Relative Accuracy Test Audit Test Report

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Billerud Quinnesec LLC Quinnesec Mill Package Boiler Outlet Duct, Waste Fuel Boiler Outlet Duct, Recovery Boiler Outlet Duct, and Lime Kiln Stack Quinnesec, Michigan Project No. M242110A



Relative Accuracy Test Audit Test Report

Billerud Quinnesec LLC Quinnesec Mill Package Boiler Outlet Duct, Waste Fuel Boiler Outlet Duct, Recovery Boiler Outlet Duct, and Lime Kiln Stack Quinnesec, Michigan Test Dates: May 21 through 23, 2024

> Report Submittal Date July 9, 2024

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Project No. M242110A

Corporate Headquarters 888 Industrial Drive Elmhurst, Illinois 60126 630-993-2100

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1.0 EXECUTIVE SUMMARY

Mostardi Platt conducted a Relative Accuracy Test Audit (RATA) test program for Billerud Quinnesec LLC at the Quinnesec, Michigan facility. This report summarizes the results of the test program and test methods used.

The test locations, test dates, and test parameters are summarized below.

TEST INFORMATION					
Test Locations	RATA Test Dates	Test Parameters			
Package Boiler Outlet Duct	May 21, 2024	Nitrogen Oxides (NOx), Carbon Monoxide (CO), and Oxygen (O ₂)			
Waste Fuel Boiler Outlet Duct	May 23, 2024	NO _x , Sulfur Dioxide (SO ₂), Carbon Dioxide (CO ₂), O ₂ , and Volumetric Flow			
Recovery Boiler Outlet Duct	May 22 and 23, 2024	NO _X , SO ₂ , O ₂ , CO, Total Reduced Sulfur (TRS), and Volumetric Flow			
Lime Kiln Stack	May 21, 2024	TRS and O ₂			

The purpose of the test program was to demonstrate the relative accuracy of the parameters listed above. Selected results of the test program are summarized below. A complete summary of emission test results, for each location, follows the narrative portion of this report.

TRS results were corrected to eight percent O_2 on the Recovery Boiler and ten percent O_2 on the Lime Kiln.

PACKAGE BOILER OUTLET DUCT								
Date	Parameter	Units	Acceptance Criteria	Relative Accuracy				
5/21/2024	NOx	lb/mmBtu	< 20% of the mean reference method value	7.35%				
	NOx	lb/hr	< 20% of the mean reference method value	3.42%				
	O ₂	D ₂ % dry <20% of the mean reference method value		1.83%				
	со	lb/mmBtu	< 5% of applicable standard of 0.12 lb/hr	3.06% of applicable standard of 0.12 lb/MMBtu				
	со	ppm	< 5 ppm mean difference + confidence coefficient	3.17 ppm mean difference + confidence coefficient				
	со	lb/hr	< 5% of applicable standard of 25.5 lb/hr	1.78% of applicable standard of 25.5 lb/hr				

WASTE FUEL BOILER OUTLET DUCT							
Date	Parameter	Units	Acceptance Criteria	Relative Accuracy			
	NOx	lb/mmBtu	< 20% of the mean reference method value	6.17%			
	NOx	lb/hr	< 20% of the mean reference method value	12.09%			
	CO ₂	% dry	< 20% of the mean reference method value	0.54%			
5/23/2024	O ₂	% dry	< 20% of the mean reference method value	3.02%			
	SO ₂	lb/mmBtu	< 20% of the mean reference method value	0.00%			
	SO ₂	lb/hr	< 10% of applicable standard of 476 lb/hr	0.51% of applicable standard of 476 lb/hr			
	Volumetric Flow	dscfm	< 20% of the mean reference method value	14.36%			

	RECOVERY BOILER OUTLET DUCT								
Date	Parameter	Units	Relative Accuracy						
	NOx	ppmvd @ 8% O2	< 20% of the mean reference method value	3.39%					
5/22/2024	0/22/2024 O2 SO2				< 20% of the mean reference method value	6.08%			
5/22/2024			< 10% of applicable standard of 50 ppmvd@ 8% O ₂	0.87% of applicable standard of 50 ppmvd @ 8% O ₂					
	со	ppmvd @ 8% O2	< 5% of applicable standard of 500 ppmvd@ 8% O ₂	1.22% of applicable standard of 425 ppmvd @ 8% O ₂					
5/22/2024 & 5/23/2024			< 20% of the mean reference method value	10.19%					
5/22/2024	12/2024 dscfm		< 20% of the mean reference method value	1.83%					

LIME KILN STACK						
Date	Parameter	Units	Acceptance Criteria	Relative Accuracy		
5/21/2024	TRS	ppmvd @ 10% O ₂	< 20% of the mean reference method value	14.23%		
	O ₂	% dry	< 20% of the mean reference method value	8.97%		

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GAS CYLINDER INFORMATION							
Parameter	Gas Vendor	Cylinder Serial Number	Cylinder Value	Expiration Date			
NOx	Airgas	XF003141B	124.8 ppm	3/4/2032			
NOx	Airgas	ALM-023821	150.8 ppm	1/24/2031			
NOx	Airgas	CC48275	300.5 ppm	1/24/2032			
SO ₂	Airgas	CC439581	12.15 ppm	6/1/2025			
SO ₂	Airgas	CC285356	12.17 ppm	10/18/2026			
SO ₂	Airgas	CC501703	25.05 ppm	10/18/2026			
SO ₂	Airgas	CC488384	248.5 ppm	8/7/2031			
SO ₂	Airgas	CC280724	496.4 ppm	9/1/2031			
O ₂	Airgas	CC35454	5.077%	2/12/2032			
O ₂	Airgas	CC403240	9.041%	2/6/2032			
O ₂	Airgas	CC47224	9.151%	2/6/2032			
O ₂	Airgas	CC440339	21.93%	7/7/2030			
CO ₂	Airgas	CC309474	9.940%	5/1/2031			
CO ₂	Airgas	CC709438	19.17%	6/23/2031			
CO	Airgas	XF003141B	78.02 ppm	3/4/2032			
CO	Airgas	000006	173.5 ppm	2/23/2027			
CO	Airgas	CC218918	470.6 ppm	3/23/2030			
CO	Airgas	CC713835	920.9 ppm	8/12/2027			

The gas cylinders used to perform the RATA are summarized below.

The identifications of the individuals associated with the test program are summarized below.

Location	Address	Contact
Test Facility	Billerud Quinnesec LLC W-679 U. S. Highway 2 Quinnesec, Michigan 49876	Ms. Paula LaFleur Environmental Engineer (906) 779-3494 (phone) paula.lafleur@billerud.com
Testing Company Representative	Mostardi Platt 888 Industrial Drive Elmhurst, Illinois 60126	Mr. Christopher Jensen Senior Project Manager (630) 993-2100 (phone) cjensen@mp-mail.com

The test crew consisted of B. Truett, J. Jimenez, T. Yanowsky, and C. Jensen of Mostardi Platt.

2.0 TEST METHODOLOGY

Emissions testing was conducted following the methods specified in 40CFR, Part 40 CFR, Part 60, Appendix A. Schematics of the test section diagrams and sampling trains used are included in Appendix A and B, respectively. Copies of example calculation and nomenclature are included in Appendix C. Copies of analyzer print-outs for each test run are included in Appendix D. CEM data and process data as provided by Billerud Quinnesec, LLC are included in Appendix E.

The following methodologies were used during the test program:

Method 1 Traverse Point Determination

Test measurement points were selected in accordance with Method 1. The characteristics of the measurement locations are summarized below.

Location	Upstream Distance	Downstream Distance	Test Parameter	Number of Sampling Points
Waste Fuel Boiler Outlet Duct	20 feet	100 feet	Volumetric	10
Recovery Boiler Outlet Duct	20 feet	80 feet	Flow	18

Method 2 Volumetric Flowrate Determination

Gas velocity was measured following Method 2, for purposes of calculating stack gas volumetric flow rate at the Waste Fuel Boiler Outlet Duct and Recovery Boiler Outlet Duct. An S-type pitot tube, differential pressure gauge, thermocouple and temperature readout were used to determine gas velocity at each sample point at each test location. Copies of field data sheets are included in Appendix F. All of the equipment used was calibrated in accordance with the specifications of the Method. Calibration data are presented in Appendix G. This testing met the performance specifications as outlined in the Method.

