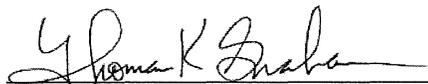
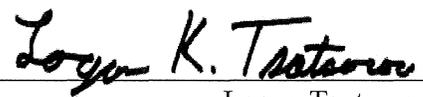


**EMISSION COMPLIANCE TEST
FOR THE
CLINKER COOLER 22, 23, 92, AND 93
PREPARED FOR
HOLCIM (US) INC. D/B/A LAFARGE, SRN B1477
AT THE
ALPENA PLANT
ALPENA, MICHIGAN
JULY 23-26, 2019**

Prepared and Reviewed by:


Thomas K. Graham, PE, QSTI
Director of Education


Logan Tsotsoros
AHU Support Staff

I, 
Michael Stockwell, QSTI
Sr. Regional Manager-Broken Arrow, OK
certify that this testing was conducted and
this report was created in conformance
with the requirements of ASTM D7036

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**Emissions Compliance Test
Clinker Cooler 22, 23, 92, and 93
Holcim (US) Inc. d/b/a Lafarge, SRN B1477
Alpena Plant
Alpena, Michigan
July 23-26, 2019**

1.0 INTRODUCTION

Air Hygiene International, Inc. (Air Hygiene) has completed the Emissions Compliance Test for particulate matter (PM), flow, moisture (H₂O), carbon dioxide (CO₂), and oxygen (O₂) from the exhaust of the Clinker Cooler 22, 23, 92, and 93 for Holcim (US) Inc. d/b/a Lafarge, SRN B1477 at the Alpena Plant near Alpena, Michigan. This report details the background, results, process description, and the sampling/analysis methodology of the stack sampling survey conducted on July 23-26, 2019.

1.1 TEST PURPOSE AND OBJECTIVES

The purpose of the test was to conduct a periodic compliance emission test to document levels of selected pollutants. The information will be used to confirm compliance with the operating permit issued by the Michigan Department of Environmental Quality (MDEQ). The specific objective was to determine the emission concentration of PM, flow, H₂O, CO₂, and O₂ from the exhaust of Holcim (US) Inc. d/b/a Lafarge, SRN B1477's Clinker Cooler 22, 23, 92, and 93 at normal operating load.

1.2 SUMMARY OF TEST PROGRAM

The following list details pertinent information related to this specific project:

- 1.2.1 Participating Organizations
 - Michigan Department of Environmental Quality (MDEQ)
 - Holcim (US) Inc. d/b/a Lafarge, SRN B1477
 - Air Hygiene
- 1.2.2 Industry
 - Cement Plant
- 1.2.3 Air Permit and Federal Requirements
 - Permit Number: MI-ROP-B1477-2012
- 1.2.4 Plant Location
 - Alpena Plant near Alpena, Michigan
 - 1435 Ford Avenue, Alpena, Michigan 49707
 - Federal Registry System No. 110015742605
 - Source Classification Code (SCC) – 30500699, 30500614
- 1.2.5 Equipment Tested
 - Clinker Cooler 22, 23, 92, and 93
- 1.2.6 Emission Points
 - Exhaust from the Clinker Cooler 22, 23, 92, and 93
- 1.2.7 Emission Parameters Measured
 - PM
 - Flow
 - H₂O
 - CO₂
 - O₂

- 1.2.8 Dates of Emission Test
 - July 23-26, 2019
- 1.2.9 Federal and State Certifications
 - Stack Testing Accreditation Council AETB Certificate No. 3796.02
 - International Standard ISO/IEC 17025:2005 Certificate No. 3796.01

1.3 KEY PERSONNEL

| | | |
|--|---|--------------|
| Holcim (US) Inc. d/b/a Lafarge, SRN B1477: | | |
| | Travis Weide (travis.weide@lafargeholcim.com) | 989-358-3321 |
| MDEQ: | Jeremy Howe | 231-878-6687 |
| Air Hygiene: | Michael Stockwell (mstockwell@airhygiene.com) | 918-307-8865 |
| Air Hygiene: | Matt McBride | 918-307-8865 |
| Air Hygiene: | James Reynolds | 918-307-8865 |
| Air Hygiene: | John Gatti | 918-307-8865 |
| Air Hygiene: | Gharabet Torossian | 918-307-8865 |
| Air Hygiene: | Adrian Lopez | 918-307-8865 |

2.0 SUMMARY OF TEST RESULTS

Results from the sampling conducted on Holcim (US) Inc. d/b/a Lafarge, SRN B1477's Clinker Cooler 22, 23, 92, and 93 located at the Alpena Plant on July 23-26, 2019 are summarized in the following tables and relate only to the items tested.

