2	246
0.28	3	6.00	9.00	5.800	0.29	72	357	1.15	1.20	3	244
0.32	4	9.00	12.00	7.600	0.32	72	356	1.27	1.30	3	244
0.34	5	12.00	15.00	9.500	0.35	72	357	1.39	1.40	4	245
0.47	6	15.00	18.00	11.520	0.50	72	360	1.97	2.00	6	245
0.53	7	18.00	21.00	13.820	0.52	72	361	2.05	2.10	7	245
0.5	8	21.00	24.00	16.200	0.49	72	360	1.93	1.90	7	245
0.38	9	24.00	27.00	18.490	0.38	72	360	1.50	1.50	6	244
0.35	10	27.00	30.00	20.520	0.32	72	355	1.27	1.30	6	244
0.22	1	30.00	33.00	22.470	0.21	72	359	0.83	0.83	5	244
0.24	2	33.00	36.00	24.050	0.24	72	362	0.95	0.95	5	244
0.28	3	36.00	39.00	25.700	0.29	72	360	1.14	1.20	6	246
0.32	4	39.00	42.00	27.500	0.32	72	360	1.26	1.30	7	246
0.34	5	42.00	45.00	29.420	0.34	72	364	1.34	1.30	7	247
0.39	6	45.00	48.00	31.360	0.38	72	364	1.49	1.50	8	247
0.4	7	48.00	51.00	33.390	0.40	72	363	1.57	1.60	9	245
0.36	8	51.00	54.00	35.420	0.35	72	362	1.38	1.40	9	245
0.34	9	54.00	57.00	37.380	0.35	72	359	1.38	1.40	10	245
0.35	10	57.00	60.00	39.370	0.34	72	358	1.34	1.40	11	245
Final DGM:					41.330						
RESULTS	Run Time		V _m	ΔP	T _m	T _s	Max Vac	ΔH	%ISO	BWS	Y _{as}
	60.0	min	39.080 ft ³	0.35 in. WC	71.8 °F	359.6 °F	11	1.383 in. WC	96.8	0.161	-2.1

Method 1 Data

Location PotlatchDeltic / Gwinn Sawmill - Gwinn, MI

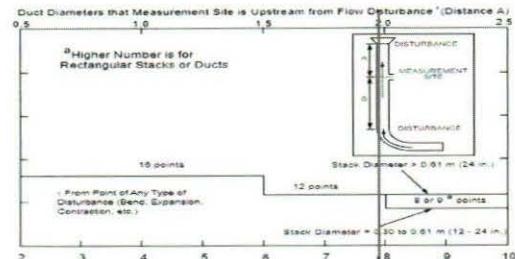
Source Boiler No. 2

Project No. AST-2024-0207

Date: 01/16/24

Stack Parameters

Duct Orientation: Vertical
 Duct Design: Circular
 Distance from Far Wall to Outside of Port: 34.00 in
 Nipple Length: 4.50 in
 Depth of Duct: 29.50 in
 Cross Sectional Area of Duct: 4.75 ft²
 No. of Test Ports: 2
 Number of Readings per Point: 1
 Distance A: 10.9 ft
 Distance A Duct Diameters: 4.4 (must be ≥ 0.5)
 Distance B: 19.1 ft
 Distance B Duct Diameters: 7.8 (must be ≥ 2)
 Actual Number of Traverse Points: 3
 Measurer (Initial and Date): COG 1/16
 Reviewer (Initial and Date): RA 1/16



