1.0 INTRODUCTION AND SUMMARY

1.1 PROGRAM OBJECTIVES

Montrose Air Quality Services, LLC (Montrose) was contracted by DTE Energy (DTE) to perform a series of air emission tests at the Renaissance Power Station (RPS) facility located in Carson City, MI. The compliance tests were conducted on one (1) Siemens EUTURBINE2SC (Unit 2) simple cycle gas turbine generator, to determine compliance with the source testing conditions of the Michigan Department of Environment, Great Lakes and Energy (EGLE).

The testing was conducted by Mr. John Hamner, Mr. Thomas Cassin, Mr. Mike Nummer, Mr. Shane Rabideau, Mr. Nicholas Woltcamp, Mr. Mathew Ojile, Mr. Trevor Tilmann, Mr. Zach Le Fever, Mr. Scott Dater, Mr. Ben Durham, and Mr. Craig Blohm of Montrose on March 16th thru 17th, 2021. Mr. John Hamner was the qualified individual on site, his QI Certifications are located in Appendix A. Mr. Mark Grigereit of DTE Energy coordinated the testing program. The tests were conducted according to a Protocol dated October 12, 2020 which was submitted to EGLE. Ms. Gina Angellotti and Ms. Lindsey Wells from EGLE were onsite and observed the testing program. Montrose performed the tests to measure the following emission parameters:

- Emission Compliance:
 - PM (total) as PM10/2.5 (lb/hr)
 - O₂ and CO₂ (% volume dry) for molecular weight & dilution calculations
 - Stack volumetric flow rate (dscfm per Method 19) and moisture content (% by volume)
 - Fuel analysis ("F_d" factor, HHV, sulfur content)

This report presents the test results and supporting data, descriptions of the testing procedures, descriptions of the facility and sampling locations, and a summary of the quality assurance procedures used by Montrose. The average emission test results are summarized and compared to their respective permit limits and performance specifications in Table 1-1. Detailed results for individual test runs can be found in Section 5.0. All supporting data can be found in the appendices.

TABLE 1-1 SUMMARY OF AVERAGE COMPLIANCE RESULTS DTE RENAISSANCE POWER STATION TURBINE UNIT 2 Base CONDITION

Parameter	Unit 2 (3/16/21 thru 3/17/21)	Permit Limit
Unit Data: Fuel Heat Input (MMBtu/hr) Total Particulate Matter (PM2.5/PM10): PM 10 lb/hr	1,948.6 5.01	 9.0

1.2 PROJECT CONTACTS

A list of project participants is included below:

Facility Information

Source Location:	Renaissance Power Plant
	950 N. Division Street
	Carson City, MI 48811
Project Contact:	Mr. Mark Grigereit
Company:	DTE Energy
Telephone:	(313) 412-0305
Email:	Mark.grigereit@dteenergy.com

Agency Information

Regulatory Agency:	/: Michigan Department of Environment, Great			
	Lakes and Energy			
Agency Contact:	Ms. Gina Angellotti	Ms. Lindsey Wells		
Telephone:	(313) 418-0895	(517) 282-2345		
Email:	AngellottiR1@michigan.gov	Wellsl8@michigan.gov		

Testing Company Information

Testing Firm:	Montrose Air Quality Services, LLC	C (Montrose)
Contact:	Barry Boulianne	John Hamner
Title:	VP Sales and Marketing	Client Project Manager
Telephone:	(313) 449-2361	(630) 715-3259
Email:	bboulianne@montrose-env.com	jhamner@montrose-env.com

2.0 SOURCE LOCATION INFORMATION

2.1 FACILITY DESCRIPTION

The plant provides electric power when requested to do so during periods of peak power demand or system need, and does not operate outside of those system requests so its operation is batch like. During periods of operation, there is not significant emissions variability.

Each turbine set consists of a compressor, combustion turbine, and generator. Mechanical energy is generated at the combustion turbine by drawing in ambient air by means of burning fuel and expanding the hot combustion gases in a four-stage turbine. The mechanical energy is converted to electrical energy through the generator.