**TABLE 2.1
CLINKER COOLER 22 PM EMISSIONS SUMMARY**

| Emission Rate Data | CC22-1 | CC22-2 | CC22-3 | Average | Units |
|-----------------------------|----------|----------|----------|----------|---------|
| Filterable PM Mass | 28.21 | 44.93 | 19.60 | 30.91 | mg |
| Filterable PM Concentration | 5.06E-04 | 7.80E-04 | 2.79E-04 | 5.22E-04 | g/dscf |
| | 7.81E-03 | 1.20E-02 | 4.30E-03 | 8.05E-03 | gr/dscf |
| Filterable PM Emission Rate | 1.52 | 2.39 | 1.05 | 1.65 | kg/hr |
| | 3.35 | 5.27 | 2.32 | 3.65 | lb/hr |
| | 14.69 | 23.09 | 10.15 | 15.98 | tpy |
| | 0.04 | 0.07 | 0.04 | 0.05 | lb/ton |

**TABLE 2.2
CLINKER COOLER 23 PM EMISSIONS SUMMARY**

| Emission Rate Data | CC23-1 | CC23-2 | CC23-3 | Average | Units |
|-----------------------------|---------------|---------------|---------------|----------------|--------------|
| Filterable PM Mass | 31.90 | 33.69 | 43.11 | 36.23 | mg |
| Filterable PM Concentration | 6.97E-04 | 7.00E-04 | 8.14E-04 | 7.37E-04 | g/dscf |
| | 1.08E-02 | 1.08E-02 | 1.26E-02 | 1.14E-02 | gr/dscf |
| Filterable PM Emission Rate | 1.70 | 1.76 | 2.30 | 1.92 | kg/hr |
| | 3.74 | 3.87 | 5.06 | 4.23 | lb/hr |
| | 16.40 | 16.95 | 22.17 | 18.51 | tpy |
| | 0.04 | 0.04 | 0.05 | 0.04 | lb/ton |

**TABLE 2.3
CLINKER COOLER 92 PM EMISSIONS SUMMARY**

| Emission Rate Data | CC92-1 | CC92-2 | CC92-3 | Average | Units |
|-----------------------------|---------------|---------------|---------------|----------------|--------------|
| Filterable PM Mass | 40.29 | 23.05 | 17.69 | 27.01 | mg |
| Filterable PM Concentration | 8.79E-04 | 5.71E-04 | 4.33E-04 | 6.28E-04 | g/dscf |
| | 1.36E-02 | 8.82E-03 | 6.68E-03 | 9.69E-03 | gr/dscf |
| Filterable PM Emission Rate | 2.45 | 1.44 | 1.13 | 1.67 | kg/hr |
| | 5.40 | 3.18 | 2.49 | 3.69 | lb/hr |
| | 23.65 | 13.92 | 10.90 | 16.16 | tpy |
| | 0.07 | 0.05 | 0.03 | 0.05 | lb/ton |

**TABLE 2.4
CLINKER COOLER 93 PM EMISSIONS SUMMARY**

| Emission Rate Data | CC93-1 | CC93-2 | CC93-3 | Average | Units |
|-----------------------------|---------------|---------------|---------------|----------------|--------------|
| Filterable PM Mass | 19.63 | 13.47 | 18.99 | 17.37 | mg |
| Filterable PM Concentration | 3.53E-04 | 2.51E-04 | 3.10E-04 | 3.05E-04 | g/dscf |
| | 5.45E-03 | 3.88E-03 | 4.79E-03 | 4.70E-03 | gr/dscf |
| Filterable PM Emission Rate | 1.22 | 0.85 | 1.20 | 1.09 | kg/hr |
| | 2.68 | 1.87 | 2.65 | 2.40 | lb/hr |
| | 11.75 | 8.19 | 11.62 | 10.52 | tpy |
| | 0.04 | 0.03 | 0.04 | 0.03 | lb/ton |