CIRCULAR DUCT

LOCATION OF TRAVERSE POINTS											
Number of traverse points on a diameter											
	2	3	4	5	6	7	8	9	10	11	12
1	14.6	16.7	6.7	--	4.4	--	3.2	--	2.6	--	2.1
2	85.4	50.0	25.0	--	14.6	--	10.5	--	8.2	--	6.7
3	--	83.3	75.0	--	29.6	--	19.4	--	14.6	--	11.8
4	--	--	93.3	--	70.4	--	32.3	--	22.6	--	17.7
5	--	--	--	--	85.4	--	67.7	--	34.2	--	25.0
6	--	--	--	--	95.6	--	80.6	--	65.8	--	35.6
7	--	--	--	--	--	--	89.5	--	77.4	--	64.4
8	--	--	--	--	--	--	96.8	--	85.4	--	75.0
9	--	--	--	--	--	--	--	--	91.8	--	82.3
10	--	--	--	--	--	--	--	--	97.4	--	88.2
11	--	--	--	--	--	--	--	--	--	--	93.3
12	--	--	--	--	--	--	--	--	--	--	97.9

*Percent of stack diameter from inside wall to traverse point.

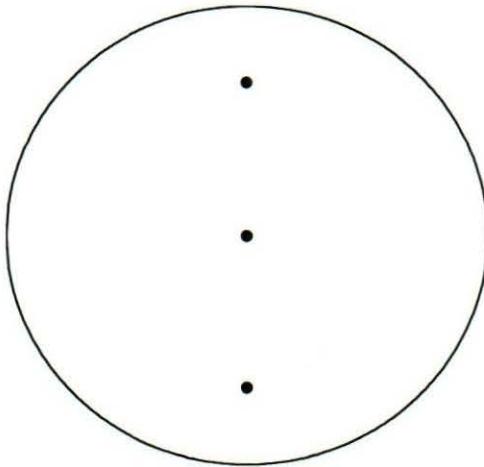
Stack Diagram

A = 10.9 ft.

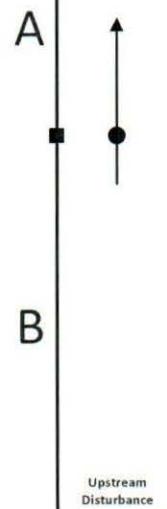
B = 19.1 ft.

Depth of Duct = 29.5 in.

Cross Sectional Area



Downstream Disturbance





Run 1 - RM Data

Location: PotlatchDeltic / Gwinn Sawmill - Gwinn, MI

Source: Boiler No. 2

Project No.: AST-2024-0207

Date: 1/16/24

Time Unit Status	O ₂ - Outlet % dry Valid	CO ₂ - Outlet % dry Valid	CO - Outlet ppmvd Valid
Uncorrected Run Average (C_{obs})	7.34	13.58	278.73
Cal Gas Concentration (C_{MA})	10.95	8.41	257.00
Pretest System Zero Response	-0.15	0.01	-0.15
Posttest System Zero Response	0.28	0.21	0.90
Average Zero Response (Co)	0.07	0.11	0.38
Pretest System Cal Response	10.98	8.32	255.14
Posttest System Cal Response	10.81	8.18	254.53
Average Cal Response (C_M)	10.90	8.25	254.84
Corrected Run Average (Corr)	7.35	13.92	281.13
13:25	7.56	13.49	236.24
13:26	7.18	13.90	394.4
13:27	6.46	14.59	567.84
13:28	6.45	14.56	439.23
13:29	6.48	14.48	283.38
13:30	7.50	13.47	206.85
13:31	7.44	13.60	333.15
13:32	6.99	14.02	453.14
13:33	6.73	14.31	543.96
13:34	6.35	14.62	359.64
13:35	7.06	13.91	264.75
13:36	7.27	13.71	231.31
13:37	7.51	13.54	193.05
13:38	8.40	12.54	155.31
13:39	8.92	12.24	178.11
13:40	7.91	13.19	292.31
13:41	7.60	13.47	177.84
13:42	6.89	14.24	348.97
13:43	7.02	13.95	185.21
13:44	8.17	12.88	206.93
13:45	7.53	13.52	186.11
13:46	8.36	12.62	161.94
13:47	8.12	13.03	224.48
13:48	7.67	13.33	216.05
13:49	7.98	13.04	192.40
13:50	8.11	12.90	180.58
13:51	8.16	12.87	193.59
13:52	7.27	13.82	222.05
13:53	7.01	14.07	253.03
13:54	7.02	13.98	206.46
13:55	7.58	13.42	180.60
13:56	7.44	13.63	229.17
13:57	7.32	13.61	165.82
13:58	8.36	12.58	155.54
13:59	8.48	12.55	277.31
14:00	7.26	13.80	501.60
14:01	7.31	13.60	255.57
14:02	7.06	14.01	298.18
14:03	6.89	13.97	218.28
14:04	7.27	13.54	271.64
14:05	7.59	13.32	179.57
14:06	7.31	13.42	358.47
14:07	6.51	14.25	733.28
14:08	6.05	14.62	293.20
14:09	7.19	13.48	221.74
14:10	7.64	13.12	224.08
14:11	8.02	12.71	158.40
14:12	7.20	13.71	497.16
14:13	6.20	14.50	346.46
14:14	7.00	13.67	209.10
14:15	7.56	13.06	186.60
14:16	7.50	13.16	223.37
14:17	7.10	13.59	308.44
14:18	6.68	14.06	446.68
14:19	7.12	13.46	203.22
14:20	7.65	13.16	238.31
14:21	7.02	13.80	368.50
14:22	6.70	14.09	416.17
14:23	6.96	13.70	276.65
14:24	7.27	13.23	192.11