Method 3A Oxygen (O₂)/ Carbon Dioxide (CO₂) Determination

Stack gas O₂ and/or CO₂ concentrations were determined in accordance with USEPA Method 3A. Servomex analyzers were used to determine the O₂ and/or CO₂ concentrations in the manner specified in the Method. Each instrument has a paramagnetic detector and the O₂ operates in the nominal range of 0% to 25% with the specific range determined by the high-level calibration gas and the CO₂ operates in the nominal range of 0 to 20% with the specific range determined by the high-level calibration gas. High-range calibrations were performed using USEPA Protocol gas. Zero nitrogen (a low ppm pollutant in balance nitrogen calibration gases) was introduced during other instrument calibrations to check instrument zero. High- and a mid-range % O₂ and/or CO₂ levels in balance nitrogen were also introduced. Zero and mid-range calibrations were performed using USEPA Protocol gas after each test run. Copies of the gas cylinder certifications are found in Appendix H. This testing met the performance specifications as outlined in the Method.

Method 4 Moisture Determination

USEPA Method 4, 40CFR60, Appendix A, was utilized to determine water (H_2O) content of the exhaust gas Waste Fuel Boiler Outlet Duct and Recovery Boiler Outlet Duct. 100 milliliters (ml) of water were added to each of the first two impingers, the third impinger was left empty, and the fourth impinger was charged with approximately 200 grams of silica gel. The impingers were placed in an ice bath to maintain the sampled gas passed through the silica gel impinger outlet below 68°F in order to increase the accuracy of the sampled dry gas volume measurement. The water volumes

of the impinger train were measured and the silica gel was weighed before and after each test run to determine the mass of moisture condensed.

Each sample was extracted through a heated stainless-steel probe and filter assembly at a constant sample rate of approximately 0.75 cubic feet per minute, which was maintained throughout the course of the test run. Approximately 21 dry standard cubic feet (dscf) were sampled for, each moisture run. After each run, a leak check of the sampling train was performed at a vacuum greater than the sampling vacuum to determine if any leakage had occurred during sampling. Following the leak check, the impingers were removed from the ice bath, water levels were measured, and the silica gel weight was recorded.

All of the equipment used was calibrated in accordance with the specifications of the Method.

Copies of field data sheets are included in Appendix F. Calibration data is presented in Appendix G. This testing met the performance specifications as outlined in the Method.

Method 6C Sulfur Dioxide (SO₂) Determination

Stack gas SO₂ concentrations and emission rates were determined in accordance with USEPA Method 6C, 40CFR60, Appendix A at the Waste Fuel Boiler Outlet Duct and Recovery Boiler Outlet Duct. A Thermo Scientific Model 43C Pulsed Fluorescence Sulfur Dioxide Analyzer was used to determine sulfur dioxide concentrations, in the manner specified in the Method. The instrument for the Recovery Boiler operated in the nominal range of 0 ppm to 100 ppm with the specific range determined by the high-level span calibration gas of 90.56 ppm. The instrument for the Waste Fuel Boiler operated in the nominal range of 0 ppm with the specific range determined by the high-level span calibration gas of 496.4 ppm.

The Model 43C High Level is based on the principle that SO₂ molecules absorb ultraviolet (UV) light and become excited at one wavelength, then decay to a lower energy state emitting UV light at a different wavelength. Specifically,

$$SO_2 + hv_1 \rightarrow SO_2^* \rightarrow SO_2 + hv_2$$

The sample is drawn into the Model 43C High Level through the sample bulkhead. The sample passes a pressure sensor then flows through a capillary and a flow sensor. The sample then flows into the fluorescence chamber, where pulsating UV light excites the SO_2 molecules. The condensing lens focuses the pulsating UV light into the mirror assembly. The mirror assembly contains four selective mirrors that reflect only the wavelengths which excite SO_2 molecules. As the excited SO_2 molecules decay to lower energy states they emit UV light that is proportional to the SO_2 concentration. The bandpass filter allows only the wavelengths emitted by the excited SO_2 molecules to reach the photomultiplier tube (PMT). The PMT detects the UV light emission from the decaying SO_2 molecules. The photodetector, located at the back of the fluorescence chamber, continuously monitors the pulsating UV light source and is connected to a circuit that compensates for fluctuations in the UV light.

The sample then flows to the pump and is exhausted out the exhaust bulkhead of the analyzer. The Model 43C High Level outputs the SO₂ concentration to the front panel display and the analog outputs.

Stack gas was delivered to the analyzer via a Teflon[®] sampling line, heated to a minimum temperature of 250°F. Excess moisture in the stack gas was removed using a refrigerated

condenser. The entire system was calibrated in accordance with the Method, using certified calibration gases introduced at the probe, before and after each test run.

A list of calibration gases used and the results of all calibration and other required quality assurance checks are found in Appendix G. Copies of the gas cylinder certifications are found in Appendix H. This testing met the performance specifications as outlined in the Method.

Method 7E Nitrogen Oxide (NO_X) Determination

Stack gas NO_X concentrations and emission rates were determined in accordance with USEPA Method 7E, 40CFR60, Appendix A, at the Package Boiler Outlet Duct, Waste Fuel Boiler Outlet Duct, and Recovery Boiler Outlet Duct. A Thermo Scientific Model 42i Chemiluminescence Nitrogen Oxides Analyzer was used to determine nitrogen oxides concentrations, in the manner specified in the Method. The instrument operated in the nominal range of 0 ppm to 500 ppm with the specific range determined by the high-level span calibration gas of 300.5 ppm.

The Model 42i operates on the principle that nitric oxide (NO) and ozone (O_3) react to produce a characteristic luminescence with an intensity linearly proportional to the NO concentration. Infrared light emission results when electronically excited NO₂ molecules decay to lower energy states. Specifically,

$$NO+O_3 \rightarrow NO_2+O_2+hv$$

Nitrogen dioxide (NO₂) must first be transformed into NO before it can be measured using the chemiluminescent reaction. NO₂ is converted to NO by a molybdenum NO₂-to-NO converter heated to about 205°C. The flue gas sample is drawn into the Model 42*i* through the sample bulkhead. The sample flows through a capillary, and then to the mode solenoid valve. The solenoid valve routes the sample either straight to the reaction chamber (NO mode) or through the NO₂-to-NO converter and then to the reaction chamber (NO_X mode). A flow sensor prior to the reaction chamber measures the sample flow. Dry air enters the Model 42*i* through the dry air bulkhead, passes through a flow switch, and then through a silent discharge ozonator. The ozonator generates the ozone needed for the chemiluminescent reaction. At the reaction chamber, the ozone reacts with the NO in the sample to produce excited NO₂ molecules. A photomultiplier tube (PMT) housed in a thermoelectric cooler detects the luminescence generated during this reaction. From the reaction chamber, the exhaust travels through the ozone (O₃) converter to the pump, and is released through the vent.

The NO and NO_X concentrations calculated in the NO and NO_X modes are stored in memory. The difference between the concentrations is used to calculate the NO₂ concentration. The Model 42i outputs NO, NO₂, and NO_X concentrations to the front panel display, the analog outputs, and also makes the data available over the serial or ethernet connection.

Stack gas was delivered to the analyzer via a Teflon[®] sampling line, heated to a minimum temperature of 250°F. Excess moisture in the stack gas was removed using a refrigerated condenser. The entire system was calibrated in accordance with the Method, using certified calibration gases introduced at the probe, before and after each test run. This testing met the performance specifications as outlined in the Method.

A list of calibration gases used and the results of all calibration and other required quality assurance checks are found in Appendix G. Copies of the gas cylinder certifications are found in Appendix H. The NO₂ to NO converter tests can be found in Appendix I. This testing met the performance specifications as outlined in the Method.

Method 10 Carbon Monoxide (CO) Determination

Stack gas CO concentrations and emission rates were determined in accordance with USEPA Method 10, 40CFR60, Appendix A at the Package Boiler Outlet Duct and Recovery Boiler Outlet Duct. A Fischer Scientific Model 48C Gas Filter Correlation Carbon Monoxide was used to determine carbon monoxide concentrations, in the manner specified in the Method. The instrument operated in the nominal range of 0 ppm to 500 ppm or 1,000 ppm with the specific range determined by the high-level span calibration gas of 173.5 ppm and 920.9 ppm.