**TABLE 2.5
CLINKER COOLER PM-CPMS SUMMARY RESULTS**

| Unit | PM Emissions lb/tons clinker | PM Limit lb/ton clinker | PM-CPMS mA | Operating Limit mA |
|------|---------------------------------|----------------------------|---------------|-----------------------|
| C22 | 0.05 | 0.07 | 4.28 | 4.28 |
| C23 | 0.04 | 0.07 | 4.48 | 4.59 |
| C92 | 0.05 | 0.07 | 5.49 | 5.50 |
| C93 | 0.03 | 0.07 | 4.48 | 4.75 |

The results of all measured pollutant emissions were below the required limits. All testing was performed without any real or apparent errors. All testing was conducted according to the approved testing protocol.

Table 2.6 represents the Clinker Cooler PM-CPMS Operating limits. The clinker coolers must comply with PC MACT Regulation 40 CFR 63, Subpart LLL. The PM-CPMS Operating Limit was calculated using the equations:

$$O_i = z + ((0.75 * L) / R) \quad \text{and} \quad R = Y_1 / (X_1 - z)$$

Where,

O_i = Operating limit for PM CPMS on a 30 day rolling average (mA)

L = Source emission limit (lb/ton clinker)

z = Instrument zero (mA)

R = Relative lb/ton of clinker per mA

Y_1 = Three run average lb/ton of clinker PM concentration

X_1 = Three run average mA

3.0 SOURCE OPERATION

3.1 PROCESS DESCRIPTION

The Lafarge Cement facility is located in Alpena, Michigan. The Raw Mill System mixes and grinds the raw materials (limestone, sand, bauxite, Bell shale, gypsum) and alternate raw materials (slag, iron ore, fly ash, and CKD) then sends the materials to the kilns.

Lafarge operates five rotary kilns, which manufacture Portland cement clinker using the dry process. A mixture of pulverized bituminous coal and petroleum coke, with a heating value of approximately 11,750 Btu per pound, serves as the primary fuel fed to the kilns. Coal and coke are fed to a Raymond bowl mill and ground to a fineness of approximately 95% passing a 200-mesh sieve.

Kiln Group 5:

Kiln Group 5 at the Lafarge Alpena plant consists of three rotary kilns (#19, #20, and #21). Specific components of Kiln Group 5 are:

- Coal/petroleum coke and combustion air delivery;
- Raw mix preparation and delivery;
- Three rotary kilns;

- Kiln burners; and
- Air pollution control system, consisting of the following components:
 - Boiler;
 - Multiclone dust collectors;
 - Baghouses;
 - SNCR;
 - Induced draft (ID) fans; and
 - Exhaust stacks.

Allis Chalmers manufactured all kilns identified as #19, #20, and #21. Each kiln is 460.5 feet long. Each kiln shell has an inside diameter of 15 feet at the feed end and 13 feet at the firing end. The kilns in Kiln Group 5 rotate at speeds of greater than 40 revolutions per hour and are driven by an electric motor.

Dracco manufactured the baghouse for Kiln 19. The baghouse has two parallel sets of six chambers and a design airflow of 175,000 cubic feet per minute (cfm) at 400°F. The maximum operating temperature is 550°F. The baghouses for kilns 20 and 21, manufactured by Wheelbrator-Frye are identical in design and construction, with two parallel sets of six chambers. Each baghouse has a design air flow of 166,000 cfm at 400°F. The maximum operating temperature is 550°F.

Kiln Group 6:

Kiln Group 6 at the Lafarge Alpena plant consists of two rotary kilns (#22 and #23). Specific components of Kiln Group 6 are:

- Coal/petroleum coke and combustion air delivery;
- Raw mix preparation and delivery;
- Two rotary kilns;
- Kiln burners; and
- Air pollution control system, consisting of the following components:
 - Boiler;
 - SNCR (mid-kiln);
 - Multiclone dust collectors;
 - Baghouses;
 - Induced draft (ID) fans; and
 - Wet gas Scrubber (WGS);
 - Common exhaust stack.