Run 2 - RM Data

Location: PotlatchDeltic / Gwinn Sawmill - Gwinn, MI

Source: Boiler No. 2

Project No.: AST-2024-0207

Date: 1/16/24

Time Unit Status	O ₂ - Outlet % dry Valid	CO ₂ - Outlet % dry Valid	CO - Outlet ppmvd Valid
Uncorrected Run Average (C_{obs})	7.59	12.73	186.77
Cal Gas Concentration (C _{MA})	10.95	8.41	257.00
Pretest System Zero Response	0.28	0.21	0.90
Posttest System Zero Response	0.26	0.22	0.91
Average Zero Response (Co)	0.27	0.22	0.91
Pretest System Cal Response	10.81	8.18	254.53
Posttest System Cal Response	10.75	8.15	249.50
Average Cal Response (C _{MA})	10.78	8.17	252.02
Corrected Run Average (Corr)	7.62	13.24	190.22

15:45	6.10	14.24	319.28
15:46	7.20	13.09	133.84
15:47	7.97	12.34	124.98
15:48	8.16	12.22	133.35
15:49	8.18	12.19	172.28
15:50	8.42	11.96	223.65
15:51	7.19	13.32	544.50
15:52	5.66	14.78	640.59
15:53	6.44	13.89	267.86
15:54	7.27	13.02	218.44
15:55	7.76	12.61	191.45
15:56	6.99	13.39	167.12
15:57	6.91	13.47	149.09
15:58	7.60	12.73	136.17
15:59	7.35	12.98	127.55
16:00	8.08	12.23	118.62
16:01	8.60	11.81	116.92
16:02	7.59	12.84	133.20
16:03	7.61	12.70	197.14
16:04	7.30	13.15	230.36
16:05	6.96	13.45	228.35
16:06	7.13	13.18	171.43
16:07	8.25	12.10	137.80
16:08	8.47	11.97	164.47
16:09	7.20	13.23	270.62
16:10	7.20	13.12	129.38
16:11	7.95	12.38	116.92
16:12	7.68	12.76	131.44
16:13	7.09	13.27	105.88
16:14	7.55	12.68	111.36
16:15	8.03	12.23	115.47
16:16	8.51	11.78	124.66
16:17	8.86	11.45	186.68
16:18	8.95	11.35	276.82
16:19	8.94	11.33	150.00
16:20	8.30	11.99	129.45
16:21	7.43	12.76	128.82
16:22	7.72	12.49	126.19
16:23	8.66	11.66	206.04
16:24	8.28	12.04	314.89
16:25	7.28	12.90	199.43
16:26	7.22	12.98	129.53
16:27	7.44	12.77	135.18
16:28	7.54	12.68	129.75
16:29	7.92	12.34	127.84
16:30	7.78	12.56	249.82
16:31	7.07	13.24	151.32
16:32	7.72	12.57	125.52
16:33	8.46	11.91	122.41
16:34	7.94	12.39	124.37
16:35	7.79	12.46	122.80
16:36	7.97	12.29	128.90
16:37	7.59	12.70	181.56
16:38	6.76	13.60	350.48
16:39	6.56	13.70	232.95
16:40	7.45	12.75	158.70
16:41	6.75	13.64	370.55
16:42	6.48	13.75	197.29
16:43	6.92	13.32	161.92
16:44	7.12	13.06	132.66