The Model 48C High Level is based on the principle that CO absorbs infrared radiation at a wavelength of 4.6 microns. Because infrared absorption is a nonlinear measurement technique, it is necessary for the instrument electronics to transform the basic analyzer signal into a linear output. The Model 48C High Level uses an exact calibration curve to accurately linearize the instrument output over any range up to a concentration of 20,000 ppm. The sample is drawn into the analyzer through the sample bulkhead. The sample flows through the optical bench. Radiation from an infrared source is chopped and then passed through a gas filter alternating between CO and N2. The radiation then passes through a narrow bandpass interference filter and enters the optical bench where absorption by the sample gas occurs. The infrared radiation then exits the optical bench and falls on an infrared detector. The CO gas filter acts to produce a reference beam which cannot be further attenuated by CO in the sample cell. The N_2 side of the filter wheel is transparent to the infrared radiation and therefore produces a measure beam which can be absorbed by CO in the cell. The chopped detector signal is modulated by the alternation between the two gas filters with an amplitude related to the concentration of CO in the sample cell. Other gases do not cause modulation of the detector signal since they absorb the reference and measure beams equally. Thus, the GFC system responds specifically to CO. The Model 48C High Level outputs the CO concentration to the front panel display and the analog outputs.

Stack gas was delivered to the analyzer via a Teflon[®] sampling line, heated to a minimum temperature of 250°F. Excess moisture in the stack gas was removed using a refrigerated condenser. The entire system was calibrated in accordance with the Method, using certified calibration gases introduced at the probe, before and after each test run.

A list of calibration gases used and the results of all calibration and other required quality assurance checks are found in Appendix G. Copies of the gas cylinder certifications are found in Appendix H. This testing met the performance specifications as outlined in the Method.

Method 16C Total Reduced Sulfur (TRS) Determination

Integrated gas samples were extracted from the Lime Kiln and Recovery Boiler Outlet Duct gas streams in accordance with Method 16C (SO2 Monitor), 40CFR60, for the determination of total reduced sulfur (TRS) emissions from stationary sources. This method selectively removed sulfur dioxide (SO₂) by bubbling the gas sample through a citrate buffer solution, then thermally oxidizing TRS compounds present to SO₂. A portion of the gas stream was conveyed to the gas analyzer for determination of SO₂ content. Prior to sampling, the SO₂ analyzer was zeroed and calibrated with high-range, mid-range, and zero gases. After each test run, zero and mid-range calibration gases were introduced to check calibration.

Interferences caused by particulate matter entering the sampling train were eliminated by the use of a heated filter medium placed at the end of the heated Teflon®-lined (or glass-lined) probe.

Prior to field sampling, an optional 30-minute system performance test was performed to validate the sampling train components and procedure. The checks involved sampling a known concentration of hydrogen sulfide (H_2S) and comparing the analyzed concentration with the known concentration. The H_2S recovery gas was mixed with combustion gas in a dilution system. The flowrates were adjusted to generate an H_2S concentration in the range of the stack gas. The samples were collected and analyzed in the same manner as a normal stack test. The sample was collected through the end of the probe to ensure extraction of a representative sample. System validations were performed following each one-hour test in the same manner as the system performance test.

A list of calibration gases used and the results of all calibration and other required quality assurance checks can be found in Appendix G. Copies of calibration gas certifications can be found in Appendix H.

3.0 TEST RESULT SUMMARIES

Client: Billerud Quinnesec, LLC Facility: Quinnesec Mill Project #: M242110 Fuel Type: Natural Gas

Location: Package Boiler Outlet Duct Date: 5/21/24 Test Method: 7E, 3A Fuel Factor: 8710

O2 based NOx Ib/mmBtu RATA

			C	EM Analyze	r Information			
NC	x Moni	tor/Model:	Therm	o 42iQ		NO _x Serial # :	11800	090011
0	2 Moni	tor/Model:	Thermo	CTL902C		O2 Serial # :	11803	390002
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM NO _x Ib/MMBtu	CEM NO _x Ib/MMBtu	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)
1	1	05/21/24	08:35	08:55	0.05	0.04	0.01	0.0001
1	2	05/21/24	09:07	09:27	0.05	0.05	0.00	0.0000
1	3	05/21/24	09:35	09:55	0.05	0.05	0.00	0.0000
0	4	05/21/24	10:04	10:24	0.05	0.04	0.01	0.0001
1	5	05/21/24	10:34	10:54	0.05	0.05	0.00	0.0000
1	6	05/21/24	11:04	11:24	0.05	0.05	0.00	0.0000
1	7	05/21/24	11:34	11:54	0.05	0.05	0.00	0.0000
1	8	05/21/24	12:04	12:24	0.05	0.05	0.00	0.0000
1	9	05/21/24	12:34	12:54	0.05	0.05	0.00	0.0000
1	10	05/21/24	13:06	13:26	0.05	0.05	0.00	0.0000
				n		9		
				t(0.975)	2.3	306		
		Mean Re	eference Me	thod Value	0.0	050	RM avg	
			Mean	CEM Value	0.049		CEM avg	
			Sum of	Differences	0.010		di	
			Mean	Difference	0.0	001	d	
	Sum of Differences Squared			0.0	000	di ²		
	Standard Deviation					sd		
(Confide	nce Coeffi	icient 2.5% I	Error (1-tail)	0.0	003	cc	
			Relativ	e Accuracy	7.	35	RA	

Location:	Package Boiler Outlet Duct
Date:	5/21/24
Test Method:	7E, 2

Applicable Standard: 41.9

NO_x lb/hr RATA

CEM Analyzer Information

NC	NO _x Monitor/Model:		Therm	o 42iQ	NO _x Serial # :		1180090011	
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM NO _x Ib/hr	CEM NO _x Ib/hr	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)
1	1	05/21/24	08:35	08:55	7.66	7.48	0.18	0.0324
1	2	05/21/24	09:07	09:27	7.74	7.52	0.22	0.0484
1	3	05/21/24	09:35	09:55	7.81	7.54	0.27	0.0729
0	4	05/21/24	10:04	10:24	7.85	7.51	0.34	0.1156
1	5	05/21/24	10:34	10:54	7.79	7.57	0.22	0.0484
1	6	05/21/24	11:04	11:24	7.79	7.55	0.24	0.0576
1	7	05/21/24	11:34	11:54	7.86	7.59	0.27	0.0729
1	8	05/21/24	12:04	12:24	7.84	7.57	0.27	0.0729
1	9	05/21/24	12:34	12:54	7.79	7.55	0.24	0.0576
1	10	05/21/24	13:06	13:26	7.83	7.56	0.27	0.0729
				n		9		
				t(0.975)		306		
		Mean Re	ference Me			790	RM avg	
				CEM Value			CEM avg	
				Differences			di	
	Mean Difference				242	d		
	Sum of Differences Squared			0.536		di ²		
	Standard Deviation			0.	0.032 sd			
(Confidence Coefficient 2.5% Error (1-tail)			0.	024	cc		
			Relativ	e Accuracy	3	.42	RA	

Client: Billerud Quinnesec, LLC Facility: Quinnesec Mill F

			C, LLC			Fackage Dolle	Outlet Duct		
Facility: Project #:					Test Method:	5/21/24 3A			
i ioject <i>ii</i> .	1012421	10		0 % (d		- Or (
					ry) RATA				
-			1		er Information		1100	200002	
02	O ₂ Monitor/Model: Thermo CTL902C					O ₂ Serial # :		390002	
1=accept 0=reject	Test Run	Test Date	Start Time	End Time			(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)	
1	1	05/21/24	08:35	08:55	3.8	3.8	0.0	0.00	
1	2	05/21/24	09:07	09:27	3.9	4.0	-0.1	0.01	
1	3	05/21/24	09:35	09:55	4.2	4.1	0.1	0.01	
1	4	05/21/24	10:04	10:24	4.0	4.0	0.0	0.00	
1	5	05/21/24	10:34	10:54	4.1	4.1	0.0	0.00	
1	6	05/21/24	11:04	11:24	4.3	4.3	0.0	0.00	
1	7	05/21/24	11:34	11:54	3.9	4.0	-0.1	0.01	
0	8	05/21/24	12:04	12:24	3.9	4.0	-0.1	0.01	
1	9	05/21/24	12:34	12:54	4.0	4.1	-0.1	0.01	
1	10	05/21/24	13:06	13:26	4.0	4.0	0.0	0.00	
				n		9			
				t(0.975)	2.3	306			
		Mean Re	eference Me		4.	022	RM avg		
				CEM Value		044	CEM avg		
				Differences		.200	di		
Mean Difference					-0.	.022	d		
Sum of Differences Squared						040	di ²		
Standard Deviation					0.	067	sd		
C	onfide	nce Coeff		Error (1-tail)		051	cc		
			Relativ	e Accuracy	1	.83	RA		

Location: Package Boiler Outlet Duct

Client: Billerud Quinnesec, LLC Facility: Quinnesec Mill Project #: M242110 Fuel Type: Natural Gas

Location: Package Boiler Outlet Duct Date: 5/21/24 Test Method: 10, 3A Fuel Factor: 8710

.