The pulverized coal/coke is pneumatically conveyed by heated air, recycled from the clinker cooler, through the outer ring of a concentric burner torch. Both rotary kilns in KilnGroup 6 were manufactured by Fuller Co. and are identical in design and operation. The kilns are 500 feet long and have a 19.5-foot outer diameter. The kilns are lined with high-temperature refractory brick. The kiln design is based on a throughput of 4.8 million Btu per ton of clinker. An induced draft fan pulls combustion gases from each kiln. After exiting the kiln, the gases pass through a set of multicyclones and then enter a fabric filter baghouse. After exiting the baghouse, the gases are routed through a breeching duct that connects the baghouse to a common reinforced concrete stack and exhaust to a wet FDG (scrubber).

The kilns rotate at a rate up to 80 revolutions per hour using two 350-hp motors. The kilns' associated air pollution control systems (APCS) are identical to one another in all aspects of design, operation, and maintenance. The APCS for Kilns 22 and 23 are identical ten-compartment baghouses. Each baghouse, manufactured by

Wheelbrator-Frye, consists of two parallel sets of five chambers and has design airflow of 285,000 cfm at 400°F. Figure 2-2 provides a process flow diagram of Kiln Group 6.

Kiln Process Instrumentation:

Instruments used to monitor kiln operating parameters are located throughout the kiln system. Parameters that will be recorded during testing are the baghouse inlet temperature, production rate, and baghouse change in pressure (delta P). Each kiln system is equipped with a differential pressure indicator system, with measurement points located in the duct prior to and exiting the baghouse. The differential pressure devices are used to monitor the pressure drop across the baghouse.

Raw Mill:

The Raw Mill System mixes and grinds the raw materials (limestone, sand, bauxite, Bell shale, gypsum) and alternate raw materials (slag, iron ore, fly ash, and CKD) then sends the materials to the kilns.

EU RAW MILL 14 (Raw Mill 14) and EU RAW MILL 15 (Raw Mill 15), further grind the raw and alternate raw materials using ball mills. The raw mix powder is then sent to one of four storage silos before the materials are sent to the kilns via air slides, screw elevators and pumps. Two storage silos are associated with Kilns 19, 20, 21, and two storage silos are associated with Kilns 22, 23. Figure 2.3 illustrates the process flow of the raw mill operations.

Clinker Coolers:

A Clinker Cooler cools the clinker, reclaims the hot air for return to the kilns, and moves clinker to FG CLINKER SYS. As the clinker is conveyed toward the clinker storage building, the recovered heat from Clinker Cooler (92) and (93) is re-circulated back to Kiln Group 5 (KG 5), the recovered heat from Clinker Cooler 22 is re-circulated back to Kiln 22, and the recovered heat from Clinker Cooler 23 is re-circulated back to Kiln 23.

3.2 SAMPLING LOCATION

KILN SAMPLING LOCATIONS:

The baghouse breaching ducts have been demonstrated as acceptable locations to conduct EPA reference method testing on all kilns. For each location the stack sampling location is in the breaching duct between each kiln's baghouse and discharge stack. Ductwork geometry is adequate for collecting a representative sample of gaseous constituents at this point.

CLINKER COOLER SAMPLING LOCATIONS:

The existing test ports from both KG5 and KG6 clinker coolers will be used to measure manual PM with EPA Method 5 during the annual re-certification test period. A total of three EPA Method 5 test runs with full particulate traverses will be conducted on each of the four clinker coolers. The signal output (mA) from each PCMS (PM monitor) will be recorded every minute during the corresponding Method 5 test runs from PM monitor from the Lafarge DHAS system. The average signal output will be used to confirm the value established for the CPMS per the PC MACT regulation.

4.0 SAMPLING AND ANALYTICAL PROCEDURES

4.1 TEST METHODS

The emission test on the Clinker Cooler 22, 23, 92, and 93 at the Alpena Plant was performed following United States Environmental Protection Agency (EPA) methods described by the Code of Federal Regulations (CFR). Table 4.1 outlines the specific methods performed on July 23-26, 2019.