Run 3 - RM Data

Location: PotlatchDeltic / Gwinn Sawmill - Gwinn, MI

Source: Boiler No. 2

Project No.: AST-2024-0207

Date: 1/17/24

Time Unit Status	O ₂ - Outlet % dry Valid	CO ₂ - Outlet % dry Valid	CO - Outlet ppmv d Valid
Uncorrected Run Average (C_{obs})	7.89	13.05	389.22
Cal Gas Concentration (C_{MA})	10.95	8.41	257.00
Pretest System Zero Response	-0.11	-0.03	0.91
Posttest System Zero Response	0.30	0.17	0.89
Average Zero Response (Co)	0.10	0.07	0.90
Pretest System Cal Response	10.87	8.14	252.00
Posttest System Cal Response	10.70	8.01	255.57
Average Cal Response (C_M)	10.79	8.08	253.79
Corrected Run Average (Corr)	7.98	13.64	394.64
11:10	8.59	12.55	250.14
11:11	7.10	14.25	443.71
11:12	6.99	14.21	562.01
11:13	8.07	13.07	362.35
11:14	7.87	13.29	404.26
11:15	7.44	13.78	457.07
11:16	8.00	13.09	388.98
11:17	8.49	12.60	300.77
11:18	9.84	11.08	240.96
11:19	9.34	11.72	237.68
11:20	8.17	12.99	242.03
11:21	7.20	14.00	401.22
11:22	7.07	14.16	337.40
11:23	7.02	14.19	300.64
11:24	7.25	13.96	472.93
11:25	7.43	13.73	374.15
11:26	8.21	12.92	323.98
11:27	8.08	13.10	349.63
11:28	7.92	13.24	347.45
11:29	7.75	13.40	396.32
11:30	7.70	13.48	307.94
11:31	7.04	14.16	544.06
11:32	7.61	13.54	407.28
11:33	8.45	12.61	322.97
11:34	7.34	13.88	679.27
11:35	7.38	13.70	420.52
11:36	7.80	13.26	340.05
11:37	7.88	13.17	350.81
11:38	8.03	12.98	348.72
11:39	7.08	13.96	536.99
11:40	6.47	14.56	757.26
11:41	6.72	14.20	590.53
11:42	8.02	12.86	373.84
11:43	7.27	13.62	486.28
11:44	7.68	13.19	382.74
11:45	7.84	13.00	370.33
11:46	8.41	12.41	317.32
11:47	7.83	13.06	486.35
11:48	6.40	14.52	868.66
11:49	7.53	13.28	429.53
11:50	7.62	13.24	401.91
11:51	7.23	13.56	404.66
11:52	8.43	12.37	265.85
11:53	8.36	12.43	219.59
11:54	7.97	12.85	265.32
11:55	8.41	12.31	235.20
11:56	8.71	12.08	288.88
11:57	6.79	13.99	680.12
11:58	7.24	13.49	540.75
11:59	7.71	13.03	385.20
12:00	7.58	13.09	481.55
12:01	8.92	11.66	293.98
12:02	9.43	11.11	218.22
12:03	8.64	12.01	324.54
12:04	8.43	12.15	277.01
12:05	9.01	11.53	244.48
12:06	8.70	11.86	267.00
12:07	7.99	12.61	356.55
12:08	9.19	11.23	294.70
12:09	8.77	11.82	392.61