Applicable Standard: 0.12

O2 based CO lb/mmBtu RATA

			U	LIVI AllaTyze	rinionnauon			
C	O Moni	tor/Model:	Therm	o 48iQ		CO Serial # :	1180	930081
0	2 Moni	tor/Model:	Thermo	CTL902C		O2 Serial # :	1180	390002
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM CO Ib/MMBtu	CEM CO Ib/MMBtu	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)
1	1	05/21/24	08:35	08:55	0.01	0.01	0.00	0.000000
1	2	05/21/24	09:07	09:27	0.00	0.01	-0.01	0.000100
1	3	05/21/24	09:35	09:55	0.00	0.00	0.00	0.000000
1	4	05/21/24	10:04	10:24	0.00	0.00	0.00	0.000000
1	5	05/21/24	10:34	10:54	0.00	0.00	0.00	0.000000
1	6	05/21/24	11:04	11:24	0.00	0.00	0.00	0.000000
1	7	05/21/24	11:34	11:54	0.01	0.01	0.00	0.000000
0	8	05/21/24	12:04	12:24	0.00	0.01	-0.01	0.000100
1	9	05/21/24	12:34	12:54	0.01	0.01	0.00	0.000000
1	10	05/21/24	13:06	13:26	0.01	0.01	0.00	0.000000
_				n t(0.975)		9		
		Mean Re	ference Me	. /		004	RM avg	
			Mean	CEM Value	0.0	006	CEM avg	
			Sum of	Differences	-0.	010	di	
			Mean	Difference	-0.	001	d	
Sum of Differences Squared					0.0	000	di ²	
	Standard Deviation					003	sd	
	Confidence Coefficient 2.5% Error (1-tail)					003	cc	
		R	elative Accu	uracy - APS	3.	06	RA	

^A Relative accuracy based upon +/- 5% of applicable standard

Location: Package Boiler Outlet Duct Date: 5/21/24

Test Method: 10

Applicable Standard: 195

CO ppmvd RATA

CEM Analyzer Information

C	O Moni	tor/Model:	Therm	o 48iQ		CO Serial # :	1180	930081
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM CO ppmvd	CEM CO ppmvd	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)
1	1	05/21/24	08:35	08:55	10.4	13.6	-3.2	10.24
1	2	05/21/24	09:07	09:27	6.3	9.1	-2.8	7.84
1	3	05/21/24	09:35	09:55	2.9	5.4	-2.5	6.25
1	4	05/21/24	10:04	10:24	4.8	7.6	-2.8	7.84
1	5	05/21/24	10:34	10:54	3.3	6.0	-2.7	7.29
1	6	05/21/24	11:04	11:24	2.5	5.2	-2.7	7.29
0	7	05/21/24	11:34	11:54	9.3	13.0	-3.7	13.69
1	8	05/21/24	12:04	12:24	5.6	8.9	-3.3	10.89
1	9	05/21/24	12:34	12:54	8.2	10.8	-2.6	6.76
1	10	05/21/24	13:06	13:26	6.4	9.9	-3.5	12.25
				n		9		
	_	Mean Re	ference Me	t(0.975) thod Value		306 600	RM avg	
			Mean	CEM Value	8.	500	CEM avg	
			Sum of	Differences	-26	.100	di	
			Mean	Difference	-2.	900	d	
		Sum	of Difference	es Squared	76.	650	di ²	
Standard Deviation					0.3	346	sd	
(Confidence Coefficient 2.5% Error (1-tail)					266	cc	
	Relative Accuracy - APS					.17	ppm + cc d	lifference ^A

^A Relative accuracy based upon alternate performance standard of +/- 5 ppm CO plus the confidence coefficient.

Location: Package Boiler Outlet Duct Date: 5/21/24 Test Method: 10, 2

Project #: M242110

Applicable Standard: 25.5

CO lb/hr RATA

CEM Analyzer Information

C	O Moni	tor/Model:	Therm	o 48iQ		CO Serial # :	11809	930081	
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM CO lb/hr	CEM CO lb/hr	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)	
1	1	05/21/24	08:35	08:55	1.4	1.8	-0.4	0.16	
1	2	05/21/24	09:07	09:27	0.8	1.2	-0.4	0.16	
1	3	05/21/24	09:35	09:55	0.4	0.7	-0.3	0.09	
1	4	05/21/24	10:04	10:24	0.6	1.0	-0.4	0.16	
1	5	05/21/24	10:34	10:54	0.4	0.8	-0.4	0.16	
1	6	05/21/24	11:04	11:24	0.3	0.7	-0.4	0.16	
1	7	05/21/24	11:34	11:54	1.2	1.7	-0.5	0.25	
0	8	05/21/24	12:04	12:24	0.7	1.2	-0.5	0.25	
1	9	05/21/24	12:34	12:54	1.1	1.4	-0.3	0.09	
1	10	05/21/24	13:06	13:26	0.8	1.3	-0.5	0.25	
				n t(0.975)	2.3				
		Mean Re	ference Me			778		Difference Difference ² (di) (di ²) -0.4 0.16 -0.4 0.16 -0.4 0.16 -0.4 0.16 -0.4 0.16 -0.4 0.16 -0.4 0.16 -0.4 0.16 -0.5 0.25 -0.5 0.25 -0.5 0.25 -0.5 0.25 -0.5 0.25 -0.5 0.25 -0.5 0.25 -0.5 0.25 -0.5 0.25 -0.5 0.25 -0.5 0.25 -0.5 0.25	
				CEM Value		178			
				Differences		600	di		
		•		Difference		400	d		
	Sum of Differences Squared					480	di ²		
	Standard Deviation					071	sd		
(Confidence Coefficient 2.5% Error (1-tail))54	cc		
	Relative Accuracy - APS					78	RA		

^A Relative accuracy based upon +/- 5% of applicable standard

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Client: Billerud Quinnesec, LLC Facility: Quinnesec Mill Project #: M242110 Fuel Type: Other

Fuel Type:	Other				Fuel Factor:	9518 .		
			O2 ba	sed NOx	b/mmBtu R	ATA		
					r Information			
		tor/Model:		o 42iQ		NO _x Serial # :		030057
0	2 Moni	tor/Model:	Thermo	CTL902C		O2 Serial # :	1180	530001
1=accept 0=reject	Test Run	Test Date	Start Time	End Time			(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)
1	1	05/23/24	08:15	08:35	0.19	0.20	-0.01	0.0001
1	2	05/23/24	08:58	09:18	0.18	0.19	-0.01	0.0001
0	3	05/23/24	09:40	10:00	0.13	0.14	-0.01	0.0001
1	4	05/23/24	10:20	10:40	0.19	. 0.19	0.00	0.0000
1	5	05/23/24	11:00	11:20	0.18	0.18	0.00	0.0000
1	6	05/23/24	11:38	11:58	0.18	0.19	-0.01	0.0001
1	7	05/23/24	12:17	12:37	0.17	0.18	-0.01	0.0001
1	8	05/23/24	12:56	13:16	0.18	0.19	-0.01	0.0001
1	9	05/23/24	13:34	13:54	0.17	0.18	-0.01	0.0001
1	10	05/23/24	14:12	14:32	0.19	0.20	-0.01	0.0001
				n		9		
				t(0.975)	2.3	306		
		Mean Re	ference Me	thod Value	0.	181	RM avg	
			Mean	CEM Value	0.	189	CEM avg	
			Sum of	Differences	-0.	070	di	
Mean Difference					-0.	008	d	
Sum of Differences Squared					0.	001	di ²	
	Standard Deviation					004	sd	
(Confide	ence Coeff		Error (1-tail)	0.	003	cc	
			Relativ	e Accuracy	6.	.17	RA	