**TABLE 4.1
SUMMARY OF SAMPLING METHODS**

| Pollutant or Parameter | Sampling Method | Analysis Method |
|------------------------|-----------------|---------------------------------|
| Sample Point Location | EPA Method 1 | Equal Area Method |
| Stack Flow Rate | EPA Method 2 | S-Type Pitot Tube |
| Oxygen | EPA Method 3A | Paramagnetic Cell |
| Carbon Dioxide | EPA Method 3A | Nondispersive Infrared Analyzer |
| Stack Moisture Content | EPA Method 4 | Gravimetric Analysis |
| Particulate Matter | EPA Method 5 | Front Half Filterables |

4.2 INSTRUMENT CONFIGURATION AND OPERATIONS FOR GAS ANALYSIS

The sampling and analysis procedures used during these tests conform with the methods outlined in the Code of Federal Regulations (CFR), Title 40, Part 60, Appendix A, Methods 1, 2, 3A, 4, and 5.

Figure 4.1 depicts the sample system used for the real-time gas analyzer tests. The gas sample was continuously pulled through the probe and transported, via heat-traced Teflon® tubing, to stainless steel minimum-contact condenser designed to dry the sample. Transportation of the sample, through Teflon® tubing, continued into the sample manifold within the mobile laboratory via a stainless steel/Teflon® diaphragm pump. From the manifold, the sample was partitioned to the real-time analyzers through rotameters that controlled the flow rate of the sample.

Figure 4.1 shows that the sample system was also equipped with a separate path through which a calibration gas could be delivered to the probe and back through the entire sampling system. This allowed for convenient performance of system bias checks as required by the testing methods.

All instruments were housed in an air-conditioned, trailer-mounted mobile laboratory. Gaseous calibration standards were provided in aluminum cylinders with the concentrations certified by the vendor.

Table 4.2 provides a description of the analyzers used for the instrument portion of the tests. All data from the continuous monitoring instruments were recorded on a Logic Beach Portable Data Logging System which retrieves calibrated electronic data from each instrument every one second and reports an average of the collected data every 30 seconds.