Each turbine is equipped with dry low-NOX burners. Each unit has its own dedicated exhaust stack areas. Each turbine has a nominal heat input rating of 1,900 million Btu per hour, and is capable of producing 215 megawatts of electricity. The facility is equipped with a Distributed Control System (DCS) to monitor heat input. NOx emissions from the exhaust are continuously monitored as required by 40 CFR, Part 75. Carbon Monoxide (CO) stack emissions are continuously monitored per 40 CFR, Part 60

2.2 Process Operating Data

During each test run, fuel flow and fuel heat input to the gas turbine were continuously recorded on a data acquisition system. The data is averaged for each test run in the final report.

2.3 SAMPLING LOCATIONS

A total of sixteen 6" flanged sample ports are installed the unit with 8 installed on each the north and south walls of the exhaust ducts. Eight ports were selected for use on this program, 4 on each side.

The test location on Unit 2 at RNPP do not meet the minimum dimensional criteria of EPA Method1 (>2stack equivalent diameters downstream and > 0.5 diameters upstream from flow disturbances. The available sample locations are in fact inside of an area for the exhaust system contains silencer baffles that are separated with gaps where the exhaust gases pass between them. In addition to the complications related to the silencer baffles, the situation is further complicated by the relatively large overall dimensions of the exhaust ducting which is approximately 20' x 20' square with ports installed on opposing walls. A diagram of the sample plane is shown below. The figure shows 16 sample ports providing access to 8 gas path openings, arranged into 8 opposing pairs.

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Traverse Points

A simplified diagram of the traverse points is provided in Figure 1.



Figure 1 Sample Point Layout

3.0 TEST DESCRIPTION

3.1 PROGRAM OBJECTIVES

The objective of this test program was to prove compliance of Unit 2 with the permit limits. The results are presented in units consistent with those stated in the permit.

3.2 TEST CONDITIONS

Emission tests were performed while the source units were operating at the conditions required by the permit. Tests were performed at the following conditions:

• Condition 1: Base Load

Plant personnel established the test conditions and collected all applicable unit-operating data. Montrose monitored the collection of process data.



3.3 TEST PROGRAM SCHEDULE

The test program schedule is presented in Table 3-1.

TEST MATRIX AND SCHEDULE Source ID/ Sample Sample Date Activity Runs Duration March 15, 2021 Set-up --------March 16, 2021 **Unit 2 Stack Base** O₂ & CO₂ 1-2 4 hour PM 1-2 4 hour March 17, 2021 **Unit 2 Stack Base** O₂ & CO₂ 3 4 hour PM 3 4 hour

TABLE 3-1

3.4 MONTROSE TEST PROCEDURES

The test procedures used for this test program are summarized in Table 3-2 below. Additional information regarding specific applications or modifications to standard procedures is presented in the following sub-sections.

TABLE 3-2 TEST PROCEDURES

Parameter	Measurement Principle	Reference Method		
Volumetric flow rate	Pitot/temperature traverse	EPA 1, 2		
Volumetric flow rate	Stoichiometric calculation	EPA 19		
O2	Paramagnetism	EPA 3A		
CO ₂	Non-dispersive infrared	EPA 3A		
Moisture	Impinger weight gain	EPA 4		
Particulate Matter	Gravimetry with condensable analysis	EPA 5/202		

3.4.1 Gaseous Emissions

Concentrations of the gaseous constituents of stack gas carbon dioxide (CO_2) and oxygen (O_2) were measured using Montrose's dry extractive reference method (RM) monitor system in accordance with Methods 3A. This system meets the requirements of EPA method for gaseous species. Pertinent information regarding the performance of the method is presented below:

- Method Deviations: None
 - Method Options: N/A

Source gas was sampled for a period of 60 minutes for each of the conditions per source.