Location: Waste Fuel boiler Outlet Duct

Date: 5/23/24

Test Method: 7E, 3A

Location: Waste Fuel boiler Outlet Duct Date: 5/23/24 Test Method: 7E, 2

Project #: M242110

Applicable Standard: 437

NO_x lb/hr RATA

CEM Analyzer Information

NC	x Moni	tor/Model:	Therm	o 42iQ		NO _x Serial # :	11800	030057
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM NO _x Ib/hr	CEM NO _x Ib/hr	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)
1	1	05/23/24	08:15	08:35	83.2	72.9	10.3	106.09
1	2	05/23/24	08:58	09:18	75.0	65.6	9.4	88.36
1	3	05/23/24	09:40	10:00	60.7	54.1	6.6	43.56
1	4	05/23/24	10:20	10:40	80.7	73.0	7.7	59.29
0	5	05/23/24	11:00	11:20	77.6	66.2	11.4	129.96
1	6	05/23/24	11:38	11:58	70.2	66.2	4.0	16.00
1	7	05/23/24	12:17	12:37	76.5	67.7	8.8	77.44
1	8	05/23/24	12:56	13:16	75.5	68.3	7.2	51.84
1	9	05/23/24	13:34	13:54	71.5	66.6	4.9	24.01
1	10	05/23/24	14:12	14:32	76.6	68.6	8.0	64.00
				n		9		
				t(0.975)		306		
		Mean Re	ference Me	thod Value	74	.433	RM avg	
1			Mean	CEM Value	67	.000	CEM avg	
				Differences		.900	di	
			Mean	Difference	7.	433	d	
		Sum	of Difference	es Squared	530	.590	di ²	
	Standard Deviation					040	sd	
(Confidence Coefficient 2.5% Error (1-tail)					568	cc	
	Relative Accuracy					2.09	RA	

Location: Waste Fuel boiler Outlet Duct Date: 5/23/24 Test Method: 3A

CO₂% (dry) RATA

CEM Analyzer Information

1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM CO ₂ % (dry)	CEM CO ₂ % (dry)	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)
1	1	05/23/24	08:15	08:35	13.0	13.0	0.0	0.00
0	2	05/23/24	08:58	09:18	13.1	13.0	0.1	0.01
1	3	05/23/24	09:40	10:00	14.5	14.6	-0.1	0.01
1	4	05/23/24	10:20	10:40	13.4	13.4	0.0	0.00
1	5	05/23/24	11:00	11:20	13.5	13.5	0.0	0.00
1	6	05/23/24	11:38	11:58	12.8	12.8	0.0	0.00
1	7	05/23/24	12:17	12:37	13.6	13.6	0.0	0.00
1	8	05/23/24	12:56	13:16	13.6	13.5	0.1	0.01
1	9	05/23/24	13:34	13:54	13.9	13.8	0.1	0.01
1	10	05/23/24	14:12	14:32	13.2	13.1	0.1	0.01
				n	9	9		
				t(0.975)	2.3	306		
		Mean Re	ference Me	thod Value	13.	500	RM avg	
			Mean	CEM Value	13.	478	CEM avg	
			Sum of	Differences	0.2	200	di	
			Mean	Difference	0.0	022	d	
		Sum	of Difference	es Squared	0.0	040	di ²	
			Standar	d Deviation	0.0	067	sd	
C	Confidence Coefficient 2.5% Error (1-tail)					051	cc	
			Relativ	e Accuracy	0.	54	RA	

Project #:	M2421	10			Test Method	: 3A		
				O ₂ % (d	ry) RATA			
				CEM Analyz	er Informatio	n		
0;	Monit	or/Model:	Thermo	CTL902C		O ₂ Serial # :	1180	530001
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM O₂ % (dry)	RM O ₂ % CEM O ₂ %		(RM-CEM) Difference ² (di ²)
0	1	05/23/24	08:15	08:35	7.1	7.4	-0.3	0.09
1	2	05/23/24	08:58	09:18	7.1	7.3	-0.2	0.04
1	3	05/23/24	09:40	10:00	5.5	5.7	-0.2	0.04
1	4	05/23/24	10:20	10:40	6.7	6.9	-0.2	0.04
1	5	05/23/24	11:00	11:20	6.6	6.8	-0.2	0.04
1	6	05/23/24	11:38	11:58	7.4	7.6	-0.2	0.04
1	7	05/23/24	12:17	12:37	6.5	6.7	-0.2	0.04
1	8	05/23/24	12:56	13:16	6.6	6.8	-0.2	0.04
1	9	05/23/24	13:34	13:54	6.3	6.5	-0.2	0.04
1	10	05/23/24	14:12	14:32	7.0	7.2	-0.2	0.04
				n		9		
				t(0.975)	2.	306		
		Mean Re	ference Me	thod Value		633	RM avg	
			Mean	CEM Value	6.	833	CEM avg	
			Sum of	Differences	-1	.800	di	
			Mean	Difference	-0	.200	d	
	Sum of Differences Squared					360	di ²	
	Standard Deviation					000	sd	
C	onfide	nce Coeff	icient 2.5% I	Error (1-tail)	0.	000	cc	
			Relativ	e Accuracy	3	.02	RA	

Location: Waste Fuel boiler Outlet Duct

Date: 5/23/24

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Client: Billerud Quinnesec, LLC Facility: Quinnesec Mill Project #: M242110 Fuel Type: Other Location: Waste Fuel boiler Outlet Duct Date: 5/23/24 Test Method: 6C, 3A

Fuel Factor: 9518

Applicable Standard: 1.2

O2 based SO2 lb/mmBtu RATA CEM Analyzer Information

SO	2 Moni	tor/Model:		o 43iQ	Timonnauon	SO ₂ Serial # :	11809	930080
0	2 Moni	tor/Model:	Thermo	CTL902C		O2 Serial # :	1180	530001
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM SO ₂ Ib/MMBtu	CEM SO ₂ Ib/MMBtu	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)
1	1	05/23/24	08:15	08:35	0.0	0.0	0.0	0.000
1	2	05/23/24	08:58	09:18	0.0	0.0	0.0	0.000
1	3	05/23/24	09:40	10:00	0.0	0.0	0.0	0.000
1	4	05/23/24	10:20	10:40	0.0	0.0	0.0	0.000
1	5	05/23/24	11:00	11:20	0.0	0.0	0.0	0.000
1	6	05/23/24	11:38	11:58	0.0	0.0	0.0	0.000
0	7	05/23/24	12:17	12:37	0.1	0.0	0.1	0.010
1	8	05/23/24	12:56	13:16	0.0	0.0	0.0	0.000
1	9	05/23/24	13:34	13:54	0.1	0.1	0.0	0.000
1	10	05/23/24	14:12	14:32	0.0	0.0	0.0	0.000
				n		9		
				t(0.975)	2.3	806		
		Mean Re	ference Me	thod Value	0.0	011	RM avg	
			Mean	CEM Value	0.0	011	CEM avg	
			Sum of	Differences	0.0	000	di	
			Mean	Difference	0.0	000	d	
		Sum	of Difference	es Squared	0.0	000	di ²	
	Standard Deviation					000	sd	
(Confidence Coefficient 2.5% Error (1-tail)					000	cc	
			Relativ	e Accuracy	0.	00	RA	