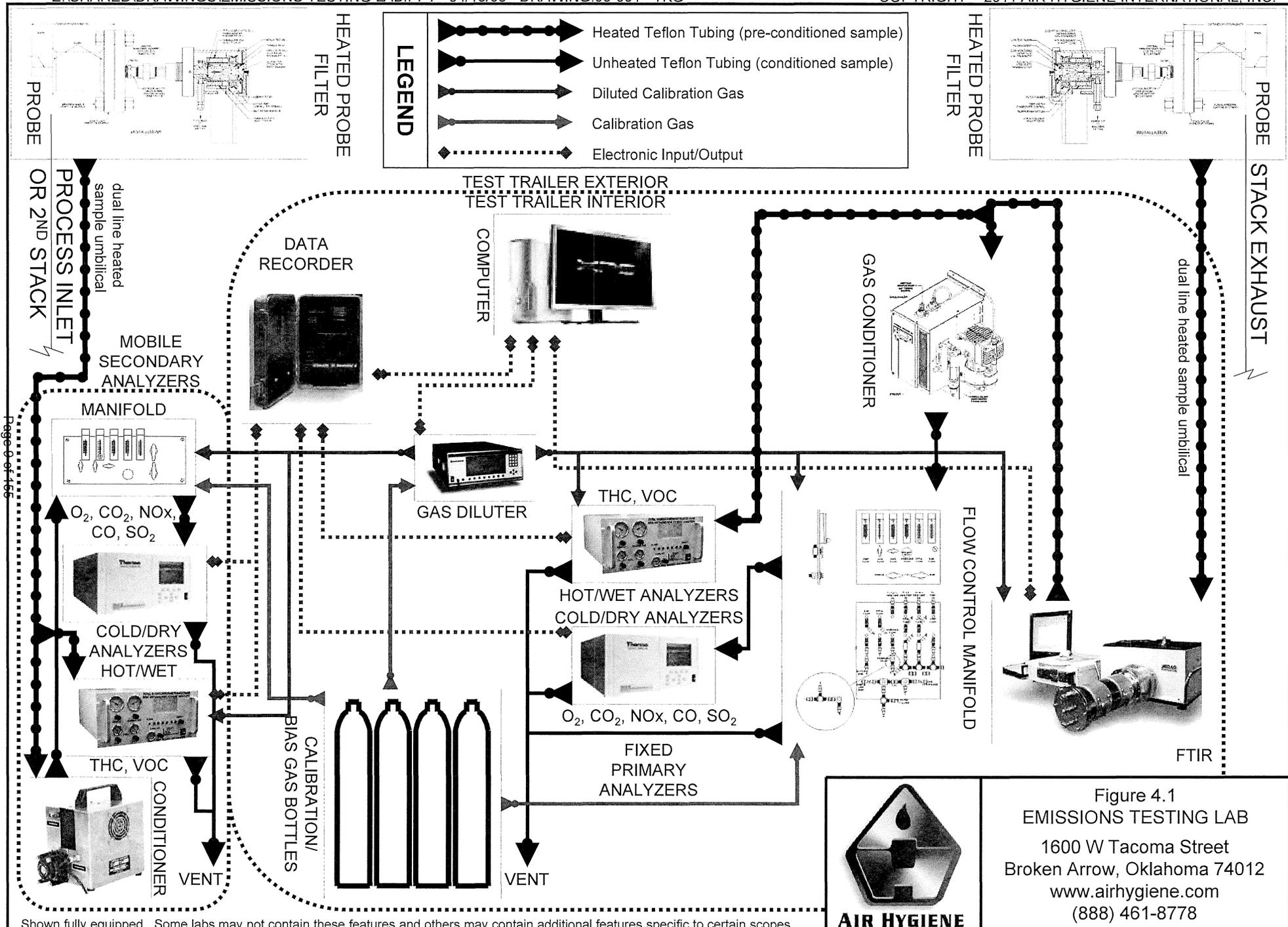
Figure 4.2 represents the sample system used for the wet chemistry tests (PM). A heated stainless steel probe with a glass liner and stainless steel nozzle was inserted into the sample ports of the stack to extract gas measurements from the emission stream through a filter and glass impinger train. Flow rates are monitored with oil filled manometers and total sample volumes are measured with a dry gas meter.

Three test runs of approximately 60 minutes each were conducted on the Clinker Cooler 22, 23, 92, and 93 at the maximum test load for PM, flow, H₂O, CO₂, and O₂.

The stack gas analysis for O₂ and CO₂ concentrations was performed in accordance with procedures set forth in EPA Method 3A. The O₂ analyzer uses a paramagnetic cell detector and the CO₂ analyzer uses a continuous nondispersive infrared analyzer.

**TABLE 4.2
ANALYTICAL INSTRUMENTATION**

| Parameter | Manufacturer and Model | Range | Sensitivity | Detection Principle |
|-----------------|------------------------|-------|-------------|---------------------------------------|
| CO ₂ | SERVOMEX 1440 | 0-20% | 0.1% | Nondispersive infrared |
| O ₂ | SERVOMEX 1440 | 0-25% | 0.1% | Paramagnetic cell, inherently linear. |