3.4.3 Particulate Matter Emissions

Emissions of total particulate matter (PM) were measured using a combination of EPA Methods 5 and 202. Pertinent information regarding the performance of the methods are presented below:

- Method Deviations: None
 - Method Options: A field train recovery blank was collected on-site; the glassware was baked for 6 hours prior to use. Additionally, pressurized nitrogen was used to purge all trains
 - Target and/or Minimum Required Sample Duration: 240 Minutes
 - Target and/or Minimum Required Sample Volume: >120 dscf
 - Analytical Laboratory: Montrose Elk Grove Village, IL

3.4.4 Volumetric Flow Rate

Stack gas volumetric flow rates were determined by the procedures outlined in EPA Method 19. Pertinent information regarding the performance of the method is presented below:

- F Factor: Oxygen based F factor, dry basis (F_d)
 - F Factor Source: Analysis of fuel samples
 - Heat Input Data: Calculated based on fuel flow rate and higher heating value
 - Higher Heating Value Source: Analysis of fuel samples.

Velocity flow rates and moisture content were determined using EPA Methods 2 and 4 in conjunction with each particulate matter test. The calculated Method 19 flow rates were used to calculate emissions in lb/hr.

3.4.6 Fuel Analysis

Sample gas from the facility's ethane blend natural gas fuel supply pipeline was collected and submitted for analysis. Pertinent information regarding the fuel analysis is presented below:

- Analytical Method: ASTM D-1945/ASTM D-3246
 - Sample Containers: Teflon-coated pressurized fuel bombs
 - Analytical Laboratory: Texas Oil Tech Laboratories, Inc., Houston



3.4.7 Process Data

The plant's unit operating data was used to document process conditions during the test runs. Unit operating data was provided by DTE personnel. Data presented in this report includes the following:

- Power output
- CEMS data
- Heat Input
- Fuel Flow

4.0 QUALITY ASSURANCE AND REPORTING

4.1 SAMPLING AND ANALYTICAL QA/QC

Montrose has instituted a rigorous QA/QC program for all of its air pollution testing. Quality assurance audits are performed as part of the test program to ensure that the final results are calculated from the highest quality data. The program ensures that the emission data reported are as accurate as possible. The procedures included in the cited reference methods were followed for all steps of preparation, sampling, calibration, and analysis. Montrose was responsible for preparation, calibration and cleaning of the sampling apparatus. Montrose also conducted the sampling and sample recovery, storage, and shipping.

Contract laboratories conducted some of the preparation and sample analyses as needed. The laboratories that were used are established leaders in development and performance of the reference methods for which they have been selected. Their credentials for adherence to the required quality assurance procedures are well known.

4.2 QUALITY CONTROL PROCEDURES

Our Quality Assurance Program provides our equipment maintenance and calibration schedule, quality control acceptance limits, and any corrective action that may be needed. For additional quality control, Montrose followed the procedures outlined below and in the method write-ups in Section 3.4.

4.2.1 Equipment Inspection and Maintenance

- Each critical piece of field equipment was assigned a unique identification number to allow tracking of its calibration history
 - All field equipment was visually inspected prior to testing and included pretest calibration checks

4.3 DATA ANALYSIS, VALIDATION, AND UNCERTAINTY

The raw data collected during the sampling and analysis procedures were used to calculate the results of the testing program. The analysis or reduction of the data to the final results followed these steps, where appropriate to the test method:



- Check field-sampling data for accuracy and calculate appropriate data averages (e.g., temperatures, pressures, volumes, etc.).
 - Double check calculation of the data averages.
 - Review all in-house and contract laboratory reports and ensure that appropriate and/or required QA/QC steps were followed.
 - Enter field and laboratory data to established and verified computer spreadsheets for calculation of volumetric flow rates, mass emission rates or other appropriate results.
 - Double-check all lab and field data inputs.
 - Perform example calculations by hand using raw data on a single test run for each type of emission result reported.
 - Compile summary tables of results and review all table inputs.

This report includes copies of spreadsheet printouts (data input and results output) and example calculation checks. The field data sheets with average data calculations are also included. Standard conditions used for data reduction are 29.92 inches of mercury and 68 °F.