Location: Waste Fuel boiler Outlet Duct Date: 5/23/24 Test Method: 6C, 2

Applicable Standard: 476

SO2 lb/hr RATA

CEM Analyzer Information

SC	2 Moni	tor/Model:	Therm	o 43iQ		SO ₂ Serial # :	11809	930080
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM SO₂ Ib/hr	CEM SO ₂ Ib/hr	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)
1	1	05/23/24	08:15	08:35	3.5	1.9	1.6	2.56
1	2	05/23/24	08:58	09:18	2.4	0.4	2.0	4.00
1	3	05/23/24	09:40	10:00	3.7	6.1	-2.4	5.76
1	4	05/23/24	10:20	10:40	5.0	6.5	-1.5	2.25
1	5	05/23/24	11:00	11:20	3.3	2.1	1.2	1.44
1	6	05/23/24	11:38	11:58	4.6	3.1	1.5	2.25
0	7	05/23/24	12:17	12:37	26.2	18.7	7.5	56.25
1	8	05/23/24	12:56	13:16	20.5	19.5	1.0	1.00
1	9	05/23/24	13:34	13:54	42.8	39.3	3.5	12.25
1	10	05/23/24	14:12	14:32	6.7	4.5	2.2	4.84
		Mean Re	ference Me	n t(0.975) thod Value	2.3	9 306 .278	RM avg	
			Mean	CEM Value	9.	267	CEM avg	
				Differences Difference		100 011	di d	
		Sum	of Difference			.350	di²	
	Standard Deviation Confidence Coefficient 2.5% Error (1-tail)					842 416	sd cc	
	Relative Accuracy - APS					.51	RA ^A	

^A Relative accuracy based upon +/- 10% of applicable standard of 476 lb/hr

		id Quinnes	ec, LLC	;		Waste Fuel Boiler O	utlet Duct			
Facility:					Test Date: 5/23/2024 Test Method: 2					
Project #:	M242	110				-				
				Vo	lumetric How RATA					
Flow	Monit	or/Model:	Det	erich	CEM Analyzer Info	Flow Serial # :	22-F-C-1	79,274797.01.1		
1=accept Test Test 0=reject Run Date			Start Time	End Time	Reference Method Flow DSCFM	CEM Flow DSCFM	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²		
1	1	05/23/24	8:15	8:35	104,865	89,326	15,539	241,460,521		
0	2	05/23/24	8:58	9:18	100,194	85,299	14,895	221,861,025		
1	3	05/23/24	9:40	10:00	98,896	85,945	12,951	167,728,401		
1	4	05/23/24	10:20	10:40	101,138	90,514	10,624	112,869,376		
1	5	05/23/24	11:00	11:20	100,878	84,678	16,200	262,440,000		
1	6	05/23/24	11:38	11:58	94,453	86,534	7,919	62,710,561		
1	7	05/23/24	12:17	12:37	102,319	88,482	13,837	191,462,569		
1	8	05/23/24	12:56	13:16	97,719	86,591	11,128	123,832,384		
1	9	05/23/24	13:34	13:54	94,153	85,942	8,211	67,420,521		
1	10	05/23/24	14:12	14:32	97,539	86,091	11,448	131,056,704		
				n	9					
				t(0.975)	2.30	06				
M	lean R	leference	Method	Value	99106	6.667	RM avg			
				l Value	87122	2.556	CEM avg			
				rences	10785		di			
	4			erence	11984		d			
	Sum	of Differe			1360981	037.000	di ²			
				viation	2924		sd			
Confidence	e Coef				2247.		cc			
		Rela	tive Ac	curacy	14.	36	RA			

Location: Recovery Boiler Outlet Duct Date: 5/22/24 Test Method: 7E, 3A

Project #: M242110

Applicable Standard: 110

NOx ppmvd @ 8% O2 RATA

CEM Analyzer Information

NC	x Moni	tor/Model:	Therm	o 42iQ		NO _x Serial # :	11800	090013
0	2 Moni	tor/Model:	Thermo	CTL902C		O ₂ Serial # :	11802	240002
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM NOx ppmvd @ 8 %O2	CEM NOx ppmvd @ 8 %O2	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)
1	1	05/22/24	09:35	09:55	83.5	81.4	2.1	4.41
1	2	05/22/24	10:18	10:38	83.7	80.7	3.0	9.00
1	3	05/22/24	11:02	11:22	87.4	84.3	3.1	9.61
1	4	05/22/24	11:46	12:06	83.0	80.5	2.5	6.25
1	5	05/22/24	12:32	12:52	83.8	81.5	2.3	5.29
1	6	05/22/24	13:14	13:34	77.0	74.6	2.4	5.76
0	7	05/22/24	13:56	14:16	78.9	75.9	3.0	9.00
1	8	05/22/24	14:38	14:58	85.4	82.5	2.9	8.41
1	9	05/22/24	15:18	15:38	86.7	84.2	2.5	6.25
1	10	05/22/24	15:58	16:18	87.8	85.2	2.6	6.76
				n		9		
				t(0.975)	2.3	06		
		Mean Re	ference Me			256	RM avg	
				CEM Value		656	CEM avg	
				Differences		400	di	
				Difference		500	d	
		Sum	of Difference	es Squared	61.	740	di ²	
	Standard Deviation					335	sd	
(Confidence Coefficient 2.5% Error (1-tail)					258	cc	
			Relativ	e Accuracy	3.	39	RA	

Project #: M242110					Test Method:	3A			
				O ₂ % (d	ry) RATA				
			(CEM Analyz	er Information	1			
02	Monit	or/Model:	Thermo (CTL902C		O2 Serial # :	11802	240002	
1=accept 0=reject	Test Test Start Time End Time		RM O ₂ % (dry)	CEM O ₂ % (dry)	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)			
1	1	05/22/24	09:35	09:55	5.2	5.4	-0.2	0.04	
1	2	05/22/24	10:18	10:38	5.3	5.5	-0.2	0.04	
1	3	05/22/24	11:02	11:22	5.3	5.6	-0.3	0.09	
1	4	05/22/24	11:46	12:06	5.5	5.8	-0.3	0.09	
1	5	05/22/24	12:32	12:52	5.3	5.6	-0.3	0.09	
1	6	05/22/24	13:14	13:34	4.8	5.1	-0.3	0.09	
0	7	05/22/24	13:56	14:16	4.6	4.9	-0.3	0.09	
1	8	05/22/24	14:38	14:58	4.8	5.1	-0.3	0.09	
1	9	05/22/24	15:18	15:38	5.0	5.3	-0.3	0.09	
1	10	05/22/24	15:58	16:18	4.9	5.2	-0.3	0.09	
				n		9			
				t(0.975)	2.3	306			
		Mean Re	ference Me		5.122		RM avg		
Mean CEM Value					5.400		CEM avg		
Sum of Differences					-2.	500	di		
Mean Difference					-0.278		d		
Sum of Differences Squared					0.710		di ²		
Standard Deviation				0.044		sd			
С	onfide	nce Coeff	icient 2.5% E	Error (1-tail)	0.034		cc		
			Relativ	e Accuracy	6	.08	RA		

Location: Recovery Boiler Outlet Duct

Date: 5/22/24

Location: Recovery Boiler Outlet Duct Date: 5/22/24 Test Method: 6C, 3A

Applicable Standard: 50

SO2 ppmvd @ 8% O2 RATA CEM Analyzer Information

SC	D ₂ Moni	tor/Model:		o 43iQ	SO ₂ Serial # :		1180090009		
0	O ₂ Monitor/Model:			Thermo CTL902C		O ₂ Serial # :		1180240002	
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM SO2 ppmvd @ 8 %O2	CEM SO2 ppmvd @ 8 %O2	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)	
1	1	05/22/24	09:35	09:55	0.4	0.7	-0.3	0.09	
1	2	05/22/24	10:18	10:38	1.0	0.6	0.4	0.16	
1	3	05/22/24	11:02	11:22	0.1	0.6	-0.5	0.25	
1	4	05/22/24	11:46	12:06	0.7	0.5	0.2	0.04	
1	5	05/22/24	12:32	12:52	0.9	0.5	0.4	0.16	
0	6	05/22/24	13:14	13:34	2.0	0.5	1.5	2.25	
1	7	05/22/24	13:56	14:16	1.5	0.5	1.0	1.00	
1	8	05/22/24	14:38	14:58	0.5	0.6	-0.1	0.01	
1	9	05/22/24	15:18	15:38	0.4	0.6	-0.2	0.04	
1	10	05/22/24	15:58	16:18	0.4	0.6	-0.2	0.04	
				n t(0.975)	2.3	9			
		Mean Re	ference Me			606 656	RM avg		
			Mean	CEM Value	0.578		CEM avg		
	Sum of Differences					0.700		di	
	Mean Difference)78	d		
	Sum of Differences Squared					1.790		di ²	
	Standard Deviation					0.466		sd	
(Confide	nce Coeffi	cient 2.5% E	Error (1-tail)	0.358 cc				
		R	elative Accu	iracy - APS	0.	87	RA ^A		