LEGEND

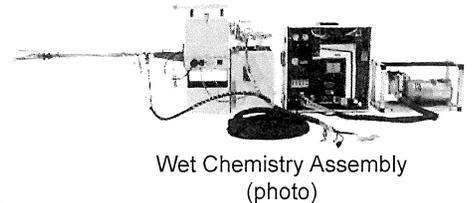
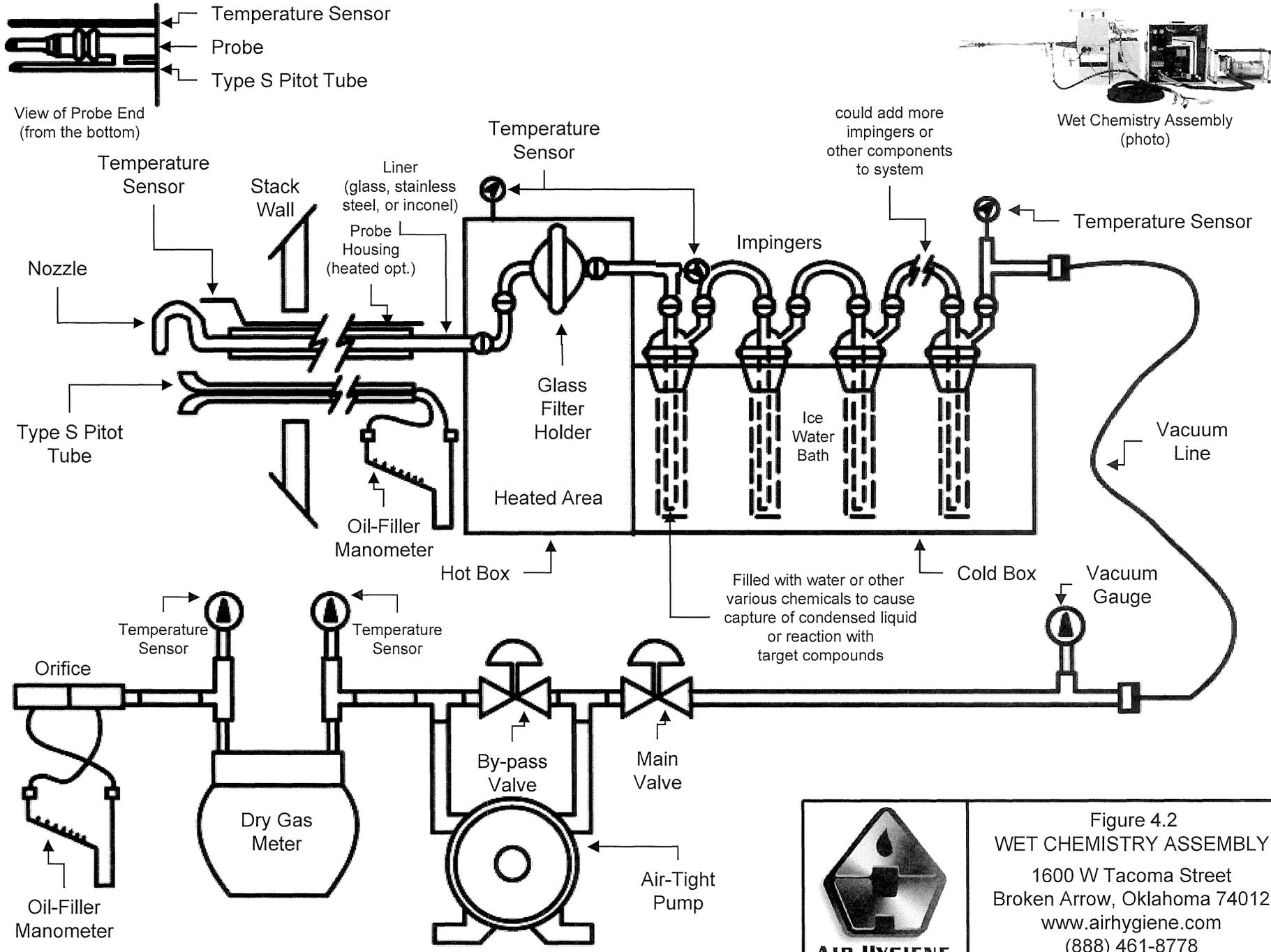
- Heated Teflon Tubing (pre-conditioned sample)
- Unheated Teflon Tubing (conditioned sample)
- Diluted Calibration Gas
- Calibration Gas
- Electronic Input/Output

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Figure 4.1
EMISSIONS TESTING LAB
 1600 W Tacoma Street
 Broken Arrow, Oklahoma 74012
 www.airhygiene.com
 (888) 461-8778

Shown fully equipped. Some labs may not contain these features and others may contain additional features specific to certain scopes.



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Figure 4.2
WET CHEMISTRY ASSEMBLY
 1600 W Tacoma Street
 Broken Arrow, Oklahoma 74012
 www.airhygiene.com
 (888) 461-8778

APPENDIX A
TEST RESULTS AND CALCULATIONS