Both qualitative and quantitative factors contribute to field measurement uncertainty and should be taken into consideration when interpreting the results contained within this report. Whenever possible, Montrose personnel reduce the impact of these uncertainty factors by using approved and validated test methods. In addition, Montrose personnel perform routine instrument and equipment calibrations and ensure that the calibration standards, instruments, and equipment used during test events meet, at a minimum, test method specifications as well as the specifications of our Quality Manual and ASTM D 7036-04. The limitations of the various methods, instruments, equipment, and materials utilized during this test have been reasonably considered, but the ultimate impact of the cumulative uncertainty of this project is not fully identified within the results of this report.

5.0 DISCUSSION OF RESULTS

5.1 DETAILED DISCUSSION OF RESULTS

The average results are compared to the performance specifications in Table 1-1. Detailed results from the individual compliance test runs are presented in Tables 5-1 through 5-3.

Additional information is included in the appendices. Appendix A presents the quality assurance information, including instrument calibration data. Data sheets and plant data is included in Appendix B. Appendix C presents the general and specific equations used for the emissions calculations and computer spreadsheets. Appendix D presents the outside lab results.

5.2 PROBLEMS/DEVIATIONS/EXCEPTIONS

No problems, deviations, or exception occurred during this test program. The data provided by the plant was off by one hour from the test data collected by Montrose due to the change in daylight savings time.

TABLE 5-1 GASEOUS TEST RESULTS UNIT 2 Base

Reference Method Test Run Data

Client:	DTE	
Facility:	Renalssance	
Source:	GT 2	
Test Location:	Stack	
Condition/Load:	Base	
Project Number:	049AS-006795	de blacken en black

Test Start Date:	Tuesday,	March 16, 2021			
Test Completion Date:	3	/17/2021			
Operator:	To	ım Cassin			
	F Facti	or Information			
	F _e	1800			
	Fd				
Reference Method Measuren	nent Basis:	Dry - Extractive			
CEMS Analyzer Measuren	nent Basis:				

Run	Test	Start	End	CO	NO,	50 ₂	0,	CO ₂
Number	Date	Minute	Minute	(ppmvd)	(ppmvd)	(ppmvd)	(% v/v Dry)	(% v/v Dry)
1	03/16/21	8:15	12:45				13.65	4.09
2	03/16/21	13:27	17:55				13.62	4.08
3	03/17/21	7:40	12:06				13.68	4.09

Moisture Basis As Measured								
Run Number	Test Date	Start Minute	End Minute	CO {ppmvd}	NO, (ppmvd)	SO ₂ (ppmvd)	O₂ (% v/v Dry)	CO3 (% v/v Dry)
1	03/16/21	8:15	12:45	-	-	international and a state of the	13.73	4.09
2	03/16/21	13:27	17:55	-			13.75	4.07
3	03/17/21	7:40	12:06	-			13.77	4.08



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TABLE 5-2 PARTICULATE TEST RESULTS UNIT 2 NORTH Base