 $^{\rm A}$ Relative accuracy based upon +/- 10% of applicable standard of 50 ppmvd @ 8% O_2

Location: Recovery Boiler Outlet Duct

Date: 5/22/24

Test Method: 10, 3A

Applicable Standard: 425

CO ppmvd @ 8% O2 RATA CEM Analyzer Information

				LIVI Analyze	er mormation			
CO Monitor/Model:			Therm	o 48iQ	CO Serial # : 117068000			800002
0	O ₂ Monitor/Model:			Thermo CTL902C		O2 Serial # :	1180240002	
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM CO ppmvd @ 8 %O2	CEM CO ppmvd @ 8 %O2	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)
1	1	05/22/24	09:35	09:55	5.4	2.9	2.5	6.25
1	2	05/22/24	10:18	10:38	35.6	33.5	2.1	4.41
1	3	05/22/24	11:02	11:22	22.9	15.7	7.2	51.84
1	4	05/22/24	11:46	12:06	22.4	18.6	3.8	14.44
1	5	05/22/24	12:32	12:52	16.7	18.0	-1.3	1.69
1	6	05/22/24	13:14	13:34	99.1	99.2	-0.1	0.01
1	7	05/22/24	13:56	14:16	73.8	75.2	-1.4	1.96
1	8	05/22/24	14:38	14:58	10.1	6.0	4.1	16.81
1	9	05/22/24	15:18	15:38	25.0	17.7	7.3	53.29
0	10	05/22/24	15:58	16:18	14.1	6.7	7.4	54.76
				n		Ð		
				t(0.975)	2.3	06		
		Mean Re	ference Me	thod Value	34.	556	RM avg	
				CEM Value	31.867		CEM avg	
		_		Differences	24.200		di	
Mean Difference					2.6	589	d	
Sum of Differences Squared					150	.700	di ²	
Standard Deviation							sd	
(Confide	nce Coeff	icient 2.5% I	Error (1-tail)	2.5	2.515 cc		
		R	elative Accu	iracy - APS	1.	22	RA	

 $^{\rm A}$ Relative accuracy based upon +/- 5% of applicable standard of 425 ppmvd @ 8% O_2

Location: Recovery Boiler Outlet Duct Date: 5/22 and 5/23 Test Method: 16C, 3A

Project #: M242110

Applicable Standard: 10

TRS as SO2 ppmvd @ 8% O2 RATA CEM Analyzer Information

TR	TRS Monitor/Model: Thermo 43iQ					TRS Serial # : 1180090014			
0	O ₂ Monitor/Model:		Thermo CTL902C		O ₂ Serial # :		1180240002		
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM TRS as SO2 ppmvd @ 8 %O2	CEM TRS ppmvd @ 8 %O2	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)	
1	1	05/22/24	12:32	12:52	1.0	1.0	0.0	0.00	
1	2	05/22/24	13:14	13:34	1.3	1.1	0.2	0.04	
1	3	05/22/24	13:56	14:16	0.8	1.0	-0.2	0.04	
1	4	05/22/24	15:18	15:38	1.1	1.1	0.0	0.00	
1	5	05/22/24	15:58	16:18	1.2	1.2	0.0	0.00	
1	6	05/22/24	16:36	16:56	1.2	1.2	0.0	0.00	
1	7	05/23/24	08:19	08:39	0.8	0.7	0.1	0.01	
1	8	05/23/24	09:06	09:26	0.7	0.6	0.1	0.01	
1	9	05/23/24	09:52	10:12	0.8	0.9	-0.1	0.01	
				n		9			
				t(0.975)		806			
		Mean Re	ference Me			989	RM avg		
				CEM Value			CEM avg		
				Differences			di		
Mean Difference					0.011		d		
Sum of Differences Squared					0.110		di ²		
	Standard Deviation					0.117		sd	
(Confide	nce Coeff	icient 2.5% E	Error (1-tail)	0.090 cc				
			Relativ	e Accuracy	10	.19	RA		

Test Location: Recovery Boiler Outlet Duct Test Date: ⁷5/22/2024 Test Method: 2 Volumetric Flow RATA - Normal Load

				· Old	CEM Analyzer Infor	mation			
Flow	Monit	or/Model:	OSI-OFS	6 2000W		Flow Serial # :	15	110807E	
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	Reference Method Flow DSCFM	CEM Flow DSCFM	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)	
1	1	05/22/24	9:00	9:25	185,457	186,915	-1,458	2,126,931	
1	2	05/22/24	9:27	9:35	186,597	186,799	-202	40,925	
1	3	05/22/24	10:10	10:15	188,452	186,177	2,275	5,173,350	
1	4	05/22/24	10:16	10:26	188,828	186,481	2,347	5,508,878	
1	5	05/22/24	10:30	10:40	189,003	186,833	2,170	4,708,900	
0	6	05/22/24	11:30	11:36	192,755	187,152	5,603	31,393,609	
1	7	05/22/24	11:37	11:47	191,713	187,631	4,082	16,658,642	
1	8	05/22/24	11:48	11:58	193,134	187,791	5,343	28,548,718	
1	9	05/22/24	12:30	12:40	189,301	187,597	1,704	2,902,253	
1	10	05/22/24	12:45	12:55	186,188	188,094	-1,906	3,632,836	
				n	9				
				t(0.975)	2.30)6			
	Mea	n Referen	ce Metho	d Value	18874	1.233	RM avg		
	_		Mean CE	M Value	18714	6.444	CEM avg		
Sum of Differences					14353	.100	di		
Mean Difference					1594.	789	d		
Sum of Differences Squared					693014	33.330	di ²		
			andard D		2408.	611	sd		
Confide	nce C	oefficient	2.5% Erro	or (1-tail)	1851.	419	cc		
Relative Accuracy					1.83 RA				

Location: Lime Kiln Date: 5/21/24

Test Method: 16C, 3A

Applicable Standard: 10

TRS as SO2 ppmvd @ 10% O2 RATA CEM Analyzer Information

TR	TRS Monitor/Model: Thermo 43iQ					TRS Serial # : 1180090014			
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM TRS as SO2 ppmvd @ 10 %O2	CEM TRS ppmvd @ 10 %O2	(RM-CEM) Difference (di)	(RM-CEM) Difference ² (di ²)	
1	1	05/21/24	09:29	09:49	2.4	2.3	0.1	0.01	
1	2	05/21/24	10:43	11:03	1.4	1.1	0.3	0.09	
1	3	05/21/24	11:22	11:42	1.2	1.1	0.1	0.01	
1	4	05/21/24	12:29	12:49	1.1	1.3	-0.2	0.04	
1	5	05/21/24	13:27	13:47	1.1	1.1	0.0	0.00	
1	6	05/21/24	14:08	14:28	1.3	1.2	0.1	0.01	
1	7	05/21/24	15:11	15:31	1.6	1.5	0.1	0.01	
1	8	05/21/24	15:58	16:18	1.7	1.4	0.3	0.09	
1	9	05/21/24	16:37	16:57	1.1	1.2	-0.1	0.01	
				n		9			
				t(0.975)	2.3	806			
		Mean Re	ference Me	thod Value	1.4	433	RM avg		
			Mean	CEM Value	1.356		CEM avg		
	Sum of Differences					0.700		di	
	Mean Difference					0.078			
	Sum of Differences Squared					0.270			
	Standard Deviation					0.164			
(Confide	nce Coeffi	cient 2.5% E	Error (1-tail)	0.126		cc		
			Relativ	e Accuracy	14	.23	RA		

Client: Billerud Quinnesec, LLC Facility: Quinnesec Mill Ρ

chent.	Dilleruu	Quinnese	C, LLC							
Facility:	Facility: Quinnesec Mill					Date: 5/21/24				
Project #:	M2421	10			Test Method: 3A					
				O ₂ % (d	ry) RATA					
				CEM Analyz	er Information		_			
O2	O2 Monitor/Model: Thrmo CTL902C					O2 Serial # :	1180	570001		
1=accept 0=reject	Test Run	Test Date	Start Time	End Time	RM O₂ % (dry)	RM O ₂ % CEM O ₂ %		(RM-CEM) Difference ² (di ²)		
1	1 .	05/21/24	09:29	09:49	2.83	3.24	-0.41	0.17		
1	2	05/21/24	10:43	11:03	4.45	4.52	-0.07	0.00		
1	3	05/21/24	11:22	11:42	4.21	4.57	-0.36	0.13		
1	4	05/21/24	12:29	12:49	3.68	4.10	-0.42	0.18		
1	5	05/21/24	13:27	13:47	4.40	4.50	-0.10	0.01		
1	6	05/21/24	14:08	14:28	4.09	4.22	-0.13	0.02		
1	7	05/21/24	15:11	15:31	3.40	3.65	-0.25	0.06		
1	8	05/21/24	15:58	16:18	4.00	4.33	-0.33	0.11		
1	9	05/21/24	16:37	16:57	4.60	4.52	0.08	0.01		
				n	9)				
				t(0.975)	2.3	806				
Mean Reference Method Value					3.962		RM avg			
Mean CEM Value					4.1	183	CEM avg			
Sum of Differences						990	di			
Mean Difference					-0.221		d			
Sum of Differences Squared					0.684		di ²			
Standard Deviation					0.175		sd			
C	onfider	nce Coeffi	cient 2.5% E	Frror (1-tail)	0.134 cc					
			Relativ	e Accuracy	8.	97	RA			

Location: Lime Kiln

4.0 CERTIFICATION

Mostardi Platt is pleased to have been of service to Billerud Quinnesec, LLC. If you have any questions regarding this test report, please do not hesitate to contact us at 630-993-2100.

As project manager, I hereby certify that this test report represents a true and accurate summary of emissions test results and the methodologies employed to obtain those results, and the test program was performed in accordance with the methods specified in this test report.

MOSTARDI PLATT

Program Manager

Christopher E. Jensen

and

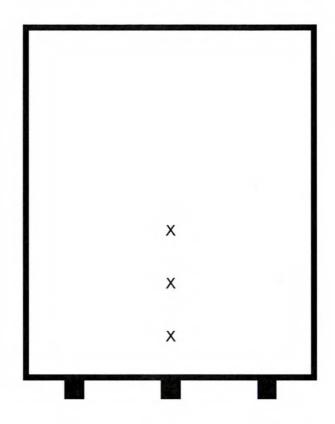
Scott W. Banach

Quality Assurance

APPENDICES

Appendix A - Test Section Diagrams

THREE POINT GASEOUS TRAVERSE FOR RECTANGULAR DUCTS



Job: Billerud Quinnesec LLC Quinnesec, Michigan

Date: May 21, 2024

Test Location: Package Boiler Duct

Length: 5.5 Feet

Width: 7.5 Feet

Area: 41.25 Square Feet

Upstream Distance: ~75 Feet

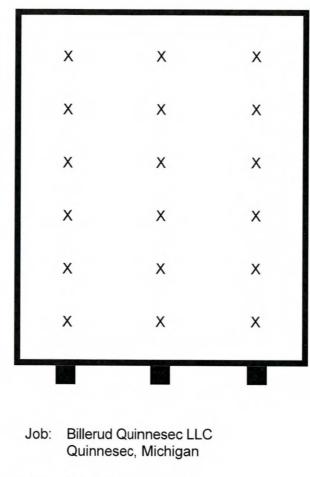
Downstream Distance: ~40 Feet

No. Test Ports: 1

Tests Points per Port: 3

Distance from Inside Wall To Traverse Point: 1. 2.0 Meters 2. 1.2 Meters 3. 0.4 Meters

EQUAL AREA TRAVERSE FOR RECTANGULAR DUCTS



Date: May 23, 2024

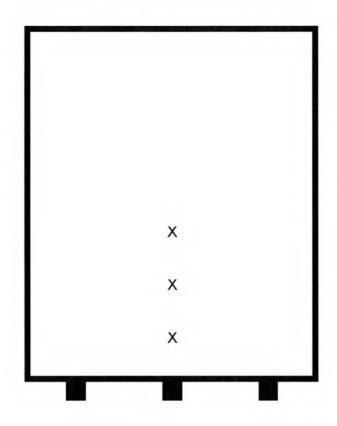
Test Location: Waste Fuel Boiler Duct

Length: 10 Feet

- Width: 7 Feet
- Area: 70 Square Feet
- No. Test Ports: 3

Tests Points per Port: 6

THREE POINT GASEOUS TRAVERSE FOR RECTANGULAR DUCTS



Job: Billerud Quinnesec LLC Quinnesec, Michigan

Date: May 23, 2024

Test Location: Waste Fuel Boiler Duct

Length: 10 Feet

Width: 7 Feet

Area: 70 Square Feet

Upstream Distance: ~100 Feet

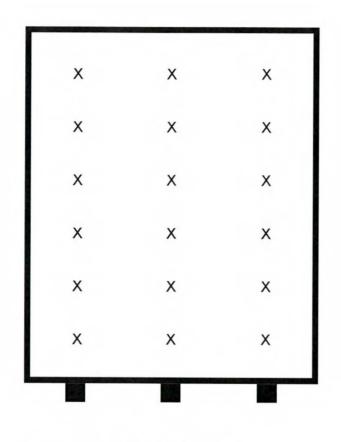
Downstream Distance: ~20 Feet

No. Test Ports: 1

Tests Points per Port: 3

Distance from Inside Wall To Traverse Point: 1. 2.0 Meters 2. 1.2 Meters 3. 0.4 Meters

EQUAL AREA TRAVERSE FOR RECTANGULAR DUCTS



Job: Billerud Quinnesec LLC Quinnesec, Michigan

Date: May 22 and 23, 2024

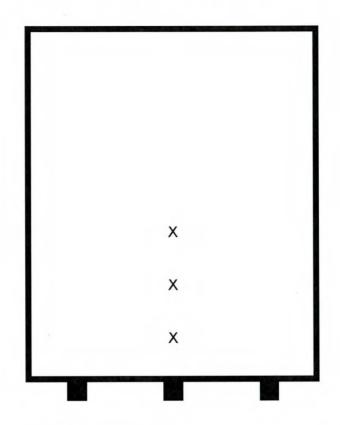
Test Location: Recovery Boiler Duct

- Length: 12.25 Feet
- Width: 8 Feet
- Area: 98 Square Feet
- No. Test Ports: 3

Tests Points per Port: 6

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THREE POINT GASEOUS TRAVERSE FOR RECTANGULAR DUCTS



Job: Billerud Quinnesec LLC Quinnesec, Michigan

Date: May 22 and 23, 2024

Test Location: Recovery Boiler Duct

Length: 12.25 Feet

Width: 8 Feet

Area: 98 Square Feet

Upstream Distance: ~90 Feet

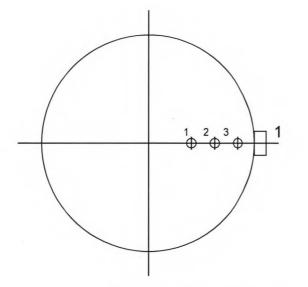
Downstream Distance: ~25 Feet

No. Test Ports: 1

Tests Points per Port: 3

Project No. M242110A 37 of 268 Package Boiler Outlet Duct, Waste Fuel Boiler Outlet Duct, Recovery Boiler Outlet Duct, and Lime Kiln Stack Distance from Inside Wall To Traverse Point: 1. 2.0 Meters 2. 1.2 Meters 3. 0.4 Meters

THREE POINT GASEOUS TRAVERSE FOR ROUND DUCTS



Billerud Quinnesec LLC Job: Quinnesec, Michigan

May 21, 2024 Date:

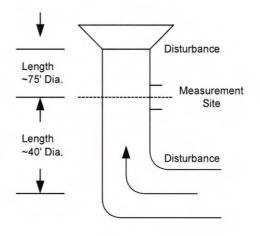
Test Location: Lime Kiln Stack

Stack Diameter: 8.0 Feet

Stack Area: 50.265 Square Feet

No. Sample Points: 3

- Upstream Disturbance: ~75 Feet
- Downstream Disturbance ~40 Feet



Distance from Inside Wall To Traverse Point:

- 1. 2.0 Meters 2. 1.2 Meters
- 3. 0.4 Meters

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