Client Unit/Location						
A (stack area), ft ²						239.785
T _{orf} [reference temperature], F						. 68
Test number.	Run 1		Fiun 2		Run 3	Áverage
Date	31621	þ.	37621	1970 -	317/21	4.5
Start / Stop time.	8:15-12:45		13:27-17:55		7:40-12.06	4 W
F, (fuel 'F' factor @ 68'F), dschMMBlu.	8615.60		8675.60		8615.20	* %
F, (fuel 'F' factor @ T,,,), dscfMMBhu	8615.60	1	3615.60	μ.	8615.20	
Fuel Density, Iblsof (fuel std condition 60°F	0.0454		0.0454		0.0453	~ 9
HHV (fuel higher heating value), Bluksci	1050,21		1050.21		1049.18	
Fuel Flow Rate, Ib/sec	11.80		1160		11.70	21 W
Fuel HeatInput, MMBTUhr	982.7	*	966.0	F	975.5	
Meter box number.	C57	F	CS7	۶P	CS7	
C, (pilot coefficient), dimensionless	0.8400	۴	0.8400		0.8400	0.8400
Y (meter calibration factor), dimensionless	0.9970	P*	0.9970	F	0.9970	0.997
e (sample time), min	240.00	F 	240.00		240.00	240.00
Nozzle diameter, in	0.178	20 10 10	0 178	pier	0.178	0.178
P _{kin} (barometric pressure), in Hg	30.00	*	30.01	er par	30.09	30.03
V _* (meter box volume), scf	147.127	P*	147.668	-	146.391	147.062
V ₄ , (impinger liquid), g	256.6		257.3	P.	246.9	253.6
T _{in} (meter temperature), 'F.	57.0	*	73.5	P*	70.8	67.1
sH (meter pressure), in H ₂ 0	1096	1994 1994	1 114	(Pr	1.146	1 119
sP (velocity head), in HCO	3.7479	ų.	3.6406	Be.	3.7230	3.7038
P, (static pressure), in Hg.	-0.38	100	-0.37	ø	-0.37	-0.37
T, (stack temperature). 'F.	1068.6	h.	1069.8	P	1070.1	1069.5
%Q, (oxygen stack gas), % volume dry.	13.73		13 75		13.27	13.75
$\% CO_{\epsilon}$ (carbon dioxide stack gas), $\%$ volume dry	4.09		4.07		4.08	4.08
m, (F½ particulate matter catch - filter), g	0.0028		0.0002		0.0031	0.0020
m, JF½ particulate matter catch - acetone rinse), g	0.0021		0.0021		0.0020	0.0021
m _{see} (B½ particulate matter catch - total condensible, blank c	0.0026		0.0032		0.0020	0.0026
m, Itotal particulate matter catchi), g.	0.0075		0.0055		0.0071	0.0067
ь. V _{arrate} (standard sample volume), dscf	150.623		146 533		148.424	147.860
 V_{vol+6} (water vapor volume), scf. 	12.098		12.131		11.640	11.956
 B_a (moisture fraction), non-dimensional 	0.0743		0.0765		0.0736	0.0748
Moisture, %	7.43		7.65		7.36	7.48
MMW try (stack gas molecular weight), dry	29 204		29.201		29.204	29,203
⊾ MW _{aa} (stack gas molecular weight), wet	28.371		28.345		28.379	28.365
 P, (absolute stack pressure), in Hg 	29 972		29.983		30.063	30.006
la V, (stack gas velocitu), filsec.	186.092		183 535		165.255	184.961
Q. (fuel heat input), dscfm.	411,307		405,467		410,593	409,122
⊫ I (isokinetic ratio), %	101.57		100.47		98.91	100-32
% G (F% græn loading), gildisof.	0.000502		0.000242		0.000537	0.000427
» M(F/i mass emissions). Ibhr	1.77		0.84		1.89	150
Set E (FY: mass emissions), IB/MMB/u	0 001797		0 000869		0.001935	0.001534
» G (B½ grein loading), gridsd	0.000266		0 000337		0.000211	0.000271
× M(BV) mass emissions), binn	0.94		1,17		0.74	0.95
H E (B½ mass emissions), IbMMBki	0.000953		0.001210		0.000759	0.000974
». G (total grain leading), gi/dscf.	0.000768		0 000579		0.000748	0.000699
 M (lotal mass emissions), lbfr 	2.71		2.01		2.63	2.45
 E [lotal mass emissions], IbMMBtu 	0.00275		0.00208		0.002693	0 002508

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TABLE 5-3 PARTICULATE TEST RESULTS UNIT 2 SOUTH Base

Client	· · · · · ·	der an		1		DTE .RENPR2-South
A (slack area), fl ²						
T _{ad} (reference temperature), 'F.						. 50
Test number	Pun 1		Plun 2	-	Aun 3	Average
U@e	3(6(2))	Þ.	316/21	Вr.	317/21	12 in
Start / Stop time.	8:15-12:45		13:27-17:55		7:40-12:06	± 11
F, (fuel 'F' factor @ 68'F), dscff/M@lu.	8615.19	p	8615.90	s.	8615.20	4 'H
F ₄ (fuel 'F' factor @ T ₂₄), dsoft/MBIu.	8615.19		8615.90	r	8615.20	
Fuel Density, Ib/scf (fuel std condition 60°F	0.0454		0.0454		0.0453	
HHV (fuel higher heating value), Btulsof	1050.21 11.80		1050.21		1049 18 11.70	
Fuel How Rate, Iblect	982.7	٣	1160 966.0	8°	975.5	
	JMc. 1	andoren eta	900.07 	an a	0.5.16 	
Meter bax number	CS4	2	CS4	F	CS4	-
C, (pitot coefficient), dimensionless	0.8400	F	0.8400	100.0	0.8400	0 8400
Y (meter calibration factor), dimensionless	1.0240	þ.	1.0240	1	10240	1.024
© (sample time), min	240.00	4	240.00		240.00	240.00
Nozzle diameter, m	0.170 30.00	P	0.170 30.01	ger.	0.170 30.09	0.170 30.03
P _{in} (barometric pressure), in Hg	.s0.00 158.600	P	30.01 154,480	ø	.30,03 154,950	
V _e (meter box volume), act V _e (impinger liquid), g	253.4	P	154.480 255.5		249.2	956.010 252.7
	253.4 58.7	8	259.5 70.6	ø	249.2 67.2	202. (65. 5
T _m (meter temperature), 'F.		şr.	70.6	¥	1421	
βH (meter pressure). m H₂0	1493	₽		9 7		1439
sP (velocity head). In: H2O	5.3944	-	4.9358	10 ⁰	5.0350	5.1217
P, (static pressure), in. Hg	-0.36		-0.36	e e	-0.36	-0.36
T, (stack temperature). 'P.	1078.9	*	1082.8	9	1080.5	1080.7
%D ₂ (oxygen stack gas), % volume dry,	13,73		13 75		13,77	13.75
%CO ₂ (carbon dioxide stack gas), % volume dry	4.09		4,07		4 08	4.08
my [F½ particulate matter catch - filter], g	0.0031		0.0002		0.0024	0.0013
m, (F½ particulate matter catch - acetone rinse), g	0.0043		0.0017		0.0030	0.0030
m _{iom} (B½ particulate matter catch - total condensible, blank c	0.0024		0.0038		0.0021	0.0028
m, (lotal particulate matter catch), g.	0.0098		0.0057		0.0075	0.0077
ъ V _{arme} (standard sample volume), dsof	166.371		158 414		160.378	161.721
ть V _{uanti} (water vapor volume), scf	11.950		12.044		11,749	11 914
k B, [moisture fraction], non-dimensional	0.0670		0 0707		0.0683	0.0686
Moisture, %	6.70		7.07		6.83	6.86
и MW _{int} [stack gas molecular weight], dry	29.204		29.201		29.204	29.203
is MW _{art} (stack gas molecular weight), wet	28 453		28.410		28 439	28:434
✓ P, (absolute stack pressure), in Hg	29.974		29,984		30.064	30.007
ia V, (stack gas velocity). Nisec.	223.682		214.358		215.943	217.994
Q ₄ (fuel heat input), dscfm	411,298		405,481		410,593	409,120
I (isokinetic ratio), %	102.21		102.17		101.99	102.13
» G (F½ gran leading), gifdsof	0.000686		0.000185		0.000520	0.000464
× M(F½ mass envisions). Ibhr	2.42		0.64		1.03	163
34 E (F% mass emissions), IbIMIMBiu	0.002457		0 000664		0.001870	0.001664
≫ G (Bl/₂ grain toading), gridsof	0.000223		0.000370		0.000202	0.000264
> M(BV/mass emissions), Ibhr	0.78		129		0 71	0.93
≥4 E (B½ mass emissions), IbMMBlu	0.000797		0.001329		0.000727	0 000951
s G (total grain loading), gildsof	0.000909		0 000555		0.000722	0.000731
M (total mass emissions), Ib/hr	3.20		1.93		2.54	2.56
≫ E (total mass emissions), IbMMBtu	0.00325		0 00199		0.002598	0.002615